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# The Thermodynamic Properties of Compressed Gaseous and Liquid Fluorine

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# The Thermodynamic Properties of Compressed Gaseous and Liquid Fluorine\*

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A <sub>i</sub> , B <sub>i</sub> , C <sub>i</sub>	Coefficients of various equations
B(T)	Second virial coefficient, 1/mol
C(T)	Third virial coefficient, (1/mol) <sup>2</sup>
$C_{\rho}(T,\rho)$	Specific heat at constant pressure, J/mol K
C <sub>P</sub> °(T)	Ideal gas specific heat at constant pressure,
	J/mol K
$C_{sat}(T)$	Specific heat of saturated liquid, J/mol K
$C_v(T,\rho)$	Specific heat at constant volume, J/mol K
C°,(T)	Ideal gas specific heat at constant volume,
	J/mol K
E	Expansion coefficient
E <sub>T</sub>	Thermal expansion coefficient of dead-weight
	gage piston-cylinder assembly
ğ	Gravity at NBS Boulder Laboratory = 9.79615 N/kg
gs	Standard gravity = 9.80665 N/kg
H(Τ,ρ)	Enthalpy, J/mol
∆H	Heat of vaporization, J/mol
К	Thermal conductivity, W/m K
L <sub>c</sub>	Cryostat capillary length = 0.71 m
L <sub>m</sub>	Height of mercury manometer column, m
Ln	Height of nitrogen column in intermediate pressure
	system = 1.04 m

LIST OF SYMBOLS AND UNITS -- Continued

М	Molecular weight of fluorine = 37.9968 g/mol
Ν	Number of g moles of fluorine
N <sub>i</sub>	Burnett apparatus cell constant
Р	Pressure, $MN/m^2$ (1 $MN/m^2 = 10^6$ newton/m <sup>2</sup> =
	9.86923 atm)
P <sub>b</sub>	Barometric pressure, MN/m <sup>2</sup>
P <sub>c</sub>	Critical pressure = $5.215 \text{ MN/m}^2$
Pn	Nominal dead-weight gage pressure, $MN/m^2$
Pt	Triple point pressure = $2.52 \times 10^{-4} MN/m^2$
R	Universal gas constant = 8.3143 J/mol K
S(Τ, <sub>ρ</sub> )	Entropy, J/mol K
Т	Absolute temperature, degrees Kelvin, on the
	International Practical Temperature Scale of 1968
T <sub>c</sub>	Critical point temperature = 144.31 K
Τ <sub>Ъ</sub>	Normal boiling point temperature = 84.950 K
Tt	Triple point temperature = 53.481 K
To	Pipet sample holder temperature, K
tm	Mercury manometer temperature, °C
U(Τ,ρ)	Internal energy, J/mol
v	Molar volume, l/mol
V <sub>dg</sub>	Volume of diaphragm cell and capillary at same
	temperature during gasometer measurements. cm <sup>3</sup>

Vn	Volume of metal necks of gasometer flasks, cm <sup>3</sup>
V <sup>o</sup> p	Normal pipet volume at zero pressure, cm <sup>3</sup>
Vo	Normal pipet volume at zero pressure and 20°C,
	cm <sup>3</sup>
W	Weight factor
Ws	Velocity of sound, m/s
Z	Compressibility factor = PV/RT
Zo	Compressibility factor of fluorine in pipet at
	Pg and To
α, γ, δ, σ,	Statistical mechanical parameters; for definitions
χ, u, X ·)	see References [52, 53]
θ	Cryostat capillary factor
λ	Volume ratio from Equation (7)
ρ	Density, mol/l
ρ <sub>c</sub>	Critical density = 15.10 mol/1
ρ <sub>m</sub>	Mercury density from Equation (15)
$\rho_{\text{melt L}}$ (T or P)	Density of liquid along liquid-solid boundary,
	mol/l
ρ <sub>n</sub>	Nitrogen density in intermediate pressure system
	from Equation (17)
$\rho_{sat L}$ (T)	Saturated liquid density, mol/l
ρ <sub>t</sub>	Liquid triple point density = 44.86 mol/l

# LIST OF SYMBOLS AND UNITS -- Continued

# Subscripts:

с	Conditions in cryostat capillary
cr	Conditions in capillary from cryostat to gasometer
d	Fluorine diaphragm cell conditions
g	Conditions in gasometer flasks
m	Gasometer manifold conditions
р	Pipet sample holder property
q	Quartz bourdon tube conditions
r	Instrument room conditions
w	Dead-weight gage conditions
calc	Calculated value
exp	Experimental value
9	Gas property
ł	Liquid property
o	Reference state property
sat	Properties at vapor-liquid saturation boundary

Superscript:

Ideal gas property

## THE THERMODYNAMIC PROPERTIES OF COMPRESSED

## GASEOUS AND LIQUID FLUORINE

#### Rolf Prydz and Gerald C. Straty

## ABSTRACT

An apparatus has been constructed and used successfully to measure vapor pressure and PVT data of fluorine from the triple point to 300 K at pressures to about 24 MN/m<sup>2</sup>. Material problems caused by the toxic and corrosive nature of fluorine were solved. A network of isotherm and isochore polynomials and a truncated virial equation were used to represent all PVT data. These equations represent the data with an average standard deviation of about 0.02 percent in density, the corresponding accuracy being estimated at 0.1 percent. Equations for the saturated liquid and vapor densities, the vapor pressure curve, the melting line, and the ideal gas properties are also presented. Comparisons are given to published values of the second virial coefficients, vapor pressures, and saturation densities. Additional comparisons are also made to measured specific heats and latent heats of vaporization. New values are reported for the triple point and critical point parameters together with the temperature and saturation densities at the normal boiling point. Finally, extensive tables of thermodynamic properties of fluorine are given which include pressure, temperature, density, isotherm and isochore derivatives, internal energy, enthalpy, entropy, specific heats at constant pressure and volume and velocity of sound.

Key Words: Density; enthalpy; entropy; fixed points (PVT); fluorine; Joule-Thomson; latent heat; melting curve; PVT measurements; saturation densities; specific heats; vapor pressure: velocity of sound; virial coefficients.

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## I. INTRODUCTION

Current increased technical and scientific interest in fluorine arises from the fact that this cryogenic fluid is being considered as a propellant oxidizer in rocket propulsion systems. The reason is that liquid fluorine is one of the most energetic oxidizers known and its use with hydrogen as a fuel results in the most favorable specific impulse of any stable oxidizer-fuel combination. Since the product of the reaction is hydrofluoric acid, the use of this combination is limited to upper stages of the rocket.

The highly toxic and reactive properties of fluorine have, however, discouraged research in determining its physical properties which are required for engineering calculations and systems development. For example, a few parts per million of fluorine in the air is fatal to humans. Also, hydrofluoric acid resulting from fluorine reactions in poorly cleaned systems may actually react with any metal used as the containment for this reactive fluid. As a result, physical property data on fluorine tend to be quite inaccurate, extremely scarce, and in many cases, nonexistent.

The primary objective of this research program was, therefore, to determine the complete PVT relationship for gaseous and liquid fluorine to be used for calculating thermal functions. These PVT measurements are also required for future experimental fluorine measurements in this laboratory of thermodynamic and transport properties such as specific heats (which have been completed at the time this is being written), velocity of sound, dielectric constant, viscosity, and thermal conductivity. Valuable knowledge concerning intermolecular forces may be gained from the PVT measurements; for instance, information about the intermolecular potential can be obtained from the temperature dependence of the second virial coefficient. Further, correlation of these PVT data to calculate thermodynamic properties also requires vapor pressure data from the triple point to the critical point presented in the form of a vapor pressure equation. Finally, to make technical design of fluorine systems possible, extensive tables of thermodynamic properties of the saturated and singlephase regions are essential.

Although reports on some specific phases of this research have been published, it is the purpose of this note to present, under a single cover, the complete and detailed results of the PVT experimental and calculational program. Extensive tables of PVT properties and derived thermodynamic functions are given. The experimental method and apparatus are discussed and calculational procedures for data correlations and thermodynamic properties computations are presented.

## II. EXPERIMENTAL PVT METHODS

Several different methods for accurate PVT data measurements are used in various laboratories throughout the world. While the procedures for measuring pressure and temperature are standard and vary little from laboratory to laboratory, drastically different methods are employed in obtaining the corresponding specific volume or density. A thorough review of these PVT measurement methods is given by Sengers [1].<sup>\*</sup>

In general there are four different procedures that are used to obtain the specific volume, namely the Piezometer Method, the Weight Method, the Isochore Method, and the Gas Expansion Method. The latter method, which is the most widely used one, will be discussed in greater detail than the other methods since it is the approach used for this work.

## A. The Piezometer Method.

This procedure uses a piezometer of known volume and a calibrated stem as shown in Figure 1.a. It is filled with the fluid under study to a pressure of 1 atmosphere and controlled at a temperature where the isotherms of the fluid are known. Thus the total amount of the fluid (the normal volume) in the piezometer is available. A capillary connects the stem to a pipet of known volume. Hence, measurements of P-V points at different pipet

<sup>&</sup>lt;sup>\*</sup>Numbers in brackets refer to citations in the bibliography.



isotherms are possible by gradually displacing the fluid from the piezometer to the pipet or vice versa. Thus the specific volume of the fluid in the pipet is easily computed from the known total sample amount and the quantity remaining in the piezometer stem which may be calculated from the known fluid properties at that temperature.

The advantage of this method is that only one normal volume determination is needed for a large range of pressures and temperatures. However, accurate volume determinations at high pressures are experimentally difficult since the ratio between volumes occupied by the fluid at 1 atmosphere and at high pressures becomes very large at low pipet temperatures. Another disadvantage of this method, which made it impractical for this work is that known P-V properties of the fluid are required at the piezometer temperature. No such data were available for fluorine.

## B. The Weight Method.

A pipet of known internal volume is suspended from a balance as shown in Figure 1.b. It is filled with a sample of fluid to a selected pressure and temperature and the increase in weight is recorded. These conditions provide the necessary information for one PVT data point.

An obvious advantage of this method is that no normal volume determination is required. However, the disadvantage associated with obtaining an accurate value for the sample weight far outweighs

this advantage. The difficulty of the sample weight determination is partly due to the fact that a compromise must be made between the freedom of motion of the pipet and its thermal contact with the surroundings. The main factor destroying the accuracy of this measurement is, however, the weight of sample being only a small fraction of the weight of the pipet.

## C. The Isochore Method.

Figure 1.c is a schematic of the apparatus used in this method. A pipet of unknown volume is filled with a sample of the fluid and the pressure is measured at a temperature where the P-V relationship of the fluid is known. This permits evaluation of the specific volume of the fluid at these conditions. P-T data for that specific isochore and for other isochores may then be obtained in the same manner. Since the pressures are usually measured at the same temperatures for each isochore the resulting PVT data are rearranged in isotherms without difficulty.

The fact that no volume calibration or measurement of normal volumes are needed, makes this method quite attractive for obtaining PVT data. However, the requirement of existing accurate high-pressure data eliminated this procedure for application to fluorine since no such data were available.

## D. The Gas Expansion Method.

The gas expansion method is generally used in most laboratories to obtain accurate PVT data, especially where large amounts

of data are required. The time consuming calibrations of the pipet volume, the volumes of the vessels, and other noxious volumes are over-shadowed by the fact that only one normal volume determination is needed for every P-T relationship (isochore) measured. Some low-density isochores for fluorine resulted in as many as 40 PVT data points.

With reference to Figure 1.d the pipet of calibrated (calibration procedure is discussed in Chapter IV) volume in the cryostat is filled with the fluid to be studied at approximately the desired density. Then P-T points are measured at conditions of nearly constant density. When either the desired maximum temperature or pressure is attained in the pipet, the fluid is released into expansion vessels of calibrated volumes, combined in such a manner as to give a final pressure close to 1 atmosphere. This pressure is then generally measured with the aid of a manometer; in the case of fluorine a quartz bourdon tube gage was used due to the extreme reactivity of fluorine gas with manometer fluids even at low pressures. The vessel temperature is precisely controlled by a bath at a temperature close to the room conditions. Thus, the total amount of sample in the pipet, the cryostat capillary, and the null pressure detector is determined applying the gas law to the state of the sample fluid in the expansion vessels. The compressibility factor, Z = PV/RT, of the gas under these conditions may be obtained from a Burnett [2] expansion experiment

as discussed in Chapter VII. To obtain the actual amount of fluid in the pipet alone, the portion of sample in the cryostat and the null pressure detector, which is dependent upon temperature, is subtracted from the total amount of sample. The experimental density at each P-T point is obtained by dividing the amount of sample in the pipet by its calibrated volume corrected for temperature and pressure effects as discussed in Chapter IV. Since the density decreases slightly with increasing temperatures along a P-T relationship, the experimental run is usually denoted as a pseudo-isochore.

This expansion method was determined to be the most practical one for fluorine for the following reasons:

 large amounts of data could be obtained with relative ease and great accuracy;

2) no initial accurate PVT data of fluorine were required, and

3) an all metal apparatus, with the exception of the lowpressure pyrex glass expansion flasks, could be utilized minimizing the hazards of data collection. The apparatus used is discussed in the next chapter.

## III. EXPERIMENTAL APPARATUS

## A. Introductory Remarks.

In the early stages of fluorine technology development, a number of failures occurred that were characterized by the chemical ignition between the fluorine and its containment. The ignition zone was usually consumed in the reaction and the reason for failure was difficult to determine. It was believed, however, that either organic contamination or incompatibility of the materials was the cause. Later tests confirmed that most common metals are compatible for use in a fluorine environment, provided that the system is maintained completely free of contamination. Consequently, the high pressure section (up to 20 MN/m<sup>2</sup>;  $1 \text{ MN/m}^2 = 9.86923 \text{ atm}$ ) of the fluorine system in this study was constructed of stainless steel, copper, and brass with packless metal valves. In the low pressure section (atmospheric and below) polytetrafluoroethylene was used in a few places and the gasometry flasks were constructed of pyrex glass. The cleaning and passivating procedure of this equipment is described in detail in Chapter VI.

The experimental apparatus, not including the electronics and instrumentation is shown schematically in Figure 2 and is similar to that used by Goodwin [3] for hydrogen and by Weber [4] for oxygen. However, several modifications were incorporated



to minimize the problems that arise due to the toxic and reactive nature of fluorine [5]. The fluorine supply system, the cryostat, and the vacuum pumps are separated from the instrument room by an explosion-proof wall. Since fluorine pressure in the gasometer glass flasks generally is atmospheric or below, the gasometer is conveniently located in the instrument room.

All system components handling fluorine are enclosed in aluminum cabinets and vented by a separate ventilation system. Thus, in case a leak should develop, fluorine would rarely be released into the laboratories. Also, the enclosures are of sufficient strength to give reasonable blast protection from direct effects of any explosive reaction.

## B. Cryostat and Pipet.

A cross-section of the metal cryostat is shown in Figure 3. The 26-cm<sup>3</sup> pipet sample holder, also called the PVT cell, is suspended in the lower portion of the cryostat by a thin-walled stainless steel reflux tube as pictured in Figure 4. Gaseous or liquid nitrogen or gaseous helium in this tube cools the pipet. This pipet is a 1.59 cm diameter cavity bored into a solid 5 cm diameter copper cylinder 21.6 cm long as described by Goodwin [3]. A plug was silver soldered into the lower end of the pipet sample holder while the cavity was filled with helium to avoid oxidation of the copper. Helical grooves were machined on



Figure 3. Cryostat and pipet.



Figure 4. Refrigerant tank and pipet.

the outside of the cylinder to carry a 32-gage, 500 ohm constantan wire heater, which permits a maximum heating rate of about 1 to 2 K per minute depending on the operating temperature. The platinum resistance thermometer was tinned and secured in the thermometer well of the pipet with Rose's alloy. A guard ring is supported about 5 cm above the pipet by the reflux tube. This ring is automatically controlled to match the pipet temperature and thermally tempers the electrical leads which are wound around this copper cylinder before they are connected to the pipet. The temperature control of the guard ring is obtained by a gold-cobalt versus copper differential thermocouple between the pipet and the guard ring. A power supply provides the current for a 36-gage, 100 ohm constantan wire heater after receiving the amplified thermocouple signal. Tempering of the electrical leads entering the cryostat at room temperature is accomplished by thermally anchoring them to a cold ring suspended from the liquid refrigerant tank. Good thermal contact on the ring is insured because all wires were assembled as one unit in a parallel plane and varnished together before they were mounted.

The pipet is surrounded by an evacuable copper jacket soldered to the refrigerant tank with Rose's alloy. This jacket, which also serves as the cold wall, and the refrigerant tank are then, in turn, enclosed in another vacuum jacketed dewar. Finally, the cryostat is immersed in an open liquid nitrogen dewar having a

three-step electronic liquid level indicator. Arrangement of forepump, diffusion pump and vacuum valving for the cryostat is shown in Figure 5.

The liquid nitrogen is supplied to the inner refrigerant tank through a permanent transfer line. A suitable valving and safety system permits pumping on the nitrogen to attain the triple point temperature of nitrogen and below.

Valves 9 and 10 (shown in Figure 2) on top of the cryostat may be operated from the instrument room through appropriate gearing and extended stems. These valves were designed by Straty [6] for the purpose of handling corrosive fluorine at more than 20 MN/m<sup>2</sup>. He modified a commercially available valve, valve A as shown in Figure 6, with bellows (valve B) such that the primary non-metallic packing was avoided.

A 0.033 cm inside diameter stainless steel capillary connects valves 9 and 10 to the pipet. The fluorine-nitrogen separator (NPD), a commercial diaphragm differential pressure cell, is connected between the pressure measuring system (Chapter III. E) and the capillary at the top of the cryostat.

## C. The Gasometer.

The gasometer consists of four calibrated volumes. These are spherical glass flasks of approximately 1 to 21 liters submerged in a precision thermostated water bath conveniently con-



Figure 5. Cryostat vacuum valving.





trolled at 295.00  $\pm$  0.01 K, the approximate instrument room temperature. A higher bath temperature was not chosen since this would have resulted in a greater bath temperature fluctuation and excessive loss of water by evaporation into the ventilation system. The temperature controller was adjusted according to a precision thermometer, readable to  $\pm$  0.001°C, and which was previously calibrated against the pipet platinum resistance thermometer.

A 0.35 MN/m<sup>2</sup> fuzed quartz bourdon tube type gage with pressure readings reproducible to 7 N/m<sup>2</sup>, was connected to the valve manifold. When the fluid in the pipet, cryostat capillary, and the diaphragm cell is released into the gasometer, a standard volume is chosen such that the final pressure in the calibrated volumes is close to 1 atmosphere. Lower pressures will cause a larger relative error in the pressure reading, whereas higher pressures may break the 6- or 21-liter bulb. The quartz bourdon tube type of gage was frequently calibrated against a high-precision air dead-weight gage (accuracy of ± 0.015 percent of reading) to eliminate any error that might arise due to possible changes in the elastic properties of the quartz tube from exposure to fluorine. Later when an apparent weakening of the tube was observed, it was used as a null indicator and the pressure measured with the deadweight gage. To compromise between low noxious volumes and adequate pumping speeds copper tubing of 0.32 cm inside diameter

was used to connect the flasks to the manifold. The brass manifold valves (valves 11, 12, 13 and 14 on Figure 2) were of the bellow seal type and were kept fully open or closed depending on whether the specific calibrated glass flask was to be filled or not.

## D. The Fluorine Supply System.

Commercial grade fluorine gas was obtained in one half pound cylinders pressurized to approximately 2.4 MN/m<sup>2</sup>. This gas was further distilled by Argonne National Laboratory to 99.99 percent purity, with the remaining impurities being mostly oxygen, nitrogen, and hydrogen fluoride as determined from residual gas analysis after reaction of the fluorine with mercury.

A double valving manifold system of brass needle type valves permits fine control of the fluorine flowrate to the hydrogen fluoride absorber (Figure 2). This HF trap consists of a section of standard 5 cm Cu-Ni pipe equipped with caps, thermowell, and electric heating wires. The absorber is packed with sodium bifluoride (NaHF<sub>2</sub>) pellets and was activated prior to installation by heating to about 300 °C while simultaneously purging with dry nitrogen. This activation procedure drove off the hydrogen fluoride leaving a porous absorbent form of sodium fluoride (NaF). The trap may be reactivated in the same manner after 8 to 11 kg of fluorine have been processed. A fluorine compatible bourdon pressure gage indicates the pressure in the absorber at any time.

The fluorine storage and recovery cylinder is a 3-liter heavy-walled AISI 304 stainless steel cylinder having a maximum operating pressure of about 12 MN/m<sup>2</sup>, which is five times the normal cylinder pressure. Figure 7 shows the fluorine supply and the cryostat cabinets.

Valves 4, 5, and 8 (Figure 2) are all Cu-Ni forged needle valves, whereas valves 6 and 7 are the same modified type as valves 9 and 10, described earlier and shown in Figure 6. Valves 6 and 7, however, are separate, single valves. The thermal booster is used to monitor the PVT cell filling pressure and to recover the fluorine after the gasometer measurements. The construction features of this unit were quite similar to those of the pipet. A cavity of 2.30 cm diameter was bored into a solid AISI type 304 stainless steel cylinder 4 cm in diameter. A plug was arc welded into the end of the booster while the filling line, a 0.32 cm outside diameter copper tube, was silver soldered into the top. A liquid nitrogen dewar may be raised and lowered around the cylinder through a hoist arrangement operated from the instrument room. Provisions were also available for lowering the temperature of the refrigerant bath to its triple point and below by pumping on the nitrogen dewar to recover more of the fluorine.


Figure 7. The fluorine supply- and cryostat cabinets.

### E. Measurement of Pressure.

### 1. Apparatus and Method

The commercial oil operated, dual range, precision deadweight gage pressure measuring system, shown in Figures 8 and 9, is the same as the one used by Weber [4] and is a modification of the system used by Goodwin [3]. The system includes two null pressure detectors, often referred to as commercial diaphragm cells, with nitrogen serving as the intermediate fluid. The first null pressure detector separates the oil in the dead-weight gage from the nitrogen gas system, whereas the second separates the nitrogen from the fluorine sample. Hence, in the event of a failure of the diaphragm in the null pressure detector, high pressure fluorine gas will not come in contact with the oil to cause a hazardous and explosive condition. Even though the diaphragms are constructed of 0.005 cm thick steel sheets, they can withstand overpressures of up to  $100 \text{ MN/m}^2$  and exhibit negligible temporary hysteresis.

The second null pressure detector shown in Figure 8 is placed on top of the cryostat to minimize noxious volumes. The rest of the pressure measuring system is located in the instrument room. The oil and the nitrogen pressures are adjusted by hand-operated screw-type pumps. With practice the two-diaphragm system may be operated with as much sensitivity as the



Figure 8. Schematic of the pressure measuring system.



one-diaphragm system of Reference [3].

The dual pressure ranges of the oil dead-weight gage are obtained by means of interchangeable piston-cylinder assemblies, the diameters of which are measured to  $\pm 1.3 \times 10^{-5}$  cm using a light-wave micrometer. The weights are equivalent to class "P" standard masses. Each weight is individually adjusted to match the effective area of the piston-cylinder assembly and is calibrated against Class "S" standard masses as certified by the National Bureau of Standards [7]. This corresponds to a 0.05 percent tolerance on the 1 psi weight decreasing to 0.002 percent on the 1000 psi weights.

The oil dead-weight gage readings are corrected for air buoyancy on the weights, the local gravity, the thermal expansion and elastic deformation of the piston and cylinder, and the barometric pressure as discussed in detail by Cross [8].

Estimates of accumulated pressure errors [3] are found in Table 1 as a function of operating pressure.

Absolute pressure, MN/m <sup>2</sup>	0.4	3	20
	Error,	$MN/m^2 \times$	< 10 <sup>4</sup>
Barometer	0.51	0.51	0.51
Null Pressure Detector	4.05	4.05	4.05
Piston-cylinder diameter	0.12	0.91	6.07
Calibration of weights	1.36	2.31	4.12
	6.04	7.78	14.75
Percent pressure error	0.151	0.026	0.007

TABLE 1. Estimates of Accumulated Pressure Errors

2. Pressure Adjustment for Sample in Capillary

The static pressure created by the sample in the capillary column of length  $L_c$  extending from the pipet to values 9 and 10 must be subtracted from the observed pressure to obtain the true pressure in the pipet. This static pressure head is given as

$$P_{c} = \frac{M L_{c} \theta}{R T_{0}} P$$
 (1)

where

M = molecular weight of fluorine = 37.9968 g/mol  $L_{c} = \text{capillary column length} = 71 \text{ cm}$   $\theta = \text{capillary factor, Equation (5)}$   $P = \text{observed pressure, MN/m}^{2}$  R = universal gas constant = 8.3143 J/mol K  $T_{o} = \text{temperature of pipet, K}$ 

For fluorine the factor  $ML_{c}^{\theta}/RT_{o}$  varies from about 0.01 to 0.0001, being less than 0.001 for more than 95 percent of the data points.

### F. Measurement of Temperature.

### 1. Instrumentation and Method

The temperature measurement and control system is shown in Figures 10 and 11. A six-decade microvolt potentiometer is used in conjunction with a 25-ohm platinum resistance thermometer calibrated by the National Bureau of Standards. Lowimpedance, unsaturated standard cells are kept in insulated boxes, providing large thermal inertia thereby reducing thermal fluctuations due to occasional temperature changes in the instrument room (this change is usually of the order of  $\pm$  0.5°C). There are three different potentiometer current supplies, one for each section of the potentiometer. The smallest current supply of 12 microamperes is provided by a small cadmium cell located inside the potentiometer, whereas the mid-section of the potentiometer requires a current of 1 milliampere supplied from four 1.35-volt mercury batteries connected in parallel. Six-volt lead-acid batteries supply a current of 10 milliamperes to the upper potentiometer section. This latter current supply is stabilized by connecting an isolated, rectified, and filtered alternating current source across the batteries.

Stable current for the platinum resistance thermometer is







Temperature measurement and control instruments. Figure 11.

obtained from four 6-volt, 200 ampere-hours, thermally insulated, and shielded batteries of low internal discharging type, connected in series. This current is adjusted when flowing through calibrated standard precision resistors. The microvolt amplifiers are coupled to 50-microamperes panel galvanometers in suitable damping and range-changing circuits. Spurious voltage effects are reduced in the thermometer and thermocouple circuits by soldering all junctions with a special cadmium-tin solder [9] resulting in negligible thermal electromotive force. All wires that connect the cryostat to the instruments are carefully shielded to avoid extraneous electrical noise and all apparatus and electrical instruments are grounded with heavy copper conductors.

The regulation and control of the pipet temperature is accomplished by balancing the cooling due to conduction down the reflux tube with Joule heating in the 500 ohm constantan wire heater. The potential across the platinum resistance thermometer, based on a thermometer current of 2 milliamperes used for all measurements, is compared to the corresponding calibrated value at the desired temperature set on the potentiometer. The difference in potential is fed through a D.C. microvolt amplifier to a power regulator [10] which adjusts the power input to the heater to maintain the pipet at the desired temperature. With an amplifier sensitivity corresponding to 0.0001 K, there is no perceptible noise.

Regulation of the guard ring temperature, identical to the pipet temperature, is accomplished in a similar manner with the exception that the potential output of a differential thermocouple between the guard ring and the pipet provides the signal that is amplified and fed to the power regulator.

When standardizing, i.e., adjusting the various potentiometer currents to give the correct voltage of the standard cell, the power regulator input switch is opened and the steady-state heating carefully adjusted by the power regulator control, so that constant temperature is still maintained.

The meter damping and range-changing circuits connected to the galvanometers are convenient when the actual potential differences are to be read.

Uncertainties introduced in the thermometry are partly due to the specification of the potentiometer of 0.01 percent of reading plus 0.02 microvolts, and partly due to the calibrated value of the 1-ohm standard resistor of 0.99999 ± 0.00001 ohms. In terms of temperature this amounts to a maximum of 2 millidegrees at 50 K, increasing to 28 millidegrees at 300 K. Uncertainty due to the calibration itself is probably less than 0.002 K.

# 2. Thermometry Checks

Prior to the PVT experiments with fluorine, vapor pressures of ultra high purity (99.99 percent or better) oxygen were

measured to check the accuracy of the thermometry. The observed vapor pressures, P<sub>obs</sub>, are compared in Table 2 to those of the literature [4, 11], P<sub>lit</sub>.

Temperature, K	P <sub>obs</sub> , MN/m <sup>2</sup>	P <sub>lit</sub> , MN/m <sup>2</sup>	Percent difference
124.000	1.2787	1.2788	-0.008
126.000	1.4234	1.4235	-0.007
130.000	1.7477	1.7478	-0.006
130.000	1.7479	1.7478	0.006
136.000	2.3291	2.3291	0.000
140.000	2.7863	2.7865	-0.007
144.000	3.3068	3.3063	0.015
144.000	3.3066	3.3063	0.009
146.000	3.5926	3.5918	0.022

TABLE 2. Thermometr	y Checks	trom	Oxygen \	√apor	Pressure	es
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Agreement is within the specification of the pressure measurement system, which indicates the thermometry to be of the desired absolute accuracy.

The platinum resistance thermometer used was calibrated according to the International Practical Temperature Scale of 1948 above 90 K and the NBS-1955 temperature scale below 90 K. The temperatures of Table 2 are therefore reported on this basis since the purpose of this table is comparison of data on the same temperature scale. All fluorine data, however, were converted in temperature to conform to the International Practical Temperature Scale (IPTS) of 1968 by applying the temperature scale differences of Appendix A using the Aitken interpolation method [12]. These differences for temperatures below and above 90 K were obtained from References [13] and [14], respectively.

### G. Safety Equipment.

Due to the hazards involved in handling fluorine at high pressures, precautions have been taken to construct and install equipment that would prevent fluorine gas from escaping into the laboratory in case of an accident.

As mentioned, all system components handling fluorine, i.e., the cryostat, the gasometer, and the fluorine supply system, are enclosed in aluminum cabinets and vented outside the laboratory by a separate ventilation system. The 0.32 cm thick aluminum plates should give reasonable blast protection in case of an explosion. In any case, the operator in the instrument room is always separated from the high pressure fluorine system by an explosion-proof wall. Also, all valves subject to high pressure fluorine are operated remotely from this room.

Should a substantial system failure accidentally develop, the fluorine may be discarded rapidly through two charcoal reactors installed in parallel outside the laboratory. The reactors are made of 9 cm diameter copper pipes lined with a layer of 1 cm thick refractive cement since the reaction of fluorine with charcoal to form inert carbontetrafluoride, is extremely exothermic.

A vacuum system for pumping fluorine out of the PVT cell (the pipet) and the gasometer flasks was also constructed. After most of the fluorine is recovered in the booster, the remaining fraction must be removed before a new run may be started. This is done by pumping the fluorine through an alumina trap where aluminum fluoride is formed and free oxygen is released through the pumps. Two pumps, one with fluorine compatible oil for the initial pumping and another regular pump capable of producing an even lower pressure, may either pump through the trap or by-pass it.

#### IV. DENSITY MEASUREMENT

There are several volumes required for the density calculations. These are the volume of the gas in the gasometer system,  $V_g$ , the volume of the pipet sample holder,  $V_p$ , and the different nuisance volumes of the gasometer manifold, valves and capillaries. The sample density, not including the corrections of Equation (19), is given approximately as

$$\rho = \frac{P}{MRT} \cdot \frac{V}{V}$$
(2)

The subscript g refers to the gasometer system and M is the molecular weight of fluorine. Hence, the ratio  $V_g/V_p$  is an important factor affecting the density calculations.

### A. Amount of Sample Measurements.

The term  $P_g V_g /MRT_g$  of Equation (2) refers to the actual number of moles of fluorine contained in the pipet, the capillary, and the diaphragm cell. This amount of sample may be determined through the previously discussed expansion process of the fluorine into the appropriate glass flasks of the gasometer. To get an accurate measure of the sample amount, it is necessary to calibrate the glass flask volumes with utmost care.

### 1. Gasometer Calibration

The volumes of the 1-,2-, and 6-liter flasks were calibrated by weighing them with distilled water which had been boiled to remove any dissolved air. Calculations to obtain the actual volumes involved corrections for thermal expansion and elastic stretching of the glass itself and for air buoyancy on the flasks and weights. Measurements of the flask volumes were also obtained by hydrogen gas expansion from one flask or combinations of flasks to the other flask or flasks. The volume of the 1-liter flask as determined from the water weighings was selected as the standard volume. Excellent agreement between volumes obtained from the hydrogen gas expansion and the water weighings was observed for the 2- and the 6-liter flasks, while the volume of the 21-liter flask was taken as the mean of eight expansion determinations. Comparison of these results are given in Table 3.

Nominal	Water weigh-	Gas expan-	Assigned	Volume of flask
volume, ł	ing, cm <sup>3</sup>	sion, cm <sup>3</sup>	cm <sup>3</sup>	metal neck, cm <sup>3</sup>
1	988.095	(988.095)	988.095	2.432
2	2028.83	2028.80	2028.83	2.751
6	6414.71	6415.75	$6415.2 \pm 1.$	5 3.099
21		21186.5	<b>2</b> 1186.5 $\pm$ 4	3.530

TABLE 3. Calibration of Gasometer Flask Volumes

Nuisance volumes of the order of a few cm<sup>3</sup> in capillaries, gasometer manifold, diaphragm cell, and the quartz bourdon tube were determined through a combination of hydrogen gas expansions from a calibrated volume of 128 cm<sup>3</sup> and gas expansions between individual volumes.

# Adjustment for Sample in Capillary and Diaphragm Cell

To obtain the actual density in the pipet as described in Section V. C. the amount of sample in the capillary and the diaphragm cell, at the conditions of each P-T point, must be subtracted from the total amount as obtained through the gasometry measurements. Some pertinent data and correlations are necessary for these calculations:

- a. The temperature of the diaphragm cell, T<sub>d</sub>,
   is measured using a calibrated thermistor as
   one leg of a Wheatstone bridge (the temperature inside the quartz bourdon tube is measured in the same manner.)
- b. The temperature  $T_x$ , corresponding to any position at a fraction x of capillary length extending from the guard ring at the pipet temperature,  $T_0$ , to the top of the cryostat at the diaphragm temperature,  $T_d$ , is calculated using the thermal conductivity, K, of stainless steel [15], from

$$x = \frac{\int_{T_0}^{T_x} K \, dT}{\int_{T_0}^{T_d} K \, dT}$$
(3)

с.

An equation of state is needed to calculate the compressibility factor,  $Z_d$ , at any pressure P and temperature  $T_d$  in the diaphragm cell and the compressibility factor  $Z_x$  at any pressure P and temperature  $T_x$  in the capillary. These are then used to obtain the amount of sample in these small volumes (the capillary volume, V<sub>c</sub>, is 0.0682 cm<sup>3</sup> while the diaphragm cell volume V<sub>d</sub>, including some other noxious volumes on top of the cryostat, is 0.480 cm<sup>3</sup>). A preliminary equation of state for fluorine was obtained by fitting corresponding states data calculated from oxygen, to the equation used by Prydz and co-workers [16] for deuterium. After the new fluorine density data had been corrected in this way, it was again fitted to this equation for further refinement. The data was then corrected

once more using the revised equation. When this procedure was repeated for a third time, no more significant changes in densities were observed. Thus, the amount of fluorine in the capillary is

$$N_{c} = \frac{P V_{c} \theta}{R T_{o}}$$
(4)

where the capillary factor  $\theta$  is given by

$$\theta = T_0 \int_0^1 \frac{dx}{T_x Z_x} .$$
 (5)

The number of moles of fluorine in the diaphragm cell is given by

$$N_{d} = \frac{P V_{d}}{R T_{d} Z_{d}}$$
 (6)

### B. Sample Volume Measurement.

The sample volume, which is only of the order of  $26 \text{ cm}^3$ , is the volume of the pipet,  $V_p$ . Since it is inversely proportional to the sample density, extreme care has to be taken to arrive at an accurate value for this volume.

### 1. Determination of Pipet Volume

The volume of the normal pipet (volume at 20°C and zero pressure) was determined by means of hydrogen gas expansions

from the pipet to the 1-liter glass flask. The expansion of gas initially at 3.5 to 5 MN/m<sup>2</sup> in the pipet sample holder to this glass flask resulted in a final pressure of approximately 1 atmosphere in the entire system. Initially four determinations gave a mean value of the normal pipet volume,  $V_0$ , equal to 25.881 cm<sup>3</sup>. Later, five redeterminations resulted in a value of 25.879 cm<sup>3</sup> for the volume which is the value accepted for the normal volume at 20 °C for the pipet. The latter value was adopted since greater internal consistency, on the order of  $\pm$  0.003 cm<sup>3</sup>, was obtained among the five measurements. Earlier measurements on the same pipet by Goodwin [3] yielded a volume at 20 °C of 25.907 cm<sup>3</sup> or 0.11 percent higher than the volume of the current work. In his oxygen work Weber [4] adopted a 0.14 percent smaller volume of 25.843 cm<sup>3</sup>.

### 2. Thermal Expansion of Pipet

As noted, the normal pipet volume is a function of temperature. The volumetric thermal expansion of the pipet was obtained using known relationships [17] for the expansion coefficient of copper. Calculated values of the ratio of the normal pipet volume,  $V_p^o$ , at various temperatures to the normal pipet volume at 20°C,  $V_o$ , were fitted to a quadratic polynomial of the form

$$\lambda = \frac{V_{p}^{\circ}}{V_{o}} = 1.0 + a(T_{o} - 293.15) + b(T_{o} - 293.15)^{2}$$
(7)

where

a = 5.9851 
$$\times 10^{-5}$$
  
b = 8.708  $\times 10^{-8}$ 

# 3. Elastic Stretching of Pipet

The relationship used to calculate the elastic stretching of the pipet due to pressure given by Goodwin [3] was modified to correspond more closely to experimental results on similar thickwalled vessels [18]. Thus, the corrected pipet volume at any pressure P and temperature  $T_0$ , is given by

$$V_{\rm p} = \lambda (1.0 + c[1.0 + d T_{\rm o}]P) V_{\rm o}$$
(8)

where

 $\lambda = \frac{V_p^{\circ}}{V_o} \text{ as obtained from Equation (7)}$ c = 2.3 × 10<sup>-5</sup> (MN/m<sup>2</sup>)<sup>-1</sup> d = 4.35 × 10<sup>-4</sup> K<sup>-1</sup>.

### V. CALCULATION OF PVT DATA FROM OBSERVATIONS

# A. Gasometry.

The number of gram moles, N, of fluorine in the particular gasometer glass flasks, the water bath manifold, the quartz bourdon tube, the capillaries, and the PVT cell during the gasometer measurements is given by

$$N = P_{g}/R \left[E_{g} V_{g}/T_{g} + (V_{n} + V_{m})/T_{m} + V_{cr}/T_{r} + V_{q}/T_{q} + V_{dg}/T_{d}\right]/Z_{g} + (V_{p} + V_{c}/2)/(T_{o} Z_{o})$$
(9)

where  $P_g$  is the fluorine pressure in the flasks in  $MN/m^2$  as given by

$$P_{g} = P_{q} [1.0 + (T_{q} - 299.0) E_{q}]$$
(10)  

$$P_{q} = quartz bourdon tube pressure, MN/m2$$
  

$$T_{q} = quartz bourdon tube temperature, K$$
  

$$E_{q} = quartz bourdon tube temperature coefficient = 1.3 \times 10^{-4} °C^{-1}$$
  

$$R = universal gas constant = 8.3143 J/mol K$$
  

$$E_{g} = glass volume pressure coefficient of flasks = 1.0 + (9.87 P_{g} - 0.825) 10^{-4}$$
  

$$V_{g} = volume of glass flasks given in Table 3, cm3$$
  

$$T_{g} = water bath temperature = 295.00 K$$
  

$$V_{n} = volume of metal necks of flasks given in Table 3, cm3$$
  

$$V_{m} = volume of gasometer manifold = 6.554 cm3$$

V<sub>cr</sub> = room capillary (from cryostat to gasometer) volume at  $T_r = 0.739 \text{ cm}^3$ T = instrument room temperature, K = volume of quartz bourdon tube =  $1.128 \text{ cm}^3$ V  $V_{dg}$  = volume of diaphragm cell and capillary at same temperature during gasometry measurements  $= 0.767 \text{ cm}^3$ = diaphragm cell temperature, K Ъ = compressibility factor of fluorine in flasks at Zg  $T_g$  and  $P_g$  from Equation (27) = 1.0 - 3.626 × 10<sup>-3</sup>  $P_g$ V p = pipet volume from Equation (8) = cryostat capillary volume = 0.0682 cm<sup>3</sup> V = temperature of pipet, K  $T_{\circ}$  $Z_{o}$  = fluorine compressibility factor in pipet at  $P_{g}$  and  $T_{o}$ = 1.0 - 3.33030  $\times 10^{-9}$  T<sub>0</sub><sup>-1</sup> + 1.72408  $\times 10^{-6}$  T<sub>0</sub><sup>-2</sup>  $-2.22556 \times 10^{-4} T_0^{-3}$ (11)

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### B. Pressure.

The fluid pressure P in MN/m<sup>2</sup> as measured in the PVT cell is defined as

$$P = P_{W} + P_{b} + P_{c} - P_{r}$$
(12)

where

$$P_{w} = \text{oil dead-weight gage pressure, } MN/m^{2}$$
$$= g/g_{s} [1.0 - E_{T}(t_{w} - 25.0)] [1.0 + 3.3 \times 10^{-7} P_{n}]P_{n} (13)$$

g = gravity at NBS Boulder Laboratory = 9.79615 N/kg  
g<sub>s</sub> = standard gravity = 9.80665 N/kg  

$$E_T$$
 = thermal expansion coefficient of dead -weight  
gage piston =  $1.5 \times 10^{-5} \circ C^{-1}$   
 $t_w$  = dead-weight gage temperature, °C  
 $P_n$  = nominal dead -weight gage pressure, MN/m<sup>2</sup>  
 $P_b$  = barometric pressure in MN/m<sup>2</sup> =  $g \circ_m L_m$  (14)  
 $\rho_m$  = mercury density in g/cm<sup>3</sup>  
= 13.5948 - 0.00245  $t_m$  [19] (15)  
 $t_m$  = mercury temperature, °C  
 $L_m$  = height of mercury column, cm  
 $P_c$  = pressure exerted by the static head of fluorine  
in the cryostat capillary from Equation (1).  
 $P_r$  = pressure exerted by nitrogen gas column in the  
instrument room =  $g \circ_n L_n$  (16)  
 $\rho_n$  = nitrogen density =  $P/(Z_n R T_r)$  (17)  
 $Z_n$  = nitrogen compressibility factor at room tempera-  
ture =  $1.00001 - 2.62516 \times 10^{-4} P$   
+  $3.24541 \times 10^{-6} P^2 - 2.53470 \times 10^{-9} P^3$  (18)

 $L_n$  = height of nitrogen column = 104 cm

C. Density

The actual density of fluorine in the PVT cell in mol/  $\rm cm^3$  is obtained from

$$\rho = \left[ N - (P/R) (V_c \theta/T_0 + V_d / (Z_d T_d)) \right] / V_p$$
(19)

where

N = total g moles of fluorine from Equation (9)

 $\theta$  = capillary factor from Equation (5)

V<sub>d</sub> = volume of diaphragm cell and including the capillary on top of the cryostat; diaphragm in the null position = 0.480 cm<sup>3</sup>

$$Z_{d} = \text{compressibility factor in diaphragm cell at P and T_{d}$$
$$= 1.0 + 2.58016 \times 10^{-4} P + 7.90641 \times 10^{-7} P^{2}$$
$$+ 1.59529 \times 10^{-9} P^{3}.$$
(20)

### VI OPERATING PROCEDURE

### A. Cleaning of Fluorine System.

Before the PVT apparatus was put together, each individual component that would be exposed to fluorine was thoroughly cleaned. When it had been assembled it was passivated with fluorine. The cleaning procedures were as follows:

- 1) Metal parts showing visible evidence of oxidation, were submerged in a bath of 10 to 20 percent nitric acid solution to remove the oxide film. The parts were then rinsed with distilled water followed by an acetone rinse and then dried with a dry nitrogen or helium gas stream.
- 2) Metal parts showing no visible evidence of oxidation, were washed in trichloroethylene, followed by an acetone rinse and then dried with dry nitrogen.
- Polytetrafluoroethylene packings were flushed with trichloroethylene and acetone followed by a drying period under vacuum.
- Specific items of equipment were obtained directly from the manufacturer ready for fluorine service.

### B. Passivation of Fluorine System.

The above cleaning procedures appear to have been satisfactory since no evidence of any reaction in the system was noted during the subsequent passivation. This passivation was performed at a remote test site since experience in fluorine handling was nonexistent at that time. Following is a description of the adopted fluorine passivation procedure:

- The system was flushed with dry nitrogen and then evacuated for several hours to insure removal of all possible moisture.
- The vacuum was broken with dry nitrogen and the system was once more evacuated.
- 3) The vacuum was then slowly broken with fluorine gas to a pressure of about 0.01 MN/m<sup>2</sup> and the system was held at this pressure for about 10 to 15 minutes. This was followed by an increase in pressure in steps of approximately 0.03 MN/m<sup>2</sup> until atmospheric pressure was reached. The pressure was then raised in steps of 0.2 to 1.4 MN/m<sup>2</sup> to somewhat above the intended maximum operating pressure and held at this pressure for several hours.

The passivation and testing proceeded without difficulty.

### C. Charging of Storage and Recovery Cylinder.

Before proceeding with any PVT measurement it was necessary to charge the storage and recovery cylinder with fluorine from the fluorine supply cylinder. Before charging the cylinder all valves (numbers of valves are given in Figure 2) were initially closed. The subsequent charging procedure is as follows:

- Open valves 1, 2, 4, 6, 7, 8, 9, and 18 and evacuate the system up to valve 10.
- 2) Close valves 1, 2, 8, and 9.
- 3) Raise liquid nitrogen dewar around booster.
- 4) Open fluorine supply cylinder valve slightly.
- 5) Slightly open valve 1 and use valve 2 to regulate the flow of fluorine into the valve manifold, booster and storage cylinder. Condense the fluorine in the booster.
- 6) Close values 1, 2, 4, and 7. Make sure value 6 is open and lower the liquid nitrogen dewar from around the booster, allowing pressure to rise in the storage cylinder.

- 7) When the pressure reaches a maximum (indicating that there is no more liquid fluorine in the booster), close valve 6. Repeat steps 5, 6, and 7 until the storage cylinder pressure reaches a pressure of 2 to 2.8 MN/m<sup>2</sup>.
- 8) Close fluorine supply cylinder valve.
- 9) Raise liquid nitrogen dewar around booster again and open valves 7, 1, 2, and 4. Allow fluorine pressure in this part of the system to drop to about 0.07 MN/m<sup>2</sup> gage pressure by condensing fluorine in the booster.
- 10) Close valve 7.
- Open valve 6 and lower the liquid nitrogen dewar from around the booster.
- 12) Close valves 1, 2, 4, and 18. Open valves17, 16, and 8 and evacuate this portion of the system.
- 13) Close valves 8, 16, and 17. The storage andrecovery cylinder is now charged with fluorine.

### D. Charging of Pipet.

To charge the pipet so that a series of P-T data points may be taken at the desired psuedo-isochore, the following steps are performed:

- Open valves 18, 15, 8, 9, 10, 11, 12, 13, and 14 and evacuate the system.
- 2) Close valves 8 and 10.
- Raise the liquid nitrogen dewar around the booster and condense the fluorine in the booster.
- 4) Close value 6; open value 7 and lower the liquid nitrogen dewar from around the booster allowing the pressure to increase in the PVT cell. When the desired filling pressure is reached, shut value 9.
- 5) Raise the liquid nitrogen dewar around the booster. When the fluorine pressure reaches a minimum, close valve 7 and open valve 6. Lower the nitrogen dewar again from around the booster.

### E. The Data Run.

# 1. P-T Measurements

The pipet is now ready for data taking. Pipet pressures are

measured at integral temperatures on the IPTS 1948 and the NBS 1955 temperature scales using the oil dead-weight gage. (The temperatures were later converted to the IPTS 1968 temperature scale as previously discussed.) Data are taken at the same temperatures for isochores in the same region of the PVT surface until either the maximum desired pressure (about 20 MN/m<sup>2</sup>) or the maximum temperature (300 K) is reached. Pressures are measured at temperature intervals of 2 K from 54 K to 150 K. Between 150 K and 200 K a temperature interval of 5 K is used, while pressures are measured at every 10 K above 200 K.

### 2. Gasometry

As noted in Chapter II, the fluorine in the pipet must be expanded into the gasometer to determine the number of moles that were charged to the pipet originally. This is done as follows:

- Close value 15 and the appropriate values associated with the calibrated glass flasks that are not to be used for the measurement. This would involve values 11, 12, 13 and 14.
- Open valve 10 slightly and carefully allow the fluorine to flow into the appropriate calibrated volumes of the gasometer.

- 3) Record the pressure in the calibrated glass flasks using the quartz bourdon tube gage. For later experimental runs the air dead-weight gage was used to measure this pressure, while the quartz bourdon tube gage served as a null indicator.
- Close valve 6 and raise the liquid nitrogen dewar around the booster.
- 5) Close valve 18. Open valves 7, 8, 9, and 15 and condense the fluorine in the booster.
- 6) Pump on liquid nitrogen around the booster to reduce temperature in the booster to increase the recovery of fluorine from the entire system. Close valve 7 when no more fluorine is condensing as determined from the quartz bourdon tube gage.
- 7) Open valve 6 and lower the nitrogen dewar from around the booster when the solid nitrogen has melted.
- 8) Open values 16 and 17 and evacuate the system. When a pressure of 13 N/m<sup>2</sup> is reached, the trap may be by-passed by closing values 16 and 17 and opening value 18.

#### VII BURNETT EXPERIMENT

#### A. Apparatus.

The fluorine compressibility factor in the glass flasks must be known to determine the amount of sample in the pipet from gasometer measurements. This compressibility factor, PV/RT, should be obtained at the water bath temperature of 295.00 K as a function of pressure. The gas expansion method introduced by Burnett [2] in 1936 was used for this purpose.

The Burnett apparatus, shown in Figure 12, consists of a heavy-walled AISI type 304 stainless steel bomb divided into two vessels of unspecified volumes. Vessel number 1, approximately 53 percent larger than the second vessel, is directly connected to a null pressure detector, which in turn is connected to the rest of the pressure measuring system as described previously in Subsection III. E.1. The two vessels are connected to each other by means of a valve and capillary tubing. The apparatus, including the null pressure detector, the valves, and the tubing is submerged in a constant temperature water bath controlled at 295.00 K, the same temperature at which the gasometry measurements were taken.



Figure 12. The Burnett apparatus.

### B. Experimental Method and Analysis.

Initially, the first vessel was filled with gaseous fluorine to the desired pressure of 2 to 3 MN/m<sup>2</sup>, while the second vessel was evacuated. The expansion valve was then opened and the pressure allowed to reach equilibrium in the two volumes. Further expansions were performed until the final pressure was low enough to allow extrapolation to zero pressure. More intermediate points on the extrapolated curve were obtained by varying the initial starting pressure for the expansions. Previous to the i<sup>th</sup> expansion, the fluorine gas in the first vessel is described by the following conditions:

$$(PV_1)_{i-1} = R(ZnT)_{i-1} .$$
 (21)

When equilibrium is reached after the expansion, the equation of state becomes:

$$P_{i}(V_{1} + V_{2})_{i} = R(ZnT)_{i}$$
 (22)

Since the temperature, T, of the water bath is constant and the number of moles, n, also remain the same,  $T_{i-1} = T_i$  and  $n_{i-1} = n_i$ . Hence, division of Equation (22) by Equation (21) yields upon rearrangement

$$\left(\frac{PN}{Z}\right)_{i} = \left(\frac{P}{Z}\right)_{i-1}$$
(23)

where

$$N_{i} = \frac{(V_{1} + V_{2})_{i}}{(V_{1})_{i-1}}$$
(24)

N<sub>i</sub> is therefore the ratio of the total volume of both vessels after the i<sup>th</sup> expansion to the volume of the first vessel before this expansion. Thus, N<sub>i</sub> is called the cell constant of the i<sup>th</sup> expansion. Since the pressures before and after the expansion are different, the change in the elastic stretching of the bomb results in a corresponding change in the volumes of the vessels. Consequently, the cell constant is also a function of pressure.

By extrapolating  $P_{i-1}/P_i$  of Equation (23) to zero pressure  $N_{\infty}$  is obtained since  $Z_i = Z_{i-1} = 1$  in the limit. The value obtained for the zero pressure cell constant is 1.65335 and was determined by a least squares fit of a quadratic equation to these data. Thus, since  $N_{\infty}$  is known, the value of  $N_i$  at any other pressure may be obtained by using the elastic stretching formulas of Roark [20]. These equations applied to this steel bomb, relate the change of either volume from before to after the expansion as

$$\Delta V/V = 2.10 \times 10^{-5} (P_{i-1} - P_i)$$
 (25)

where P is in  $MN/m^2$ . Thus, even at the highest operating pressures of 3  $MN/m^2$  this does not amount to more than a 0.004 percent change.

Substituting values of  $(P/Z)_{i-1}$  for  $i = 2, 3, \ldots$  successively into the equation for the first expansion (i = 1), results in
$$\frac{P_{i}N_{1}N_{2}\cdots N_{i}}{Z_{i}} = \left(\frac{P}{Z}\right)_{0}$$
(26)

where the subscript on the right-hand term denotes the starting pressure for each series of expansions. The zero pressure limit of  $P_i N_1 N_2 \dots N_i$  is  $(P/Z)_0$  since  $\lim_{i \to 0} Z_i = 1.0$ . Values of  $P_i^{\to 0}$ 

 $(P/Z)_0$  for the different expansion series may, in turn, be substituted into Equation (26), which then relates the compressibility factor of fluorine at the water bath temperature as a function of pressure. Analytically the results are represented as

$$Z(295.00 \text{ K}) = 1.0 - 3.626 \times 10^{-3} \text{ P(MN/m}^2)$$
 (27)

at relatively low pressures of a few atmospheres and are shown graphically in Figure 13.

Since no other data were available for fluorine for comparison purposes, experimental runs were also performed using oxygen and hydrogen to check for accuracy. These data agreed with published values [11,21] to within 0.005 percent. The agreement was even better near atmospheric pressures, and provided confidence that the fluorine compressibility data possessed similar accuracies.



Figure 13. Compressibility factor of fluorine at 295.00 K.

#### VIII COMPUTATIONS FROM PSEUDO-ISOCHORES

#### A. Saturation Densities.

Saturation densities derived in this study were obtained by extrapolating the experimental isochores to their intersection with the vapor pressure equation (Equation (32)) as discussed previously [22]. By fitting the first few points of the experimental isochores to low order polynomials, the intersection of the two curves was obtained using an iterative procedure. The accuracy of the extrapolation depends on the vapor pressure equation, the length of extrapolation to the intersection temperature, but mostly on the difference in slope between the experimental isochore and the vapor pressure curve. Thus the uncertainty of the intersection temperatures ranges from about 0.001 K for saturated liquid densities near the triple point, to more than 0.1 K for saturation densities near the critical density where the isochores become colinear with the vapor pressure curve. These temperature uncertainties were used to calculate the relative weight factor applied to each data point (listed in Table 4) in fitting the saturation densities to the following equation

$$\left(\frac{\mathbf{T}_{c}-\mathbf{T}}{\mathbf{T}}\right) = \left|\frac{\rho-\rho_{c}}{\rho_{c}}\right|^{3} \left[A_{1}\ln\rho + \sum_{i=2}^{9} A_{i}\rho^{i-2}\right].$$
(28)

# TABLE 4 Derived Fluorine Saturation Densities

Т	Dens., exp	Dens., calc	Pct	Weight
K	mol/l	mol/l	diff	0
	,	,		
53.4811	44.86	44.862	-0.01	•000
54.541	44.690	44.696	-0.01	4109
55.572	44.541	44.533	0.02	4871
57.516	44.223	44.224	-0.00	4918
59.837	43.858	43.851	0.02	5351
59.840	43.857	43.851	0.01	4708
61.601	42,000	420200	-0.01	4977
62.607	420234	430243	-0.02	4107
65.717	42.887	42.891	=0.01	5186
67.709	42.564	42.560	0.01	5552
69.842	42,206	42.202	0.01	5392
69.850	42.205	42.201	0.01	5381
71.703	41.888	41.887	0.00	5401
73.796	41.528	41.528	-0.00	5258
73.824	41.525	41.523	0.00	5292
73.834	41.521	41.522	-0.00	5290
75.381	41.252	41.254	-0.00	4748
77.421	40.894	40.897	-0.01	5100
79.813	40.470	40.474	-0.01	4970
(9.811 91 927	40 • 470	40.474	-0.01	4984
81-838	40.112	40.110	0.00	4901
83.832	39.747	39.747	0.00	4822
83.840	39.745	39.746	-0.00	4788
85.898	39.370	39.366	0.01	4710
87.855	39,005	39.000	0.01	4587
89.622	38.667	38.665	0.00	4519
91.284	38.343	38•345	-0.01	4388
93.466	37,919	37.919	0.00	4324
93.470	37.915	37.918	-0.01	4318
95.544	37.499	37.505	-0.01	3275
97.722	37.066	37.063	0.01	4089
99.972	30.596	30 + 5 7 6 26 - 5 0 1	0.00	3835
970970	20,000	26 259	-0.01	2967
101.723	36,223	36,224	-0.00	3815
03.274	35,892	35.890	0.01	3783
105.589	35.380	35.378	0.00	3603
105.589	35,380	35.378	0.00	3573
107.242	35.006	35.004	0.00	3481
L09.943	34.373	34.374	-0.00	3337
109.969	34.363	34.368	-0.01	3172
11.813	33.925	33.923	0.00	3132
13.792	33.434	33.432	0.01	3117
13.784	33.432	33.434	-0.01	3119
15.916	32.887	32.886	0.00	2975
17.676	22.881 22.410	52.0886	0.00	2953
10,652	31 003	32.418	0.00	2011
19.587	31.890	31.890	-0.00	2680

 TABLE 4
 Derived Fluorine Saturation Densities -- Continued

T K	Dens.,exp mol/l	Dens.,calc mol/l	Pct diff	Weight
121.682	31.288	31.287	0.00	2473
123.443	30.761	30.757	0.01	184
123.944	30.600	30.602	-0.01	2332
123.944	30.600	30.602	-0.01	2332
129.378	28.765	28.766	-0.00	1835
131.805	27.830	27.829	0.00	1604
131.805	27.830	27.829	0.00	1522
134. (53	20.030	200747	-0.04	598
120.075	220421	220421	0.02	487
140.614	23.031	240100	=0.06	68
141,950	21.876	21.822	0.25	3
141.945	21.868	21.827	0.19	13
142.948	20.672	20.594	0.38	
143.782	19.822	19.002	4.31	•026
144.052	18,753	18.123	3.48	.011
144.415	17.928			
<b>144</b> •978	15.773			
144.507	14.498			
144.414	13.423	10.000		0.05
144.121	11.928	12.380	-3.79	.005
143.000	10.009	10+875	-0.03	0120
142.751	9.0213	9.0381	-0.29	3
141.530	8,3853	8.3801	0.06	4
140.606	7.6858	7.7038	-0.23	8
139.209	6.8755	6.8793	-0.05	45
138.660	6.5942	6.6004	-0.09	29
137.526	6.0828	6.0837	-0.01	119
136.012	5.4888	5.4899	-0.02	76
133.730	4.7445	4.7443	0.00	346
129.430	3.6640	3.6611	0.08	716
123.881	20400	200473	-0.02	1380
114.481	1,5138	1.5127	0.08	2412
110.080	1.1438	1.1445	-0.06	2587
104.344	0.77679	0.77647	0.04	2894
99.742	0.55397	0.55436	-0.07	1099
94.251	0.35765	0.35702	0.18	648
88.461	0.21181	0.21210	-0.14	1267
84.355	0.14035	0.14025	0.07	1142
80.000	0.08598	0.08603	-0.06	862
18 145	0.04529	0.04540		1123
73.703	0.03787	0.03785	0-05	920
70.000	0.02158	0.02157	0.03	366
65.000	0.00897	0.00897	-0.05	216
60.000	0.00315	0.00315	-0.06	422
54.000	0.00067	0.00067	0.23	380
53.4811	0.00057	0.00057	-0.19	384

For details of weighted least-squares fitting techniques the reader is referred to Hust and McCarty [23]. Equation (28) was recently developed by Goodwin [24] for estimating the critical parameters of pure fluids. These are obtained directly as the parameters resulting in the smallest variance between the experimental data and this equation. Compared to the conventional methods this procedure eliminates the need in this temperature range for fitting the saturated liquid and saturated vapor data separately, interpolating to get the rectilinear diameter, and finally obtaining the intersection of the saturation correlations with the rectilinear diameter. The conventional method also requires better than 10<sup>-6</sup> percent accuracy in the saturated liquid and vapor representation to obtain an accuracy of 0.1 percent in the calculated saturated fluorine vapor densities near the triple point. This requirement is estimated by using Equation (28). Finally, accurate saturation data in the critical region are not needed as the form of Equation (28) is more reliable in this region than the derived experimental data.

The experimental data above 120 K were fitted to Equation (28) by the method of weighted least-squares and the critical parameters were selected as those which resulted in the smallest variance between the data and the equation. (Identical values for these parameters were also obtained by analyzing the experimental data using the conventional method). Only data above 120 K were used since a better representation of the data in the critical region was

thus achieved.

When the estimated critical parameters (T<sub>c</sub> = 144.31 K and  $\rho_c = 15.10 \text{ mol}/1$ ) had been obtained, the saturated liquid and vapor data were fitted to separate functions, each being constrained to the critical point. This was done to obtain a better correlation of the vapor density data near the triple point. The saturated liquid density representation suggested earlier [24] was modified so that no systematic deviations between the equation and the experimental data were apparent. This new equation is as follows:

$$\left(\frac{\rho - \rho_{e}}{\rho_{e}}\right) = B_{1} Z^{\circ \cdot 35} + \sum_{i=2}^{6} B_{i} Z^{i-1}$$
(29)

where

$$Z = 1 - T/T_{c}$$

The coefficients resulting from this weighted least-squares fit of the saturated liquid densities are

$$B_{1} = 1.81881076$$

$$B_{2} = 8.75236491 \times 10^{-1}$$

$$B_{3} = -8.50458910 \times 10^{-1}$$

$$B_{4} = 1.37284761$$

$$B_{5} = -1.01331503$$

$$B_{6} = 2.73840128 \times 10^{-1}$$

The number of significant figures given for these coefficients and for those of subsequent equations is not justified on the basis of the uncertainty of the data, but is presented to enable duplication of the calculated values. Applied weight factors and the deviations between the experimental and calculated densities are given in the upper part of Table 4.

Similarly, all vapor densities were represented by the equation suggested by Goodwin [24]

$$\ln\left(\frac{\rho}{\rho_{c}}\right) = C_{1}\left(\frac{Z}{Z-1}\right) + C_{2}Z^{\circ\cdot35} + \sum_{i=3}^{7}C_{i}Z^{i-2}.$$
 (30)

Calculated saturated vapor data below 80 K were also fitted to insure a representative equation that gives saturation densities approaching the ideal gas value at the triple point (vapor pressure =  $252 \text{ N/m}^2$ ). These data were based on the vapor pressure equation and an equation of state for fluorine [25] which represents the PVT surface in this region to within the uncertainty of the data. The following coefficients are obtained from this fit:

$$C_1 = 4.85547085$$
  
 $C_2 = -1.96015519$   
 $C_3 = -1.88066900 \times 10^{-1}$   
 $C_4 = 6.21165939$   
 $C_5 = -2.29600897 \times 10^{-1}$ 

$$C_6 = 4.69524623 \times 10^{1}$$
  
 $C_7 = -4.30650270 \times 10^{1}$ 

In the final analysis, however, the thermodynamic properties were calculated basing the saturated vapor densities below 6.0 mol/1 (T = 137.327 K) on the virial equation (34). Experimental data above 144.31 K in Table 4 were used in Equation (28) to estimate the critical parameters but were not used in Equations (29) and (30) for obvious reasons (Z becomes negative). The reported temperatures in all equations (as discussed earlier) were based on the IPTS 1968 temperature scale.

Saturated liquid density data from other sources [26, 27, 28, 29, 30, 31] have been compared to Equation (29). All data were adjusted, wherever possible, for temperature scale differences. These data were not, however, included in the final fit of the equation as they deviate from the new data by as much as 28 percent in density (e. g. Kanda's density data [26] are too low by 27-28 percent). Kilner et al. [27] report one density measurement at 77 K which is 1.0 percent too low (their reported saturated liquid density for oxygen is low by about 1.7 percent). Saturated liquid densities reported graphically by Dunn and Millikan [28] are the same data for which Elverum and Doescher [29] of the same laboratory later reported numerical values. These data appear to be about 0.6 percent too high in density. The density data by White, Hu and Johnston [30] are the smoothest of the old data but are too high by about 0.4 percent. Reported measurements by Jarry and Miller [31] agree well with those of Reference [30], but they exhibit larger internal scatter (0.3 percent). Early measurements of the saturated liquid density at the normal boiling point [32, 33, 34] were also compared in this study. These data points deviate considerably from the new data due to large uncertainties in the temperature measurements as well as the density determinations.

No published saturated vapor density data exist but calculated values based on the Berthelot equation of state by Fricke [35] deviate from Equation (30) by as much as + 10 percent in density at 140 K.

## B. The Critical Point.

The critical temperature and density of fluorine estimated from Equation (28) are given in Table 5. Also given is the critical pressure obtained from the vapor pressure equation (see Equation (32)). Critical parameters from other sources are also compared to the new values in this table.

Fricke [35] calculated the critical density from the Berthelot equation of state, while Baker and Adamson [36] used the critical temperature from Reference [37] and obtained the critical density by generalized properties techniques. Goodwin [24] based his findings on the equation of state [25] that does not represent the experimental data in the critical region well.

T <sub>c</sub> , IPTS 1968 K	ρ <sub>c</sub> mol/1	P <sub>c</sub> MN/m <sup>2</sup>	Reference
143.9	15.1		[24]
	12.4		[35]
	15.0		[36]
144		5.57	[37]
144.31 ± 0.05	15.10 ± 0.04*	5.215	This research

TABLE 5 Fluorine Critical Parameters

\* The estimates of the uncertainty in these critical parameters were based on the experience gained through the analysis of the data since no direct statistical measure is obtained from this iterative fitting procedure.

## C. Melting Line Determination.

Fourteen pressure-temperature data points were measured along the fluorine melting line during experimental runs no. 121 and 122 as reported earlier [38]. Measurements were made at 0.1 K intervals from 1.3 to 13.7 MN/m<sup>2</sup>. These data, given in Table 6, were fitted to the Simon melting equation

$$P = P_{t} + P_{o} \left[ (T/T_{t})^{C} - 1 \right]$$
(31)

where the subscript t refers to the triple point. By varying the values of c and  $T_t$  a best fit was obtained with the following

 $P_t = 2.52 \times 10^{-4} MN/m^2$  (from Equation (32))  $P_o = 249.975 MN/m^2$  c = 2.1845 $T_t = 53.4811 K.$ 

Only two measurements on the normal melting point and none at higher pressures have been made prior to this study. Hu, White, and Johnston's [39] value of 53.53 K agrees fairly well with the new triple point temperature, whereas Kanda's [40] measurement of 55.2 K appears to be too high. The reason for the differences may be due to impurities in the fluorine sample of the earlier data or temperature scale differences.

T K	P exp MN/m <sup>2</sup>	P calc MN/m <sup>2</sup>	Diff MN/m²
53.610	1.3141	1.3136	0.0005
53.709	2.3350	2.3371	-0.0021
53.809	3.3653	3.3628	0.0025
53.909	4.3943	4.3907	0.0036
53.909	4.3901	4.3907	-0.0006
54.009	5.4182	5.4208	-0.0026
54.109	6.4487	6.4539	-0.0052
54.209	7.4857	7.4889	-0.0032
54.309	8.5322	8.5258	0.0064
54.408	9.5650	9.5649	0.0001
54.508	10.6060	10.6060	-0.0000
54.608	11.6500	11.6493	0.0007
54.708	12.6979	12.6949	0.0030
54.808	13.7392	13.7427	-0.0035

TABLE 6Fit of the Simon Equation to Melting Curve Data

#### IX VAPOR PRESSURE DETERMINATION

Fluorine vapor pressure data are reported in the literature by several experimenters [37, 39, 41, 42]. However, these are inconsistent measurements covering the range from the triple point to just a few degrees above the normal boiling point. To insure accuracy in the subsequent thermodynamic properties calculations it was necessary to obtain consistent vapor pressure measurements extending from the triple point to the critical point. This was done using the PVT pressure measuring system together with the gasometer pressure gages as shown schematically in Figure 14 [43].

### A. Experimental Approach.

Pressures were measured by three different procedures in overlapping ranges from the triple point to the critical point. Pressures below about 0.2 MN/m<sup>2</sup> were measured directly using the fused quartz bourdon tube pressure gage previously calibrated to the air dead-weight gage. Pressures above 0.003 MN/m<sup>2</sup> to about 4 MN/m<sup>2</sup> were measured by referencing the fluorine to nitrogen pressures derived directly from the air piston deadweight gage using a diaphragm type differential pressure transducer. Above 0.13 MN/m<sup>2</sup>, pressures were referenced to the oil dead-weight gage using two differential pressure transducers with an intermediate nitrogen system separating the oil and the fluorine





for safety purposes.

Each vapor pressure reading was made at least twice at a given temperature with some fluorine being removed from the cell between readings. Identical pressure readings verified the fact that two-phase conditions existed in the cell during a measurement.

#### B. Correlation of Vapor Pressure Data.

The fluorine vapor pressure data in Table 13 obtained as a result of this work were represented by the following equation:

$$\ln \left(\frac{P}{P_{t}}\right) = A_{1}X + A_{2}X^{2} + A_{3}X^{3} + A_{4}X \left(1 - X\right)^{A_{5}}$$
(32)

where

$$X = (1 - T_t/T)/(1 - T_t/T_c)$$

$$P_t = 2.52 \times 10^{-4} \text{ MN/m}^2$$

$$T_t = 53.4811 \text{ K}$$

$$T_c = 144.31 \text{ K}$$

The subscripts t and c refer to the triple point and the critical point, respectively. A trial and error method was used to select the value of the triple point pressure which resulted in the smallest sum of the squared deviations between the data and the corresponding calculated values. Changes in this pressure of the order of 0.5 percent were directly reflected in larger deviations all the way to the critical point. The obtained value agrees well (0.3 percent) with the pressure calculated by Ziegler and Mullins [44]. Equation (32) was recently developed by Goodwin [45] through a comprehensive study of vapor pressure equations. It is nonanalytic at the critical point, i.e., the curvature is infinite, and exhibits a reliable slope dP/dT over the entire liquid range, a requirement that the polynomial type equations do not always meet.

The coefficients,  $A_i$ 's, of Equation (32) were determined by a least-squares fit of the experimental data in Table 13. An iterative procedure was adopted such that the chosen value for  $A_5$ minimized the weighted sum of the squared deviations. However, this value of  $A_5$  must be between 1.0 and 2.0 to give infinite curvature at the critical point. The selected coefficients for the vapor pressure equation with P in MN/m<sup>2</sup> and T in degrees K, are

$$A_1 = 7.89592346$$
  
 $A_2 = 3.38765063$   
 $A_3 = -1.34590196$   
 $A_4 = 2.73138936$   
 $A_5 = 1.4327$ 

All parameters of this equation are significant at a level better than 99.9 percent when the standard F-test is applied.

The weight factors, W, in the least-squares fit were defined as the inverse of the sum of the variance in pressure and an equivalent variance, defined according to the error propagation formula, due to errors in temperature. Hence,

$$W = \frac{1}{\sigma_{P}^{2} + \left(\frac{\partial P}{\partial T} \sigma_{T}\right)^{2}}$$

where  $\sigma_P^2$  and  $\sigma_T^2$  are the respective variances in pressure and temperature.

### C. Discussion.

The experimental data are compared to the vapor pressure equation in Figure 15. Pressure deviations are defined as  $(P_{exp} - P_{calc}) \times 100/P_{exp}$ , where  $P_{exp}$  is the experimental pressure and P is the value calculated from Equation (32). Data by other experimenters [37, 39, 41] were adjusted in temperature whenever possible to conform with the IPTS 1968 temperature scale and compared to the new data in Figure 15. Rigorous calculated values [44] based on thermodynamic data such as latent heats due to phase changes, heat capacity and mean molal volume of the liquid, etc. and fluorine molecular constants [46] are also compared in this figure. However, the data from these sources were not included in the final fit of the vapor pressure equation since they deviate from the new data by as much as 16 percent. These large deviations are partly due to problems involved in the early fluorine vapor pressure measurements, which involved reaction of fluorine with mercury in the glass



Figure 15. Deviations of vapor pressure data from Equation(32).

equalizing manometer [37] and the difficulty in obtaining a pure fluorine sample. The data by Claussen [42] were not considered as they were given in terms of a vapor pressure equation. Deviations of the data from this equation were reported to be as much as 2.5 percent.

No previous measurements of fluorine vapor pressure exist above 89.4 K, but values given by Landau and Rosen [47] obtained by extrapolating the data of Cady and Hildebrand [37] to higher temperatures, appear to be in error by as much as - 15 percent.

By interpolating the data in Table 7 directly, a normal boiling point temperature of  $84.95_0 \pm 0.003$  K on IPTS 1968 was obtained. This agrees well with published values of 85.03 K [39] and 84.95 K [37], corrected for temperature scale differences.

Calculated vapor pressures [44] are based on the normal boiling point of [39] and hence agree well with that data in this region, but they deviate by as much as + 15 percent from [39] at the triple point.

#### X REPRESENTATION OF SINGLE-PHASE PVT DATA

All experimental single-phase PVT data in both the compressed liquid and vapor regions are given in Table 14. The column of this table labeled "IDENT" contains the identification number of each data point. The last two digits represent the point number while the remaining digits are the number of the run or experimental isochore. Entries in runs 120 and 121 which contain no value for the density are pressures measured on the melting curve.

Some attempts were made to fit this data with an equation of state used successfully for other cryogenic fluids [25]. However, this equation was not capable of representing the data to within its precision, a fact particularily evident in the critical region. Therefore, to obtain the best possible representation of all the data, it was decided to divide the PVT surface into two regions as pictured in Figure 16. The data in each region were correlated separately as discussed below. No other published single-phase fluorine PVT data were available for comparison to the new data.

#### A. Low Density Region.

Experimental PVT data of densities less than 0.22 mol/l were obtained indirectly as gasometer measurements at these low densities were not possible. Pressures were



Figure 16. Density-temperature diagram showing the divided surface used for computations of thermodynamic properties.

obtained using the air dead-weight gage while the density was derived by heating the PVT cell to 175 K using the known pressuredensity relationship for that isotherm. These data together with all other experimental PVT data below 6.0 mol/l in density were represented by the truncated virial equation

$$P = RT \left[\rho + B(T)\rho^{2} + C(T)\rho^{3}\right].$$
(34)

The second and third virial coefficients were expressed as a function of temperature by

$$B(T) = \sum_{i=1}^{5} B_{i} T^{(1-i)/4}$$
(34a)

and

$$C(T) = \sum_{i=1}^{6} C_i T^{(1-i)/2}, \qquad (34b)$$

respectively. An iterative method was used to optimize both the number of coefficients of B(T) and C(T) and their temperature dependency.

The decision to use 6.0 mol/l as a maximum density value for the virial surface was based on the results obtained by fitting the experimental data to Equation (34). By varying the maximum experimental density included in the fit of this equation, the data exhibited definite systematic deviations from the equation in density as well as temperature for all maximum densities

greater than 6.0 mol/l. Equation (34) was based on the 329 PVT data points in the virial region. Further, 26 experimental singlephase specific heat (C.) data points [48] between 6.5 and 6.8 mol/1 at temperatures from 140 K to 300 K were compared to extrapolated C, values calculated from the virial equation. The reason for this was to ascertain that the apparent deviations were fairly constant and not a function of temperature. The coefficients of Equations (34a) and (34b) and their significance level obtained through a weighted least-squares fit of all the PVT data in this region are given in Table 7. Weight factors [23] used in the fitting of Equation (34) were similar to those used for the vapor pressure equation (32), except variances in density were also considered. PVT data below 100 K were weighted much lower than above this temperature as the uncertainty of the measurements in this region increases rapidly with decreasing density. The weighted standard deviation in density between the virial surface and all of the 329 PVT data points is 0.041 percent. For consistency, Equation (34) was constrained to give the same saturation temperature (137.327 K) for the 6.0 mol/l isochore as is obtained from Equation (30).

The second and third virial coefficients, calculated from Equations (34a) and (34b), are given in Table 8. Also given in this table are the quantities  $\delta B$  and  $\delta C$  which are the respective estimated uncertainties of the coefficients based on the experience

Coefficient	Least squares estimate of coefficient	Standard deviation of coefficient	Significance level in percent*
B <sub>1</sub>	-4.43719523	1.10	99.9+
B <sub>2</sub>	6.88646977 x 10	1.61 x 10	99.9+
B <sub>3</sub>	-4.00652537 x 10 $^{2}$	8.85 x 10	99.9+
B <sub>4</sub>	$1.04730534 \times 10^{3}$	2.15 x 10 <sup>2</sup>	99.9+
В <sub>Б</sub>	-1.05492603 x 10 <sup>3</sup>	1.96 x 10 <sup>2</sup>	99.9+
C <sub>1</sub>	3.97288149 x 10 <sup>-1</sup>	6.38 x $10^{-2}$	99.9+
C 2	-2.80769183 x 10	4.33	99.9+
C <sub>3</sub>	7.95698766 x 10 $^{2}$	1.18 x 10 <sup>2</sup>	99.9+
C $_4$	-1.12867697 x 10 $^{4}$	$1.59 \times 10^{3}$	99.9+
C <sub>5</sub>	8.01450388 x 10 $^4$	$1.08 \times 10^{4}$	99.9+
C <sub>6</sub>	-2.27594177 x 10 $^{5}$	$2.93 \times 10^4$	99.9+

TABLE 7Least Squares Estimate of the Coefficients

of Equation (34)

\* These parameters are significant at the level indicated when applying the standard F-test.

FABLE 8 Second and Third Virial Coefficients of Fluorin
---

Т	В	δΒ x 10 <sup>3</sup>	С	$\delta C \times 10^{3}$
K		l/mol		(1/mol) <sup>2</sup>
80 -	0.2396	40	-0.022557	20
85 -	0.2132		-0.013548	
90 -	0.1910		-0.007748	
95 -	0.1722		-0.004016	
100 -	0.1561	10	-0.001624	3
105 -	0.1422		-0.000106	
110 -	0.1301		0.000838	
115 -	0.1194		0.001409	
120 -	0.1100		0.001736	
125 -	0.1017	2	0.001905	• 5
130 -	0.0942		0.001973	
135 -	0.0875		0.001979	
140 -	0.0815		0.001947	
145 -	0.0759		0.001893	
150 -	0.0709	• 3	0.001828	•03
155 -	0.0663		0.001758	
160 -	0.0621		0.001689	
165 -	0.0582		0.001621	
170 -	0.0546		0.001557	
175 -	0.0512		0.001498	
180 -	0.0481		0.001442	
185 -	0.0452		0.001391	
190 -	0.0425		0.001344	
195 -	0.0400	0	0.001301	
200 -	0.0376	• 3	0.001261	•03
205 -	0.0354		0.001224	
210 -	0.0332		0.001190	
215 -	0.0313		0.001159	
220 -	0.0274		$() \bullet 001150$	
220 -	0.0210		0.00104	
230 -	0.02/3		0.001057	
235 -	0.0243		0.001037	
240 -	0.0210		0.001037	
250 -	0.0200	. 3	0.001013	. 03
255 -	0.0197	• •	0.001003	.05
250 -	0.0175		000976	
265 -	0.0163		0.000976	
270 -	0.0152		0.000957	
275 -	0.0141		0.000951	
280 -	0.0131		0.000947	
285 -	0.0122		0.000946	
290 -	0.0112		0.000946	
295 -	0.0104		0.000949	
300 -	0.0095	• 3	0.000955	•04

( $\delta$ B and  $\delta$ C are estimated uncertainties)

gained when fitting the virial surface. A comparison of the second virial coefficient with values obtained by White, Hu, and Johnston [49] is given in Figure 17. In the calculation of their data these authors neglected the contribution of the third and higher order virial coefficients, which is the probable reason for their larger negative values, especially at lower temperatures. Temperature scale differences could account for part of the deviations. Since the data from Reference [49] do not represent just the second virial coefficient, further comparisons with Equation (34a) were made by converting values from oxygen [4] and argon [50] using the corresponding states approach based on critical parameters as follows:

$$B_{\text{converted}} = B(X) \frac{\rho_{c}(X)}{\rho_{c}(F_{c})}$$

and

$$T_{converted} = T(X) \frac{T_{c}(F_{2})}{T_{c}(X)}$$

where X represents either oxygen or argon. The agreement is good as may be seen from Figure 17. In fact, the correspondence between values calculated from the second virial coefficient of oxygen and Equation (34a) is better than one may justifiably expect from the principle of corresponding states.

No published values for the third virial coefficient of fluorine were available for comparison to Equation (34b).



Figure 17. Comparisons of second virial coefficients of fluorine.

#### B. High Density Region.

## l. Isotherms

The high density region (see Figure 16) bounded by the 6.0 mol/l isochore, the vapor-liquid coexistence boundary, the melting curve, and the 21 MN/m<sup>2</sup> isobar was represented by 70 isotherm polynomials of the form

$$P = RT\rho + \sum_{i=1}^{n} A_{i} \rho^{i-1} , \qquad (35)$$

where  $A_1 = A_2 = 0$  for  $T > T_c$  or  $\rho < \rho_c$ .

Data points for a fictitious liquid isotherm at 53.4 K, used for the purpose of extrapolating to the melting curve, were obtained from an extrapolation of isobars calculated from the isotherms between 56 K and 64 K. A few points on the 54 K isotherm were also obtained in this manner. The density of the liquid in equilibrium with the solid derived from the mentioned isobars, was expressed as a function of either temperature or pressure by

$$\rho_{melt L} = \rho_t + 0.208 (T - T_t), mol/l$$
 (36)

or

$$\rho_{melt L} = \rho_t + 0.020 P(MN/m^2).$$
 (37)

A value of 44.86  $_2$  mol/l was used for the liquid density,  $\rho_t$ , at the triple point.

No more than 3 coefficients were used for the isotherms below 60 K since these consisted of only 4 P- $\rho$  data points each. As many as 9 coefficients were necessary for the 146 K and 148 K isotherms (slightly above the critical temperature) to adequately represent the data. From 4 to 7 coefficients were needed to represent all of the remaining isotherms. The isotherms in the compressed liquid and gaseous phases below the critical temperature were constrained to the corresponding saturation density of Equations (29) and (30), respectively. Above 138 K the isotherms were also fitted to the low density data in the virial region to provide a better match of the surfaces around the 6.0 mol/l isochore.

The standard deviation of the 381 experimental data points in the compressed liquid was only 0.005 percent in density while the 540 compressed vapor data points exhibit a larger deviation of 0.018 percent. The latter value is higher due mainly to the contribution from the isotherms just above the critical temperature where the deviations are much larger than over the rest of the surface. However, this is what one normally would expect.

## 2. Isochores

Most calculations of thermodynamic properties require knowledge of the quantities  $(\partial P/\partial T)_{\rho}$  and  $(\partial^2 P/\partial T^2)_{\rho}$ . In the low density region these derivatives may be calculated directly from

Equation (34) while for densities above 6.0 mol/l it was necessary to calculate pressures at even density increments. These isochores were then represented using functions of the form

$$P = \sum_{i=1}^{n} A_{i} T^{(3-2i)}$$
(38)

Density increments of 0.5 mol/l were used for the 80 isochores between 5.5 and 45.0 mol/l. The number of terms of Equation (38) varied from 7 at the lowest density to 3 at the 45.0 mol/l isochore. The good fit of the isotherms was directly carried over in the correlation of these isochores.

#### XI DERIVED THERMODYNAMIC PROPERTIES

Additional data to the PVT measurements are necessary in the calculations of derived thermodynamic properties. These are mainly thermodynamic functions of the ideal gas; however, specific heat data of the single-phases and the saturated liquid also help to improve the accuracy of the calculations.

## A. Thermodynamic Functions of Ideal Gas.

Since new measurements of the dissociation energy of fluorine [51] recently became available, it was decided to recompute the ideal gas thermodynamic functions of this fluid. Maximum changes in the functions compared to earlier values [46] were less than 0.1 percent for temperatures of 300 K and below. These thermodynamic functions were calculated according to the statistical mechanical treatment of Mayer and Mayer [52] for diatomic molecules. The relationships based on their approach include first order corrections to the harmonic oscillator-rigid rotator for: vibrational anharmonicity, rotational stretching, and rotationvibration interaction. No attempt will be made here to define all different parameters. The conventional nomenclature for these variables may be obtained from standard texts [52, 53]. The correlations are as follows:

Translational and rotational contributions:

$$-(F^{\circ} - H^{\circ}_{\circ})/RT = 1.5 \ln M + 2.5 \ln T - 3.6644173$$
$$-\ln \sigma + \sigma/3 + \sigma^{2}/90$$
(39)

$$(H^{\circ} - H^{\circ}_{o})/RT = 3.5 - \sigma/3 - \sigma^{2}/45$$
 (40)

$$C_{P}^{2}/R = 3.5 + \sigma^{2}/45$$
 (41)

where 
$$\sigma = (B_e - \alpha_e/2) hc/kT = 1.27028/T.$$
 (42)

Vibrational contributions:

$$-(F^{\circ} - H^{\circ}_{0})/RT = -\ell n (1 - e^{-u})$$
(43)

$$(H^{\circ} - H^{\circ}_{0})/RT = ue^{-u}/(1 - e^{-u})$$
 (44)

$$C_{p}^{\circ}/R = u^{2} e^{-u}/(1 - e^{-u})^{2}$$
 (45)

where 
$$u = (\omega_e - 2\chi_e \omega_e) hc/kT = 1283.30/T.$$
 (46)

# Anharmonicity contributions:

$$-(F^{\circ} - H^{\circ}_{\circ})/RT = 8\gamma^{2}/\sigma + \delta e^{-u}/(1 - e^{-u}) + 2X u e^{-2u}/(1 - e^{-u})^{2}$$
(47)

$$(H^{\circ} - H^{\circ}_{\circ})/RT = 8 \gamma^{2}/\sigma + \delta u e^{-u}/(1 - e^{-u})^{2} + 4X u^{2} e^{-2u}/(1 - e^{-u})^{3}$$
$$- 2X u e^{-2u}/(1 - e^{-u})^{2}$$
(48)

$$C_{P}^{\circ}/R = 16 \gamma^{2}/\sigma - \delta u^{2} e^{-u}/(1 - e^{-u})^{2} + 2 \delta u^{2} e^{-u}/(1 - e^{-u})^{3}$$
$$- 8X u^{2} e^{-2u}/(1 - e^{-u})^{3} - 4X u^{3} e^{-2u}/(1 - e^{-u})^{3}$$
$$+ 12X u^{3} e^{-2u}/(1 - e^{-u})^{4}$$
(49)

where

$$\delta = \alpha / B_{0} = 0.02107 \tag{50}$$

$$8\gamma^2 = 2D / B = 7.5095 \times 10^{-6}$$
 (51)

$$X = w_{e} \chi_{e} / w_{e} = 0.02064.$$
 (52)

Finally, values of entropy were computed from the following relationship

$$S^{\circ}/R = (H^{\circ} - H^{\circ}_{0})/RT - (F^{\circ} - H^{\circ}_{0})/RT.$$
 (53)

The variables  $\sigma$ , u,  $\delta$ ,  $\gamma$ , and X were calculated from the new measurements of the dissociation energy of fluorine [51] and the Raman spectrum measurements of Andrychuk [54].

Table 9 list some representative values of the ideal gas functions used in the calculations of the thermodynamic properties of fluorine. Further checks on the ideal gas enthalpy, H°, and entropy, S°, were obtained by numerically integrating the ideal gas specific heat at constant pressure, C° (Equations (41, 45, 49)) and C° /T as functions of temperature, respectively. All deviations from the values given in Table 9 were less than 0.001 percent. H° was taken to be zero in all calculations.

## B. Calculational Methods.

Obviously no integration with respect to density of the thermodynamic equations was possible until a final density was determined for a given temperature and pressure. This was.done

Τ,	C°	H° - H°	S°
K	R	RT	R
50	3.50061	3.49181	18.05212
60	3.50072	3.49329	18.69036
70	3.50084	3.49436	19.23001
80	3.50098	3.49518	19.69749
90	3.50120	3.49583	20.10986
100	3.50163	3.49639	20.47877
110	3.50250	3.49690	20.81255
120	3.50407	3.49743	21.11736
130	3.50668	3.49803	21.39793
140	3.51062	3.49878	21.65794
150	3.51617	3.49974	21.90033
160	3.52350	3.50099	22.12748
170	3.53271	3.50258	22.34136
180	3.54381	3.50455	22.54359
190	3.55675	3.50695	22.73553
200	3.57140	3.50980	22.91833
210	3.58762	3.51311	23.09297
220	3.60520	3.51689	23.26027
230	3.62396	3.52114	23.42093
240	3.64370	3.52583	23.57558
250	3.66420	3.53095	23.72474
260	3.68530	3.53648	23.86886
270	3.70681	3.54239	24.00835
280	3.72857	3.54865	24.14355
290	3.75045	3.55523	24.27477
300	3.77233	3.56210	24.40228
310	3.79410	3.56924	24.52633

by an iterative process of the virial equation for densities below 6.0 mol/l and of the isotherms for densities above 6.0 mol/l. Once the density had been established, the calculations were performed using the following equations.

For densities less than critical at T less than  $T_2$  (= 160 K) and for all densities for  $T \ge T_2$ , the thermodynamic properties were calculated as follows:

$$H(T, \rho) = H^{\circ}(T) + \frac{P}{\rho} - RT + \int_{O}^{\rho} \left[\frac{P}{\rho^{2}} - \frac{T}{\rho^{2}} \left(\frac{\partial P}{\partial T}\right)_{\rho}\right] d\rho , \qquad (54)$$

$$S(T, \rho) = S^{\circ}(T) - R \ln \left(\frac{R T \rho}{P_{o}}\right) + \int_{0}^{\rho} \left[\frac{R}{\rho} - \frac{1}{\rho^{2}} \left(\frac{\partial P}{\partial T}\right)_{\rho}\right] d\rho , \qquad (55)$$

where  $P_0 = 1$  atm;

$$C_{v} (T, \rho) = C_{v}^{\circ} (T) - T \int_{O}^{\rho} \frac{1}{\rho^{2}} \left( \frac{\partial^{2} P}{\partial T^{2}} \right)_{\rho} d\rho .$$
 (56)

The ideal gas properties for enthalpy, entropy, and specific heat, H°, S°, and  $C_v^{\circ}(=C_p^{\circ}-R)$ , respectively were obtained from Equations (39) through (53). All integrations in the high density region of Figure 16 were carried out numerically using the trapezoidal rule. For the development of these and the following
equations the reader is referred to References [55, 56].

For densities greater than the critical between temperaatures  $T_1 = 135$  K and  $T_2 = 160$  K the starting points for the calculations are taken as those calculated from the above equations at  $T_2$  and a density  $\rho_1 = 26.4276$  mol/l. The specific heats along this isochore, given by Equation (69), were used to compute the changes in properties as a function of temperature:

$$H(T, \rho_{1}) = U(T_{2}, \rho_{1}) + \int_{T_{2}} C_{v}(T, \rho_{1}) dT + P(T, \rho_{1})/\rho_{1} , \qquad (57)$$

$$S(T, \rho_1) = S(T_2, \rho_1) + \int_{T_2}^{T} [C_v(T, \rho_1)/T] dT$$
(58)

where the internal energy was obtained from

$$U(T_{2}, \rho_{1}) = H(T_{2}, \rho_{1}) - P(T_{2}, \rho_{1})/\rho_{1}.$$
(59)

Further computations were made along isotherms using

$$H(T, \rho) = H(T, \rho_1) + \int_{\rho_1}^{\rho} [P - T (\partial P / \partial T)_{\rho}] / \rho^2 d\rho$$

+ 
$$P(T, \rho)/\rho - P(T, \rho_1)/\rho_1$$
, (60)

$$S(T, \rho) = S(T, \rho_1) - \int_{\rho_1}^{\rho} [(\partial P / \partial T)_{\rho} / \rho^2] d\rho , \qquad (61)$$

and

$$C_{v}(T, \rho) = C_{v}(T, \rho_{1}) - T \int_{\rho_{1}}^{\rho} \left[ (\partial^{2} P / \partial T^{2})_{\rho} / \rho^{2} \right] d\rho.$$
 (62)

For the compressed liquid at temperatures less than  $T_1$  (= 135 K) use was made of the properties of saturated liquid at ( $T_1$ ,  $\rho_1$ ) as a starting point for the computations. Changes in properties along the saturated liquid curve were calculated from the following equations:

$$H(T, \rho_{sat L}) = H(T_{1}, \rho_{sat L}) + \int_{T_{1}}^{T} C_{sat} dT$$

$$P_{sat}(T)$$

$$+ \int_{P_{sat}(T_{1})} (1/\rho_{sat L}) dP, \qquad (63)$$

$$S(T, \rho_{sat L}) = S(T_{1}, \rho_{sat L}) + \int_{T_{1}} (C_{sat} / T) dT,$$
(64)

and

$$C_{v}(T, \rho_{sat L}) = C_{sat}(T) + \frac{T}{\rho_{sat L}^{2}} \left(\frac{d\rho_{sat L}}{dT}\right) \left(\frac{\partial P}{\partial T}\right)_{v} .$$
 (65)

Since the integral of Equation (64) cannot be solved analytically and since  $(1/\rho_{sat L})$  was not correlated as a function of the vapor pressure, these integrals were obtained numerically. C<sub>sat</sub> (T) is the saturated liquid specific heat as discussed in the following section and given by Equation (68). Further computations in the compressed liquid region along isotherms were made using Equations (60), (61) and (62) in which  $\rho_{sat L}$  (T) was substituted in place of  $\rho_1$ .

Calculations of internal energy and specific heats at constant pressure were performed using

$$U(T, \rho) = H(T, \rho) - P(T, \rho)/\rho,$$
(66)

and

$$C_{P}(T, \rho) = C_{v}(T, \rho) + (T/\rho^{2})(\partial P/\partial T)_{0}^{2}/(\partial P/\partial \rho)_{T}.$$
(67)

### C. Specific Heat Data Used

Specific heat measurements of fluorine [48, 57], recently completed in this laboratory, were used to improve the accuracy of the thermodynamic properties and make the thermodynamic calculations more consistent. In the calculations for the compressed liquid and the compressed gas below 160 K use was made of the specific heat of saturated liquid [57],  $C_{sat}$  (this quantity does not include the specific heat of the corresponding saturated vapor), expressed in the following form

$$C_{sat}(T) = A_{1}(T_{c} - T) + \sum_{i=3}^{A_{2}} A_{i} T^{i-3}$$
 (68)

The coefficients for this equation are given in Table 10. The root-mean square deviation of the 34  $C_{sat}$  data points between the triple and the critical point is 0.11 percent.

 $C_v$  measurements by Prydz and Goodwin [48] along an isochore of density  $\rho_1 = 26.4276$  mol/l were also used for the thermodynamic properties calculations. Since the  $C_v$  data close to this density were measured at pseudo-isochores, the data points were adjusted to  $\rho_1$  using the experimental PVT data in this region according to Equation (62). This  $C_v$  isochore intersects the liquid saturation boundary at a temperature of 135.000 K (T<sub>1</sub>) and the 160 K (T<sub>2</sub>) isotherm (T<sub>2</sub> = 160.010 K on IPTS 1968) at a pressure of 20.8 MN/m<sup>2</sup>. Analytically, these specific heat measurements at the  $\rho_1$  - isochore were represented by

$$C_{v}(\rho_{1}) = \sum_{i=1}^{4} A_{i} T^{i-3}$$
 (69)

where the coefficients are given in Table 10. To obtain even more consistent results, Equation (69) was constrained at  $C_v(T_1, \rho_1)$ = 28.282 J/mol as calculated by the following expression

$$C_{v}(T_{1}, \rho_{1}) = C_{sat}(T_{1}) + \frac{T_{1}}{\rho_{1}^{2}} \left[ \left( \frac{d \rho_{sat L}}{dT} \right) \left( \frac{\partial P}{\partial T} \right)_{\rho_{1}} \right]_{T_{1}}.$$
 (70)

Equation (69) was based on 20 adjusted (to  $\rho_1$ ) experimental C v points which exhibit a root-mean-square deviation of 0.09 percent when the equation is constrained. Prior to constraining Equation (69) the value of C v(T 1,  $\rho_1$ ) calculated from this equation (Eq. (69)) was about 0.2 percent less than that obtained from Equation (70). This is certainly within the accuracy of  $C_{sat}$  (135 K). Further, the quantity (d  $\rho_{sat L}/dT$ ) is the temperature dependency of the

Coefficient	Equation (68)	Equation (69)
A <sub>1</sub>	$2.05286929 \ge 10^2$	5.06916112 x 10 <sup>6</sup>
Az	-0.593	-9.49753733 x $10^4$
A <sub>3</sub>	-4.29836188	$6.25979166 \ge 10^2$
A <sub>4</sub>	2.08808261	-1.27643818
A <sub>5</sub>	-3.45371635 x 10 <sup>-2</sup>	
A <sub>6</sub>	2.40274037 x $10^{-4}$	
A <sub>7</sub>	-6.13321958 x 10 <sup>-7</sup>	

TABLE 10 Coefficients for Equations (68) and (69)

saturated liquid density (Equation (29)) and  $(\partial P/\partial T)_{\rho_1}$  is the terminal slope of the  $\rho_1$ -isochore at the vapor-liquid coexistence boundary. These slopes cannot be estimated with confidence by extrapolating the PVT data because the isochores in this terminal region may have maximum curvature. Considering that  $C_{sat}$  is about  $3C_v$  at  $T_1$  (135 K) and that the bases for the thermodynamic properties calculation are Equations (68) and (65) below  $T_1$  while Equation (69) is used as a starting point above this temperature, the reason for constraining Equation (69) becomes self-evident.

### D. Calculated Results.

Calculated points on the Joule-Thomson inversion curve

are given in Table 11. This curve is defined as the locus of points where the Joule-Thomson coefficient is equal to zero. This condition may be described in classical thermodynamics by the relationship

$$-\frac{\mathrm{T}}{\rho^{z}}\left(\frac{\partial\rho}{\partial\mathrm{T}}\right)_{p} = \frac{1}{\rho}$$
(71)

or more conveniently

$$T \left(\frac{\partial P}{\partial T}\right)_{\rho} = \rho \left(\frac{\partial P}{\partial \rho}\right)_{\tau}.$$
 (72)

Equation (72) may be solved by an iterative technique using the isotherm derivative,  $(\partial P/\partial \rho)_T$ , and the isochore derivative,  $(\partial P/\partial T)_{\rho}$ , obtained from Equations (35) and (38), respectively. The computed pressure errors in Table 11 are based on an assumed uncertainty of 1 percent in these derivatives.

Tables 15 and 16 present the results of all thermodynamic property calculations on the vapor-liquid saturation boundary and on selected isobars, respectively. The velocity of sound,  $W_s$ , was calculated from the following relationship

$$W_{s} = \left[ (C_{p}/C_{v}) (\partial P/\partial \rho)_{T} \right]^{1/2} .$$
(73)

The variation of  $C_p$  with temperature along several isobars is illustrated in Figure 18, while Figure 19 shows the density dependence of  $C_v$  along various isotherms.

TABLE 11 The Joule-Thomson Inversion Curve

T K	P MN/m²	Density mol/l	∆P* MN/m²
118	2.732	32.615	0.19
120	4.340	32.411	0.21
122	6.092	32.250	0.22
124	7.649	32.058	0.23
126	9.288	31.895	0.23
128	10.861	31.727	0.25
130	12.373	31.556	0.25
132	13.824	31.381	0.26
134	15.278	31.214	0•26
136	16.583	31.024	0.28
138	17.980	30.864	0.27
140	19.155	30.664	0.26
142	20.811	30.573	0.31
144	21.668	30.322	0.31

\* These estimated pressure errors are due to a 1 percent assumed uncertainty in either the isotherm or the isochore derivative.



Figure 18. Specific heat at constant pressure, C<sub>p</sub>, along selected isobars.



Figure 19. Specific heat at constant volume,  ${\tt C}_{\tt v}\,,$  along selected isotherms.

E. Discussions Concerning the Derived Properties.

The best estimates of the accuracy of the derived thermodynamic properties are obtained by making comparisons with experimental values for these properties. In general, though, such data are often scarce, limited in scope, or of poor accuracy. In the case of fluorine, thermodynamic property data are practically nonexistent.

Internal consistency checks may be made by performing closed loop computations for different regions of the PVT surface. Because of the somewhat roundabout method used to calculate the enthalpy of the liquid as described in Section B of this chapter, it is particularly desirable to make comparisons with liquid enthalpies obtained by different methods. This may be done by comparing heats of vaporization reported by different sources as given in Table 12. The second and third columns of this table present values of  $\Delta H$  and T $\Delta S$  obtained from Table 15. The differences between these two columns need to be explained.  $\triangle H$  should not differ from  $T \triangle S$  by more than a few J/mol if all correlations used for the computations provide the "true" value for a particular variable. An error offset in the vapor pressure at the triple point of 2 percent would alter the  $T \triangle S$  value at this temperature by 9 J/mol due to a change in the entropy value of the vapor as a result of the R  $\ell$ n (RT $\rho$ /P $_{o}$ ) term in Equation (55). Obviously,  $\Delta H$  in

	Ca	lculated - Th	iis Research			
	Tal	ble 15		Ref. [44]	Ref. [35]	Other Sources
Ч			Clapeyron	Clapeyron	Clapeyron	Clapeyron
K	$\Delta H$	$T \Delta S$	Equation	Equation	Equation	Equation
53.481 <sub>1</sub>	7578	7543	7506	7510		
60 <sup>1</sup>	7407	7377	7341	7323		
70	7130	7106	7060	7032		
80	6825	6807	6759	6714		
84.71	6667	6652	6605			6544*, 6519 [39]
84.93	6659	6644	6597			6443 [37]
84.95	6659	6644	6597			
85.03	6656	6641	6594	6532		
85.19	6650	6635	6589			6615 [41]
85.21	6649	6635	6588			6527 [42]
06	6475	6462	6418		6116	
00	6056	6048	6009		5648	
10	5539	5534	5501		5117	
20	4877	4875	4852		4472	
30	3977	3976	3965		3636	
40	2481	2481	2472		2247	
44	943	943	935		564	

\* Calorimetric data.

TABLE 12 Comparison of Heats of Vaporization,  $\Delta H$ , J/mol

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the second column of Table 12 would not be altered. The differences, however, may also be due to errors in the saturated liquid specific heat,  $C_{sat}$  (Equation (68)). An average error in  $C_{sat}$  of -2 percent between 53.5 K and 135 K would change  $\Delta H$  at the triple point temperature by about -103 J/mol and T $\Delta S$  by approximately -60 J/mol, resulting in a net difference of essentially 43 J/mol. Other heats of vaporization in Table 12 are calculated by the Clapeyron equation

$$\Delta H = T(V_{qy} - V_{\ell}) \frac{dP}{dT} , \qquad (74)$$

where  $(V_{q_1} - V_{q_2})$  is the difference in the molar volumes of the saturated gaseous and liquid phases and dP/dT is the slope of the vapor pressure curve. These  $\Delta H$  - values, however, suffer from relatively large uncertainties in dP/dT and V<sub>q</sub> at low temperatures. Calculations by Ziegler and Mullins [44] agree well with the new data ( $\Delta H_{elap}$ ) near the triple point but the deviations increas as the temperature approaches 85 K. This is to be expected since Ziegler and Mullins' vapor pressures are based on the normal boiling point of Reference [39], as may be noted from Figure 15. Fricke [35] based his  $\Delta H$  - calculations on the Berthelot equation of state which gives vapor densities differing from Equation (31) by as much as 10 percent at 140 K.

The entropy value of the saturated liquid at the triple point calculated using the method described in Section B of this chapter,

is 60.862 J/mol K. Hu, White, and Johnston [39] report a value of 61.028 ± 0.25 J/mol K based on their solid fluorine calorimetric data. More recent calculations by Ziegler and Mullins [44] resulted in 60.777 J/mol K, the difference being attributed primarily to improved calculations of the entropy change in the extrapolated region from 0 - 14 K. In any case, it may be concluded that the agreement among the three values is consistent with the Third Law of Thermodynamics. Thus, the T∆S values are more likely to represent the correct values of the heats of vaporization since large errors in the vapor pressure equation are not probable.

Experimental specific heats,  $C_v$ , measured by Prydz and Goodwin [48] agree well with values calculated from the PVT surface for densities above the critical and temperatures below 160.01 K. This is to be expected since the calculated specific heats in this region of the PVT surface were based on the experimental values for  $C_v$  [48] and the  $C_{sat}$  measurements of Goodwin and Prydz [57]. Over the rest of the surface the measured  $C_v$  values are larger than the values calculated from the PVT data. The disagreement is within the combined uncertainty of the two experiments, although at high pressures (20 MN/m<sup>2</sup>) and 160.01 K maximum discrepancies of about 3 percent in  $C_v$  are apparent.

Calculated specific heats at constant pressure,  $C_p$ , are not as smooth as may be desired. These quantities are based on the

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ratio of the square of the isochore derivative,  $(\partial P/\partial T)_{\rho}^{2}$ , to the isotherm derivative,  $(\partial P/\partial \rho)_{T}$ , which are not likely to be completely smooth in the terminal regions of the PVT surface. In these regions a density error of 0.01 percent can result in relatively large errors in the slopes. Also, the integration of the second derivative of the isochores as indicated by Equation (62) increases the probability of a somewhat erratic behavior. The actual values of the  $C_{\rho}$ 's, however, should be as accurate as may be calculated from an equation of state and indicate better what uncertainty in the computed values may be expected from the calculations.

No experimental sound velocities for fluorine have been reported in the literature. However, the divergence of  $C_v$  which has been observed for several fluids, including fluorine [48], near the critical point, implies the vanishing of the isentropic sound velocity as proposed by Yang and Yang [58]. Recent measurements by Barmatz [59] on He<sup>4</sup> also show similar behavior. Calculated velocities of sound for fluorine presented in Tables 15 and 16, tend to indicate such a trend.

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#### XII CONCLUSIONS

An apparatus has been constructed and used successfully to measure about 150 vapor pressure data points and more than 1000 PVT points for fluorine from the triple point to 300 K at pressures to about 24 MN/m<sup>2</sup>. The problems associated with the high reactivity and extreme toxicity of this element which impose severe requirements on system compatibility and provisions for personal safety, were solved.

A network of isotherms and isochores and a virial equation were adopted to represent all PVT data. These equations represent the data to within its precision, which is of the order of 0.05 percent in density over the whole PVT surface. The actual accuracy of the densities predicted from the equations is estimated to be about 0.1 percent. Uncertainties in the temperature and pressure measurements are about 0.01 percent, increasing somewhat in the lower terminal regions. In the critical region the densities obtained at various pressures are necessarily less accurate because of the high isothermal compressibility. However, even though the nonanalytic character that causes the specific heats to diverge in the vicinity of the critical point has not been included in the form of the isotherm and isochore equations, tabulated values of the derived properties given in Tables 15 and 16 are believed to qualitatively show the right behavior in

this region. However, caution should be exercised near the critical point when extrapolating or interpolating on the derived properties. This is particularly true for both the heat capacities and the velocity of sound since these properties supposedly exhibit anomalies in this part of the surface.

Due to the fact that this study is relatively complete (it is also based on experimental specific heats), it is believed that measurements from only a few other experiments would help to confirm or improve the accuracy of the PVT data and the derived properties. Some additional measurements utilizing other experimental techniques [60, 61, 62] covering selected portions of the surface would be valuable for the purpose of checking the accuracy of the PVT correlations obtained in this study. PVT measurements covering the critical region would also help to improve the surface. Such data were recently obtained by Weber [63] in his critical region studies of oxygen by means of dielectric measurements. Corresponding measurements for fluorine would be possible since a compatible insulating material for the electrical leads entering the pressure bomb, has now been found [64]. Thus, the critical parameters could be evaluated with a technique that is more accurate than the one used in this study. Finally, very accurate (preferably better than 0.1 percent) experimental heats of vaporization measurements would help to clarify as to which  $\triangle H$  - column in Table 12 gives the more correct values.

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### TABLE 13. EXPERIMENTAL VAPOR PRESSURES OF LIQUID

FLUORINE

Τ, Κ	P, MN/m <sup>2</sup>	P, atm
54.009	0.000301	0.00297
55.007	0.000410	0.00404
56.005	0.000534	0.00527
<mark>56.</mark> 005	0.000540	0.00533
<b>57.</b> 003	0.000712	0.00702
57.003	0.000713	0.00704
58.002	0.000928	0.00916
58.002	0.000928	0.00916
59.000	0.00120	0.0118
59.000	0.00120	0.0119
59.999	0.00155	0.`0153
59.999	0.00154	0.0153
59.999	0.00155	0.0153
60.999	0.00197	0.0195
61.998	0.00249	0.0245
62.999	0.00311	0.0307
63.999	0.00387	0.0382
63.999	0.00386	0.0380
65.000	0.00477	0.0471
65.000	0.00478	0.0471
66.000	0.00585	0.0577
67.001	0.00710	0.0701
68.001	0.00859	0.0847
69.001	0.01030	0.1017
70.000	0.01231	0.1215
70.000	0.01231	0.1215
71.099	0.01485	0.1466

### TABLE 13. EXPERIMENTAL VAPOR PRESSURES OF LIQUID FLUORINE--Continued

Т, К	$P, MN/m^2$	P, atm
71.998	0.01725	0.1702
72.997	0.02026	0.2000
73.996	0.02369	0.2338
74.994	0.02758	0.2722
74.994	0.02760	0.2724
75.993	0.03196	0.3155
76.992	0.03688	0.3640
76.992	0.03690	0.3642
77.991	0.04241	0.4186
78.991	0.04858	0.4794
79.991	0.05540	0.5467
79.991	0.05540	0.5468
80.991	0.06297	0.6215
81.992	0.07135	0.7041
82.994	0.08059	0.7953
83.995	0.09072	0.8953
84.997	0.10186	1.0053
84.997	0.10187	1.0054
86.000	0.11404	1.1255
87.002	0.12730	1.2564
88.005	0.14172	1.3987
88.005	0.14169	1.3983
88.005	0.14170	1.3985
89.007	0.15726	1.5521
89.007	0.15740	1.5534
90.010	0.17420	1.7192
90.010	0.17424	1.7196

# TABLE 13. EXPERIMENTAL VAPOR PRESSURES OF LIQUID FLUORINE -- Continued

Т, К	P, MN/m²	P, atm
90.010	0.17420	1.7192
90.010	0.17415	1.7187
91.011	0.19250	1.8998
91.011	0.19240	1.8988
92.012	0.21204	2.0927
92.012	0.21204	2.0927
93.012	0.23320	2.3015
94.013	0.25591	2.5256
95.013	0.28018	2.7651
96.013	0.30610	3.0210
97.013	0.33389	3.2952
98.012	0.36356	3.5880
99.011	0.39497	3.8981
100.010	0.42839	4.2279
100.010	0.42848	4.2288
101.009	0.46390	4.5783
102.008	0.50157	4.9501
103.007	0.54132	5.3424
104.005	0.58345	5.7582
105.004	0.62799	6.1978
106.002	0.67481	6.6599
107.001	0.72434	7.1487
108.000	0.77623	7.6608
108.999	0.83094	8.2007
109.998	0.88840	8.7678
109.998	0.88838	8.7676
110.997	0.94876	9.3635
111.996	1.01183	9.9860

### TABLE 13. EXPERIMENTAL VAPOR PRESSURES OF LIQUID FLUORINE--Continued

Т, К	$P, MN/m^2$	P, atm
112.995	1.07805	10.6396
113.995	1.14730	11.3230
114.994	1.21970	12.0375
114.994	1.21971	12.0376
115.993	1.29551	12.7857
116.992	1.37439	13 <b>.56</b> 41
117.991	1.45689	14.3784
118.990	1.54270	15.2253
119.989	1.63224	16.1090
119.989	1.63234	16.1099
119.989	1.63220	16.1086
120.989	1.72550	17.0293
121.988	1.82242	17.9859
122.987	1.92335	18.9820
123.987	2.02779	20.0128
124.987	2.13705	21.0911
125.987	2.24992	22.2050
126.987	2.36742	23.3646
127.987	2.48879	24.5624
128.987	2.61529	25.8109
129.987	2.74590	27.0999
129.987	2.74548	27.0957
130.987	2.88128	28.4361
131.987	3.02153	29.8202
132.987	3.16649	31.2508
133.988	3.31707	32.7370
134.988	3.47235	34.2694
135.989	3.63326	35.8575

## TABLE 13. EXPERIMENTAL VAPOR PRESSURES OF LIQUID FLUORINE -- Continued

Т, К	P, MN/m²	P, atm
136.990	3.80012	37.5043
13 <b>7.</b> 990	3.97266	39.2071
138.991	4.15065	40.9637
138.991	4.15115	40.9687
139.992	4.33565	42.7896
139.992	4.33586	42.7916
139.992	4.33565	42.7895
140.992	4.52689	44.6769
140.992	4.52711	44.6791
141.993	4.72527	46.6348
141.993	4.72518	46.6339
142.994	4.93044	48.6597
142.994	4.93038	48.6590
143.494	5.03628	49.7043
144.31	*5.215	*51.47

\* Critical pressure calculated from Equation (32).

TABLE 14. TEMPERATURE-FRESSURE-DENSITY OBSERVATIONS ON FLUORINE

ТЕМР К	PRESSURE MN/M <sup>2</sup>	DENSITY MOL/L	IDENT	TEMP K	PRESSURE MN/M <sup>2</sup>	DENSITY MOL/L	IDENT
74.994	0.0231	0.0379	13101	115 993	1.2050	1.5135	8101
79,991	0.0249	0.0378	13102	117,991	1.2348	1.5132	8102
84.997	0.0265	0.0378	13103	119,989	1.2641	1.5128	8103
90.010	0.0280	0,0378	13104	121.988	1.2932	1.5125	8104
95.013	0.0296	0.0378	13105	123.987	1.3221	1.5121	8105
100.010	0.0312	0.0378	13106	125.987	1.3510	1.5118	8106
109.998	0.0343	0.0377	13107	127.987	1.3794	1.5114	8107
119.989	0.0374	0.0377	13108	129.987	1.4080	1.5111	8108
129.987	0.0405	0.0377	13109	131.987	1.4363	1.5107	8109
139.992	0.0436	0.0376	13110	133.988	1.4645	1.5104	8110
				135.989	1.4925	1.5101	8111
79,991	0.0479	0.0740	13001	137.990	1.5206	1.5097	8112
84.997	0.0513	0.0739	13002	139.992	1.5486	1.5094	8113
90.010	0.0544	0.0739	13003	141.993	1.5765	1.5090	8114
95.013	0.0575	0.0738	13004	143.995	1.6042	1.5087	8115
100.010	0.0606	0.0738	13005	145.996	1.6319	1.5083	6116
109.998	0.0667	0.0737	13006	147.990	1 6 9 7 4	1 50 77	0117
119.989	0.0729	0.0737	13007	150.000	1 7556	1 5069	8110
129.987	0.0789	0.0736	13008	160.010	1.8237	1.5059	8120
139.992	0.0850	0.0735	13009	165.014	1.8916	1.5051	8121
				170.019	1,9592	1.5042	8122
84,997	0.0955	0.1403	12901	175.024	2.0264	1,5033	8123
90.010	0.1020	0.1403	12902	180.027	2.0936	1.5025	8124
95.013	0.1080	0.1402	12903	185.030	2.1603	1.5016	8125
100.010	0.1139	0.1401	12904	190.032	2.2268	1.5007	8126
105.004	0.1198	0.1401	12905	195.034	2.2931	1.4998	8127
119.989	0.1373	0.1398	12906	200.035	2.3592	1.4990	8128
129.987	0.1489	0.1397	12907	210.033	2.4909	1.4972	8129
139.992	0.1605	0.1396	12908	220.030	2.6218	1.4954	8130
				220.030	2.6214	1.4954	8131
90.010	0.1516	0.2118	12801	230.025	2.7517	1.4935	8132
95.013	0.1609	0.2117	12802	240.020	2.8812	1.4917	8133
100.010	0.1699	0.2116	12803	250.014	3.0103	1.4898	8134
105.004	0.1789	0.2115	12804	260.008	3.1389	1.4880	8135
109.998	0.1879	0.2114	12805	270.002	3.2670	1.4861	8130
119.989	0.2057	0.2111	12806	219.991	3.3940	1 4822	8138
129.987	0.2234	0.2109	12807	207.994	3.5484	1 4803	8139
139.992	0.2410	0.2107	12808	2000002	3.0404	1.4000	010)
05 047	0.264.0	0 7576	10764	121.988	1.6805	2.1162	12601
920UI3	0.2040	0 3570	12301	124.987	1.7449	2.1154	12602
100.010	0 2112	0.3574	12302	129.987	1.8504	2.1141	12603
119,989	0.3417	0.3567	12304	134.988	1.9543	2.1129	12604
129,987	0.3721	0.3563	12305	139.992	2.0568	2.1116	12605
139.992	0.4022	0.3559	12306	144.995	2.1583	2.1104	12606
10,00,00		0 00 0 0 0 0	12000	150.000	2.2589	2.1091	12607
102.008	0.4305	0.5538	12701	405 007	0 0750	2 61.70	7/.01
105.004	0.4454	0.5537	12702	127.907	2.01.00	2 6472	7401
109.998	0.4699	0.5534	12703	127.907	2 1 2 5	2 6466	7402
114.994	0.4942	0.5531	12704	131.987	2.2411	2.6459	7404
119.989	0.5183	0.5528	12705	133.988	2.2954	2.6453	7405
129.987	0.5661	0.5522	12706	135,989	2.3491	2.6446	7406
139.992	0.6136	0.5516	12707	137,990	2.4026	2.6440	7407
				139,992	2.4558	2.6433	7408
105.004	0.6031	0.7767	12501	141.993	2.5088	2.6427	7409
109.998	0.6390	0.7763	12502	143.995	2.5614	2.6420	7410
114.994	0.6740	0.7759	12503	145.996	2.6138	2.6414	7411
119.989	0.7086	0.7755	12504	147.998	2.6659	2.6407	7412
124.987	0.7430	0.7751	12505	150.000	2.7180	2.6401	7413
129.987	0.7772	0.7746	12506	155.005	2.8470	2.6384	7414
139.992	0.3451	0.7738	12507	160.010	2.9751	2.6368	7415
				165.014	3.1021	2.6352	7416
111.996	0.9141	1.1436	12402	170.019	3.2284	2.6336	7417
114.994	0.9465	1.1432	12403	175.024	3.3538	2.6319	7418
119.989	0.9997	1.1426	12404	180.027	3.4784	2.0303	7419
129.987	1.1044	1.1413	12405	185.030	3.6024	2.0201	7420
139.992	1.2075	1.1400	12406	190.032	3. 1200	2.6254	7421
				1 177.034	0.0400	C. 0 C ) 7	1746

TABLE 14. TEMPERATURE-PRESSURE-DENSITY OBSERVATIONS ON FLUORINE--CONTINUED

T EMP K	PRESSURE MN/M <sup>2</sup>	DENSITY MOL/L	IDENT	TEMP K	PRESSURE MN/M <sup>2</sup>	DENSITY MOL/L	IDENT
195.034	3.8486	2.6254	7422	165.014	4.9344	4.7240	7012
200.035	3.9711	2.6238	7423	170.019	5.1861	4.7208	7013
210.033	4.2145	2.6204	7424	175.024	5.4345	4.7176	7014
220.030	4.4562	2.6171	7425	180.027	5.6819	4.7144	7015
230.025	4.6964	2.6138	7426	185.030	5.9278	4.7113	7016
240.020	4 . 9347	2.6104	7427	190.032	6.1719	4.7081	7017
230.025	4.6968	2.6140	7428	195.034	6.4144	4.7049	7018
240.020	40 90 90 5 1772	2 6072	7429	240 037	000000 7 1767	4.7018	7019
250.014	5.4893	2.6038	7430	220 070	7 6004	4.0994	7020
270.002	5.6446	2.60.04	7432	210.033	7.1364	4.6952	7021
279,997	5.8785	2.5969	7433	220.030	7.6091	4.6888	7022
289.994	6.1114	2.5933	7434	230.025	8.0796	4.6824	7024
299.992	6.3432	2.5897	7435	240.020	8.5464	4.6759	7025
				250.014	9.0103	4.6693	7026
				260.008	9.4713	4.6627	7027
129.987	2.6958	3.6637	7201	270.002	9.9295	4.6560	7028
131.987	2.7788	3.6627	7202	279.997	10.3848	4.6493	7029
133.988	2.8604	3.6617	7203	289.994	10.8367	4.6425	7030
135.989	2.9410	3.6608	7204	299.992	11.2072	4.6357	7031
137.990	3.0209	3.6598	7205				
139.992	3.1001	3.6588	7206				
141.993	3.1786	3.6579	7207	137.990	3.7717	5.4871	8301
143.995	3.2565	3.6559	7208	139.992	3.9057	5.4855	8302
145.996	3.3341	3.0500	7209	141.993	4.0376	5.4839	8303
147.998	3.4110	3 8 5 7 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9	7214	143.995	4.10/9	5.4823	8304
155 005	3.4070	3:0540	7212	147.990 147.00R	4.2909	2 · 40 U0	0309
160.010	3,8649	3-6493	7213	150.000	4.5515	5.4776	8307
165-014	4.0507	3.6470	7214	155.005	4.8645	5.4737	8308
170.019	4.2350	3.6446	7215	160.010	5.1727	5.4699	8309
175.024	4.4179	3.6423	7216	165.014	5.4770	5.4660	8310
180.027	4.5994	3.6399	7217	170.019	5.7784	5.4622	8311
180.027	4.5995	3.6401	7218	175.024	6.0765	5.4585	8312
185.030	4.7802	3.6378	7219	180.027	5.3724	5.4547	8313
190.032	4.9597	3.6354	7220	185.030	6.6661	5.4509	8314
195,034	5.1383	3.6330	7221	190.032	6.9578	5.4471	8315
200.035	5.3160	3.6307	7222	195.034	7.2477	5.4433	8316
210.033	5.6689	3.6259	7223	200.035	7,5357	5.4395	8317
220.030	6.0188	3.6211	7224	210.033	8.10/1	5.4319	8318
230,025	6 3002	3.0103	7226	220.030	0.0730	2 · 4 C 4 C	0319
240.020	0.110	3.0114	7227	220.030	0 07 28	204241 5 4165	0320
260.008	7.3946	3.6015	7228	240-020	9.7891	5.4087	8322
270.002	7.7335	3-5966	7229	250.014	10.3417	5.4008	8323
279.997	8.0706	3,5915	7230	260.008	10.8902	5.3929	8324
289.994	8,4063	3.5865	7231	270.002	11.4359	5.3849	8325
299.992	8.7404	3.5813	7232	279.997	11.9776	5.3769	8326
				289.994	12.5164	5.3687	8327
				299.992	13.0526	5.3605	8328
150.000	3.9137	4.3084	8501				
165.014	4.6013	4.2998	8502				
180.027	5.2692	4.2913	8503	137.990	3.9283	6.0824	6901
200.035	6.1393	4.2799	8504	139.992	4.0827	6.0805	6902
230.025	7.4114	4.2626	8505	141.993	4.2341	6.0787	6903
				143.995	4.3832	6.0769	6904
477 000	7 2005	1. 7/17	7004	145.996	4.5308	6.U/51 6.0777	6905
175 080	3.2925	4 . 1443	7001	150 000	4.00/0/	0.U/33 6 071E	6946
137.990	3 6476	4.7430	7002	155 005	4.0213	6.0671	0707 A 11 0 A
139.992	3.5110	407410	7003	160 010	5.5288	6.0627	6000
141.993	3.7366	4.7389	7005	165-014	5.8752	6.0583	6910
143.995	3-8445	4.7376	7006	170,019	6.2174	6.0540	6911
145.996	3,9514	4.7363	7007	175-024	6.5565	6.0496	6912
147.998	4.0575	4.7350	7008	180.027	6.8924	6.0453	6913
150.000	4.1629	4.7337	7009	185.030	7.2260	6.0410	6914
155.005	4.4233	4.7304	7010	190.032	7.5572	6.0366	6915
160.010	4.6804	4.7272	7011	195.034	7.8860	6.0323	6916

T EMP K	PRESSURE	DENSITY MOL/L	IDENT	ТЕМР К	PRESSURE MN/M <sup>2</sup>	DENSITY MOL/L	IDENT
200.035	8.2131	6.0279	6917	289.994	15.6802	6.7219	2727
210.033	8.8617	6.0192	6918	299.992	16.3876	6.7111	2728
220.030	9.5038	6.0105	6919				
230.025	10.1405	6.0017	6920				
240.020	10.7703	5.9929	6921	141.993	4.5958	7.6840	7501
250.014	11.3966	5.9841	6922	143.995	4.8006	7.6815	7502
260.008	12.0190	5.9751	6923	145.996	5.0015	7.6791	7503
270.002	12.6373	5,9662	6924	147.998	5.2001	7.6767	7504
279.997	13.2518	5.9571	6925	150.000	5.3960	7.6743	7505
289.994	13.8633	5.9479	6926	155.005	5.8780	7.6683	7506
299.992	14.4706	5.9387	6927	160.010	6.3513	7.6624	7507
				165.014	6.8179	7.6565	7508
				170.019	7.2790	7.6507	7509
139.992	4.2052	6.5928	7801	175.024	7.7353	7.6449	7510
141.993	4.3745	6.5908	7802	180.027	8.1862	7.6392	7511
143.995	4.5407	6.5888	7803	185.030	8.6352	7.6334	7512
145.996	4.7050	6.5868	7804	190.032	9.0807	7.6276	7513
147.998	4.8670	6.5848	7805	190.032	9.0802	7.6275	7514
150.000	5.0275	6.5828	7806	195.034	9.5228	7.6217	7515
155.005	5.4232	6.5779	7807	200.035	9.9626	7.6159	7516
160.010	5.8120	6.5730	7808	210.033	10.8353	7.6043	7517
165.014	6.1955	6.5681	7809	220.030	11.6987	7.5926	7518
170.019	6.5732	6.5633	7810	230.025	12.5549	7.5808	7519
175.024	6.9484	6.5586	7811	240.020	13.4022	7.5689	7520
180.027	7.3206	6.5538	7812	250.014	14.2444	7.5570	7521
185.030	7.6898	6.5490	7813	260.008	15.0797	7.5449	7522
190.032	8.0560	6.5442	7814	270.002	15.9091	7.5327	7523
195.034	8.4200	6.5395	7815	279.997	16.7342	7.5203	7524
200.035	8.7819	6.5346	7816	289.994	17.5523	7.5078	7525
210.033	9.4992	6.5251	7817	299.992	18.3667	7.4953	7526
220.030	10.2098	6.5154	7818				
230.025	10.9136	6.5058	7819				
230.025	10.9148	6.5061	7820				
240.020	11.6123	6.4962	7821	185.030	8.9694	8.0302	8401
250.014	12.3046	6.4862	7822	195.034	9.9172	8.0179	8402
260.008	12.9920	6.4762	7823	210.033	11.3172	7.9994	8403
270.002	13.6750	6.4661	7824	230.025	13.1530	7.9743	8404
279.997	14.3536	6.4559	7825				
289.994	15.0284	6.4456	7826				
299.992	15.6989	6.4353	7827	143.995	4.9168	8.3819	11901
				145.996	5.1430	8.3791	11902
				147.998	5.3652	8.3764	11903
139.992	4.2620	6.8747	2701	150.000	5.5847	8.3737	11904
141.993	4.4415	6.8725	2702	155.005	6.1242	8.3671	11905
143.995	4.6175	6.8704	2703	160.010	6.6540	8.3605	11906
145.996	4.7909	6.8683	2704	165.014	7.1759	8.3539	11907
147.998	4.9623	6.8662	2705	170.019	7.6922	8.3474	11908
150.000	5.1318	6.8642	27 06	175.024	8.2027	8.3409	11909
155.005	5.5490	6.8590	2707	180.027	8.7093	8.3345	11910
160.010	5.9593	6.8540	2708	185.030	9.2117	8.3280	11911
165.014	6.3637	6.8489	2709	190.032	9.7107	8.3215	11912
170.019	6.7637	6.8439	2710	195.034	10.2065	8.3150	11913
175.024	7.1593	6.8389	2711	200.035	10.6993	8.3085	11914
180.027	7.5515	6.8339	2712	210.033	11.6/72	8.2955	11915
185.030	7.9406	6.8290	2713	220.030	12.6444	8.2825	11916
190.032	8.3270	6.8240	2714	210.033	11.6741	8.2952	11917
195.034	8.7109	6.8190	2715	220.030	12.6416	8.2821	11918
2011-035	9.0924	6.8140	2716	230.025	13.5995	8.2689	11919
210.033	9.8489	6.8040	2717	240.020	14.5502	0.2556	11920
220.030	10.59/7	6.7940	2718	250.014	15.4923	0.2422	11921
230.025	11.3398	6.7839	2719	260.008	16.4281	8.2287	11922
220.030	10.5990	6.7943	2720	270.002	11.35/3	8.2151	11923
230.025	11.3409	6.7842	2/21	2/9.99/	10.2003	8.4071	11924
240.020	12.07/1	6.7740	2722	289.994	19.1973	0.10/4	11929
220.014	12.8074	6./638	2723	299.992	20.1092	8.1732	11950
200.000	13.5329	6.7535	2724				
279.007	14.0680	0 • 7 4 3 U	2725	1/1 007	1. 711.0	8 7/ 00	7103

### TABLE 14. TEMPERATURE-PRESSURE-DENSITY OBSERVATIONS ON FLUORINE -- CONTINUED

TEMP K	PRESSURE	DENSITY Mol/L	IDENT	ТЕМР К	PRESSURE MN/M <sup>2</sup>	DENSITY MOL/L	IDENT
143.005	4 9577	8 7468	31.07	200 075	42.4756	0 6800	7641
145.996	5.2069	8.71.39	3104	210 033	17 7767	9.0009	7615
147.998	5.4421	8.741	3105	220.030	11. 5208	9+0047 0 6/88	7615
150.000	5.6739	8 7382	3105	270 025	15 6077	0 6726	7617
155 005	5 244A	8.7712	3107	230.025	15 6957	9.0320	7619
160 010	6 9033	0 0 1 312	3108	230.025	100000	9.0329	7610
165 014	7 7548	8 7471	3100	240.020	10.0013	9.0100	7619
170 010	7.0002	8 7405	3110	250.014	10.100	9.0000	7620
175 024	P 1300		3110	200.000	19+1045	9.0000	7622
180 027	0.4355	0.1031	3111	270.002	20.0049	90000	1022
195 030	0.5155	0.0909 8.6004	3112				
100 032	40 0342	0.0701	3113	447 005	E 1071	10 0000	0.0.0.1
105 034	10.0342	0.00000	2114	445.995	5.1231	10 8617	0001
200 075	11 0708	0.0703	3113	142.990	5+4415	10 0047	0002
200+032	42 4477	0.009/	3110	150 000	5.0578	10.0000	0003
210.033	12 0 1 1 3 3	0.0000	3117	150.000			0004
	13.1303	0.0423	3110	160 040	2 5540	10 9797	0000
220.030	13+1341	8.6410	3119	100.010	7.00019	10.0384	8006
230.022	14.14/0	0.0270	3120	109.014	0.2047	10.8291	8007
240.020	15.1530	8.6140	3121	170.019	9.0100	10.0199	8008
250.014	10.1502	8.6000	3122	1/5.024	9.0306	10.0100	8009
260.008	17.1403	8.5859	3123	180.027	10.4459	10.8016	8010
270.002	18.1231	8.5/1/	3124	185.030	11.1567	10.7925	8011
2/9.99/	19.0990	8.5572	3125	190.032	11.8630	10.7834	8012
289.994	20.0680	8.5426	3126	195.034	12.5659	10.7742	8013
299.992	21.0320	8.5278	3127	200.035	13.2650	10.7650	8014
				210.033	14.6522	10.7466	8015
				220.030	16.0262	10.7279	8016
143.995	4.9995	9.0187	8201	230.025	17.3881	10.7092	8017
145.996	5.2489	9.0157	8202	240.020	18.7385	10.6903	8018
147.998	5.4935	9.0127	8203	250.014	20.0784	10.6712	8019
150.000	5.7349	9.0097	8204	260.008	21.4083	10.6519	8020
155.005	6.3276	9.0024	8205				
160.010	6.9099	8.9953	8206				
165.014	7.4838	8.9881	8207	145.996	5.5018	11.9244	7902
170.019	8.0512	8.9809	8208	147.998	5.8491	11.9201	7903
175.024	8.6132	8.9738	8209	150.000	6.1922	11.9159	7904
180.027	9.1705	8.9667	8210	155.005	7.0392	11.9053	7905
185.030	9.7235	8.9596	8211	160.010	7.8758	11.8948	7906
190.032	10.2729	8.9524	8212	165.014	8.7053	11.8843	7907
195.034	10.8190	8.9453	8213	170.019	9.5289	11.8739	7908
200.035	11.3619	8.9381	8214	175.024	10.3471	11.8634	7909
143.995	4.9977	9.0186	8215	180.027	11.1599	11.8530	7910
170.019	8.0504	8.9805	8216	185.030	11.9686	11.8425	7911
200.035	11.3610	8.9378	8217	190.032	12.7733	11.8321	7912
210.033	12.4354	8.9234	8218	195.034	13.5742	11.8216	7913
220.030	13.5009	8.9090	8219	200.035	14.3705	11.8111	7914
230.025	14.5573	8.8945	8220	210.033	15.9527	11.7900	7915
240.020	15.6029	8.8798	8221	220.030	17.5202	11.7687	7916
250.014	16.6415	8.8650	8222	230.025	19.0742	11.7472	7917
260.008	17.6717	8.8501	8223	240.020	20.6152	11.7254	7918
270.002	18.6956	8.8349	8224				
279.997	19.7114	8.8197	8225	ļ			
289.994	20.7215	8.8043	8226	145.996	5.5529	13.4190	7701
				147.998	5.9507	13.4141	7702
				150.000	6.3460	13.4092	7703
143.995	5.0676	9.7709	7601	155.005	7.3299	13.3969	7704
145.996	5.3447	9.7675	7602	160.010	8.3087	13.3846	7705
147.998	5.6161	9.7641	7603	165.014	9.2833	13.3724	7706
150.000	5.8835	9.7608	7604	170.019	10.2538	13.3601	7707
155.005	6.5404	9.7527	7605	175.024	11.2199	13.3478	7708
160.010	7.1858	9.7446	7606	180.027	12.1821	13.3355	7709
165.014	7.8231	9.7366	7607	185.030	13.1408	13.3232	7710
170.019	8.4535	9.7286	7608	190.032	14.0952	13.3108	7711
175.024	9.0778	9.7206	7609	195.034	15.0452	13.2983	7712
180.027	9.6972	9.7127	7610	200.035	15.9911	13.2858	7713
185.030	10.3125	9.7047	7611	210-033	17.8715	13.2606	7714
190.032	10.9239	9.6968	7612	220.030	19.7353	13.2351	7715
195.034	11.5312	9.6888	7613	230.025	21,5840	13.2092	7716

TABLE 14. TEMPERATURE-PRESSURE-DENSITY OBSERVATIONS ON FLUORINE--CONTINUED

.

TEMP K	PRESSURE MN/M <sup>2</sup>	DENSITY MOL/L	IDENT	TEMP K	PRESSURE MN/M 2	DENSITY MOL/L	IDENT
145.996	5.5803	14.4938	7301	185.030	19.8847	19.6335	9108
147.998	5.0136	14.4884	7302	190.032	21.6917	19.6097	9109
155,005	0.4479 7.5346	14.4829	7303				
160.010	8.6223	14.4556	7305	143,995	5,2963	20.6673	11401
165.014	9.7090	14.4418	7306	145.996	6.0273	20.6582	11402
170.019	10.7932	14.4280	7307	147.998	6.7749	20.6488	11403
175.024	11.8746	14.4143	7308	150.000	7.5327	20.6392	11404
180.027	12.9527	14.4004	7309	155.005	9.4574	20.6149	11405
105.030	14.0275	14.3865	7310	160.010	11.4063	20.5904	11406
195.034	16,1651	14.3586	7312	170.019	15,3332	20.5059	11407
200,035	17.2279	14.3445	7313	175.024	17.2983	20.5162	11409
210.033	19.3406	14.3161	7314	180.027	19.2617	20.4911	11410
220.030	21.4361	14.2873	7315	185,030	21.2213	20.4656	11411
145.996	5.6063	15.7701	7102	143.995	5.5541	21.8571	11701
147.998	6.0859	15.7641	7103	145.996	6.3880	21.8467	11702
150.000	6.5689	15.7580	7104	147.998	7.2345	21.8361	11703
155.005	7.7889	15.7427	7105	150.000	8.0903	21.8253	11704
165.014	30,2677	15,7118	7105	155.005	10.2004	21.7981	11705
170.019	11.4795	15.6962	7108	165.014	14.6396	21.7433	117 07
175.024	12.7098	15.6806	7109	170.019	16.8381	21.7157	11708
180.027	13.9387	15.6650	7110	175.024	19.0347	21.6877	11709
185.030	15.1641	15.6493	7111	180.027	21.2276	21.6595	11710
190.032	15.3858	15.5335	7112				
200 035	18 8182	15.6015	7113	1/3 005	5 5550	21 8658	11301
210.033	21.2328	15.5691	7115	145.996	6.3896	21.8554	11302
				147.998	7.2372	21.8448	11303
				150.000	8.0928	21.8339	11304
145.996	5.6826	17.9228	11801	155.005	10.2602	21.8066	11305
147.998	6.2544	17.9156	11892	160.010	12.4475	21.7792	11306
150.000	0.0000	17 8806	11003	105.014	14.0451	21.7278	11307
160-010	9.8205	17.8706	11805	175-024	19,0414	21.6959	11309
165.014	11.3329	17.8516	11806	180.027	21.2361	21.6675	11310
170.019	12.8497	17.8324	11807				
175.024	14.3668	17.8131	11808				
180.027	15.8834	17.7937	11809	141.993	5.0864	23.0236	6801
100.030	1/039/3 48 0083	17 7545	11811	143.995	0.0185 6.05/8	23.0124	6807
195.034	20.4147	17.7346	11812	147.998	7,9207	22.9885	6874
2,55,000,	2001211			150.000	8.8832	22.9762	6805
				155.005	11.3096	22.9458	6806
145.996	5.7462	18.7458	1150	160.010	13.7511	22.9154	6807
147.998	6.3635	18.7380	1156	165.014	16.1970	22.8849	6808
150.000	5.9921 8 502/	18.7301	11503	170.019	18.0432	22.8741	6810
160.010	10.2157	18,6895	11504	179.024	21.0044		0010
165.014	11.8507	18.6689	11506				
170.019	13.4911	18.6482	11507	139.992	4.6408	24.1656	11201
175.024	15.1326	18.6273	11508	141.993	5.6875	24.1528	11202
180.027	16.7728	18.6063	11509	143.995	6.7473	24.1395	11203
185.030	18.4107	18.5851	11510	145.996	/ •0162 8 8047	24.1259	11204
195.034	21.6738	18.5422	1:512	150,000	9,9710	24.1989	11205
2 2 2 4 3 0 4	2200100	LUIJTEE	/	155.005	12.6845	24.0653	11207
				150.010	15.4054	24.0316	11208
150.000	7.2527	19.7940	9101	165.014	18-1249	23.9977	11209
155.005	9.0246	19.7716	9102	170.019	20,8398	23.9633	11210
165,014	10.0210	19.7489	9103				
170.019	14.4455	19.7032	9105	137.990	4.3981	25.4197	11101
175.024	16.2603	19.6802	9106	139.992	5.5916	25.4051	11102
180.027	18.0749	19.6569	9107	141.993	6.7956	25.3899	11103

TABLE 14. TEMPERATURE-PRESSURE-DENSITY OBSERVATIONS ON FLUORINE -- CONTINUED

TABLE 14. TEMPERATURE-PRESSURE-DENSITY OBSERVATIONS ON FLUORINE -- CONTINUED

TEMP K	PRESSURE MN/M <sup>2</sup>	DENSITY MOL/L	IDENT	TEMP K	PRESSURE MN/M <sup>2</sup>	DENSITY MOL/L	IDENT
143.995	8.0063	25.3744	. 11104	137,990	15.9751	30.4277	3308
145.996	9.2228	25.3591	11105	139.992	17.9331	30.4041	3309
147.998	10.4416	25.3440	11106	141.993	19-8854	30.3804	3310
150.000	11.6629	25.3290	11107	143.995	21.8300	30.3565	3311
155.005	14.7193	25.2915	11108				
160.010	1/ 0//35	25,2537	11109	123.087	2.5342	30 7537	11001
162.014	20.0210	27 . 2194	11110	125.987	4-5717	30.7266	11001
				127,987	6-6241	30.7009	11002
135,989	4.2576	26.5253	6701	129.987	8.6274	30.6770	11004
137,990	5,5957	26.5094	6702	131.987	10.6449	30.6528	11005
139.992	6,9422	26.4921	6703	133.988	12.6542	30.6288	11006
141.993	8.2923	26.4750	6704	135.989	14.6559	30.6048	11807
143.995	9.6452	26.4584	6705	137.990	16.6506	30.5808	11008
145.996	11.0021	26.4420	6706	139.992	18,6381	30.5568	11009
147.998	12.3580	26.4255	6707	141.993	20.6167	30.5326	11010
150.000	13.7136	26.4091	6708				
155.005	17.1002	26,3679	6709				
160.010	20.4746	26.3261	6710	121.988	2.1204	31.2838	6501
				123.987	4.2621	31.2549	6502
475 000	6 4700	07 7004	06.04	125.987	6.3997	31.2282	6503
135.989	0.2435	27.7894	8601	127.987	0.52/5	31.2031	6504
109.992	9.2435	27 6054	8607	171 097	10 0420	31 1529	6505
150 000	16 8861	27 6570	00003	177.988	14 8557	31 1230	6500
190.000	10.0001	21.0019	0004	135.989	16-9441	31.1032	6508
				137,990	19,0306	31.0783	6509
131.987	3.1337	27.8278	3801	139.992	21.1040	31.0533	6510
133.988	4.6569	27.8076	3002				
135.989	6.1838	27.7893	3003				
137.990	7.7142	27.7695	3004	119.989	2.0538	31.8837	10901
139.992	9.2456	27.7509	3005	121.988	4.3243	31.8531	10902
141.993	10.7772	27.7324	3006	123.987	6.5827	31.8252	18903
143.995	12.3076	27.7139	3007	125.987	8.8306	31.7984	10904
145.996	13.8350	27.6954	3008	127.987	11.0664	31.7717	10905
147.998	15.3607	21.06/69	3009	129.987	13,2909	31.7452	10906
155 005	20 6776	27 6116	3010	131.987	15.50/4	31./189	10907
1))*00)	20.0770	21.00110	2011	175 080	10 0058	31.0920	10900
				137,990	22.0927	31.6304	10909
129.987	3.1750	28.7586	6601	10/0550	2200721	01:00.04	10210
131.987	4.8498	28,7366	6602				
133.988	6.5264	28.7154	6603	119,989	2.0907	31.8967	9901
135.989	8.2033	28.6953	6604	121.988	4.3610	31.8659	9902
137.990	9.8768	28.6752	6605	123.987	6.6209	31.8379	9903
139.992	11.5492	28.6552	6606	125.987	8.8700	31.8109	9904
141.993	13.2188	28.6352	6607	127.987	11.10/2	31.7840	9905
143.995	14.8842	28.6153	6608	129.987	13.3333	31.7573	9906
142.996	10.5472	20.5953	6619	131.987	15.5502	31 • / 308	9907
150.000	19.8604	20.07/02	6611	135.989	19-9523	31.6777	9900
152.002	21.5104	28.5348	6612	137,990	22-1410	31.6508	9909
172 0002	210704	20.0040	0012	1070550	2201410	01.0000	5510
129.987	5.1513	29.5967	8/01	117.991	1.80/3	32.4136	5601
133.988	8.7944	29.5529	0/U2	121 000	4 • 1910 6 E6/.0	32 3019	5602
147 000	24 / 04 0	29.40/0	8704	123,987	0 · 2040 8 · 0247	32.3929	56U3 5604
1	CT040I0	2 2 4 4 0 0 2	01.04	125,987	11.2704	32.2967	5605
				127.987	13.6024	32.2691	5606
123.987	2,0663	30.5991	3301	129.987	15.9198	32.2416	5607
125.987	4.0717	30.5717	3302	131.987	18.2273	32.2141	5608
127.987	6.0736	30.5458	3303	133.988	20.5256	32.1863	5609
129.987	8.0687	30.5223	3304				
131.987	10.0571	30.4985	3305				
133.988	12.0370	30.4748	3306	117.991	3.8594	32.8504	8801
135.989	14.0095	30.4512	3307	121.988	8 - 8046	32.7903	8802

TEMP K	PRESSURE MN/M <sup>2</sup>	DENSITY Mol/L	IDENT	ТЕМР К	PRESSURE MN/M <sup>2</sup>	DENSITY MOL/L	IDENT
125.987	13.6829	32.7320	8803	109.998	4.9055	34.9504	9702
131.987	20.9035	32.6457	8804	111.996	7.8958	34.9153	9703
				113.995	10.8562	34.8796	9704
				115.993	13.7914	34.8451	9705
115.993	1.3862	32.8854	3501	117.991	16.7036	34.8109	9706
117.991	3.8764	32.8507	3502	119.989	19.5986	34.7764	9707
119,989	6.3523	32.8203	3503	121.988	22.4815	34.7415	9708
121.988	8.8139	32.7911	3504				
123.987	11.2577	32.7619	3505	106 000	4 70/0	75 7740	5704
122.987	13.0090	32 01 332	3506	108.000	1.0049	32+3/10	5301
120 087	18 5101	32 6761	3507	100.000	7.5173	35 2016	5302
131.987	20.9029	32.6473	3500	111,996	10,5819	35.2546	5304
1010 000	2000020	02:004/0	0,00,0	113.995	13.6157	35,2192	5305
				115.993	16.6268	35.1841	5306
113,995	1.4096	33.4281	2801	117.991	19.6241	35.1489	5307
115.993	4.0243	33.3920	2802	119.989	22.6020	35.1132	5308
117.991	6.6219	33.3603	2803				
119.989	9.2038	33.3296	2804				
121.988	11.7677	33.2990	2805	108.000	4.4294	35.3292	8901
123.987	14.3135	33.2691	2806	111.996	10.5904	35.2558	8902
125.987	16.8497	33.2396	2807	115.993	16.6385	35.1848	8903
127.987	19.3713	33.2097	2818	119.989	22.6077	35.1134	8904
129.987	21.8803	33.1795	2809				
113,995	1.3999	33,4316	9311	104.005	1.7569	35.8759	9801
115.993	4.0187	33.3942	9302	106.002	5.0226	35.8326	9802
117.991	6.6221	33.3625	9303	108.000	8.2535	35.7945	9803
119.989	9.2074	33.3315	9304	109.998	11.4495	35.7565	9804
121.988	11.7742	33.3008	9305	111.996	14.6184	35.7196	9805
123.987	14.3248	33.2707	9306	113.995	17.7614	35.6826	9806
125.987	16.8605	33.2407	9307	115.993	20.8837	35.6453	9807
127.987	19.3844	33.2106	9308				
129.987	21.8939	33.1800	9309				
				102.008	0.9747	36,2163	5501
				104.005	4.3398	36.1697	5502
111.996	1.2522	33.9215	6401	106.002	7.6717	36.1303	5503
113.995	3.9918	33.8833	6402	108.000	10.9641	36.0910	5504
115.993	6.7161	33.8504	6403	109.998	14.2237	36.0531	5505
117.991	9.4152	33.8181	6404	111.996	17.4597	36.0153	5506
119.989	12.0947	33.7862	6405	113.995	20.6766	35.9771	5507
121.988	14.7578	33.7550	6406				
123.987	1/.4042	33.7239	6407	400.000	4 0777	76 01 1 0	5704
129.987	20.0399	33.6925	6408	102.008	1.23//	36.2449	5701
121.901	22.0590	22.0003	6409	104.005	4.0110	36.1990	5702
				100.002	14 250L	30.1334	5705
111 006	3 7877	31. 3287	0/.01	100.000	14.5134	36.0819	5705
117.005	6 6219	34.3201	9401	111.996	17.7568	36.0440	5706
115.093	0.1336	34.2606	9402	113,995	20,9811	36,0056	5707
117.991	12.2178	34.2276	9405	11000000	LUUJULL	0000000	5101
119,989	14,9846	34,1951	9404				
121.988	17.7393	34.1625	9405	102.008	3,9537	36.5444	9501
123.987	20.4747	34,1298	9400	104.005	7,4001	36,5033	9502
	2001111	O TOLL DO	5101	106.002	10.7999	36-4627	9513
				108-000	14.1678	36.4237	9504
109.998	0.9643	34.3721	3201	109.998	17.5067	36.3846	9505
111.996	3.8173	34.3315	3202	111.996	20.8277	36.3452	9506
113.995	6.6497	34.2974	3203				
115.993	9.4560	34.2637	3204				
117.991	12.2408	34.2307	3205	100.010	0.4947	36.5951	2901
119.989	15.0052	34.1983	3206	102.008	3.9704	36.5447	2902
121.988	17.7529	34.1658	3207	104.005	7.4128	36.5043	2903
123.987	20.4844	34.1332	3208	106.002	10.8108	36.4638	2904
				108.000	14.1772	36.4249	2905
4.0.0 0.0.0				109.998	17.5172	36.3861	2906
T09°000	1.8893	34.9904	9701	111.996	20.8393	36.3469	2907

### TABLE 14. TEMPERATURE-PRESSURE-DENSITY OBSERVATIONS ON FLUORINE--CONTINUED

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TEMP K	PRESSURE MN/M <sup>2</sup>	DENSITY MOL/L	IDENT	TEMP K	PRESSURE MN/M <sup>2</sup>	DENSITY MOL/L	IDENT
98.012	0.8850	37.0590	5101	88.005	4.7505	39.3046	10101
100.010	4.5114	37.0089	5102	90.010	9.1162	39.2535	10102
102.008	8.0937	36,9662	5103	92.012	13.4113	39.2043	10103
104.005	11.6289	36.9252	5104	94.013	17.6633	39.1551	10104
106.002	15.1285	36.8847	5105	96.013	21.8822	39.1052	10105
108.000	18.6042	36.8442	5106				
109.998	22.0614	36.8031	5107	87.005	0 11 50	70 7/05	40504
				83.995	0.4499	39.7405	10501
09 04 2	1. 0669	77 1.1.64	0.2.0.4	00.000	2 0 L 34	39.0704	10502
102 008	12.3521	37 3597	9201	90.010	13.9204	39.5735	10505
104.005	15.9787	37.3177	9202	92.012	18,3051	39.5229	10505
106.002	19.5824	37,2755	9205	94.013	22.6595	39.4713	10506
108.000	23.1667	37.2326	9205			• • • • • • •	20700
				83.995	0.4651	39.7423	4501
94.013	1.3101	37.9022	10001	86.000	5.0379	39.6788	4502
96.013	5.2104	37.8533	10002	88.005	9.5411	39.6268	4503
98.012	9.1596	37.8054	10003	90.010	13.9741	39.5764	4504
100.010	12.8559	37.7618	10004	92.012	18.3629	39.5259	4505
102.008	16.6183	37.7182	10005	94.013	22.7325	39.4744	4506
			10000				
01 047	4 7400	77 0010		81.992	0.4370	40.1067	10801
94.013	1.3182	37.9060	5001	83.995	5.1394	40.0403	10802
90.013	5 • Z Z U U	31.00012	5002	86.000	9.7620	39.9880	10803
100.010	12.8621	37.7659	5003	00.002	18 9/17	39.9359	10004
102.008	16.6237	37.7225	5004	90.010	23.3386	39.0030 39.0030	10002
104.005	20.3536	37.6789	5006	92.012	20:0000	5 56 6 5 6 5	10000
				81,992	0.4377	40.1072	4201
92.012	1.6868	38.3248	9601	83.995	5.1391	40.0409	4202
94.013	5.7328	38.2752	9602	86.000	9.7704	39.9887	4203
96.013	9.7164	38.2263	9603	88.005	14.3384	39.9367	4204
98.012	13.6445	38.1812	9604	90.010	18.8670	39.8846	4205
100.010	17.5364	38.1360	9605	92.012	23.3699	39.8314	4206
102.008	21.4026	38.0904	9606				
				79.991	0 - 4890	40.4642	10201
90.010	0.9805	38.6564	5201	81.992	5.3375	40.3965	10202
92.012	5.1494	38.6036	5202	83.995	10.0991	40.3430	10203
94.013	9.2524	38.5525	5203	86.000	14.7862	40.2894	10204
96.013	13.2953	30.5052	5204	88.005	19.4396	40.2353	10205
100 010	21 2828	30+40UL 39 1/135	5205				
100.010	2102020	00.4100	2200	70 001	0 4945	40 4640	1.1.0.4
				81,992	5.3375	40.4040	4401
90.010	4.7415	38,9389	9001	83,995	10.0956	40.3432	4402
94.013	13.1362	38.8416	9002	86.000	14.7864	40.2897	4405
98.012	21.3414	38.7459	9003	88.005	19.4439	40.2359	4405
88.005	0.4645	39.0005	4601	77.991	1.4832	40.8761	10301
90.010	4.7619	38.9402	4602	79.991	6.4748	40.8127	10302
92.012	8,9965	38.8907	4603	81.992	11.3732	40.7571	10303
94.013	13.1625	38.8431	4604	83.995	16.2170	40.7016	10304
98.013	21.3782	38.7476	4606	00,000	21.0321	40.0455	10305
				75,993	1,6270	41,2328	6704
86.000	0.3367	39.3667	3401	77.991	6.7642	41.1688	6302
88.005	4.7559	39.3037	3402	79.991	11.7882	41.1121	6303
90.010	9.1085	39.2529	3403	81.992	16.7735	41.0553	6304
92.012	13.3967	39.2040	3404	83.995	21.7365	40.9977	6305
94.013	17.6480	39.1552	3405				
96.013	21.8622	39.1059	3406				

TABLE 14. TEMPERATURE-PRESSURE-DENSITY OBSERVATIONS ON FLUORINE--CONTINUED

TABLE 14. TEMPERATURE-PRESSURE-DENSITY OBSERVATIONS ON FLUORINE -- CONTINUED

TEMP K	PRESSURE	DENSITY MOL/L	IDENŤ	TEMP K	PRESSURE MN/M <sup>2</sup>	DENSITY MOL/L	IDENT
73.996	0.4564	41.5151	4301	61.998	1.2361	43.5478	5801
75.993	5.7320	41.4434	4302	63.999	7.4169	43.4718	5802
77.991	10.8956	41.3856	4303	66.000	13.4638	43.4033	5803
79.991 81 002	15,9845	41.3278	4304	60.001	19.4467	43.3348	5804
01.995	CI 0 0 4 9 I	4102031	4305				
				59.999	0.5011	43.8506	4701
73.996	0.4815	41.5190	10601	61.998	6.8268	43.7690	4702
75.993	5.7438	41.4471	10602	63.999	13.0040	43.6990	4703
77.991	10.8992	41.3889	10603	66.000	19.1342	43.6290	4704
79.991 81 992	15.9884	41.3308	10604				
01.0352	21.0041	4102719	T0005	59,999	0.5139	43.8515	11601
				61.998	6.8361	43.7701	11602
73.996	0.5595	41.5209	10401	63.999	13.0332	43.7001	11603
75.993	5.8320	41.4497	10402	66.000	19.1699	43.6300	11604
77.991	10.9885	41.3914	10403				
79.991	16.0681	41.3333	10404				
81.992	21.1332	41.2744	10405	58.002	1.5812	44.2038	4801
				59.999	8.0600	44.1262	4802
71 008	0 9279	14 9772	64.04	67 998	14.4207	44.0544	4803
73,996	6.2426	41.8068	6101	03.555	2001419	43.9022	4004
75,993	11.5453	41.7467	6103				
77.991	16.7781	41.6867	6104	56.005	1.4389	44.5234	6201
79.991	21.9801	41.6259	6105	58.002	8.0623	44.4435	6202
				59.999	14.5535	44.3698	6203
				61.998	21.0109	44.2954	6204
70.000	0.4372	42.1990	10701				
71.998	6.0066	42.1238	10702				
73.996	11.4350	42.0624	10703	56.005	4.8597	44.6360	12201
75.993	16.8041	42.0012	10704	58.002	11.4722	44.5618	12202
//.991	22.1545	41.9388	10705	61.998	18.0087 24.5494	44.4877 44.4105	12203
70,000	0.4585	42,1996	4101				
71.998	6.0266	42.1252	4102	53,610	1 - 31 4 1		12001
73.996	11.4696	42.0640	4103	53.709	2.3350		12002
75.993	16.8566	42.0028	4104	53.809	3.3653		12003
77.991	22.2168	41.9406	4105	53.909	4.3943		12004
				54.009	5.0652	44.9752	12005
	_			54.109	5.4099	44.9721	12006
68.001	0.8566	42.5531	6001	54.209	5.7571	44.9682	12007
70.000	6.55/1	42.4798	6002	55.007	8.5036	44.9373	12008
77 996	17 6677	42.4104	6003		18 58/6	44.0909	12009
75.993	23.1733	42.2884	6005	50.002	1040040	44.0225	12010
			0000				
				53.909	4.3901		12101
66.000	0.8508	42.8768	5901	54.009	5.4182		12102
	0.1209	₩2•8U21 1.2 7772	5902	54.209	7 4857		12103
70.000	18.1377	42.6724	59U3 59N	54.309	8.5322		12104
73.996	23.7925	42.6058	5905	54.408	9.5650		12106
				54.508	10.6060		12107
				54.608	11.6500		12108
63.999	0.9133	43.2041	5401	54.708	12.6979		12109
66.000	6.9342	43.1279	5402	54.808	13.7392		12110
68.001	12.8113	43.0610	5403	54.907	14.7088	45.1393	12111
10.000	18.6316	42.9941	5494	55.007	15.0681	45.1353	12112
				56.005	18.4968	45.0966	12114
63.999	1.2662	43.2189	4901		200,000		
66.000	7.2989	43.1446	4902				
68.001	13.1924	43.0780	4903				
70.000	19.0462	43.0114	4904				

# TABLE 15. THERMODYNAMIC PROPERTIES OF FLUORINEON THE SATURATION BOUNDARY

The number of significant figures given in this table is not justified on the basis of the uncertainty of the data, but is presented to maintain internal consistency. TABLE 15. THERMODYNAMIC PROPERTIES OF FLUORINE ON THE SATURATION BOUNDARY\*

TEMPERATURE (IPTS 1968)	PRESSURE	DENSITY	ISOTHERM DERIVATIVE	ISOCHORE DERIVATIVE	INTERNAL ENERGY	ENTHALPY	ENTROPY	Cv	Сp	VELOCITY
к	MN/m <sup>2</sup>	MOL/L	J/MOL	MN/m <sup>2</sup> -K	J/MOL	J/MOL	J/MOL-K	J / MOL	- к	M/S
53•4811	0•00025	44.8623	26740	4.308	-6025.1	-6025.1	60.86	36.51	54.96	1029
53•4811	0•00025	0.00057	444		1108.0	1552.5	201.90	20.80	29.12	128
54	0 • 0 0 0 3 0	44.7808	26701	4 • 284	-5996.8	-5996.8	61.39	36.42	54.94	1029
54	0 • 0 0 0 3 0	0.00066	449		1118.7	1567.6	200.84	20.80	29.12	129
56	0•00054	44 <b>.4648</b>	26280	4.189	-5887.4	-5887•3	63.38	36.07	54.99	1027
56	0•00054	0.00115	465		1160.1	1625•5	196.95	20.80	29,13	131
58	0•00093	44 <b>.146</b> 3	25976	4.090	-5777.3	-5777•3	65•31	35 <b>.70</b>	54.86	1025
58	0•00093	0.00193	481		1201.4	1683•2	193•39	20 <b>.81</b>	29.15	133
60	0•00155	43.8251	25738	3 • 988	-5666.7	-5666•7	67.18	35.31	54.62	1024
60	0•00155	0.00311	498		1242.5	1740•7	190.13	20.81	29.17	135
62 62	0.00249	43•5012 0•00484	25561	3 • 884	-5555.7	-5555.6	69.00 187.14	34 <b>.9</b> 2	54.25	1022
64	0.00397	62 1744	24 0 2 7		5444 3	5444 3	70 77	24 61	54 25	1010
64	0+00387	0.00729	529	30110	1324.1	1854•8	184.38	20.84	29.24	1013
66	0•00584	42•8446	23657	3•672	-5332.5	-5332.4	72.49	34.10	54.60	998
66	0•00584	0•01068	545	0•0001	1364.5	1911.2	181.84	20.85	29.29	142
68	0•00858	42.5117	22808	3.566	-5220.4	-5220.2	74.17	33.69	54.67	987
68	0•00858	0.01525	560	0.0001	1404.6	1967.1	179.49	20.88	29.36	144
70	0•01230	42.1756	21592	3•460	~5108.0	-5107•7	75.80	33 <b>.28</b>	55.10	970
70	0•01230	0.02128	574	0•0002	1444.2	2022•3	177.31	20.90	29.44	146
72	0∘01725	41.8360	20430	3.354	-4995.3	-4994.9	77.38	32 <b>.87</b>	55.52	953
72	0∘01725	0.02907	588	0.0002	1483.3	2076.8	175.28	20.94	29.54	148
74	0•02372	41.4929	20177	3 • 249	-4882.3	-4881.8	78.93	32.46	54.95	948
74	0•02372	0.03897		0 • 0003	1521.8	2130.3	173.40	20.98	29.66	150
76 76	0.03201	41.1460	19216	3.145	-4769.1	-4768•3	80.44	32.07	55.17	933
78	0.04246	40.7952	17992	3.041	-4655.6	-4654.5	81.91	31.68	55.78	913
78	0.04246	0.06660	627	0.0006	1596.7	2234 • 3	103*33	21.08	29.97	153
80	0•05547	40.4401	17116	2•939	-4541.8	-4540•4	83•36	31.31	56.00	898
80	0•05547	0.08515	638	0•0007	1633.0	2284•5	168•44	21.15	30.17	155
82	0•07144	40.0807	16310	2.837	-4427.6	-4425•8	84•77	30 <b>.96</b>	56.15	882
82	0•07144	0.10745	648	0.0009	1668.3	2333•2	166•99	21.22	30.40	156
84	0•09081	39.7165	15452	2.737	-4313.2	-4310.9	86.14	30.62	56.43	866
84	0•09081	0.13397	657	0.0011	1702.7	2380.5	165.62	21.31	30.67	158
86	0•11403	39.3472	14495	2.637	-4198.3	-4195•4	87•50	30.30	56.96	847
86	0•11403	0.16523		0.0014	1735.9	2426•1	164•32	21.41	30.97	159
88	0 <b>.1416</b> 1	38.9727	13638	2.539	-4083.0	-4079•4	88.82	30.01	57.39	829
88	0.14161	0.20174		0.0017	1768.0	2469•9	163.09	21.51	31.32	160
90 90	0.17403	38,5924	12602	2.442	-3967.3	-3962.8	90.12 161.93	29.73 21.64	58.33 31.71	807 162
92	0 21184	38 2060	12012	2 247	-3851 1	-3845.5	91.40	20 / 8	58 37	791
92	0.21184	0.29280	682	0.0026	1828.2	2551.7	160.81	21.77	32.15	163
94	0。25558	37.8131	11449	2.253	-3734.3	-3727•5	92.66	29.24	58.39	776
94	0。25558	0.34857	684	0.0031	1856.2	2589•4	159.75	21.92	32.65	164
96	0•30581	37.4131	10621	2 <b>.161</b>	-3616.8	-3608.6	93.89	29.03	59.18	755
96	0•30581	0.41203	686	0.0037		2624.8	158.73	22.08	33.20	165
98	0•36309	37.0055	10013	2.070	-3498.6	-3488.8	95.11	28.85	59.46	737
98	0•36309	0.48389	685	0.0044		2657.7	157.74	22.26	33.82	166
100	0•42802	36.5897 0.56491	9296	1.981	-3379.7	-3368.0	96.32 156.80	28.68 22.46	60.21	717

TABLE 15. THERMODYNAMIC PROPERTIES OF FLUORINE ON THE SATURATION BOUNDARY - CONTINUED

TEMPERATURE	PRESSURE	DENSITY	ISOTHERM	ISOCHORE	INTERNAL	ENTHALPY	ENTROPY	⊂v	Cp	VELOCITY
(IPTS 1968) K	MN/m <sup>2</sup>	MOL/L	DERIVATIVE J/MOL	DERIVATIVE MN/m <sup>2</sup> -K	ENERGY J/MOL	J/MOL	J/MOL-K	J/N	10L - K	OF SOUND M/S
102	0。50120	36•1651	8751	1•894	-3259.9	-3246.0	97.50	28.52	60.49	699
102	0。50120	0•65591	680	0•0060	1951.4	2715.5	155.88	22.66	35.29	167
104	0•58321	35•7307	8206	1.809	-3139.1	-3122•7	98.68	28.39	60.86	680
104	0•58321	0 <b>•7</b> 5778	674	0.0070	1970.5	2740•2	154.99	22.89	36.16	167
106	0•67469	35 <b>.28</b> 59	7486	1.725	-3017.2	-2998.1	99 <b>.84</b>	28.27	62.12	658
106	0•67469	0.87151		0.0082	1987.5	2761.7	154.13	23.13	37.12	168
108	0•77624	34.8295	6862	1.643	-2894.1	-2871.8	100.99	28.17	63.21	637
108	0•77624	0.99817	658	0.0095		2779.9	153.28	23.39	38.20	168
110	0.88851	34.3606	6291	1.564	-2769.7	-2743.9	102.14	28.08	64.29	616
110	0.88851	1.13899	647	0.0110	2014.6	2794.6	152.45	23.66	39.42	168
112	1•0121	33.8777	5886	1.485	-2643.9	-2614•0	103•28	28.00	64•58	598
112	1•0121	1.29532	633	0.0126	2024.3	2805•6	151•63	23.95	40•79	168
114	1•1477	33.3795	5247	1.409	-2516.4	-2482.0	104.41	27.93	66.64	574
114	1•1477	1.46873	618	0.0145	2031.2	2812.6	150.82	24.26	42.34	168
116 116	1•2960 1•2960	32.8641 1.66102	4784	1.334 0.0167	-2387.1	-2347.7 2815.3	105.54 150.02	27.87 24.59	67.83 44.11	553 168
118 118	1•4576 1•4576	32.3297 1.87430	4252	1.260 0.0191	-2255.8	-2210•7 2813•2	106.67 149.22	27.83 24.94	70.02 46.15	531 168
120 120	1•6333 1•6333	31.7736 2.11108	3817	1.188	-2122.1	-2070.7 2806.0	107.80	27.80	71.75	509
122	1.8236	31.1929	3429	1.117	-1985.9	-1927.4	108.93	27.79	73,39 51,30	488
124	2+0294	30.5841	2982	1.046	-1846.7	-1780.3	110.07	27.91	76,49	465
126	2.2515	29.9424	2608	0.977	-1704.0	~1628.8	111.23	27.84	79.28	442
128	2.4905	29.2619	473 2245	0.908	-1557.1	-1472.0	145.55	27,91	82.81	419
130	2.7475	28.5347	1862	0.840	-1405.4	-1309.1	145.08	28.01	88.49	393
130	2.7475	3.78483	402	0.0434	1941.7	2667.6	144.18	27.62	70,19	368
132	3.0233	4.26412	360	0.0501	1901.8	2610.8	143.22	28.22	78.87	163
134	3.3188	26.8915	1211	0.705	-1081.9	-958.5	116.09	28.26	104 <b>.31</b>	343
134	3.3188	4.32072	314	0.0582	1850.3	2538.7	142.19	28.91	91.15	161
136	3•6354	25.9350	933	0.634	-906.6	-766.5	117.42	28.44	115.43	316
136	3•6354	5.48158	263	0.0683	1783.0	2446.2	141.04	29.71	110.06	160
138	3•9742	24.8388	635	0.561	-718.0	-558•0	118.85	29.90	140.66	280
138	3•9742	6.29098	210	0.0795	1692.6	2324•4	139.73	30.96	136.11	156
140	4•3371	23.5205	384	0.489	-504.5	-320.1	120.45	31.07	188.62	248
140	4•3371	7.32264	152	0.0957	1569.0	2161.3	138.17	33.10	190.40	152
142	4•7263	21.7690	186	0.402	-246.6	-29.5	122.39	32.15	293.49	211
142	4•7263	8.78540	85	0.121	1385.7	1923.7	136.14	35.45	350.23	149
144	5•1464	18.3271	7	0.282	182.9	463.7	125.69	42.95	5191,48	145
144	5•1464	11.8884	12	0.173	973.7	1406.6	132.24	41.44	2537,44	140
144.31	5•2153 5•2153	15.1000	0	0.227	562.3 562.3	907•6 907•6	128.74		00 00	

\* THE FIRST ENTRY FOR EACH TEMPERATURE REFERS TO THE LIQUID PHASE.

### TABLE 16. THERMODYNAMIC PROPERTIES OF FLUORINE

The number of significant figures given in this table is not justified on the basis of the uncertainty of the data, but is presented to maintain internal consistency. 0.01 MN/m<sup>2</sup> ISOBAR

IEMPERATURE	DENSITY	ISOTHERM	ISOCHORE	INTERNAL	ENTHALPY	ENTROPY	Cv	Cp	VELOCITY
K (1915-1968)	MOL/L	J/MOL	MN/m <sup>2</sup> -K	J/MOL	J/MOL	J/MOL-K	J / MC	)L - K	M/S
* 53.482	44.8775	26743	4.3103	-6027.0	-6026.8	60.83	36.51	54.95	1029
54	44.7927	26705	4.3099	-5938.4	-5998.2	61.36	36.42	55.14	1032
58	44.1409	25951	4.2042	-5776.8	-5776.6	65.32	35.70	55.98	1035
60	43.8254	25739	4.1275	-5666,9	-5666.7	67.18	35.31	55.99	1036
64	43.5015 43.1678	25561 24864	4.0613 3.9690	-5555.9 -5443.5	-5555.7 -5443.3	69.00 70.79	34.92 34.50	56.06 56.26	1039
66	42.8327	23699	3.8247	-5331.0	-5330.7	72.52	34.08	56.29	1015
* 68.835	42.5119	22346	3.5216	-5173.5	-5220.2	74.85	33.59	55.51 54.80	995
★ 68.835	0.0175724	566	0.0001	1421.2	1990.2	178.56	23.89	29.39	145
70 72	0.0172751	576	0.0001	1445.6	2024.5	179.05	20.88	29.37	146
74	0.0163278	610	0.0001	1529.4	2141.9	180.68	20.87	29.33	150
76 78	0.0158926	627	0.0001	1571.3	2200.5	181.46	20.86	29.31	152
80	0.0150890	660	0.0001	1655.0	2317.7	182.97	20.85	29.28	156
82	0.0147172	677		1696.8	2376.3	183.69	20.85	29.27	158
86	0.0140265	711	0.0001	1780.4	2493.3	185.08	20.84	29.25	162
88		728	0.0001	1822.2	2551.8	185.76	20.84	29.24	164
92	0.0131048	761	0.0001	1905.7	2668.7	187.05	20.83	29.22	168
94	0.0128241	778	0.0001	1947.4	2727.2	187.68	20.83	29.22	169
98	0.0122975	812	0.0001	2030.9	2844.0	188.90	20.83	29.21	173
100	0.0120501	828	0.0001	2072.6	2902.4	189.49	20.83	29.20	175
102	0.0116126	845 862	0.0001	2114.3 2156.0	2960.8 3019.2	190.07	20.83 20.83	29.20 29.19	177
106	0.0113647	879	0.0001	2197.7	3077.6	191.19	20.83	29.19	180
108	0.0111533	895 912	0.0001	2239.4 2281.1	3136.U 3194.4	191.74	20.83	29.19 29.19	182
112	0.0107533	929	0.0001	2322.8	3252.7	192.80	20.83	29.18	185
114 116	0.0105640	945	0.0001	2364.5	3311.1 3369.5	193.32	20.83	29.18 29.18	187
118	0.0102046	979	0.0001	2447.9	3427.8	194.32	20.83	29.18	190
120	0.0000000	996	0.0001	2489.6	3486.2	194.81	20.83	29.18	192
124	0.0097093	1029	0.0001	2573.0	3603.0	195.77	20.84	29.19	195
126	0.0095548	1046	0.0001	2614.7	3661.3	196.24	20.84	29.19	196
130	0.0092600	1079	0.0001	2698.2	3778.1	197.15	20.85	29.19	199
132	0.0091193	1096	0.0001	2739.9	3836.5	197.59	20.86	29.20	201
136	0.0088505	1129	0.0001	2823.4	3953.3	198.47	20.87	29.21	204
138	0.0087219	1146	0.0001	2865.2	4011.7	198.89	20.88 20.88	29.21	205
142	0.0084757	1179	0.0001	2948.8	4128.6	199.73	20.89	29.23	20.8
144	0.0083578	1196	0.0001	2990.6	4187.1	200.14	20.90	29.23	210
146	0.0082431	1212	0.0001	3032+4	4245.5	200.54	20.91	29.24	211
150	0.0080229	1246	0.0001	3116.1	4362.5	201.33	20.93	29.26	214
152	0.0079171	1262	0.0001	3158.0	4421.1	201,72	20.94	29.27	216
156	0.0077138	1296	0.0001	3241.8	4538.2	202.48	20.96	29.29	218
160 160	0.0076160	1312	0.0001	3283.8 3325.7	4596.8 4655.4	202.85 203.22	20.97 20.99	29.30 29.32	220 221
165	0.0072925	1371	0.0001	3430.8	4802.1	204.12	21.02	29.35	224
175	0.0068753	1454	0.0001	3641.5	5096.0	205.00	21.11	29.39	231
180	0.0066841	1496	0.0001	3747.2	5243.3	206.68	21.15	29.48	234
190	0.0063320	1537	0.0001	3959.3	5538.6	208.28	21.20	29.53	240
195	0.0061695	1620	0.0001	4065.7	5686.6	209.05	21.32	29.64	244
205	0.0058683	1662	0.0001	4279.6	5983.7	210.53	21.38 21.45	29.71	247
210	0.0057285	1745		4387.0	6132.7	211.25	21.52	29.84	252
215 220	0.0055952 0.0054679	1787 1829		4494.8 4603.0	6282.1 6431.8	211.95 212.64	21.59 21.66	29.91 29.98	255 258
225	0.0053463	1870		4711.5	6581.9	213.32	21.74	30.06	261
23U 235	0.0052300	1912		4029.7	6883.3	213.98	21.82 21.90	30.14	266
240	0.0050120	1995		5039.4	7034.6	215.27	21.98	30.30	269
250	0.0049097	2078		5260.1	7338.5	215.89 216.51	22.15	30.47	272
255	0.0047171	2120		5371.1	7491.1	217.11	22.24	30.56	277
265	0.0045390	2203		5594.4	7797.5	218.29	22.42	30.74	282
270	0.0044543	2245		5706.7	7951.4	218.86	22.51	30.83	284
275	0.0043739	2286		5819.5 5932.7	8105.8	219.43 219.99	22.60	30.92 31.01	287 289
285	0.0042204	2369		6046.4	8415.8	220.54	22.78	31.10	292
290 295	0.0041476	2411 2453		616U.5 6275.1	85/1.6	221.08 221.61	22.87	31.19	294
300	0.0040093	2494		6390.1	8884.3	222.14	23.05	31.37	299

\* TWO-PHASE BOUNDARY

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#### TABLE 16. THERMODYNAMIC PROPERTIES OF FLUORINE

0.02 MN/m<sup>2</sup> ISOBAR

TEMP	ERATURE	OENSITY	ISOTHERM	ISOCHORE	INTERNAL	ENTHALPY	ENTROPY	Cv	Cp	VELOCITY
(19)	K (	MOL/L	J/MOL	MN/m <sup>2</sup> -K	J/MOL	J/MOL	J/MOL-K	J / MOL	- к	M/S
4	53.483	44.8777	26748	4.3103	-6027.3	-6026.8	60.83	36.51	54.95	1029
	54	44.7930	26709	4.3100	-5998.7	-5998.2	61.36	36.42	55.14	1032
	56	44.4657	26286	4.2989	-5887.9	-5887.5	53.38	30.07	55.98	1036
	58 60	44.1413 43.8257	25953 25740	4.2044 4.1275	-5777.1	-5776.6 -5666.8	65.32 67.18	35.70 35.31	55.98 55.99	1035
	62	43.5019	25560	4.0613	-5556.2	-5555.7	69.00	34.92	56.06	1039
	64 66	43.1082	24862	3.9690	-5443.8	-5443.3	70.79	34.50	56.20	1033
	68	42.5124	228 08	3.6373	-5220.7	-5220.3	74.17	33.69	55.52	995
	70	42.1819	21605	3.5182	-5109.0	-5108.6	75.78	33.28	55.82	977
#	72,913	41.6798	20432	3.4154	-4994.8	-4994.3	77.39 78.09	32.86	55.72	960
4	72.913	0.0333111	595	0.0003	1500.9	2101.3	174.41	20.95	29.59	149
	74	0.0328081	604	0.0003	1523.9	2133.5	174.84	20.95	29.57	150
	78	0.0310836	638	0.0003	1608.2	2251.6	175.63	20.93	29.50	154
	8 0	0.0302891	655	0,0003	1650.3	2310.6	177.14	20.91	29.47	156
	82	0.0295351	673	0.0002	1692.3	2369.5	177.87	24.90	29.44	158
	84 86	0.0281361	707	0.0002	1776.3	2428.3	179.27	20.90	29.42	160
	88	0.0274860	724	0.0002	1818.3	2545.9	179.95	20.88	29.38	164
	90	0.0268657	741	0.0002	1860.2	2604.6	180.61	20.88	29.36	166
	92	0.0257066	774	0.0002	1944.0	2722.0	181.88	20.87	29.34	169
	96	0.0251642	791	0.0002	1985.9	2780.7	182.50	20.86	29.31	171
	98 100	0.0246444 0.0241460	8 0 8 8 25	0.0002	2027.7 2069.6	2839.3 289 <b>7.</b> 9	183.11 183.70	20.86 20.86	29.30 29.29	173 175
	102	0.0236675	842	0.0002	2111.4	2956.4	184.28	20.85	29.28	176
	104	0.0232077	859	0.0002	2153.2	3015.0	184.85	20.85	29.27	178
	108	0.0223403	893	0.0002	2236.8	3132.1	185.95	20.85	29.26	182
	110	0.0219307	909	0.0002	2278.6	3190.6	186.49	20.85	29.25	183
	112	0.0215359	926	0.0002	2320.4	3249.1	187.01	20.85	29.25	185
	116	0.0207878	960	0.0002	2403.9	3366.0	188.04	20.85	29.24	188
	118 120	0.0204330 0.0200902	977 993	0.0002	2445.7 2487.5	3424.5 3483.0	188.54 189.03	20.85 20.85	29.24 29.23	190 191
	122	0.0197588	1010	0.0002	2529.2	3541.4	189.51	20.85	29.23	193
	124	0.0194382	1027	0.0002	2571.0	3599.9	189.99	20.85	29.23	195
	128	0.0188273	1060	0.0002	2654.6	3716.8	190.92	20.86	29.23	198
	130	0.0185362	1077	0.0002	2696.3	3775.3	191.37	20.86	29.23	199
	132	0.0182539	1094	0.0002	2738.1	3833.8	191.62	20.87	29.24	201
	136	0.0177145	1127	0.0001	2821.7	3950.7	192.69	20.88	29.24	204
	138 140	0.0174566 0.0172062	1144 1161	0.0001 0.0001	2863.5 2905.3	4009.2 4067.7	193.12 193.54	20.88	29.25 29.25	205 207
	142	0.0169629	1177	0.0001	2947.2	4126.2	193.95	20.90	29.26	208
	144	0.0167264	1194	0.0001	2989.0	4184.7	194.36	20.91	29.26	210
	146	0.0164964	1211	0.0001 0.0001	3030.9	4243.3	194.77	20.91	29.28	211
	150	0.0160549	1244	0.0001	3114.7	4360.4	195.56	20.93	29.29	214
	152	0.0158429	1261	0.0001	3156.6	4419.0	195.95	20.94	29.29	215
	156	0.0154354	1294	0.0001	3240.5	4536.2	196.71	20.95	29.30	217
	158 160	0.0152394	1311	0.0001	3282.4	4594.8	197.08	20.98	29.33	220 221
	165	0.0145911	1370	0.0001	3429.6	4800.3	198.35	21.03	29.37	224
	170	0.0141609	1411	0.0001	3534.9	4947.2	199.23	21.07	29.41	228
	175	0.0137554	1453	0.0001	3640.4	5094.3	200+08	21.16	29.45	231
	185	0.0130103	1536	0.0001	3852.0	5389.3	201.72	21.21	29.54	237
	190	0.0126673	1578	0.0001	3958.3	5537.1	202.51	21.26	29.60	240
	200	0.0120329	1661	0.0001	4064+8	5833.7	203.20	21.32	29.00	243
	205	0.0117390	1703	0.0001	4278.7	5982.4	204.77	21.45	29.78	249
	210	0.0114591	1745	0.0001	4386.2	6131.5	205.48	21.52	29.85	252
	215 220	0.0111923 0.0109376	1786 1828	0.0001 0.0001	4494.0 4602.2	6280.9 6430.7	206.19 206.88	21.59 21.66	29.92	255
	225	0.0106942	1870	0.0001	4710.7	6580.9	207.55	21.74	30.07	261
	235	0.0104615	1911	0.0001	4019.b 4929.0	6882.3	208.86	21.82	30.19	266
	240	0.0100252	1995	0.0001	5038.7	7033.7	209.50	21.98	30.31	269
	245	0.0098204	2030	0.0001	5148.9	7185.4	210.13	22.07	30.39	272
	255	0.0094350	2119	0.0001	5370.5	7490.2	211.34	22.24	30.57	277
	260	0.0092534	2161	0.0001	5481.9	7643.3	211.94	22.33	30.65	279
	265 270	0.0090787 0.0089104	2203 2244	0.0001	5593.8 5706.1	7796.8 7950.7	212.52 213.10	22.42 22.51	30.74 30.83	282 284
	275	0.0087483	2286	G.0001	5818.9	8105.1	213.67	22.60	30.92	287
	285	0.0084412	2327	0.0001	5932.2	8415.2	214.22	22.09	31.10	289
	290	0.0002956	2411	0.0001	6160.0	8570.9	215.31	22.87	31.19	294
	295	0.0081549	2452 2494	0.0001	6274.6 6339.7	8727.1	215.85	22.96	31.28	297
#### 0.04 MN/m<sup>2</sup> ISOBAR

TEMP	ERATURE	DENSITY	ISOTHERM	ISOCHORE	INTERNAL	ENTHALPY	ENTROPY	Cv	Сp	VELOCITY
(16)	K K	MOL/L	J/MOL	MN/m <sup>2</sup> + K	J/MOL	J/MOL	J/MOL-K	J / MC	с – к	M/S
	53.485	44.8781	26756	6 3104	-6027 7	-6026 8	60 87	36.50	54 95	1030
	54	44.7938	26717	4.3101	-5999.2	-5998.3	61.36	36.42	55.13	1032
	56	44.4665	26292	4.2992	-5888.4	-5887.5	63.38	36.07	55.98	1036
	58 60	44.1421 43.8265	25956 25744	4.2047	-5777.6	-5776.7 -5666.9	65.32 57.18	35.70 35.31	55.98 55.99	1035 1036
	6.2	43.5027	25550	4 0611	-5555 8	-5555 8	69.00	31, 02	56.06	10.39
	64	43.1690	24857	3.9689	-5444.4	-5443.4	70.79	34.50	56.27	1033
	66	42.8340	23694	3.8251	-5331.8	-5330.9	72.52	34.09	56.30	1015
	68	42.5133	22809	3.6377	-5221.3	-5220.4	74.16	33.69	55.52	995
	70	42.1828	21607	3.5184	-5109.6	-5108.7	75.78	33.28	55.82	977
	74	41.4937	20174	3,3355	-4882.8	-4881.9	78.93	32.46	56.17	958
	76	41.1465	19215	3.1955	-4769.3	-4768.4	80.44	32.07	55.92	939
4	77.568	40.8714	18078	3.0638	-4680.1	-4679.2	81.60	31.76	55.88	915
4	77.568	0.0630412	624	0.0005	1588.8	2223.3	170.34	21.07	29.93	153
	80	0.0610351	628 646	0.0005	1598.U 1640.0	2236.2	170.50	21.06	29.92	153
	82	0.0594828	663	0.0005	1683.2	2355.6	172.00	21.02	29.80	157
	84	0.0580105	681	0.0005	1725.6	2415.2	172.71	21.00	29.74	159
	86	0.055281/	698	0.0005	1768.1	2474.6	173.41	20.99	29.70	161
	90	0.0540139	733	0.0005	1852.7	2593.2	174.09	20.97	29.62	165
	92	0.0528048	750	0.0004	1894.9	2652.4	175.41	20.95	29.58	167
	94	0.0516501	767	0.0004	1937.1	2711.6	176.05	20.94	29.55	169
	96	0.0505461	785	0.0004	1979.3	2770.6	176.67	20.93	29.52	171
	98	0.0484769	8U2 819	0.0004	2021.4 2063.5	2829.7 2888.6	177.28	20.92	29.50 29.47	172
	102	0.0475058	836	0.0004	2105.6	2947.6	178.46	20.91	29.45	176
	104	0.0465736	853	0.0004	2147.6	3006.4	179.03	20.90	29.43	178
	106	0.0456780	870	0.0004	2189.6	3065.3	179.59	20.90	29.42	180
	110	0.044010/	904	0.0004	2273.6	3182.9	180.68	20.09	29.40	183
	112	0.0431895	921	0.0004	2315.5	3241.7	181.21	20.88	29.37	185
	114	0.0424201	938	0.0004	2357.5	3300.4	181.73	20.88	29.36	186
	116	0.0416780	955	0.0003	2399.4	3359.1	182.24	20.88	29.35	188
	120	0.0402699	989	0.0003	2483.2	3476.5	183.23	20.88	29.34	191
	122	0.0396014	1006	0.0003	2525.1	3535.2	183.72	20.88	29.33	193
	124	0.0389549	1023	0.0003	2567.0	3593.8	184.19	20.88	29.32	194
	128	0.0377240	1040	0.0003	2650.8	3711.1	185.13	20.88	29.32	198
	130	0.0371375	1073	0.0003	2692.6	3769.7	185.58	20.88	29.31	199
	132	0.0365691	1090	0.0003	2734.5	3828.3	186.03	21.89	29.31	201
	134	0.0360180	1107	0.0003	2776.4	3887.0	186.47	20.89	29.31	202
	136	0.0354834	1124	0.0003	2818.3	3945.6	186.90	20.90	29.31	204 .
	140	0.0344609	1197	0.0003	2902.1	4062.8	187.75	20.91	29.31	207
	142	0.0339715	1174	0.0003	2944.0	4121.5	188.17	20.91	29.32	208
	144	0.0334960	11 91	0.0003	2985.9	4180.1	188.58	20.92	29.32	210
	146	0.0325840	1208	0.0003	3027.49	4238.8	188.38	20.93	29.33	211
	150	0.0321465	1241	0.0003	3111.8	4356.1	189.78	20.95	29.34	214
	152	0.0317206	1258	0.0003	3153.7	4414.8	190.16	20.95	29.34	215
	154	0.0313060	1275	0.0003	3195.7	4473.4	190.55	20.97	29.35	217
	156	0.0309021	1292		3237.8	4532.2	190.93	20.98	29.36	218
	160	0.0301250	1325	0.0003	3321.8	4649.6	191.67	21.00	29.38	221
	165	0.0292071	1367	0.0002	3427.1	4796.6	192.57	21.03	29.41	224
	176	0.0276302	1409	0.0002	353205	4943+7	193.45	21.07	29.44	228
	180	0.0267622	1493	0.0002	3743.9	5238.6	195.14	21.16	29.52	234
	185	0.0260360	1535	0.0002	3850.0	5386.3	195.95	21.21	29.57	237
	190	0.0253483	1576	0.0002	3956.3	5534.3	196.74	21.27	29.62	240
	195	0.0246961	1618	0.0002	4062.9	5682.6	197.51	21.33	29.68	243
	200	0 0234877	1702	0.0002	4109.7	5980.0	198.20	21.39	29.74	246
	210	0.0229269	1743	0.0002	4384.5	6129.1	199.71	21.52	29.87	252
	215	0.0223923	1785	0.0002	4492.3	6278.6	200.42	21.59	29.94	255
	220	0.0213048	1869	0.0002	4000.9	6578.8	201+11	21.07	30.00	258
	230	0.0209287	1910	0.0002	4818.1	6729_4	202.44	21.82	30.16	264
	235	0.0204825	1952	0.0002	4927.5	6880.4	203.09	21.90	30.24	266
	240	0.0200550	1994	0.0002	5037.3	7031.8	203.73	21.99	30.32	269
	245	0.0196449	2035	0.0002	5147.5	/183.6	204.36	22.07	30.41	272
	255	0.0192914	2119	0.0002	5369-2	7488-6	204+97	22.24	30-58	214
	260	0.0185098	2160	0.0002	5480.7	7641.7	206.17	22.33	30.67	279
	265	0.0181600	2202	0.0002	5592.6	7795.2	206.76	22.42	30.75	282
	275	0.0174988	2285	0.0001	5817-8	8103-6	207.90	22.60	30.93	287
	280	0.0171860	2327	0.0001	5931.1	8258.5	208.46	22.69	31.02	289
	285	0.0168841	2369	0.0001	6044.8	8413.9	209.01	22.78	31.11	292
	290	0.0165927	2410	0.0001	6159.0	8569.7	209.55	22.87	31.20	294
	295	0.0163112	2452	0.0001	62/3.6	8725.9	210.08	22.96	51.29	297

# TABLE 16. THERMOOYNAMIC PROPERTIES OF FLUORINE

#### 0.06 MN/m<sup>2</sup> ISOBAR

TEMPERATURE	OENSITY	ISOTHERM DERIVATIVE	ISOCHORE OFRIVATIVE	INTERNAL	ENTHALPY	ENTROPY	Cv	Сp	VELOCITY OF SOUND
K	MOL/L	J/MOL	MN/m <sup>2</sup> -K	J/MOL	J/MOL	J/MOL-K	J / MI	0L – K	M/S
* 53.487	44.8786	26764	4.3105	-6028.1	-6026.8	60.83	30.50	54.94	1030
56	44.4672	26724	4.3102	-5889.0	-5998.4	63.37	36+42	55.98	1032
58	44.1428	25960	4.2050	-5778.2	-5776.8	65.32	35.70	55.97	1035
60	43.8273	25747	4.1278	-5668.3	-5667.0	67.18	35.32	55.99	1036
62 64	43.5034 43.1698	25558 24853	4.0610 3.9688	~5557.3 -5444.9	-5555.9 -5443.5	69.00 70. <b>7</b> 8	34.92 34.50	56.06 56.27	1039 1033
66	42.8348	23691	3.8253	-5332.4	-5331.0	72.51	34.09	56.30	1015
68 70	42.1838	22810	3.6381 3.5187	+5221.9	-5220.5	74.16	33.69	55.52	995
72	41.8341	20431	3.4155	-4996.0	-4994.6	77.39	32.87	56.36	960
74	41.4947	20171	3.3356	-4883.5	-4882.0	78.93	32.47	56.17	958
78	41.1475	17992	3.1957	-4656.1	-4/68.5	81.91	32.07	55.93	939
80	40.4404	17116	2.9789	-4541.9	-4540.4	83.36	31.31	56.67	903
* 80.609 * 80.609	40.3312 0.0915190	1596 <b>1</b> 641	2.9079	-4507.1	~4505.6 2299.5	83.79	31.20	57.46 30.24	879 155
82	0.0898642	653	0.0008	1673.8	2341.5	168.51	21.15	30.17	157
84	0.0875939	671	0.0007	1716.8	2401.7	169.24	21.12	30.09	159
88	0.0833981	7.07	0.0007	1799.6	2461.9	159.94	21.09	30.02	161
90	0.0814545	7 25	0.0007	1845.0	2581.7	171.30	21.05	29.89	165
92	0.0796033	743	0.0007	1887.6	2641.4	171.96	21.03	29.83	166
94	0.0761519	760	0.0007	1930.2	2760.5	172.00	21.00	29.78	168
98	0.0745400	795	0.0006	2015.0	2820.0	173.84	20.99	29.70	172
100	0.0729971	812	0.0006	2057.4	2879.3	174.44	24.97	29.66	174
102	0.0715188	830	0.0006	2099.7	2938.6	175.03	20.96	29.63	176
104	0.0701009	847	0.0006	2141.9	2997.8	175.60	20.95	29.60	177
108	0.0674316	882	0.0006	2226.3	3116.1	176.72	20.94	29.55	181
110	0.0661737	899	0.0006	2268.5	3175.2	177,26	20.93	29.52	183
112	0.0649628	916	0.0005	2310.6	3234.2	177.79	20.92	29.50	184
116	0.0626720	950	0.0005	2394.8	3352.2	178.83	20.91	29.47	188
118	0.0615874	967	0.0005	2436.9	3411+1	179.33	20.91	29.45	189
120	0.0605403	984	0.0005	2478.9	3470.0	179.83	20.91	29.44	191
122	0.0595288	1001	0.0005	2520.9	3528.8	180.31	20.91	29.43	193
126	0.0576056	1036	0.0005	2604.9	3646.5	181.26	20.91	29.41	196
128	0.0566905	1053	0.0005	2646.9	3705.3	181.72	20.91	29.40	197
130	U.U558U45 0.0549461	1070	0.0005	2688.9	3764.1	182.18	20.91	29.39	199
134	0.0541141	1103	0.0005	2772.9	3881.7	183.07	20.91	29.38	202
136	0.0533072	1120	0.0004	2814.9	3940.4	183.51	20.91	29.38	204
138 140	0.0525243 0.0517643	1137 1154	0.0004	2856.9 2898.8	3999.2 4057.9	183.93 184.36	20.92	29.38 29.38	205
142	0.0510262	1171	0.0004	2940.8	4116.7	184.77	20.93	29.38	208
144	0.0503091	1188	0.0004	2982.6	4175.5	185.19	20.93	29.38	209
140	0.0489343	1222	0.0004	3066.8	4293.0	185.99	20.95	29.38	212
150	0.0482750	1239	0.0004	3108.9	4351.8	186.38	20.96	29.39	214
152	0.0476333	1255	0.0004	3150.9	4410.5	186.77	20.97	29.39	215
156	0.0464002	1289	0.0004	3235.0	4528.1	187.54	20.99	29.41	218
158	0.0458075	1306	0.0004	3277.1	4587.0	187.91	21.00	29.41	219
100	0.0452299	1323	0.0004	3319.2	4645.8	108.28	21.01	29.42	221
170	0.0435480	1365	0.0004	3424.6	4793.U 4940.3	199.19	21.04	29.45	228
175	0.0413245	1449	0.0003	3635.8	5087.8	190.92	21.12	29.51	231
180	0.0401691	1491	0.0003	3741.7	5235.4	191.75	21.17	29.56	234
190	0.0390770	1533	0.0003	3847.9	5383.3	192.57	21.27	29.60	237
195	0.0370625	1616	0.0003	4060.9	5679.8	194.13	21.33	29.70	243
200	0.0361314	1658	0.0003	4167.9	5828.5	194.88	21.39	29.76	246
205	0.0352462 0.0344035	1700 1742	0.0003	4275.2 4382.7	5977.5 6126.7	195.61 196.33	21.46 21.53	29.82 29.89	249
215	0.0336003	1784	0.0003	4490.7	6276.4	197.04	21.60	29.96	255
220	0.0328338	1826	0.0003	4598.9	6426.3	197.73	21.67	30.03	258
230	0.0314015	1909	0.0003	4707.0 4816.6	6727-4	199.07	21.83	30.18	264
235	0.0307314	1951	0.0003	4926.0	6878.4	199.72	21.91	30.26	266
240	0.0300893	1993	0.0003	5035.9	7029.9	200.35	21.99	30.34	269
250	0.0288826	2034	0.0002	5256.8	7181.8	200.98	22.16	30.42	274
255	0.0283149	2118	0.0002	5367.9	7486.9	202.20	22.25	30.59	277
260	0.0277692	2160	0.0002	5479.4	7640.1	202.80	22.33	30.66	279
265 270	0.0272441 0.0267386	2201 2243	0.0002	5591.4 5703.8	7793.7 7947.7	203.38 203.96	22.42 22.51	30.77 30.85	282 284
275	0.0262515	2285	0.0002	5816.6	8102.2	204.52	22.60	30.94	267
280	0.0257819	2326	0.0002	5929.9	8257.2	205.08	22.69	31.03	289
290	0.0248914	2368	0.0002	6157.9	0412.0 8568.4	205.63	22.88	31.12	294
295	0.0244688	2451	0.0002	6272.6	8724.7	206.71	22.97	31.30	297
300	0.0240604	2493	0.0002	6387.7	8881.4	207.23	23.06	31.39	299

#### 0.08 MN/m<sup>2</sup> ISOBAR

TEMPERATURE	OENSITY	ISOTHERM	I SOCHORE	INTERNAL	ENTHALPY	ENTROPY	Cv	Сp	VELOCITY
К К	MOL/L	J/MOL	MN/m <sup>2</sup> -K	J/MOL	J/MOL	J∕MOL-K	J / MO	Е – К	M/S
* 53,489	44.8790	26773	4.3106	=6028.5	=6026.7	60.83	36.50	54.93	1030
54	44.7953	26732	4.3103	-6000.3	-5998.5	51.36	36.42	55.12	1032
56	44.4680	26302	4.2998	-5889.5	-5887.7	63.37	36.07	55.98	1036
58 60	44.1436 43.8281	25963 25750	4.2053 4.1279	-5778.7 -5668.9	-5776.9 -5667.1	65.32 67.18	35.70 35.32	55.97 55.98	1035 1036
62	43.5042	25558	4.0609	-5557.9	-5556.0	69.00	34.92	56.06	1039
64	43.1706	24848	3.9687	-5445.5	-5443.7	70.78	34.51	56.27	1033
66	42.8357	23688	3.8255	-5333.0	-5331.1	72.51	34.09	56.31	1015
50	42.5150	22611	3.6385	-5222.5	-5220+6	74.16	33.69	55.53	995
72	41.8351	20430	3.4155	-4996.7	-4994.7	77.38	32.87	56.36	960
74	41.4957	20168	3.3357	-4884.1	-4882.2	78.93	32.47	56.18	958
76	41.1486	19212	3.1958	-4770.6	-4768.7	80.44	32.07	55,93	939
80	40.4416	17992	2.9790	-4556.8	-4654.8 -4540.6	81.91 83.35	31.69 31.31	56.39 56.68	918 903
82	40.0715	16323	2.8636	-4426.5	-4424.5	84.78	30.94	56.60	886
* 82.930	39.9119	15700	2.7904	-4374.4	-4372.4	85.41	30.80	56.62	872
* 82.930	U • 119231 0 • 117587	652	0.0010	1084.4	2355.4	166.34	21.26	30.52	157
86	0.114641	681	0.0010	1751.0	2448.8	167.45	21.20	30.35	160
88	0.111849	699	0.0010	1794.2	2509.5	168.15	21.17	30.26	162
90	0.109198	717	0.0009	1837.3	2569.9	158.82	21.14	30.17	164
92	0.100078	753	0.0009	1000.2	2630.1	109.49	21.12	30.10	166
96	0.101988	771	0.0009	1965.9	2750.3	170.77	21.07	29.96	170
98	0.0998017	788	0.0008	2008.5	2810.1	171.38	21.05	29.91	172
100	0.0977114	806	0.0008	2051.2	2869.9	171.99	21.03	29.86	174
102	0.0957105	824	0.0008	2093.7	2929.6	172.58	21.02	29.81	175
106	0.0919538	859	0.0008	2178.6	3048.6	173.72	20.99	29.73	179
108	0.0901877	876	0.0008	2221.0	3108.1	174.28	20.98	29.70	181
110	0.0884903	894	0.0007	2263.4	3167.4	174.82	20.97	29.66	182
112	0.0852859	911	0.0007	2348.0	3286.0	175.88	20.96	29.61	186
116	0.0837715	946	0.0007	2390.2	3345.2	176.40	20.95	29.59	187
118 120	0.0823113 0.0809025	963 980	0.0007 0.0007	2432.4 2474.6	3404.3 3463.4	176.90 177.40	20.94 20.94	29.56 29.54	189 191
122	0,0795421	997	0.0007	2516.7	3522.5	177.89	20.93	29.53	192
124	0.0782278	1014	0.0007	2558.9	3581.5	178.37	20.93	29.51	194
126	0.0769571	1031	0.0006	2601.0	3640.5	178.84	20.93	29.50	196
128		1049	0.0006	2643+1	3699.5	179.30	20.93	29.49	197
132	0.0733855	1083	0.0006	2727.3	3817.4	180.21	20.93	29.47	200
134	0.0722689	1100	0.0006	2769.4	3876.3	180.65	20.93	29.46	202
136	0.0711862	1117	0.0006	2811.4	3935.3	181.09	20.93	29.45	203
138 140	0.0691169	1134 1151	0.0006	2893.5 2835.6	3994.2 4053.0	181.52	20.94	29.45 29.44	205
142	0.0681273	1168	0.0006	2937.6	4111.9	182.36	20.94	29.44	208
144	0.0671661	1185	0.0006	2979.7	4170.8	182.77	20.95	29.44	209
146	0.0662320	1202	0.0005	3021.8	4229.7	183.18	20.96	29.44	211
150	0.0644405	1236	0.0005	3106.0	4347.4	183.97	20.97	29.44	214
152	0.0635811	1253	0.0005	3148.1	4406.3	184.36	20.98	29.44	215
154	0.0627445	1270	0.0005	3190.2	4465.2	184.75	20.99	29.45	217
156	0.0619299	1287	0.0005	3232.3	4524.1	185.13	21.00	29.45	218
160	0.0603632	1320	0.0005	3316.6	4641.9	185.87	21.02	29.40	221
165	0.0585139	1363	0.0005	3422.1	4789.3	186.78	21.05	29.49	224
170	0.0551797	1405	0.0005	3527.8	4936.8	187.66	21.09	29.51	227
180	0.0535935	1489	0.0004	3739.6	5232.3	189.35	21.17	29.59	231
185	0.0521334	1531	0.0004	3845.8	5380.3	190.16	21.22	29.63	237
190	0.0507513	1573	0.0004	3952.3	5528.6	190.95	21.28	29.68	240
195	0.0494410	1615	0.0004	4029.0	56//.1	191.72	21.34	29.73	243
205	0.0470145	1699	0.0004	4273.4	5975.0	193.21	21.40	29.85	249
210	0.0458888	1741	0.0004	4381.0	6124.4	193.93	21.53	29.91	252
215	0.0448161	1783	0.0004	4489.0	6274.1	194.64	21.60	29.98	. 255
225	0.0428148	1866	0.0004	4706.0	6574.5	196.00	21.75	30.12	261
230	0.0418801	1908	0.0003	4815.1	6725.3	196.67	21.83	30.20	264
235	0.0409854	1950	0.0003	4924.6	6876.5	197.32	21.91	30.27	266
240	0.0401282	2034	0.0003	5144.7	7180.0	198,58	22.08	30.35	269
250	0.0385175	2075	0.0003	5255.5	7332.4	199.20	22.16	30.52	274
255 260	0.0377599	2117 2159	0.0003	5366.6 5478.2	7485.2	199.80 200.40	22.25	30.60	277
265	0.0363308	2201	0.0003	559u.2	7792.1	200,98	22.43	30.78	282
270	0.0356562	2242	0.0003	5702.6	7946.3	201.56	22.52	30.87	284
275	0.0350063	2284	0.0003	5815.5	8100.8	202.13	22.61	30.95	287
280	0.0343797	2326	0.0003	5928.8	8255.8	202.69	22.70	31.04	289
290	0.0331916	2409	0,0003	6156.9	8567.1	203.78	22.88	31.22	294
295	0.0326279	2451	0.0003	6271.6	8723.5	204.31	22.97	31.31	297
300	0.0320830	2493	0.0003	6386.7	8880.2	204.84	23.06	31.40	299

# TABLE 16. THERMODYNAMIC PROPERTIES OF FLUORINE

## 0.101325 MN/m<sup>2</sup> (1 ATM) ISOBAR

TEMPERATURE	OENSITY	ISOTHERM	ISOCHORE	INTERNAL	ENTHALPY	ENTROPY	Cv	Сp	VELOCITY
K (1F12 1966)	MOL/L	JZMOL	MN/m <sup>2</sup> -K	J/MOL	J/MOL	J/MOL÷K	J/MI	оц <del>-</del> К	M/S
* 53.491	44.8794	26 <b>78</b> 2	4.3107	-6029.0	-6026.7	60.83	36.50	54.93	1030
54	44.7961	26741	4.3104	-6000.9	-5998.6	61.36	36.42	55.11	1032
58	44.1444	25967	4.2056	-5779.3	-5777.0	65.31	35.70	55.97	1037
60	43.8289	25754	4.1280	-5669.5	-5667.2	67.18	35.32	55.98	1037
62 64	43.5051 43.1714	25557 24843	4.0608 3.9686	-5558.5 -5446.1	-5556.2	69.00 70.78	34.93 34.51	56.06 56.28	1039
66	42.8366	23685	3.8258	-5333.6	-5331.3	72.51	34.09	56.32	1015
68	42.5159	22812	3.6389	-5223.1	-5220.8	74.16	33.69	55.53	995
70	42.1057	20430	3.4155	-4997.3	-4994.9	77.38	32.87	55.02 56.36	977
74	41.4968	20165	3.3358	-4884.7	-4882.3	78.92	32.47	56.19	958
76	41.1497	19210	3.1960	-4771.3	-4768.8	80.43	32.07	55.94	939
80	40.4428	17116	2.9791	-4543.3	-4540.8	83.35	31.32	56.68	903
82	40.0728	16321	2.8638	-4427.2	+4424.7	84.78	30.94	56.60	886
* 84.950	39.5418	14790	2.6894	-4258.7	-4256.1	86.79	30.47	57.04	854
* 84.950	0.148191	661	0.0013	1718.6	2402.4	165.00	21.35	30.81	158
86	0.146200	671	0.0013	1741.6	2434.7	165.37	21.33	30.73	160
90	0.139127	708	0.0012	1828.8	2557.1	166.76	21.25	30.49	164
92	0.135860	727	0.0012	1872.2	2618.0	167.43	21.21	30.39	166
94	0.132755	745	0.0011	1915.4	2678.7	168.09	21.18	30.30	167
98	0.126976	781	0.0011	2001.6	2799.5	169.35	21.13	30.14	171
100	0.124282	7 99	0.0011	2044.5	2859.8	169.95	21.10	30.07	173
102	0.121706	817	0.0010	2087.3	2919.8	170.55	21.08	30.01	175
104	0.119240	835	0.0010	2130.0	2979.8	171.13	21.05	29.96	177
108	0.114610	870	0.0010	2215.3	3099.4	172.26	21.03	29.86	180
110	0.112432	888	0.0009	2257.9	3159.1	172.81	21.02	29.82	182
112	U+11U339 0+108326	905	0.0009	2300.4	3218.7	173.34	21.01	29.78	184
116	0.106387	940	0.0009	2385.3	3337.7	174.39	20.99	29.71	187
118 120	0.104518 0.102716	958 975	0.0009	2427.6 2470.0	3397 <b>.1</b> 3456.4	174.90 175.39	20.98 20.97	29.68 29.66	189 191
122	0.100977	993	0.0008	2512.3	3515.7	175.88	20.97	29.63	192
124	0.0992975	1010	0.0008	2554.5	3575.0	176.37	20.96	29.61	194
128	0.0961049	1044	0.0008	2639.0	3693.3	177.31	20.95	29.59	195
130	0.0945863	1062	0.0008	2681.2	3752.5	177.76	20.95	29.56	199
132	0.0931159	1079	0.0008	2723.4	3811.6	178.22	20.95	29.55	200
136	0.0903111	1113	0.0008	2807.8	3929.7	179.10	20.95	29.53	202
138	0.0889724	1130	0.0007	2849.9	3988.8	179.53	20.95	29.52	205
140	0.0876736	1147	0.0007	2892.1	4047.8	179.95	20.96	29.51	206
142	0.0864128	1165	0.0007	2934.2	4106.8	180.37	20.96	29.51	208
146	0.0839989	1199	0.0007	3018.6	4224.8	181.19	20.97	29.50	211
148	0.0828426	1216	0.0007	3060.7	4283.8	181.59	20.98	29.50	212
150	0.0817182	1233	0,0007	3102.9	4342.8	181.99	20.98	29.50	214
154	0.0795598	1267	0.0007	3187.2	4460.8	182.76	21.00	29.50	215
156	0.0785234	1284	0.0007	3229.4	4519.8	183.14	21.01	29.50	218
158	0.0775141 0.0765307	1301 1318	0.0006	3271.6 3313.8	4578.8	183.52	21.02	29.51 29.51	219
165	0.0741792	1360	0.0006	3419.5	4785.4	184.80	21.06	29.53	224
170	0.0719695	1402	0.0006	3525.2	4933.1	185.68	21.10	29.55	227
180	0.0679263	1445	0.0006	3737.3	5229.0	187.37	21.18	29.62	234
185	0.0660719	1529	0.0006	3843.6	5377.1	188.19	21.23	29.66	237
190	0.0643168	1571	0.0005	3950.1	5525.6	188.98	21.28	29.70	240
200	0.0610741	1655	0.0005	4164.1	5823.1	190.50	21.34	29.81	246
205	0.0595732	1697	0.0005	4271.5	5972.3	191.24	21.47	29.87	249
210	0.0581447	1739	0.0005	4379.2	6121.8	191.95	21.53	29.93	252
220	0.0554849	1823	0.0005	4407.2	6421.8	192.67	21.60	30.07	255
225	0.0542447	1865	0.0005	4704.4	6572.3	194.03	21.75	30.14	261
230	0.0519243	1907	0.0004	4923-0	6874-4	194.70	21.83	30.21	264
240	0.0508373	1991	0.0004	5033.0	7026.1	195.98	22.00	30.37	269
245	0.0497951	2033	0.0004	5143.3	7178.1	196.61	22.08	30.45	272
250	0.0487949	2075	0.0004	5254.0 5365.2	7483-5	197.23	22.25	30.53	274
260	0.0469108	2158	0.0004	5476.8	7636.8	198.43	22.34	30.70	279
265 270	0.0460225	2200	0.0004 0.0004	5588.9 5701.4	7790.5	199.01 199.59	22.43	30.79	282 284
275	0.0443435	2284	0.0004	5814.3	8099.3	200.16	22.61	30.97	287
280	0.0435492	2325	0.0004	5927.7	8254.3	200.72	22.70	31.05	289
290	0.0420434	2409	0.0004	6155.8	8565.8	201.81	22.88	31.23	292
295	0.0413289	2451	0.0003	6270.5	8722.2	202.34	22.97	31.32	297
300	0.0406384	2492	0.0003	6385.7	8879.0	202.87	23.06	31.41	299

## 0.15 MN/m<sup>2</sup> ISDBAR

TEMPERATURE	DENSITY	ISOTHERM	I SOCHORE DERIVATIVE	INTERNAL	ENTHALPY	ENTROPY	Cv	Ср	VELOCITY OF SOUND
К К	MOL/L	J/MOL	MN/m <sup>2</sup> -K	J/MOL	J/MOL	J∕MOL-K	J / MC	)L - K	M/S
* 53,496	44,8805	268.02	4.3109	-6030.0	-6026.7	60.83	36.50	54.92	1030
54	44.7979	26760	4.3106	-6002.2	-5998.8	61.35	36.42	55.10	1032
56	44.4707	26321	4.3009	-5891.4	-5888.1	63.37	36.07	55.97	1037
58 60	43.8308	25762	4.1283	-5670.8	-5667.4	67.17	35.70	55.98	1035
62	43.5070	25554	4.0605	-5559.9	-5556.4	68.99	34.93	56.06	1039
66	42.8386	23678	3.8263	-5335.0	-5331.5	72.51	34.09	56.33	1015
68	42.5181	22813	3.6399	-5224.6	-5221.0	74.15	33.70	55.54	995
70	42.1879	21617	3.5196	-5112.9	-5109.4	75.77	33.29	55.83	977
74	41.4992	20157	3.3361	-4990.0	-4999.2	78.92	32.48	56.20	958
76	41.1522	19206	3.1965	-4772.8	-4769.2	80.43	32.08	55.95	939
78 80	40.8012 40.4457	17992 17117	3.0800 2.9794	-4659.1 -4544.9	-4655.4 -4541.2	81.90 83.35	31.69 31.32	56.40 56.68	918 903
82	40.0757	16317	2.8641	-4428.9	-4425.1	84.77	30.95	56.62	886
84	39.7203	15455	2.7493	-4315.2 -4199.6	-4311.4	86.14	30.63	56.78	868
88	38.9733	13639	2.5104	-4083.4	-4079.5	88.82	30.01	56.77	824
* 88.549	38.8689	13183	2.5124	-4051.3	-4047.5	89.18	29.93	57.99	820
* 88.549 90	0.208860	674	0.0018	1808.9	2527.1	163.28	21.50	31.28	161
92	0.203753	707	0.0018	1853.3	2589.5	163.96	21.44	31.11	164
94	0.198917	726	0.0017	1897.5	2651.6	164.63	21.39	30.96	166
96	0.194327	746	0.0017	1941.5	2713.4	105.20	21.34	30.82	168
100	0.185811	783	0.0016	2028.9	2836.2	166.53	21.27	30.59	172
102	0.181850	802 820	0.0016	2072.4	2897.2	167.14 167.73	21.23	30.49 30.40	174 176
106	0.174448	838	0.0015	2159.0	3018.9	168.31	21.17	30.32	178
108	0.170984	857	0.0015	2202.1	3079.4	168.87	21.15	30.25	180
110	0.167663	893	0.0014	2288.2	3139.8	169.43	21.13	30.10	183
114	0.161415	911	0.0014	2331.0	3260.3	170.50	21.09	30.06	185
116	0.158472	929	0.0013	2373.9	3320.4	171.03	21.07	30.01	187
120	0.152910	964	0.0013	2459.3	3440.3	172.04	21.05	29.92	190
122	0.150280	982	0.0013	2501.9	3500.1	172.54	21.04	29.89	192
126	0.145292	1017	0.0012	2587.1	3619.5	173.50	21.02	29.82	195
128	0.142925	1035	0.0012	2629.6	3679.1	173.97	21.01	29.79	196
130	0.138423	1052	0.0012	2672+1	3738.6	174.43	21.01	29.76	198
134	0.136280	1087	0.0011	2756.9	3857.6	175.33	21.00	29.72	201
136	0.134205	1105	0.0011	2799.3	3917.0	175.77	21.00	29.70	203
138	0.132193	1122	0.0011	2841.7 2884.1	3976.4 4035.8	176.21 176.63	21.00	29.68 29.67	204
142	0.128351	1157	0.0011	2926.4	4095.1	177.05	21.00	29.66	207
144	0.126515	1174	0.0011	2968.8	4154.4	177.47	21.00	29.65	209
146	0.122999	1209		3053.4	4273.0	178.28	21.00	29.63	210
150	0.121315	1226	0.0010	3095.8	4332.2	178.68	21.01	29.62	213
152	0.119678	1243	0.0010	3138.1	4391.5	179.07	21.02	29.62	215
156	0.116535	1260	0.0010	3222.8	4509.9	179.84	21.03	29.62	218
158	0.115026	1294	0.0010	3265.1	4569.2	180.22	21.04	29.62	219
160	0.113556	1312	0.0010	3307.5	4628.4	180.59	21.05	29.62	220
165	0.110043	1354	0.0009	3413.4	4776.5	181.50	21.08	29.63	224
175	0.103641	1440	0.0009	3625.6	5072.9	183.25	21.15	29.66	231
180	0.100716	1482	0.0008	3732.0	5221.3	184.08	21.20	29.69	234
185	0.0979527	1525	0.0008	3838.5	5369.9 5518.6	184.90	21.24	29.73	237
195	0.0928627	1609	0.0008	4052.3	5667.6	186.46	21.35	29.82	243
200	0.0905131	1652	0.0008	4159.5	5816.8	187.22	21.41	29.87	246
205 210	0.0882806 0.0861565	1694 1736	0.0007	4267.1 4375.0	5966.2 6116.0	187.96	21.48 21.54	29.92 29.98	249 252
215	0.0841331	1778	0.0007	4483.2	6266.0	189.38	21.61	30.04	255
220	0.0822034	1820	0.0007	4591.7	6567.2	190.08	21.69	30.11 30.18	258
230	0.0785996	1905	0.0007	4809.8	6718.2	191.42	21.84	30.25	263
235	0.0769145	1947	0.0006	4919.5	6869.7	192.07	21.92	30.33	266
240	0.0753006	1989	0.0006	5029.5	7021.5	192.71	22.00	30.41	269
250	0.0722690	2073	0.0006	5250.8	7326.4	193.95	22.17	30.57	274
255 260	0.0708434 0.0694733	2115 2156	0.0006 0.0006	5362.1 5473.8	7479.4 7632.9	194.56 195.16	22.26	30.65 30.73	277 279
265	0.0681555	2198	0.0006	5585.9	7786.8	195.74	22.44	30.82	282
270	0.0668870	2240	0.0006	5698.5	7941.1	196.32	22.53	30.91	284
280	0.0644872	2324	0.0005	5925.0	8251.0	197.45	22.71	31.08	289
285	0.0633510	2366	0.0005	6038.9	8406.6	198.00	22.80	31.17	292
290	0.0622544	2408	0.0005	6153.2	8562.7	198.54	22.89	31.26	294
300	0.0601716	2491	0.0005	6383.3	8876.2	199.60	23.07	31.44	299

## TABLE 16. THERMOOYNAMIC PROPERTIES OF FLUORINE

## 0.2 MN/m<sup>2</sup> ISOBAR

TEMPERATURE	OENSITY	ISOTHERM	ISOCHORE	INTERNAL	ENTHALPY	ENTROPY	Cv	Cp	VELOCITY
(IPTS 1968) K	MOL/L	J/MOL	MN/m <sup>2</sup> -K	ENERGY J/MOL	J/MOL	J/MOL-K	J / MC	ы - к	OF SOUNO M/S
	11 004C	04 0 0 7			6 A A C	6 A A 7	36 50	51 00	10.70
* 53.501 54	44.8815	26780	4.3112	-6003.5	-5999.0	50.83 61.35	36.41	55.09	1030
56	44.4726	26334	4.3016	-5892.8	-5888.3	63.36	36.07	55.96	1037
58 60	44.1482 43.8327	25985 25771	4.2071 4.1286	-5782.0 -5672.2	-5777.5 -5667.7	65.31 67.17	35.70 35.32	55.97 55.97	1035 1037
62	43.5089	25552	4.0602	-5561.3	-5556.7	68.99	34.93	56.06	1039
64	43.1754	24822	3.9681	-5449.0	-5444.3	70.77	34.52	56.30	1032
68	42.5203	22815	3.6409	-5226.1	-5221.3	74.15	33.70	55.55	995
70	42.1902	216 22	3.5201	-5114.5	-5109.7	75.77	33.29	55.83	977
72	41.8410	20427	3.4158	-5000.4	-4995.6	77.37	32.87	56.37 56.21	960
76	41.1548	19202	3.1970	-4774.4	-4769.6	80.42	32.08	55.97	939
78	40.8040	17992	3.0802	-4660.7	-4655.8	81.90	31.70	56.40	918
80	40.4486	17117	2.9797	-4546.6	-4541.6	83.34	31.33	56.69	903
82 84	40.0788 39.7236	16313 15459	2.8645	-4430.6 -4316.9	-4425.6 -4311.9	84.77 86.13	30.95 30.63	56.63 56.67	886 868
86	39.3532	14503	2.6294	-4201.4	-4196.3	87.49	30.31	56.78	846
88	38.9770	13644	2.5107	-4085.2	-4080.0	88.81	30.01	56.77	824
* 91.405	38.3217	12196	2.3751	-3885.7	-3880.5	91.02	29.55	58.34	796
* 91.405	0.277595	681	0.0024	1819.6	2540.1	161.14	21.73	32.01	162
92	0.275490	687	0.0024	1833.1	2559.1	161.35	21.71	31.94	163
96	0.262240	727	0.0023	1923.3	2686.0	162.70	21.55	31.51	167
98	0.256144	747	0.0022	1968.0	2748.8	163.34	21.50	31.33	169
100	0.250358	766	0.0022	2012.4	2811.3	163.97	21.45	31.17	171
102	0.244856	786	0.0021	2056.7	2873.5	164.59	21.40	31.02	173
104	0.234617	824	0.0020	2144.6	2935.4	165.78	21.35	30.77	175
108	0.229841	842	0.0020	2188.3	3058.5	166.35	21.28	30.67	179
110	0.225272	861	0.0019	2231.9	3119.7	166.91	21.25	30.57	181
114	0.216698	898	0.0019	2318.7	3241.7	168.00	21.19	30.49	184
116	0.212668	916	0.0018	2302.0	3302.4	168.53	21.17	30.33	186
118 120	0.208796 0.205071	935 953	0.0018	2405 <b>.1</b> 2448.2	3363•0 3423•5	169.05 169.56	21.15 21.13	30.27 30.21	188 189
122	0.201484	971	0.0017	2491.2	3483.8	170.06	21.11	30.15	191
124	0.198027	989	0.0017	2534.1	3544.1	170.55	21.10	30.10	193
120	0.194694	1007	0.0016	2577.0	3664.3	171.03	21.09	30.02	194
130	0.188368	1043	0.0016	2662.6	3724.3	171.97	21.07	29.98	198
132	0.185364	1060	0.0016	2705.3	3784.3	172.42	21.06	29.94	199
134	0.182459	1078	0.0015	2748.0	3844+1	172.87	21.05	29.91	201
138	0.176924	1114	0.0015	2833.2	3963.7	173.75	21.04	29.86	204
140	0.174285	1131	0.0015	2875.8	4023.4	174.18	21.04	29.84	205
142	0.171726	1149	0.0014	2918.4	4083.0	174.61	21.04	29.82	207
144	0.169245	1166	0.0014	2960.9	4142.6	175.02	21.04	29.80	209
148	0.164497	1201	0.0014	3045.9	4261.8	175.84	21.04	29.77	211
150	0.162225	1219	0.0014	3088.4	4321.3	176.24	21.05	29.76	213
152	0.160016	1236	0.0013	3130.9	4380.8	176.63	21.05	29.75	214
156	0.155780	1271	0.0013	3215.9	4499.8	177.40	21.06	29.73	217
158	0.153747	1288	0.0013	3258.4	4559.2	177.78	21.07	29.73	219
160	U.151768	1305	0.0013	3300.9	4618.7	178.10	21.08	29.73	220
165	0.147041	1349	0.0012	3407.1	4767.3	179.07	21.10	29.73	224
175	0.138435	1434	0.0012	3619.9	5064.6	180.82	21.17	29.75	230
180	0.134506	1477	0.0011	3726.5	5213.4	181.66	21.21	29.77	234
185	0.127291	1520	0.0011	3833+3	5362.4	182.48	21.31	29.80	237
195	0.123971	1605	0.0010	4047.4	5660.7	184.05	21.36	29.88	243
200	0.120821	1648	0.0010	4154.9	5810.2	184.80	21.42	29.92	246
205	0.117830 0.114985	1690 1733	0.0010	4262.6 4370.6	5960.0 6110.0	185.54 186.27	21.49 21.55	29.98 30.03	249 252
215	0.112276	1775	0.0009	4479.0	6260.3	186.97	21.62	30.09	255
220	0.109693	1817	0.0009	4587.6	6410.9	187.67	21.69	30.16	258
229	0.10/22/	1902	0.0009	4806.1	6713.2	189.01	21.85	30.29	261
235	0.102616	1944	0.0009	4915.8	6864.8	189.66	21.93	30.37	266
240	0.100458	1986	0.0008	5026.0	7016.8	190.30	22.01	30.44	269
245	0.0983894	2028	0.0008	5247.5	7322.1	190.93	22.18	30.52	274
255	0.0944994	2113	0.0008	5358.8	7475.3	192.15	22.27	30.68	277
260	0.0926684	2155	0.0008	5470.6	7628.9	192.75	22.35	30.77	279
265 270	0.0909074	2197 2239	0.0008	5582.9 5695.5	7782.9 7937.4	193.34 193.92	22.44	30.85	282 284
275	0.0875803	2281	0.0007	5808.6	8092.3	194.48	22.62	31.02	287
280	0.0860069	2323	0.0007	5922.2	8247.6	195-04	22.71	31.11	289
285	0.0844895	2365	0.0007	6150.6	8403.3	195.59	22.81	31.20	292
295	0.0816107	2449	0.0007	6265.5	8716.2	196.67	22.99	31.37	297
300	0.0802440	2491	0.0007	6380.8	8873.2	197.20	23.08	31.46	299

## 0.3 MN/m<sup>2</sup> ISOBAR

TEMPERATURE	OENSITY	ISOTHERM	ISOCHORE	INTERNAL	ENTHALPY	ENTROPY	Cv	Сp	VELOCITY
(1P35 1968) K	MOL/L	J/MOL	MN/m <sup>2</sup> -K	J/MOL	J/MOL	J/MOL-K	J / MC	DL - К	M/S
€ 53.510	44.8836	26865	4.3116	=6033.2	÷6026.5	60.84	36.50	54.88	1031
54	44.8035	26820	4.3113	-6006.1	-5999.5	61.34	36.41	55.06	1033
56	44.4764	26361	4.3031	-5895.5	-5888.7	63.35	36.06	55.95 55.96	1037
60	43.8366	25787	4.1292	-5675.0	-5668.2	67.16	35.32	55.96	1037
62	43.5128	25548	4.0597	-5564.1	-5557.2	68.98	34.94	56.06	1039
64 66	43.1794	24800 23656	3.9676	-5451.8	-5444.9	70.76	34.53	56.31 56.38	1032
68	42.5247	22819	3.6428	-5229.0	-5221.9	74.14	33.70	55.57	995
70 72	42.1949	21631	3.5211	-5117.5	-5110.3	75.76	33.29	55.83 56.37	977
74	41.5066	20134	3.3358	-4890.9	-4883.7	78.90	32.49	56.23	958
76	41.1600	19194	3.1979	-4777.6	-4770.3	80.41	32.09	55.99	939
80	40.4544	17119	2.9802	-4549.9	-4542.5	83.33	31.34	56.70	903
82	40.0849	16304	2.8653	-4434.0	-4426.5	84.76	30.96	56.66	886
84 86	39.7300 39.3601	15465	2.7510	-4320.4	-4312.8	86.12	30.64	56.79	868 846
88	38.9843	13655	2.5115	-4088+8	-4081.1	88.80	30.01	56.76	824
90	38.6024	12629	2.4431	-3972.1	-3964.3	90.11	29.75	58.30	807
94	37.8170	11454	2.2641	-3736.0	-3728.1	92.65	29.25	58.67	778
+ 95.782	37.4571	10686	2.1705	-3629.6	-3621.6	93.76	29.06	59.15	757
* 95.782 96	0.404713	688	0.0036	1879.8	2621+0	128.84	22.07	33.14	165
98	0.393451	710	0.0035	1931.6	2694.1	159.59	21.94	32.76	167
100	0.383921	7 31	0.0034	1977.9	2759.3	160.25	21.85	32.47	169
102	0.374922	752	0.0033	2023.9	2824.0	160.89	21.58	32.21	171
106	0.358320	793	0.0031	2114.7	2952.0	162.12	21.62	31.78	175
108	0.350636	813	0.0030	2159.7	3015.3	162.71	21.56	31.59	177
110	0.336335	833	0.0029	2204.5	3078.3	163.29	21.50	31.43	179
114	0.329664	872	0.0028	2293.4	3203.5	164.41	21.41	31.14	183
116	0.323281	892	0.0028	2337.6	3265.6	164.95	21.37	31.02	185
120	0.311298	930	0.0027	2425.6	3389.3	166.00	21.30	30.81	188
122	0.305664	949	0.0026	2469.3	3450.8	166.50	21.27	30.72	190
124	0.295035	986	0.0025	2556.5	3573.4	167.49	21.22	30.04	192
128	0.290015	1005	0.0025	2600.0	3634.4	167.97	21.20	30.49	195
130	0.285175 0.280504	1023	0.0024	2643.3	3695.3	168.45	21.19	30.43	197
134	0.275995	1060	0.0023	2729.8	3816.8	169.37	21.16	30.32	200
136	0.271637	1078	0.0023	2773.0	3877.4	169.81	21.15	30.27	202
140	0.263345	1115	0.0022	2859.1	3998.3	170.69	21.13	30.18	205
142	0.259396	1133	0.0022	2902.1	4058.6	171.12	21.12	30.15	206
144	0.255570	1151	0.0022	2945.0	4118.9	171.54	21.12	30.11	208
148	0.248263	1186	0.0021	3030.8	4239.2	172.36	21.11	30.06	211
150	0.244772	1204	0.0021	3073.6	4299.3	172.77	21.11	30.03	212
154	0.238087	1240	0.0020	3159.3	4419.3	173.56	21.11	29.99	214
156	0.234886	1258	0.0020	3202.1	4479.3	173.94	21.12	29.98	217
158	0.231773	1293	0.0020	3287.6	4539.2 4599.1	174.33	21.12	29.95	218
165	0.221519	1337	0.0019	3394.5	4748.8	175.62	21.15	29.93	223
170	0.208397	1381	0.0018	3501.5	4898.4	176.52	21.17	29.92	227
180	0.202418	1468	0.0017	3715.6	5197.6	178.23	21.24	29.93	233
185	0.196781	1511	0.0017	3822.8	5347.3	179.05	21.29	29.95	237
195	0.186419	1597	0.0016	4037.8	5647.0	180.63	21.39	30.00	243
200	0.181645	1640	0.0015	4145.6	5797.1	181.39	21.44	36.04	246
205	0.17/114	1683	0.0015	4362.0	5947.5 6098.0	182.85	21.51 21.57	30.14	249
215	0.168709	1769	0.0014	4470.6	6248.8	183.56	21.64	30.19	255
220	0.164804	1812	0.0014	4579.6 4688.8	6399.9 6551.3	184.26	21.71	30.25	258
230	0.157519	18 97	0.0013	4798.5	6703.0	185.61	21.86	30.38	263
235	0.154116	1939	0.0013	4908.5	6855.1	186.26	21.94	30.45	266
240	0.150859	2024	0.0013	5129.6	7160.2	187.53	22.02	30.59	269
250	0.144746	2067	0.0012	5240.8	7313.4	188.15	22.19	30.67	274
255 260	0.141874 0.139114	2109 2151	0.0012	5352.4 5464.4	7466.9 7620.9	188.76 189.36	22.28 22.37	30.75 30.83	277 279
265	0.136461	2194	0.0011	5576.8	7775.2	189.94	22.46	30.91	282
270	0.133909	2236	0.0011	5689.6	7930.0	190.52	22.55	30.99	284
280	0.129082	2320	0.0011	5916.6	8240.7	191.65	22.73	31.16	289
285	0.126798	2362	0.0011	6030.8	8396.8	192.20	22.82	31.25	292
290	0.124595 0.122467	2405	0.0010	6145.4 6260.5	8553.2 8710.1	192.75	22.91	31.33 31.42	294
300	0.120411	2489	0.0010	6375.9	8867.4	193.81	23.09	31.51	299

#### 0.4 MN/m² ISOBAR

TEMPERATURE (IPTS 1968)	DENSITY	ISOTHERM OERIVATIVE	ISOCHORE OERIVATIVE	INTERNAL ENERGY	ENTHALPY	ENTROPY	Cv	Cp	VELOCITY OF SOUND
К	MOL/L	J/MOL	MN/m <sup>2</sup> ~ K	J/MOL	J/MOL	J/MOL-K	J / MC	)L - К	M/S
* 53.520	44.8857	26907	4.3121	-6035.3	-6026.4	60.84	36.49	54.85	1032
56	44.4801	26387	4.3046	-5898.2	-5889.2	63.35	36.06	55.94	1034
58	44.1559	26020	4.2101	-5787.5	-5778.5	65.29	35.69	55.96	1036
60	43.8405	25804	4.1298	-5677.8	-5668.7	67.15	35.32	55.95	1037
62	43.5167	25544	4.0592	-5566.9	-5557.7	68.97	34.95	56.07	1039
66	42.8492	23642	3.8291	-5342.3	-5333.0	72.48	34.11	56.41	1014
68	42.5290	22824	3.6447	-5232.0	-5222.5	74.13	33.70	55.59	995
70	42.1995	21641	3.5221	-5120.5	-5111.0	75.75	33.30	55.83	977
72	41.8508	20423	3.4163	-5006.5	-4997.0	77.35	32.89	56.38	960
76	41.1652	19186	3.1988	-4780.8	-4771.1	80.40	32.10	56.02	939
78	40.8151	17993	3.0811	-4607.2	-4657.4	81.88	31.72	56.42	918
80	40.4603	17120	2.9808	-4553.2	-4543.3	83.32	31.35	56.71	903
8 2 84	40.0911	16296	2.8661	-4437.3	-4427.4	84.75	30.97	56.69 56.69	886 868
86	39.3670	14524	2.6324	-4208.4	-4198.3	87.46	30.32	56.80	846
88	38.9916	13665	2.5123	-4092.4	-4082.2	88.79	30.02	56.76	825
90	38.6103	12650	2.4432	-3975.8	-3965.5	90.09	29.77	58.26	807
94	37.8257	11466	2.2647	-3739.9	-3729.4	92.64	29.27	58.66	778
96	37.4220	10639	2.1670	-3620.6	-3610.0	93.88	29.05	59.31	756
98	37.0092	10020	2.0803	-3500.2	-3489.4	95.11	28.85	59.76	7 3 9
* 99.107	0.529979	5545	2.0178	-3429.4	-3410.5	95.82 157.19	22.37	34.22	166
100	0.524224	694	0.0047	1941.1	2704.1	157.47	22.31	34.03	167
102	0.511035	717	0.0046	1989.0	2771.7	158.14	22.18	33.61	169
104	0.498641	740	0.0044	2036+4	2838.6	158.79	22.06	33.24	171
108	0.475917	783	0.0042	2129.8	2970.3	160.04	21.87	32.64	175
110	0.465454	8 0 4	0.0041	2176.0	3035.3	160.63	21.78	32.39	177
112	0.455519	825	0.0040	2221.8	3099.9	161.21	21.71	32.16	179
114	0.437053	866	0.0038	2312.5	3227.7	162.33	21.58	31.78	183
118	0.428447	886	0.0037	2357.5	3291.1	162.88	21.53	31.61	185
120	0.420219	906	0.0036	2402.3	3354.2	163.41	21.48	31.46	187
122	0.412338	926	0.0036	2446.9	3417.0	163.93	21.44	31.33	189
126	0.397528	965	0.0034	2535.6	3541.8	164.93	21.37	31.09	192
128	0.390556	984	0.0034	2579.7	3603.9	155.42	21.34	30.99	194
130	0.383848	1004	0.0033	2623.7	3665.8	165.90	21.31	30.90	196
134	0.371162	1042	0.0032	2711.3	3789.0	166.83	21.29	30.81	197
136	0.365154	1060	0.0031	2755.0	3850.4	167.29	21.25	30.67	201
138	0.359354	1079	0.0031	2798.6	3911.7	167.74	21.23	30.60	202
140	0.353749	10.99	0.0050	2042.1	3972.9	100.10	21.22	30.94	204
142	0.348329	1116	0.0030	2885.5	4033.9	168.61	21.21	30.49	206
146	0.338005	1153	0.0029	2972.2	4155.6	169.46	21.19	30.39	209
148	0.333084	1172	0.0028	3015.5	4216.4	169.87	21.18	30.35	210
150	0.328312	1190	0.0028	3058.7	4277.0	170.28	21.18	30.32	212
154	0.319192	1226	0.0020	3145.0	4398.2	171.07	21.17	30.25	213
156	0.314829	1244	0.0027	3188.1	4458.7	171.46	21.17	36.22	216
158 160	0.310591 0.306470	1262 1280	0.0026	3231.2	4519.1 4579.5	171.85	21.17	30.20 30.18	218 219
165	0.296654	1325	0.0025	3381.9	4730.2	173.16	21.19	30.14	223
170	0.287474	1370	0.0024	3489.4	4880.8	174.05	21.21	30.11	226
175	0.278866	1414	0.0024	3596.9	5031.3	174.93	21.24	30.09	230
180	0.270778	1458	0.0023	3704.5	5332.2	175.60	21.27	30.09	233
190	0.255974	1546	0.0022	3920.0	5482.7	177.40	21.36	30.11	239
195	0.249180	1589	0.0021	4028.0	5633.3	178.18	21.41	30.13	243
200	0.242747	1633	0.0020	4136.2	5784.0	178.95	21.47	30.16	246
210	0.230852	1720	0.0019	4353.3	6086.0	180.42	21.59	30.24	252
215	0.225341	1763	0.0019	4462.2	6237.3	181.13	21.66	30.29	255
220	0.220092	1806	0.0019	4571.5	6388.9	181.83	21.73	30.34	258
230	0.210310	1892	0.0018	4790.9	6692.9	183.18	21.88	30.46	263
235	0.205743	1935	0.0017	4901.1	6845.3	183.84	21.96	30.52	266
240	0.201374	1977	0.0017	5011.8	6998.1	184.48	22.04	30.59	269
245	0.197190	2020	0.0017	5234.1	7304.7	185.73	22.21	30.74	274
255	0.189330	2105	0.0016	5345.9	7458.6	186.34	22.29	30.81	277
260	0.185634	2148	0.0016	5458.1	7612.9	186.94	22.38	30.89	279
265	0.182082	2190	0.0015	5570.7	7767.5	187.53	22.47	30.97	282
275	0.175375	2233	0.0015	5797.2	8078.0	188.68	22.65	31.13	287
280	0.172205	2318	0.0014	5911.1	8233.9	189.24	22.74	31.22	289
285	0.169150	2360	0.0014	6025.4	8390.2	189.79	22.83	31.30	292
295	0.165202	2402	0.0014	6255.4	8704-0	190.34	22.92	31.47	294
300	0.160608	2487	0.0013	6371.0	8861.6	191.41	23.11	31.55	299

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## 0.5 MN/m<sup>2</sup> ISOBAR

TEMPERATURE	OENSITY	ISOTHERM	ISOCHORE	INTERNAL	ENTHALPY	ENTROPY	Cv	Ср	VELOCITY
К К	MOL/L	J/MOL	MN/m <sup>2</sup> - K	J/MOL	J/MOL	J/MOL-K	J / MO	L <del>-</del> K	M/S
# 53 530	44 8878	269/8	1. 3126	-6037 /	-6026 2	50 8/	76 1.0	E/. 83	1032
54	44.8109	268.98	4.3122	-6011.5	-6000.3	61.32	36.41	55.00	1034
56	44.4839	26413	4.3061	-5900.9	-5889.7	63.34	36.06	55.93	1038
58	44.1598	26038	4.2116	-5790.3	-5779.0	65.28	35.69	55.95	1036
60	43.8444	25821	4.1304	-5680.6	-5669.2	67.14	35.32	55.95	1037
62 64	43.5207	25540	4.0587	-5569.7	-5558.2	68.96 70.75	34.95	56.07 56.35	1038
66	42.8534	23628	3.8301	-5345.2	-5333.6	72.48	34.12	56.43	1014
68	42.5334	22828	3.6466	-5234.9	-5223.1	74.12	33.71	55.60	996
70	42.2041	21651	3.5231	-5123.5	-5111.6	75.74	33.30	55.83	977
72	41.8557	20421	3.4165	-5009.6	-4997.6	77.34	32.89	56.39	960
74	41.5166	20104	3.3353	-4897.2	-4885.1	78.88	32.51	56.27	957
76	41.1705	19178	3.1998	-4783.9	-4771.8	80.39	32.11	56.04	939
80	40.4661	17122	2.9813	-4556.5	-4544.2	83.31	31.36	56.72	903
82	40.0972	16288	2.8669	-4440.7	-4428.3	84.74	30.98	56.72	886
84	39.7429	15479	2.7533	-4327.3	-4314.7	86.10	30.66	56.70	868
86	39.3738	14534	2.6338	-4212.0	-4199.3	87.45	30.33	56.81	846
88	38,9989	13676	2.5132	-4096.0	-4083.2	88.78	30.03	56.75	8 2 5
90	38.0182	12672	2.4433	-3979.6	- 3966.6	90.08	29.79	58.22	807
94	37.8344	11477	2.2653	-3763.9	-3730.7	92.62	29.29	58.65	7 7 8
96	37.4314	10657	2.1677	-3624.7	~3611.3	93.87	29.07	59.28	756
98	37.0192	10037	2.0808	-3504.4	-3490.9	95.09	28.88	59.73	739
100	36.5975	9311	1.9915	-3382.8	-3369.1	96.30	28.69	60.49	719
+ 101.969	36.1717	8759	1.8952	-3261.7	-3247.9	97.49	28.53	60.48	699
° 101.969	0.654419	680	0.0060	1951.1	2715.1	155.89	22.66	35.28	167
104	0.637109	705	0.0058	2001.4	2786.2	156.58	22.69	34.72	169
106	0.621175	729	0.0056	2050.2	2855.2	157.24	22.34	34.25	171
108	0.606217	752	0.0055	2098.4	2923.2	157.88	22.21	33.83	174
110	0.592129	775	0.0053	2146.1	2990.5	158.50	22.09	33.47	176
112	0.578821	797	0.0052	2193.3	3057.1	159.10	21.99	33.15	178
114	0.554255	819	0.0000	2240.1	3123.1	159.68	21.90	32:00	180
118	0.542876	861	0.0049	2332.6	3253.6	160.80	21.75	32.38	184
120	0.532031	882	0.0047	2378.3	3318.1	161.35	21.68	32.17	186
122	0.521679	903	0.0046	2423.8	3382.3	161.88	21.62	31.99	188
124	0.511780	923	0.0045	2469.1	3446.1	162.40	21.57	31.82	189
126	0.502302	944	0.0044	2514.1	3509.6	162.90	21.52	31.67	191
128	0.493214	964	0.0043	2559.0	357208	163.40	21.48	31.53	193
132	0.476105	1003	0.0041	2648.2	3698.4	164.37	21.41	31.29	196
134	0.468037	1023	0.0040	2692.5	3760.8	164.84	21.38	31.18	198
136	0.460267	1042	0.0040	2736.8	3823.1	165.30	21.35	31.09	200
138	0.452777	1062	0.0039	2730.9	3885.2	165.75	21.33	31.00	202
140	0.445550	1081	0.0038	2824.9	3947.1	166.20	21.31	30.92	203
142	0.438571	1100	0.0038	2868.8	4008.9	166.63	21.29	30.84	205
144	0.431827	1119	0.0037	2912.6	4070.5	167.07	21.28	36.78	206
146	0.425304	1138	0.0037	2956.3	4132.0	167.49	21.26	30.71	208
148	0.418991	1157	0.0036	3000.0	4193.3	167.91	21.25	30.66	210
152	0.412077	1196	0.0035	3043.0	42740	168.72	21.24	30.56	213
154	0.401206	1212	0.0034	3130.6	4376.8	169.12	21.23	30.52	214
156	0.395632	1231	0.0034	3174.0	4437.8	169.52	21.23	30.48	216
158	0.390221	1249	0.0033	3217.4	4498.8	169.90	21.23	30.44	217
160	0.384965	1268	0.0033	3260.8	4559.6	170.29	21.23	30.41	219
165	0.372459	1313	0.0032	3369.1	4711.5	171.22	21.24	30.35	222
170	0.360782	1359	0.0031	3411.2	4863.1	172.13	21.27	30.30	226
180	0.349050	1404	0.0029	3202+4	5165.8	173.86	21.31	30.25	223
185	0.329941	1493	0.0028	3801.6	5317.0	174.69	21.34	30.24	236
190	0.320845	1537	0.0027	3909.9	5468.3	175.49	21.39	30.25	239
195	0.312255	1581	0.0026	4018.3	5619.5	176.28	21.43	30.26	242
200	0.304129	1625	0.0026	4126.8	5770.9	177.04	21.49	30.28	246
205 210	0.296428 0.289119	1669 1713	0.0025 0.0024	4235.6 4344.6	5922.3 6074.0	177.79 178.52	21.55 21.61	30.31 30.34	249 252
215	0.282171	1757	0.0024	4453.8	6225.8	179.24	21.68	30.39	255
220	0.275558	1800	0.0023	4563.3	6377.8	179.94	21.75	30.43	257
225	0.269256	1843	0.0023	4673.2	6530.1	180.62	21.82	30.49	260
230	0.263243	1887	0.0022	4783.3	6682.7	181.29	21.89	30.54	263
235	0.257498	1930	0.0022	4893.8	6835.5	181.95	21.97	36.60	266
240	0.252004	1973	0.0021	5004+6	5908.7	182.59	22.05	30.67	269
250	0.240/49	2016	0.0021	5227-4	7296.1	183.85	22.22	30.81	271
255	0.236870	2102	0.0020	5339.4	7450.3	184.46	22.31	30.88	277
260	0.232228	2145	0.0020	5451.8	7604.9	185.06	22.40	30.95	279
265	0.227768	2187	0.0019	5564.6	7759.8	185.65	22.48	31.03	282
270	0.223479	2230	0.0019	5677.8	7915.2	186.23	22.57	31.11	284
275	0.219351	2273	0.0018	5791.5	8070.9	186.80	22.66	31.19	287
285	0.215375	2315	0.0018	5905.5	8387 6	187 02	22.05	31.27	289
290	0.207847	2350	0.0017	6135-0	8540.6	188-47	22.94	31-43	296
295	0.204280	2443	0.0017	6250.3	8698.0	189.00	23.03	31.52	297
300	0.200834	2485	0.0017	6366.1	8855.7	189.53	23.12	31,60	299

TABLE 16. THERMOOYNAMIC PROPERTIES OF FLUORINE

0.6 MN/m<sup>2</sup> ISOBAR

TEMPERATURE	DENSITY	ISOTHERM	ISOCHORE	INTERNAL	ENTHALPY	ENTROPY	Cv	Сp	VELOCITY
(IPTS 1968) K	MOL/L	OERIVATIVE J/MOL	0ERIVATIVE MN/m <sup>2</sup> - K	ENERGY J/MOL	J/MOL	J/MOL-K	J / MC	ч <b></b> к	OF SOUNO M/S
× 53 51 0		00000		(				51	
* 53.54U 54	44.8899	26990	4.3130	-6014.1	-6026.1	60.84	36.48	54.80	1033
56	44.4877	26440	4.3076	-5903.6	-5890.1	63.33	36.06	55.92	1039
58	44.1636	26056	4.2131	-5793.0	-5779.4	65.27	35.69	55.95	1037
6 <b>U</b>	43.0402	22030	4.1311	-9003.4	-2003-1	67.13	35.32	22.34	1030
62 64	43.5246 43.1915	25537 24736	4.0582 3.9662	-5572.5	-5558.7	68.95 70.74	34.96 34.55	56.07 56.37	1038 1031
66	42.8576	23614	3.8312	-5348.1	-5334.1	72.47	34.13	56.46	1014
68	42.5378	22832	3.6485	-5237.8	-5223.7	74.11	33.71	55.62	996
70	42.2087	21661	3.5241	-5126.5	-5112.3	75.73	33.31	55.83	978
74	41.5216	20419	3.3350	-4900.3	-4885.9	78.88	32.52	56.29	960
76	41.1757	19171	3.2007	-4787.1	-4772.5	80.38	32.12	56.07	939
78	40.8262	17995	3.0820	-4673.7	-4659.0	81.86	31.73	56.43	918
80	40.4720	17124	2.9819	-4559.8	-4545.0	83.30	31.37	56.73	903
82	40.1034	16281	2.8676	-4444.1	-4429.2	84.72	30.99	56.75	886
86	39.3807	14544	2.6353	-4215.5	-4200.3	87.44	30.34	56.82	847
88	39.0062	13687	2.5149	-4099.7	-4084.3	88.77	30.03	56.76	825
90	38.6261	12693	2.4435	-3983.3	-3967.8	90.07	29.80	58.18	808
92	38.2383	12074	2.3598	-3866.0	-3850.3	91.35	29.56	58.58	794
94	37.6431	11489	2.1684	-3628.8	= 3612.7	92.61	29.09	50.04	756
98	37.0292	10054	2.0814	-3508.5	-3492.3	95.08	28.90	59.70	739
100	36.6082	9331	1.9924	-3387.1	-3370.7	96.29	28.71	60.46	719
102	36.1763	8768	1.9080	-3264.3	-3247.7	97.49	28.55	60.91	702
104	35.7328	8208	1.8169	-3139.8	-3123.0	98.68	28.39	61.15	682
* 104.383	0.778634	673	0.0072	1973.9	2744.5	154.82	22.93	36.33	168
106	0.761762	694	0.0070	2015.2	2802.8	155.38	22.77	35.79	169
108	0.742184	719	0.0068	2065.4	2873.8	156.04	22.59	35.21	172
110	0.723874	744	0.0066	2114.8	2943.7	156.68	22.44	34.70	174
114	0.690496	791	0.0062	2211.8	3080.8	157.91	22.18	33.87	178
116	0.675201	813	0.0061	2259.5	3148.1	158.49	22.07	33.52	180
118	0.660715	836	0.0059	2306.8	3214.9	159.06	21.98	33.22	182
120	0.646963	858	0.0058	2353.6	3281.0	159.62	21.89	32.94	184
122	0.633879	880	0.0056	2400.1	3346.7	160.16	21.81	32.70	186
126	0.609501	922	0.0054	2492.2	3476.6	161.21	21.68	32.28	190
128	0.598113	943	0.0053	2537.8	3541.0	161.72	21.63	32.10	192
130	0.587207	963	0.0051	2583.2	3605.0	162.21	21.58	31.93	194
132	0.576747	984	0.0050	2628.4	3668.7	162.70	21.54	31.78	195
134	0.557048	1024	0.0049	2718.2	3795.3	163.64	21.50	31.53	197
138	0.547756	1044	0.0048	2762.9	3858.3	164.10	21.43	31.41	201
140	0.538805	1064	0.0047	2807.4	3921.0	164.55	21.40	31.31	202
142	0.530174	1083	0.0046	2851.8	3983.5	165.00	21.38	31.21	204
144	0.521844	1103	0.0045	2896.1	4045.8	165.43	21.36	31.13	206
146	0.513798	1122	0.0044	2940.2	4100.0	165.28	21.34	30.98	207
150	0.498496	1161	0.0043	3028.3	4231.9	166.70	21.31	30.91	210
152	0.491212	1180	0.0042	3072.2	4293.7	167.11	21.30	30.85	212
154	0.484156	1199	0.0042	3116.0	4355.3	167.51	21.29	30.79	214
158	0.470682	1218	0.0041	3203.5	4410.0	167.91	21.29	30.74	215
160	0.464244	1255	0.0040	3247.2	4539.6	168.69	21.28	30.65	218
165	0.448946	1302	0.0038	3356.2	4692.7	169.63	21.28	30.56	222
170	0.434686	1348	0.0037	3465.0	4845.3	170.54	21.29	30.50	225
175	0.421357	1393	0.0036	3573.7	4997.7	171.42	21.31	30.45	229
185	0.397127	1484	0.0034	3791.0	5301.8	173.11	21.37	30.39	236
190	0.386076	1529	0.0033	3899.7	5453.8	173.92	21.41	30.39	239
195	0.375649	1573	0.0032	4008.5	5605.7	174.71	21.46	30.39	242
200	0.365793	1618	0.0031	4117.4	5757.7	175.48	21.51	30.40	245
210	0.347609	1706	0.0029	4335.8	6061.9	176.23	21.57	30.42	248
215	0.339201	1750	0.0029	4445.4	6214.2	177.68	21.69	30.49	254
220	0.331203	1794	0.0028	4555.2	6366.8	178.38	21.76	30.53	257
225	0.323585	1838	0.0027	4665.3	6519.5	179.07	21.83	30.57	260
230	0.316319	1882	0.0027	4//5.7	6825 8	179.74	21.91	30.68	263
240	0.302749	1968	0.0026	4997.5	6979.3	181.05	22.07	30.74	269
245	0.296402	2012	0.0025	5108.9	7133.2	181.68	22.15	30.81	271
250	0.290321	2055	0.0024	5220.7	7287.4	182.31	22.24	30.87	274
255	0.284491 0.278896	2098 2141	0.0024	5332.9 5445.5	7442.0	182.92	22.32	30.94 31.02	277 279
265	0.273521	2184	0.0023	5558.5	7752.1	184.11	22,50	31.09	282
270	0.268353	22 27	0.0023	5671.9	7907.8	184.69	22.59	31.17	284
275	0.263380	2270	0.0022	5785.7	8063.8	185.27	22.68	31.24	287
280	0.258592	2313	0.0022	5900.0	8220.2	185.83	22.77	31.32	289
205	0.249529	2355	0.0021	6129.7	8574.3	186.93	22.95	31-40	292
295	0.245236	2441	0.0021	6245.3	8691.9	187.47	23.04	31.57	297
300	0.241090	2483	0.0020	6361.2	8849.9	188.00	23.14	31.65	299

#### 0.7 MN/m<sup>2</sup> ISOBAR

TEMPERATURE	DENSITY	ISOTHERM	ISOCHORE	INTERNAL	ENTHALPY	ENTROPY	Cv	Cp	VELOCITY
(IPTS 1968) K	MOL/L	DERIVATIVE J/MOL	DERIVATIVE MN/m <sup>2</sup> -K	ENERGY J/MOL	J/MOL	J/MOL-K	J / M0	с – к	OF SOUND M/S
* 53.550	44.8920	27031	4.3135	-6841.6	-6026.0	60.85	36.48	54.77	1033
56	44.8184 44.4915	26977 26466	4.3132 4.3091	-6016.8	-6001.2	61.31 63.32	36.41 36.06	54.94 55.91	1035
58	44.1674	26074	4.2145	-5795.8	-5779.9	65.26	35.69	55.94	1037
60	43.8521	25855	4.1318	-5686.2	÷5670.2	67.13	35.33	55.93	1038
62	43.5285	25533	4.0578	-5575.3	-5559.3	68.95	34.97	56.07	1038
66	42.8619	23601	3.8322	-5351.0	-5334.7	70.73	34.50	56.49	1014
68	42.5422	22837	3.6504	-5240.8	-5224.3	74.11	33.72	55.64	996
72	41.8655	20418	3.4171	-5015.7	-4999.0	77.33	32.91	56.40	960
74	41.5265	20075	3.3348	-4903.4	-4886.6	78.87	32.53	56.31	956
78	40.8318	17997	3.0825	-4676.9	-4659.8	81.85	31.74	56.44	918
80	40.4778	17126	2.9824	-4563.2	-4545.9	83.29	31.38	56.74	903
82	40.1095	16273	2.8684	-4447.5	-4430.1	84.71	31.00	56.77	886
84 86	39.7559 39.3876	15493 14555	2.7555	-4334.2	-4316.6	86.08 87.43	30.68 30.35	56.82	868
88	39.0136	13697	2.5168	-4103.3	-4085.3	88.75	30.04	56.77	825
90	38.634U 38.2466	12714 12090	2.4438 2.3601	-3987.1 -3869.9	-3969.U -3851.6	90.05 91.33	29.82 29.58	58.14 58.55	8U8 794
94	37.8518	11501	2.2666	-3751.7	-3733.2	92.60	29.33	58.64	778
96	37.4501 37.0391	10693	2.1691 2.0820	-3632.8	-3614.1 -3493.8	93.84 95.06	29+11 28+92	59.23 59.67	739
100	36.6189	9351	1.9934	-3391.4	-3372.3	96.27	28.73	60.42	719
102	36.1877	8786	1.9089	-3268.7	-3249.4	97.47	28.57	60.87	702
104	35.7449	8224	1.8183	-3144.4	-3124+8	98.66	28.41	61.14	682
* 106.518	35.1688	7265	1.7038	-2985.4	-2965.5	100.14	28.24	62.65	651
* 106.518	0.903026	665	0.0085	1991.6	2766.7	153.90	23.19	37.39	168
110	0.861338	711	0.0080	2081.9	2894.6	155.09	22.82	36.11	172
112	0.839642	737	0.0077	2132.5	2966.2	155.73	22.64	35.52	174
116	0.880254	786	0.0073	2231.5	3106.2	156.96	22.35	34.54	179
118 120	0.782270 0.765269	810 833	0.0071 0.0069	2280.1 2328.1	3174.9 3242.8	157.55	22.22	34.14 33.79	181 183
4.2.2	0.71.045.7	0.55	0.0007	077.57	7740 4	150 (7	00.00		
124	0.733853	878	0.0066	2422.9	3310.1	158.67	22.02	33.47	185
126	0.719284	900	0.0064	2469.7	3442.9	159.74	21.86	32.94	189
130	0.692118	922	0.0061	2562.3	3573.7	160.26	21.79	32.50	191
132	0.679419	964	0.0060	2608.2	3638.5	161.26	21.67	32.31	195
134	0.655576	1006	0.0058	2699.3	3767.1	162.22	21.58	31.99	198
138	0.644361	1026	0.0056	2744.6	3830.9	162.69	21.54	31.85	200
140	0.000011	1047	0.00000	210,00	00,40,	103.14	21.50	-	
142	0.623191 0.613183	1067	0.0054	2834.6 2879.3	3957.8 4020.9	163.59	21.47	31.60 31.49	203
146	0.603529	1107	0.0052	2923.9	4083.8	164.47	21.42	31.39	207
148	0.594209	1126	0.0052	2968.4 3012.8	4146.5	164.89	21.40	31.30	208
152	0.576495	1165	0.0050	3057.1	4271.4	165.73	21.37	31.14	211
154	0.559906	1185	0.0048	3101+3	4395.7	166.53	21.36	31.08 31.01	213
158	0.551997	1223	0.0048	3189.5	4457.6	166.93	21.34	30.95	216
100	0.544320	1242	0.0047	3233.5	4019.0	107.32	21.33	20.90	210
165	0.526130	1290	0.0045	3343.2	4673.7	168.27	21.33	30.79	221
175	0.493395	1383	0.0042	3562.0	4980.7	170.07	21.35	30.63	229
180	0.478603	1429	0.0041	3671.1 3780.3	5133.7 5286.5	170.94	21.37 21.40	30.58 30.55	232
190	0.451668	1520	0.0039	3889.4	5439.2	172.59	21.44	30.53	239
195	0.439363	1566 1611	0.0037	3998.6 4107.9	5591.8 5744.4	173.38	21.48 21.53	30.52 30.52	242
205	0.416746	1655	0.0035	4217.4	5897.1	174.91	21.59	30.54	248
210	0.406325	1700	0.0035	4327 • U	6049.8	1/5.64	21.65	30.56	251
215	0.396432	1744	0.0034	4436.9	6202.7	176.36	21.71	30.59	254
225	0.378073	18 33	0.0032	4657.4	6508.9	177.75	21.85	30.66	260
230	0.369538	1877	0.0031	4768.1	6662.3	178.43	21.93	30.71	263
240	0.353607	1964	0.0030	4990.4	6970.0	179.74	22.08	30.82	269
245	0.346161	2008	0.0029	5102.0	7124.2	180.37	22.17	30.88	271
255	0.332195	2094	0.0028	5326.4	7433.6	181.61	22.34	31.01	277
260	0.325637	2138	0.0027	5439.2	7588.9	182.21	22.42	31.08	279
265	0.319339	2181	0.0027	5552.4	7744.4	182.81	22.51	31.15	282
270	0.313285	2224	0.0026	5780.0	7900.4 8056.7	183.39	22.60	31.23 31.30	284
280	0.301856	2310	0.0025	5894.4	8213.4	184.53	22.78	31.38	289
285	0.296455 0.291248	2353 2396	0.0025	6009.2 6124.5	8370.5 8527.9	185.08 185.63	22.87 22.97	31.46 31.53	292
295	0.286224	2439	0.0024	6240.2	8685.8	186.17	23.06	31.61	297
300	0.281374	2481	0.0024	6356.3	8844.1	186.70	23.15	31.69	299

## TABLE 16. THERMOOYNAMIC PROPERTIES OF FLUORINE

## 0.8 MN/m<sup>2</sup> ISOBAR

TEMPERATURE	OENSITY	ISOTHERM	ISOCHORE	INTERNAL	ENTHALPY	ENTROPY	Gv	Сp	VELOCITY
(IPTS 1968) K	MOL/L	OERIVATIVE J/MOL	OERIVATIVE MN/m <sup>2</sup> -K	ENERGY J/MOL	J/MOL	J/MOL-K	J / M0	L - K	OF SOUNO M/S
* 57 560	66 8064	27072	4 714.0	-601.77	-6025 0	60.05	76 / 9	54 <b>75</b>	1074
54	44.8221	27012	4.3136	-6019.4	-6001.6	61.30	36.40	54.92	1034
56	44.4953	26493	4.3106	-5909.0	-5891.0	63.31	36.06	55.89	1040
58 60	44.1713 43.8560	25091	4.2160 4.1326	-5798.5	-5780.4 -5670.7	65.26 67.12	35.69 35.33	55.94 55.92	1037
62	43.5324	25530	4.0574	-5578.2	-5559.8	68.94	34.98	56.07	1038
64	43.1996	24696	3.9653	-5466.1	-5447.6	70.72	34.57	56.40	1030
68	42.5466	228 41	3.6522	-5243.7	-5224.9	74.10	33.72	55.66	996
70	42.2179	21681	3.5261	-5132.5	-5113.5	75.71	33.31	55.84	978
72	41.8704	20415	3.4174	-5018.8 -4906.5	-4999.7	78.86	32.91	56.32	960
76	41.1861	19157	3.2025	-4793.5	-4774.0	80.37	32.13	56.12	938
78 80	40.8373 40.4836	17998 17128	3.0829 2.9830	-4680.2 -4566.5	-4660.6 -4546.7	81.84 83.28	31.75 31.39	56.45 56.75	918 903
82	40.1156	16266	2.8692	-4450.9	-4431.0	84.70	31.01	56.80	885
84	39.7623	15500	2.7566	-4337.7	-4317.6	86.06	30.68	56.73	868
86	39.3945	14566	2.5186	-4222.6	-4202.3	87.42	30.35	56.83	847
90	38.6418	127 35	2.4440	-3990.8	-3970.1	90.04	29.84	58.11	808
92	38.2548	12106	2.3604	-3873.7	-3852.8	91.32	29.60	58.53	794
94	37.4595	11513	2.2672	-3755.7	-3734.5	92.58	29.35	58.53	778
98	37.0490	10089	2.0826	-3516.9	-3495.3	95.05	28.95	59.64	740
100	36.6296	9372	1.9943	-3395.7	-3373.9	96.26	28.75	60.38	720
102	36.1991 35.7571	8804 8240	1.9097	-3273.1 -3149.0	-3251.0	97.45	28.60	60.84	702
106	35.3026	7515	1.7263	-3023.2	-3000.5	99.82	28.29	62.02	658
108	34.8330	6869	1.6421	-2895.3	-2872.3	100.99	28.17	63.12	636
✓ 108.440 ✓ 108.440	34.7275	656	1.0297	2005.2	2783.5	101.25	23.45	38.46	168
110	1.00532	678	0.0095	2047.1	2842.9	153.64	23.25	37.74	170
112	0.978328	705	0.0092	2099.8	2917.6	154.31	23.02	36.95	173
116	0.929838	758	0.0086	2202.3	3062.7	155.59	22.65	35.68	177
118	0.907891	783 807	0.0083	2252.4	3133.5	156.19	22.49	35.17	179
422	0 067760	9.74	0.0070	2750 5	7272 /	157 75	22.00	74.74	102
124	0.849322	854	0.0077	2398.8	3340.7	157.90	22.13	33.96	186
126	0.831830	877	0.0075	2446.6	3408.3	158.44	22.04	33.64	188
128	0.815199	900	0.0073	2493.9	3475.3	158.97	21.95	33.30	190
132	0.784233	944	0.0070	2587.6	3607.7	159.99	21.81	32.87	194
134	0.769777	966	0.0068	2634.0	3673.3	160.48	21.75	32.67	195
138	0.742665	1008	0.0066	2726.0	3803.2	161.44	21.65	32.40	197
140	0.729924	1029	0.0064	2771.6	3867.6	161.90	21.60	32.15	201
142	0.717678	1050	0.0063	2817.1	3931.8	162.36	21.57	32.00	203
144	0.705893	1071	0.0062	2862.3	3995.6	162.80	21.53	31.87	204
148	0.683597	1111	0.0060	2952.4	4122.7	163.67	21.48	31.64	208
150	0.673033	1131	0.0059	2997.2	4185.9	164.10	21.45	31.54	209
152	U.652966	1151	0.0058	3041.9	4248.8	164.93	21.43	31.45	211 212
156	0.643424	1191	0.0056	3131.0	4374.3	165.33	21.40	31.29	214
158 160	0.634185 0.625235	1210 1230	0.0055	3175.4 3219.7	4436.8 4499.2	165.73 166.12	21.39 21.38	31.22 31.15	216 217
165	0.604026	1278	0.0052	3330.1	4654.6	167-08	21.37	31.01	221
170	0.584328	1326	0.0050	3440.3	4809.4	168.00	21.37	30.90	225
175	0.565972	1373	0.0049	3550.2	4963.7	158.90	21.38	30.82	228
185	0.532734	1419	0.0046	3769.5	5271.2	170.60	21.40	30.79	235
190	0.517627	1512	0.0044	3879.1	5424.6	171.42	21.46	30.67	238
195	0.503401	1558	0.0043	3988.7	5577.9	172.22	21.51	30.65	242
205	0.477286	1648	0.0041	4208.3	5884.4	173.75	21.61	30.65	248
210	0.465266	1693	0.0040	4318.3	6037.7	174.49	21.67	30.66	251
215	0.453864	1738	0.0039	4428.4	6191.1	175.21	21.73	30.69	254
225	0.432722	1827	0.0037	4649.5	6498.2	176.61	21.87	30.75	260
230	0.422900	1871	0.0036	4760.4	6652.1	177.29	21.94	30.80	263
235	0.413530	1916	0.0035	4871.7	6806.2	177.95	22.02	30.84	266
245	0.396023	2003	0.0034	5095.1	7115.2	179.24	22.18	30.95	271
250	0.387830	2047	0.0033	5207.3	7270.1	179.86	22.26	31.01	274
260	0.372451	2134	0.0031	5432.9	7580.9	181.08	22.44	31.14	279
265	0.365222	2178	0.0031	5546.3	7736.7	181.67	22.53	31.21	282
270	0.358276	2221	0.0030	5660.1	7893.0	182.26	22.61	31.28	284
280	0.345166	2308	0.0029	5888.8	8206.6	183.40	22.80	31.43	289
285	0.338973	2351	0.0029	6003.8	8363.9	183.96	22.89	31.51	292
290	0.333003	2394	0.0028	6119.3	8521.6	184.50	22.98	31.58	294
300	0.321686	2480	0.0027	6351.4	8838.3	185.58	23.16	31.74	299

#### 0.9 MN/m<sup>2</sup> ISOBAR

TEMPERATURE	DENSITY	ISOTHERM	ISOCHDRE	INTERNAL	ENTHALPY	ENTROPY	Cv	Сp	VELOCITY
K	MOL/L	J/MOL	MN/m <sup>2</sup> =K	J/MOL	J/MOL	J∕MOL-K	J / MC	с – к	M/S
* 53.569	44.8962	27113	4 3144	-60/6 8	=6025 8	60.85	36.47	54.72	1.135
54	44.8258	27056	4.3141	-6022.1	-6002.0	61.29	36.40	54.89	1036
56	44.4990	26519	4.3121	-5911.7	-5691.5	63.30	36.05	55.88	1040
58 60	44.1751 43.8598	26109 25888	4.2175 4.1333	-5801.2 -5691.7	-5780.9 -5671.2	65.25 67.11	35.69 35.33	55.93 55.91	1038 1038
- 62	43.5363	25527	4.0570	=5581.0	= 5560.3	68.93	34.98	56.07	10.38
64	43.2037	24676	3.9649	-5469.0	-5448.2	70.71	34.58	56.42	1029
66	42.8704	23575	3.8343	-5356.9	-5335.9	72.44	34.15	56.55	1014
68	42.5509	22846	3.6540	-5246.7	-5225.5	74.09	33.72	55.67	996
70	42.2226	21691	3.5271	~5135.5	~5114.2	75.70	33.32	55.84	978
74	41.5365	200410	3.3345	-4909.7	-4888.0	78.85	32.55	56.34	956
76	41.1913	19150	3.2034	-4796.6	-4774.8	80.36	32.14	56.14	938
78	40.8429	18000	3.0834	-4683.4	-4661.4	81.83	31.76	56.46 56.76	918
	4.0 4.24.9	16260	2 8600	-64.54 7		94. 60	71 0.2	56 97	885
84	39.7688	15507	2.7577	-4341.1	-44318.5	86.05	30.69	56.74	869
86	39.4013	14576	2.6395	-4226.1	-4203.3	87.40	30.36	56.84	847
88	39.0281	13720	2.5205	-4110.5	-4087.5	88.73	30.05	56.80	826
90	38.6497	12756	2.4443	~3994.6	-3971.3	90.03	29.85	56.07	808
92	37.8692	11525	2.2678	-30/7.5	-3054+0	91.31	29.02	58.62	7 7 8
96	37.4688	10730	2.1706	-3640.9	-3616.9	93.81	29.14	59.17	757
98	37.1589	10107	2.0832	-3521.0	-3496.7	95.03	28.97	59.61	740
100	36.0405	5552	1. 3392	-3400.0	-337919	07.44	20.00	60.04	720
104	35.7692	8256	1.8212	-3153.6	-3128.4	98.62	28.45	61.11	683
106	35.3159	7538	1.7280	-3027.9	-3002.4	99.80	28.31	61.97	659
108	34.8475	6894	1.6436	-2900.3	-2874.4	100.97	28.19	63.04	637
110	34.3624	6294	1.5675	-2770.3	-2744.1	102.14	28.08	64.45	617
+ 110+194 + 110,194	1.15345	645	0.0111	2015.6	2795.9	152.37	23.69	39.55	168
112	1.12353	672	0.0107	2065.4	2866.4	153.00	23.43	38.60	171
114	1.09287	701	0.0103	2119.2	2942.7	153.68	23.19	37.72	173
116	1.06446	728	0.0100	2171.9	3017.4	154.33	22.97	36.96	176
120	1.01323	781	0.0094	2274.4	3162.7	155.56	22.62	35.73	180
122	0.989969	806	0.0091	2324.5	3233.6	156.15	22.47	35.24	182
124	0.968051	830	0.0088	2373.9	3303.6	156.72	22.34	34.80	184
126	0.947336	854	0.0086	2422.8	3372.8	157.27	22.23	34.41	187
128	0.927706	878	0.0082	24/1.2	3441.3	158.33	22.03	34.00	189
132	0.891313	924	0.0080	2566.6	3576.3	158.85	21.95	33.47	193
134	0.874388	946	0.0078	2613.7	3643.0	159.35	21.88	33.22	194
136	0.858219	968	0.0077	2660.5	3709.2	159.84	21.82	32.99	196
138	0.827922	1012	0.0073	2707.U 2753.3	3775.U 3840.3	160.32 160.79	21.76	32.60	198
142	0.813696	1033	0.0072	2799.3	3905.4	161.25	21.60	32.43	202
144	0.800028	1054	0.0071	2845.1	3970.1	161.70	21.62	32.27	203
146	0.786882	1075	0.0069	2890.7	4034.5	162.15	21.59	32.13	205
148	0.774223	1096	0.0068	2936.1	4098.6	162.58	21.55	32.00	207
150	0.750250	1137	0.0067	3026.5	4102+4	163.43	21.50	31.77	209
154	0.738883	1157	0.0065	3671.5	4289.5	163.85	21.48	31.67	212
156	0.727897	1177	0 0064	3116.3	4352.8	164.26	21.46	31.58	213
158 160	0.717271 0.706986	1197 1217	0.0063	3161.1 3205.7	4415.8 4478.7	164.66 165.05	21.45 21.44	31.49 31.41	215 217
165	0.682649	1266	0.0059	3317.0	4635.4	166 02	21.42	31.26	220
170	0.660087	1314	0.0057	3427.8	4791.2	166.95	21.41	31.11	224
175	0.639097	1362	0.0055	3538.3	4946.5	157.85	21.42	31.01	228
180	0.619505	1410	0.0053	3648.6	5101.3	168.72	21.43	30.92	231
185	0.601166	1457	0.0052	3758.7	5255.8	169.57	21.46	30.86	235
190	0.503955	1503	0.0050	3000.0	5410.0 5564 0	170.39	21.63	30.79	238
200	0.552500	1596	0.0047	4088.9	5717.9	171.97	21.58	30.77	245
205	0.538081	1641	0.0046	4199.1	5871.7	172.73	21.63	30.77	248
210	0.524435	1687	0.0045	4309.4	6025.6	173.47	21.68	30.77	251
215	0.511498	1732	0.0044	4419.9	6179.5	174.19	21.75	30.79	254
225	0.499213	1822	0.0043	4530.0	6487.6	175-59	21.88	30.84	257
230	0.476405	1866	0.0041	4752.8	6641.9	176.27	21.96	30.88	263
235	0.465797	1911	0.0040	4864.2	6796.4	176.94	22.03	30.92	266
240	0.455668	1955	0.0039	4976.0	6951.2	177.59	22.11	30.97	268
245	0.445986	1999	0.0038	5088.2	7106.2	178.23	22.19	31.00	271
255	0.430/22	2043	0.0036	5313-4	7417-0	179.47	22.36	31.14	274
260	0.419338	2131	0.0036	5426.6	7572.9	180.08	22.45	31.21	279
265	0.411170	2175	0.0035	5540.2	7729.1	180.67	22.54	31.27	282
270	0.403324	2218	0.0034	5654.1	7885.6	181.26	22.63	31.34	284
275	0.395/81	2262	0.0033	5883-2	8199.7	182-40	22.81	31.49	287
285	0.381531	2349	0.0032	5998.4	8357.3	182.96	22.90	31.56	292
290	0.374795	2392	0.0032	6114.0	8515.3	183.51	22.99	31.63	294
295	0.368297	2435	0.0031	6230.0	8673.7	184.05	23.08	31.71	297
500	1. 362027	24/8	0.0031	b.546.4	88.52.4	184.58	2.1.18	51.19	299

#### TABLE 16. THERMOOYNAMIC PROPERTIES OF FLUORINE

#### 1.0 MN/m<sup>2</sup> ISOBAR

TEMPERATURE	OENSITY	ISOTHERM	ISOCHORE	INTERNAL	ENTHALPY	ENTROPY	Cv	Сp	VELOCITY
K (1F13 1900)	MOL/L	J/MOL	MN/m <sup>2</sup> - K	J/MOL	J/MOL	J/MOL-K	J / MC	р – к	M/S
* 53.579	44.8983	27153	4.3149	-6047.9	-6025.7	60.85	36.47	54.70	1035
54	44.8295	27095	4.3145	-6024.8	-6002.4	61.28	36.40	54.86	1037
56	44.5028	26545	4.3128	-5914.4	-5892.0	63.30	36.05	55.86	1040
60	43.8637	25905	4.1341	-5694.5	-5671.7	67.10	35.33	55.90	1039
62	43.5402	25524	4.0567	~ 5583.8	-5560.8	68.92	34.99	56.08	1038
66	43.2077	24057	3.9044	-5359.8	-5336.4	72.43	34.59	56.57	1029
68	42.5553	22851	3.6558	-5249.6	-5226.1	74.08	33.73	55.69	996
70	42.2272	21702	3.5282	-5138.5	-5114.8	75.69	33.32	55.84	978
72	41.8802	20415	3.4181	-5025.0	-5001.1	77.30	32.93	56.42	959
76	41.1966	19144	3.2043	-4799.8	-4775.5	80.35	32.15	56.17	938
78	40.8484	18002	3.0839	-4686.7	-4662.2	81.82	31.77	56.46	918
80	40.4953	17133	2.9840	-4573.1	-4548.4	83.26	31.41	56.77	903
8 2 84	40.1279 39.7752	16254 15515	2.8707 2.7588	-4457.7 -4344.6	-4432.7 -4319.4	84.68 86.04	31.04 30.70	56.85 56.75	885 869
86	39.4082	14587	2.6409	-4229.6	-4204.3	87.39	30.37	56.85	848
88	39.0354	13731	2.5223	-4114.1	-4088.5	88.72	30.05	56.81	827
90	38.2713	12/77	2.3612	-3998.3	-3972+4	90.01	29.87	58.49	808
94	37.8779	11537	2.2684	-3763.5	-3737.1	92.55	29.38	58.61	778
96	37.4781	10749	2.1714	-3644.9	-3618.3	93.79	29.16	59.14	757
98	37.0688	10124	2.0839	-3525.2	-3498.2	95.02	28.99	59.58	740
100	30.0010	9412	1.9901	-3404+3	-3377.0	90.23	20.19	60.31	720
102	36.2218	8840	1.9114	-3282.0	-3254.4	97.42	28.64	60.77	703
106	35.3291	7561	1.7297	-3032.7	-3004.4	99.78	28.32	61.93	660
108	34.8620	6919	1.6451	-2905.2	-2876.5	100.95	28.20	62.96	638
110	34.3762	6321	1.5694	-2775.5	-2746.4	102.11	28.10	64.36	617
* 111.812	1.27991	635	0.0125	2023.5	2804.8	151.71	23.93	40.65	168
112	1.27623	638	0.0124	2028.9	2812.4	151.78	23.89	40.53	169
114	1.23896	668	0.0119	2085.2	2892.3	152.48	23.59	39.38	171
118	1.17305	726		2193.5	2970.0	153.81	23.10	37.58	174
120	1.14361	753	0.0107	2246.0	3120.4	154.43	22.90	36.87	179
122	1.11611	780	0.0104	2297.6	3193.5	155.04	22.72	36.25	181
124	1.09031	806	0.0101	2348.3	3265.5	155.62	22.57	35.71	183
128	1.04310	855	0.0095	2447.8	3406.5	156.74	22.31	34.81	187
130	1.02139	879	0.0093	2496.6	3475.7	157.28	22.20	34.44	189
132	1.00079	903	0.0091	2545.0	3544.2	157.80	22.11	34.10	191
136	0.981200	920	0.0087	2593.0	3679.5	158.81	22.02	33.53	193
138	0.944695	972	0.0085	2687.8	3746.3	159.30	21.88	33.29	197
140	0.927643	994	0.0083	2734.6	3812.6	159.78	21.82	33.07	199
142	0.911310	1016	0.0081	2781.3	3878.6	160.24	21.76	32.87	201
144	0.895645	1038	0.0080	2827.6	3944.1	160.70	21.71	32.68	203
140	0.866133	1059	0.0077	2013.1	4009.3	161.59	21.63	32.36	204
150	0.852207	1101	0.0075	2965.4	4138.8	162.03	21.60	32.22	208
152	0.838788	1122	0.0074	3010.9	4203.1	162.45	21.57	32.09	210
154	0.813350	1143	0.0073	3056.3	4267.2	162.87	21.55	31.98	211
158	0.801276	1184	0.0070	3146.6	4394.7	163.69	21.51	31.77	215
160	0.789600	1204	0.0069	3191.6	4458.1	164.09	21.49	31.68	216
165	0.762014	1254	0.0066	3303.7	4616.0	165.06	21.46	31.48	220
175	0.712778	1352	0.0062	3526.3	4929.3	166.90	21.45	31.20	227
180	0.690680	1400	0.0060	3637.2	5085.0	167.78	21.46	31.10	231
185	0.670022	1448	0.0058	3747.8	5240.3	168.63	21.49	31.02	235
190	0.632457	1495	0.0056	3858.4	5395+3	169.46	21.52	30.95	238
200	0.615315	1588	0.0053	4079.4	5704.5	171.04	21.60	30.90	245
205 210	0.599134 0.583832	1634 1680	0.0051	4189.9 4300.6	5859.0 6013.4	171.81	21.65 21.70	30.88 30.88	248 251
215	0.56977/	17.26	0.0049	4411 4	6167 8	173, 28	21.76	30 89	254
220	0.555576	1771	0.0048	4522.4	6322.3	173.99	21.83	30.91	257
225	0.542500	1817	0.0046	4633.6	6476.9	174.68	21.90	30.93	260
230	0.530054	1861	0.0045	4745.1	6631.7	175.36	21.97	30.97	263
235	0.506870	1906	0.0044	4050.0	6941.A	176.68	22.13	31.01	268
245	0.496052	1995	0.0042	5081.2	7097.1	177.32	22.21	31.10	271
250	0.485705	2040	0.0041	5193.9	7252.7	177.95	22.29	31.15	274
255 260	0.475796 0.466297	2084 2128	0.0040	5306.9 5420.3	7408.7 7564.9	178.57 179.18	22.38	31.21 31.27	277
265	0.457184	2172	0.0039	5534.1	7721.4	179.77	22.55	31.33	282
270	0.448431	2216	0.0038	5648.2	7878.2	180.36	22.64	31.40	284
275	0.440017	2259	0.0037	5762.7	8035.4	180.94	22.73	31.54	287
285	0.424131	2346	0.0036	5993.0	8350.8	182.06	22.91	31.61	292
290	0.416622	2390	0.0035	6108.8	8509.0	182.61	23.01	31.69	294
295	0.409382	2433	0.0035	6224.9	8667.6	183.16	23.10	31.76	297
500	00402390	2410	0.0034	0.041+0	0020.0	103.03	C 0. 1 3	01004	200

#### 1.2 MN/m<sup>2</sup> ISOBAR

TEMPERATURE	OENSITY	ISOTHERM	ISOCHORE	INTERNAL	ENTHALPY	ENTROPY	Cv	Сp	VELOCITY
(1915-1968) K	MOL/L	J/MOL	MN/m <sup>2</sup> - K	J/MOL	J/MOL	J/MOL-K	J / MC	)L - К	OF SOUND M/S
* 53.598	44.9024	27234	4.3158	-6052.1	-6025.4	60.86	36.46	54.65	1036
54	44.8372	27168	4.3154	-6030.1	-6003.3	61.27	36.40	54.81	1038
56	44.5103	26598	4.3136	-5919.8	-5892.9	63.28	36.05	55.82	1041
60	43.8714	25938	4.1357	-5700.1	-5672.7	67.08	35.33	55.89	1039
62	43,5481	25520	4.0561	-5589.4	-5561.9	68.90	35.00	56.08	1037
66	42.8831	23538	3.8372	-5365.6	-5337.6	72.41	34.17	56.63	1013
68	42.5641	22860	3.6593	-5255.5	-5227.3	74.06	33.74	55.72	997
70	42.2364	21722	3.5302	-5144.5	-5116.1	75.68	33.33	55.84 56.43	979
74	41.5515	20010	3.3340	-4919.0	-4890.1	78.82	32.58	56.39	955
76	41.2070	19132	3.2060	-4806.1	-4777.0	80.33	32.17	56.21	938
80	40.5070	17139	2.9849	-4579.7	-4550.1	83.23	31.43	56.78	903
82 84	40.1403	16242	2.8722	-4464.4	-4434.5	84.66	31.06	56.90	885
86	39.4219	14609	2.6437	-4236.7	-4206.3	87.37	30.39	56.86	848
88	39.0500	13754	2,5259	-4121.4	-4090.6	88.69	30.06	56.83	827
90	38.2878	12820	2.3620	-4005.8	-3974.7	91.27	29.90	57.97	794
94	37.8952	11562	2.2696	-3771.3	-3739.7	92.53	29.42	58.58	778
96	37.4967	10786	2.1730	-3653.0	-3621.0	93.76	29.19	59.09	758
100	36.6721	9454	1.9980	-3412.9	-3380.2	96.19	28.83	60.23	721
102	36.2444	8876	1.9131	-3290.9	-3257.8	97.39	28.69	60.70	703
106	35.3555	7607	1.7332	-3042.2	-3008.2	99.74	28.36	61.84	661
108	34.8908	6970	1.6481	-2915.1	-2880.7	100.91	28.23	62.80	639
110	34.4097 33.9095	5923	1.4898	-2654.0	-2618.6	102.07	28.03	64.2U	599
114	33.3894	5264	1.4116	-2519.4	-2483.4	104.40	27.94	66.64	575
* 114.725 * 114.725	33.1947	5094	1.3816	-2469.7	-2433.6	104.82	27.91	66.92	567
116	1.50529	633	0.0148	2071.0	2868.2	151.00	24.14	41.97	170
118 120	1.46051 1.41952	666 696	0.0142	2129.2 2185.6	2950.8 3031.0	151.71 152.38	23.81 23.52	40.65 39.55	173 176
122	1.38173	726	0.0132	2240.6	3109.1	153.03	23.28	38.61	178
124	1.34668	755	0.0128	2294.4	3185.5	153.65	23.06	37.81	180
128	1.28341	809	0.0120	2399.0	3334.0	154.83	22.71	36.51	185
130	1.25467	835	0.0116	2450.1	3406.5	155.39	22.56	35.98	187
132	1.22757	861 886	0.0113	2500.4	3478.0	155.93	22.43	35.09	189
136	1.17765	910	0.0108	2599.4	3618.4	156.98	22.21	34.72	194
138 140	1.15456 1.13258	934 958	0.0105 0.0103	2648.1 2696.4	3687.5 3755.9	157.49 157.98	22.12 22.04	34.38 34.08	195 197
142	1.11161	981	0.0101	2744.3	3823.8	158.46	21.97	33.81	199
144	1.07238	1004	0.0098	2791+8	3891.2	158.93	21.91	33.51	201
148	1.05399	1049	0.0094	2886.0	4024.6	159.85	21.80	33.14	205
150	1.03633	1071	0.0093	2932.7	4090.7	160.29	21.75	32.95	207
154	1.00304	1115	0.0089	3025.4	4221.8	161.15	21.68	32.63	210
156	0.987309	1136	0.0088	3071.5	4286.9	161.57	21.65	32.49	212
158 160	0.972144 0.957508	1157 1178	0.0086 0.0085	3117.4 3163.1	4351.7 4416.3	161.98 162.39	21.62 21.60	32.35 32.23	213 215
165	0.923034	1230	0.0081	3276.8	4576.8	163.38	21.56	31.98	219
175	0.891261	1281	0.0075	3502.2	4730.2	165.25	21.54	31.60	223
180	0.834516	1381	0.0073	3614.2	5052.2	166.14	21.53	31.46	230
185	0.809031	1430	0.0070	3725.9	5209.2 5365.7	167.00	21.54	31.35	234
195	0.762841	1526	0.0066	3948.8	5521.9	168.64	21.60	31.20	241
200	0.741824	1574	0.0064	4060.1	5677.8	159.43	21.64	31.15	244
205	0.722018	1621	0.0062	41/1.4 4282.8	5989.0	170.20	21.69	31.12 31.11	247
215	0.685619	1714	0.0059	4394.3	6144.5	171.68	21.80	31.10	254
225	0.652923	1806	0.0056	4617.7	6455.6	173.10	21.93	31.12	260
230	0.637782	1852	0.0055	4729.7	6611.2	173.78	22.00	31.14	263
235	0.623363	1897	0.0053	4954.5	6922.9	175.11	22.16	31.1/	268
245	0.596489	1987	0.0051	5067.3	7079.1	175.75	22.24	31.25	271
250	0.583942	2032	0.0050	5180.4 5293.8	7235.4	176.38	22.32	31.29	274
260	0.560433	2121	0.0048	5407.6	7548.8	177.61	22.49	31.40	279
265	0.549403	2166	0.0047	5521.8 5636.3	7706.U 7863.4	178.21	22.58	31.46	282
275	0.528644	2254	0.0045	5751.2	8021.2	179.38	22.76	31.58	287
280	0.518862	2298	0.0044	5866.5	8179.2	179.95	22.85	31.65	289
290	0.500383	2386	0.0042	6098.2	8496.4	181.06	23.03	31.79	292
295	0.491644	2429	0.0042	6214.7	8655.5	181.61	23.12	31.86	297
300	0.483215	2473	0.0041	6331.6	8815.0	182.14	23.22	31.93	299

## TABLE 16. THERMOOYNAMIC PROPERTIES OF FLUORINE

## 1.4 MN/m<sup>2</sup> ISOBAR

TEMPERATURE	OENSITY	ISOTHERM	ISOCHORE	INTERNAL	ENTHALPY	ENTROPY	Cv	Cp	VELOCITY
K	MOL/L	J/MOL	MN/m <sup>2</sup> - K	J/MOL	J/MOL	J/MOL-K	J/MO	)L + К	MZS
* 53.618	44.9065	27313	4.3167	-6056.3	-6025.2	60.86	36.46	54.60	1038
56	44.5179	26650	4.3163	-6035.4	-5893.8	63.26	30.39 36.04	55.78	1039
58	44.1942	26197	4.2249	-5814.9	-5783.3	65.21	35.68	55.91	1039
60	43.8791	25972	4.1374	~5705.6	-5673.7	67.07	35.33	55.87	1040
62 64	43.5559 43.2240	25516 24583	4.0556 3.9628	-5595.0 -5483.3	-5562.9 -5450.9	68.89 70.67	35.02 34.62	56.08 56.50	1037 1028
66	42.8916	23515	3.8390	-5371.4	-5338.8	72.40	34.19	56.68	1013
68	42.5728	22870	3.6628	-5261.4	-5228.5	74.04	33.74	55.84	997
72	41.8997	20415	3.4196	-5037.3	-5003.8	77.26	32.95	56.44	959
74	41.5615	19987	3.3338	-4925.2	-4891.5	78.80	32.60	56.43	954
76	41.2175	19121	3.2077	-4812.5	-4//8.5	80.31 81.78	32.19	56.49	938
80	40.5187	17145	2.9857	-4586.3	-4551.8	83.21	31.46	56.79	903
82 84	40.1526	16232	2.8737	-4471.2	-4436.3	84.64 86.00	31.08	56.95 56.78	885
86	39.4356	14632	2.6464	-4243.8	-4208.2	87.35	30.40	56.87	849
88	39.0645	13778	2.5294	-4128.6	+4092.7	88.67	30.07	56.85	828
90	38.6887	12862	2.4464	-4013.2	-3977.0	89.96	29.93	57.91	809
94	37.9125	11588	2.2708	-3779.1	-3742.2	92.50	29.46	58.56	779
96	37.5152	10823	2.1750	-3661.1	-3623.7	93.74	29.23	59.04	759
98	37.1082	10196	2.0867	-3541.8	+3504.0 -3383.3	94.96	29.07	59.47	741
102	36.2668	8913	1.9150	= 3296.7	= 3261.1	97.36	28.73	60.63	704
104	35.8295	8338	1.8280	-3176.3	-3137.2	98.54	28.55	61.02	685
106	35.3817	7654	1.7365	-3051.6	+3012.0	99.71	28.39	61.75	662
110	34.4410	6428	1.5771	-2796.2	-2755.5	102.03	28.17	64.05	620
112	33.9432	5962	1.4937	-2664.7	+2623.4	103.19	28.05	64.43	600
114	33.4272	5327	1.4164	-2530.7	-2488.8	104.35	27.96	66.38	577
* 117.306	32.5174	4439	1.2858	-2301.6	-2258.5	106.27	27.85	69.16	539
* 117.306	1.79777	587	0.0183	2035.8	2814.5	149.50	24.82	45.41	168
118	1.71988	635	0.0179	2057.8 2119.4	2933.4	149.76	24.26	44.72	169
122	1.66848	669	0.0164	2178.8	3017.9	151.20	23.92	41.56	175
124	1.62150	701	0.0158	2236.4	3099.8	151.87	23.63	40.38	178
128	1.53817	761	0.0147	2347.2	3257.4	153.12	23.15	38.51	183
130	1.50086	790	0.0142	2400.9	3333.7	153.71	22.96	37.77	185
132	1.46595	817	U.U138 0.0134	2453.5	3408.5	154.28	22.64	36.55	187
136	1.40230	870	0.0131	2556.4	3554.8	155.37	22.51	36.05	192
138 140	1.37311 1.34546	896 921	0.0127 0.0124	2606.9 2656.7	3626.5 3697.3	155.89 156.40	22.39 22.28	35.61 35.21	194 196
142	1.31919	946	0.0121	2706.1	3767.3	156.90	22.19	34.85	198
144	1.29419	970	0.0118	2754.9	3836.7	157.39	22.11	34.53	200
148	1.24756	1017	0.0118	2851.5	3905.5	158.32	22.04	33.98	202
150	1.22576	1041	0.0111	2899.2	4041.4	158.78	21.91	33.74	205
152	1.20486	1063	0.0109	2946.7	4108.6	159.22	21.86	33.52	207
156	1.16554	1108	0.0105	3040.8	4241.9	160.09	21.78	33.14	211
158 160	1.14700 1.12914	1130 1152	0.0103	3087.5 3134.0	4308.1 4373.9	160.51 160.92	21.74 21.71	32.97 32.82	212 214
165	1.08722	1206	0.0097	3249.4	4537.1	161.93	21.60	32.49	218
170	1.04875	1259	0.0093	3364.0	4698.9	162.89	21.62	32.23	222
175	1.01325	1311	0.0089	3477.8	4859.4	163.83	21.60	32.01	226
185	0.949802	1412	0.0083	3703.8	5177.8	165.60	21.60	31.69	233
190	0.921274	1461	0.0081	3816.3	5336.0	166.44	21.62	31.57	237
195	0.894575	1510	0.0078	3928.6	5493.6 5650.8	167.26	21.65	31.49	240
205	0.845949	1607	0.0074	4152.9	5807.8	168.83	21.73	31.37	247
210	0.823724	1655	0.0071	4264.9	5964.5	169.58	21.78	31.33	250
215	0.802724	1702	0.0070	4377.1	6121.1	170.32	21.84	31.31	253
225	0.763992	1795	0.0066	4601.7	6434.2	171.74	21.96	31.30	260
230	0.746084	1842	0.0064	4714.3	6590.7	172.43	22.03	31.32	262
235	0.729047	1888	0.0063	4827.0	6747.3	173.11	22.11	31.33	265
245	0.697332	1979	0.0060	5053.3	7061.0	174.41	22.26	31.39	271
250	0.682542	2025	0.0059	5166.9	7218.0	175.05	22.35	31.43	274
260	0.654856	2115	0.0056	5395.0	7532.8	176.28	22.52	31.53	279
265	0.641878	2160	0.0055	5509.5	7690.6	176.88	22.61	31.58	282
275	0.629427	2204	0.0054	5739.6	7848.6 8007.0	178.06	22.69	31.69	284
280	0.605980	2293	0.0052	5855.3	8165.6	178.63	22.87	31.76	289
285	0.594926	2338	0.0051	5971.3	8324.5	179.19	22.97	31.82	292
295	0.574029	2426	0.0049	6204.5	8643.4	180.29	23.15	31.95	297
300	0.564142	2470	0.0048	6321.7	8803.3	180.83	23.24	32.02	299

# 1.6 MN/m<sup>2</sup> ISOBAR

TEMPERATURE	OENSITY	ISOTHERM	ISOCHORE	INTERNAL	ENTHALPY	ENTROPY	Cv	Сp	VELOCITY
(IP)5 1966) K	MOL/L	J/MOL	MN/m <sup>2</sup> ~K	J/MOL	J/MOL	J/MOL-K	U Z MC	)L - К	M/S
<b># 57 679</b>	64 0107	27702	/ 7/75	6.0 C 0. C	( ) 2 ( )	60.07	76.45		4470
54	44.8519	27326	4.3172	-6040.7	-6005.0	61.24	36.39	54.50	1039
56	44.5254	26703	4.3152	-5930.6	-5894.7	63.25	36.04	55.74	1043
58	44.2018	26233	4.2278	-5820.4	-5784.2	65.19	35.67	55.90	1040
60	43.8868	26005	4.1393	-5711.2	-5674.7	67.05	35.34	55.86	1040
62	43.5638	25513	4.0552	-5600.7	-5563.9	68.87	35.03	56.09	1037
64	43.2321	24549	3.9620	-5489.0	-5452.0	70.65	34.64	56.54	1027
60	42.9001	23493	3.8408	-53/7.2	-5339.9	72.38	34.21	56.73	1013
70	42.2548	21765	3.0001	-5207+3	-5229.7	74.03	33.19	55.40 55.85	998
72	41.9095	20416	3.4205	-5043.4	-5005.2	77.24	32.96	56,45	959
74	41.5715	19964	3.3337	-4931.5	-4893.0	78.78	32.62	56.46	954
76	41.2279	19111	3.2094	-4818.8	-4780.0	80.29	32.20	56.30	938
78	40.8818	18017	3.0869	-4706.1	-4667.0	81.75	31.82	56.50	918
00	40.5303	1/153	2.9866	~4592.9	-4553.5	83.19	31.48	56.00	903
82	40.1649	16223	2.8752	-4477.9	-4438.1	84.61	31.10	57.00	885
84	39.8130	10002	2.6404	-4365.2	-4325+0	05.97	30.75	50.00	870
88	39.0790	138.02	2.5329	-4250.0	-4094.8	88.65	30.08	56.87	829
90	38.7043	12904	2.4475	-4020.6	-3979.3	89.94	29.96	57.85	810
92	38.3206	12237	2.3638	-3914.3	-3862.5	91.21	29.75	58.36	795
94	37.9297	11614	2.2720	-3786.9	-3744.7	92.47	29.50	58.54	779
96	37.5336	10861	2.1771	-3669.1	-3626.5	93.71	29.26	59.00	759
98	37.1278	10232	2.0883	-3550.0	-3506.9	94.93	29.12	59.42 60.08	741
4.0.2	76 2802	0050	4.0460	7700 5	7964 4	07 70	0.0 77	(0.57	7.0./
102	30.2092	8950	1 8307	-3300.5	-3264.4	97.032	20.11	60.08	704
106	35.4077	77 0 0	1.7398	-3061.0	-3015.8	99.67	28.42	61.66	663
108	34.9478	7072	1.6541	-2934.8	-2889.0	100.83	28.29	62.50	641
110	34.4720	6482	1.5808	-2806.4	-2760.0	101.99	28.20	63.89	622
112	33.9766	6003	1.4975	-2675.3	-2628.2	103.15	28.08	64.32	602
114	33.4645	5390	1.4211	~2542.0	-2494.2	104.30	27.99	66.13	579
116	32.9271	4875	1.3401	-2405.2	-2356.6	105.46	27.91	67.32	556
¥ 110 670	36+3669	4303	1.2012	-2166 9	-2215.4	100.03	27.04	71 26	532
* 119.634	2.06582	562	0.021/	2033.2	2807.8	148.57	25.25	48.05	168
120	2.05204	569	0.0212	2045.6	2825.3	148.71	25.15	47.59	168
122	1.98188	608	0.0201	2110.8	2918.2	149.48	24.68	45.38	171
124	1.91902	644	0.0192	2173.3	3007.1	150.20	24.29	43.60	174
126	1.86208	678	0.0184	2233.5	3092.8	150.89	23.95	42.14	177
128	1.81002	/11	0.0177	2291.8	31/5.8	151.54	23.66	40.92	180
172	1 71760	7 4 2	0.0165	24040	3290.0	152 77	23.40	39.89	185
134	1.67634	801	0.0160	2458.2	3412.7	153.35	22.99	38.24	187
136	1.63766	829	0.0155	2511.5	3488.5	153.91	22.82	37.57	190
138	1.60134	857	0.0151	2563.9	3563.0	154.46	22.68	36.99	192
140	1.56711	884	0.0147	2615.5	3636.5	154.99	22.54	36.47	194
142	1.53477	910	0.0143	2666.4	3708.9	155.50	22.43	36.01	196
144	1.50412	935	0.0140	2716.8	3780.5	156.00	22.33	35.59	198
146	1.47501	961	0.0136	2766.6	3851.3	156.49	22.23	35.22	200
148	1.44730	985	0.0133	2815.9	3921.4	156.97	22.15	34.89	202
150	1.42087	1010	0.0130	2864.8	3990.9	157.43	22.08	34.59	204
152	1 39902	10.54	0.0125	2913+4	4059.8	157.09	24.06	34:31	206
156	1.34829	1080	0.0123	3000.6	4196.1	158.77	21.90	33.84	210
158	1.32606	1103	0.0120	3657.0	4263.6	159.20	21.87	33.63	211
160	1.30470	1126	0.0118	3104.3	4330.6	159.62	21.83	33.44	213
165	1.25472	1182	0.0113	3221.6	4496.8	160.65	21.75	33.04	217
170	1.20905	1236	0.0108	3337.8	4661.1	161.63	21.70	32.70	221
175	1.16/08	1290	0.0104	3453.0	4823.9	162.57	21.67	32.44	225
185	1 00238	13942	0.0097	3207.02	4900+0 51/6 2	164.36	21.60	3206	229
190	1.05892	1445	0.0097	3795.0	5306.0	165.22	21.67	31.89	233
195	1.02768	1495	0.0090	3908.2	5465.1	166.04	21.70	31.78	244
200	0.998422	1544	0.0088	4021.3	5623.8	166.85	21.73	31.69	243
205	0.970940	1593	0.0085	4134.1	5782.0	167.63	21.77	31.61	247
210	0.945067	1642	0.0082	4247.0	5940.0	168.39	21.82	31.56	250
215	0.920655	1690	0.0080	4359.8	6097.7	169.13	21.87	31.53	253
225	0.875700	1785	0.0076	4412.1	6412 7	170.56	22,00	31 /0	250
230	0.85/062	18.32	0.0074	4698.8	6570.2	171 26	22.07	31.49	262
235	0.835243	1879	0.0072	4812.1	6727.7	171.93	22.14	31.50	265
240	0.816472	1925	0.0071	4925.6	6885.2	172.60	22.21	31.52	268
245	0.798579	1971	0.0069	5039.3	7042.9	173.25	22.29	31.54	271
250	0.781501	2017	0.0067	5153.3	7200.7	173.88	22.37	31.58	274
255	0.765180	2063	0.0066	5267.6	7358.6	174.51	22.46	31.61	276
260	0.749563	2109	0.0064	5382.2	1510.8	175.12	66.54	31.60	279
265	0.734606	2154	0.0063	5497.2	7675.2	175.73	22.63	31.70	282
275	0.706/00	2199	0.0061	5728 1	7992 4	176 00	22.81	31 81	204
280	0.693273	2289	0.0059	5844-1	8151.9	177.48	22.90	31.87	290
285	0.680557	2333	0.0058	5960.4	8311.4	178.04	22.99	31.93	292
290	0.668320	2378	0.0057	6077.1	8471.2	178.60	23.08	31.99	294
295	0.656534	2422	0.0056	6194.3	8631.3	179.14	23.18	32.05	297
300	0.645173	2467	0.0055	6311.8	8791.7	179.68	23.27	32.12	299

# TABLE 16. THERMOOYNAMIC PROPERTIES OF FLJORINE

## 1.8 MN/m<sup>2</sup> ISOBAR

TEMPERATURE	DENSITY	ISOTHERM	ISOCHORE	INTERNAL	ENTHALPY	ENTROPY	Cv	Сp	VELOCITY
(IPTS 1968) K	MOL/L	OERIVATIVE J/MOL	OERIVATIVE MN/m <sup>2</sup> -K	ENERGY J/MOL	J/MOL	J∕MOL-K	J / M0	DL - К	OF SOUNO M/S
¥ 53.657	44.9148	27471	4.3184	=6064.8	=6.024.7	60.87	36.44	54 50	1040
54	44.8592	27402	4.3180	-6046.0	-6005.9	61.22	36.39	54.64	1040
56	44.5328	26755	4.3160	-5936.0	-5895.6	63.23	36.04	55.70	1043
58 60	44.2094 43.8945	26268 26039	4.2307 4.1412	-5825.9 -5716.7	-5785.1 -5675.7	65.17 67.03	35.67 35.34	55.89 55.85	1041 1041
62	43.5716	25510	4.0549	-5606.3	-5565.0	68.85	35.04	56.09	1037
64	43.2403	24516	3.9612	-5494.8	-5453.1	70.63	34.66	56.57	1026
68	42.5903	22892	3.6694	-5273.2	-5230.9	74.01	33.76	55.81	998
70	42.2640	21787	3.5363	-5162.5	-5119.9	75.62	33.35	55.85	980
72	41.9193	20418	3.4214	-5049.5	-5006.6	77.22	32.97	56.46	959
76	41.2384	19102	3.2110	-4825.1	-4781.5	80.27	32.22	56.34	938
78 80	40.8928 40.5420	18024 17161	3.0880 2.9874	-4712.6 -4599.5	-4668.6 -4555.1	81.73 83.17	31.84 31.50	56.51 56.81	918 903
82	40.1772	16215	2.8767	-4484.7	-4439.9	84.59	31.12	57.04	884
84	39.8267	15578	2.7673	-4372.1	-4326.9	85.95	30.78	56.81	870
86	39.4629	14678	2.6517	-4257.8	-4212.2	87.30	30.43	56.89	850
90	38.7197	12946	2.4488	-4028.1	-3981.6	89.91	29.98	57.79	810
92	38.3369	12270	2.3648	-3911.9	-3864.9	91.19	29.78	58.31	795
94	37.9469	11641	2.2732	-3/94./	-3747.3	92.45	29.53	58.51	779
98	37.1473	10268	2.0899	-3558.3	-3509.8	94.90	29.16	59.37	742
100	36.7352	9577	2.0035	-3438.5	-3389.5	96.10	28.95	60.00	723
102	36.3115	8988 8405	1.9188	-3317.2	-3267.7	97.29	28.81	60.50 60.94	705 686
106	35.4336	7746	1.7431	-3070.4	-3019.6	99.64	28.45	61,56	664
108	34.9759	7123	1.6572	-2944.6	-2893.1	100.80	28.31	62.36	643
112	34.0098	6045	1.5016	-2685.9	-2633.0	103.10	28.11	64.22	603
114	33,5014	5451	1.4257	-2553.2	-2499.5	104.25	28.02	65.89	581
116	32.9679	4934	1.3451	-2417.0	-2362.4	105.41	27.92	67.06	558
120	31.8169	3876	1.1909	-2133.3	-2076.8	107.74	27.81	71.19	511
* 121.760	31.2639	3478	1.1253	-2002.4	-1944.8	108.79	27.79	73.14	491
122	2.33037	540	0.0245	2034.7	2807.2	147.81	25.59	50.54	168
124	2.24541	582	0.0232	2103.8	2905.4	148.61	25.06	47.81	171
126	2.10252	621	0.0221	2169.3	2998.8	149.35	24.61	45.64	174
130	2.04116	692	0.0203	2292.7	3174.5	150.08	23.90	42.44	180
132	1.98499	725	0.0195	2351.3	3258.2	151.37	23.63	41.23	182
134	1.93321	756	0.0188	2408.5	3339.6	151.98	23.38	40.20	185
138	1.84044	816	0.0177	2518.9	3496.9	152.57	22.99	38.55	190
140	1.79854	845	0.0171	2572.5	3573.3	153.68	22.82	37.88	192
142	1.75918	873	0.0167	2625.3	3648.5	154.22	22.68	37.29	194
144	1.68698	900	0.0162	2677.3	3722.5	154.73	22.56	36.30	196
148	1.65371	953	0.0154	2779.3	3867.7	155.73	22.34	35.88	201
150	1.62211	978	0.0151	2829.5	3939.1	156.21	22.26	35.51	203
152	1.59201	1003	0.0147	2928.4	4009.8	156.60	22.18	35.17	205
156	1.53585	1052	0.0141	2977.3	4149.3	157.58	22.05	34.59	208
158 160	1.50958 1.48439	1076 1100	0.0138 0.0136	3025.8 3074.0	4218.2 4286.6	158.02 158.45	22.00 21.95	34.33 34.10	210 212
165	1.42568	1158	0.0129	3193.3	4455.9	159.49	21.85	33.61	216
170	1.37228	1214	0.0124	3311.2	4622.9	160.49	21.79	33.21	221
175	1.32339	1269	0.0119	3427.9	4788.0	161.45	21.75	32.86	225
185	1.23680	1323	0.0114	3658.9	5114.3	163.26	21.72	32.40	232
190	1.19818	1428	0.0106	3773.5	5275.8	164.12	21.73	32.22	236
195	1.16219	1479	0.0103	3887.7	5436.5	164.96	21.75	32.07	240
205	1.09700	1580	0.0097	4115.3	5756.1	166.56	21.81	31.90	246
210	1.06735	1629	0.0094	4228.9	5915.3	167.32	21.86	31.80	250
215	1.03942	1678	0.0091	4342.4	6074.1	168.07	21.91	31.74	253
225	0.988076	1775	0.0086	4569.5	6391.2	159.51	22.03	31.68	259
230	0.964416	1822	0.0084	4683.2	6549.6	170.21	22.10	31.67	262
235	0.941949	1870	0.0082	4797.0	6708.0	170.89	22.17	31.67	265
245	0.900229	1964	0.0078	5025.3	7024.8	172.21	22.32	31.70	271
250	0.880818	2010	0.0076	5139.7	7183.3	172.85	22.40	31.72	274
260	0.844553	2056	0.0075	5254.5 5369.5	7342.0 7500.8	173.48	22.48	31.79	275
265	0.827583	2148	0.0071	5484.8	7659.8	174.70	22.66	31.83	282
270	0.811321 0.795720	2194	0.0070	5600.5	7819.1	175.30	22.15	31.87	284
280	0.780740	2284	0.0067	5832.8	8138.3	176.46	22.93	31.97	290
285	0.766342	2329	0.0066	5949.5	8298.3	177.02	23.02	32.03	292
290	0.739156	23/4	0.0063	6184-D	8619.2	178.13	23.11	32.15	295
300	0.726307	2464	0.0062	6301.8	8780.1	178.67	23.29	32.21	299

## 2.0 MN/m<sup>2</sup> ISOBAR

TEMPERATURE	DENSITY	ISOTHERM	ISOCHORE	INTERNAL	ENTHALPY	ENTROPY	Cv	Сp	VELOCITY
(1PTS 1968) K	MOL/L	J/MOL	MN/m <sup>2</sup> - K	J/MOL	J/MOL	J∕MOL-K	J / MO	L <del>~</del> К	M/S
		0754.0	( 7400		6004	60.07	36.14	54 45	1041
54	44.9108	2740	4.3189	-6051.3	-6024.4 -6006.7	61.20	36.38	54.59	1042
56	44.5403	26807	4.3167	-5941.4	-5896.5	63.22	36.03	55.66	1044
58 60	44.2171 43.9022	26303 26072	4.2336	-5831.3	-5786.1	65.16 67.02	35.67 35.34	55.88 55.83	1041 1041
62	43.5794	25509	4.0548	-5611 9	-5566.0	58.84	35.05	56.119	1036
64	43.2484	24484	3.9605	-5500.5	-5454.2	70.62	34.67	56.60	1026
66	42.9171	23453	3.8441	-5388.8	-5342.2	72.34	34.24	56.82	1012
68	42.5990	22903	3.6726	-5279.0	-5232.1	73.99	33.77	55.84	998
70	42.2731	21809	3.5384	-5168.5	-5121.1	75.60	33.35	55.85	980
74	41.5916	19925	3.3336	-4943.9	-4895.8	78.74	32.66	56.52	953
76	41.2489	19094	3.2127	-4831.4	-4783.0	80.25	32.24	56.38	937
78 80	40.9039 40.5536	18031 17169	3.0890	-4719.1 -4606.1	-4670.2 -4556.8	81.71 83.15	31.85 31.52	56.53 56.82	918 903
82	40.1896	16209	2.8781	-4491.5	-4441.7	84.57	31,14	57.08	884
84	39.8395	15595	2.7694	-4379.0	-4328.8	85.93	30.80	56.82	870
86	39.4765	14702	2.6543	-4264.9	-4214.2	87.28	30.45	56.90	850
88	39.1079	13852	2.5397	-4150.2	-4099.0	88.60	30.11	56.90	830
90	38.7552	12988	2.45U1 2.3658	-4035.5	-3983.8	89.89	29.82	58.27	795
92	37.9641	11668	2.2744	-3802.5	-3749.8	92.42	29.57	58.48	779
96	37.5703	10936	2.1812	-3685.1	-3631.9	93.65	29.32	58.91	760
98 100	37.1667 36.7560	10304 9p19	2.0916 2.0053	-3566.5 -3446.9	-3512.7 -3392.5	94.87 96.07	29.20 28.98	59.32 59.93	742 723
102	36 . 3337	9025	1.9208	-3326.0	-3270.9	97.26	28.85	60.44	705
104	35,9010	8440	1.8359	-3203.4	-3147.7	98.44	28.67	60.90	687
106	35.4594	7793	1.7463	-3079.8	-3023.4	99.60	28.48	61.47	665
108	35.0039	7173	1.6605	-2954.3	-2897.1	100.76	28.34	62.22	644
110	34.5332	6588 6087	1.58//	-2826.8	+2768.9	101.91	28.13	64.14	624
114	33.5379	5511	1.4301	-2564.3	-2504.7	104.21	28.04	65.66	583
116	33.0082	4992	1.3500	-2428.7	-2368.1	105.36	27.94	66.81	560
118 120	32.4544 31.8680	4442 3944	1.2741 1.1969	-2289.9 -2146.7	-2228.2 -2083.9	106.52 107.68	27.88 27.82	68.82 70.74	537 514
122	31.2440	3484	1.1221	-1998.5	+1934.5	108.87	27.80	72,96	491
* 123.723	30.6702	3042	1.0561	-1866.1	-1800.9	109.91	27.80	76.04	468
<b>* 123.723</b>	2.62538	508	0.0282	2015.1	2776.9	146.90	26.08	54.12	167
124	2.50916	515	0.0263	2025.0	2895.5	147.85	25.39	50.23	171
128	2.42063	600	0.0250	2167.0	2993.2	148.62	24.89	47.64	174
130	2.34181	639	0.0239	2232.3	3086.4	149.34	24.47	45.58	177
132	2.27075	675	0.0228	2295.1	3175.8	150.03	24.12	43.91	180
134	2,20607	710	0.0220	2355.6	3262.2	150.68	23.82	42.52	183
138	2.09188	743	0.0212	2471.6	3427.7	151.89	23.33	40.34	188
140	2.04095	805	0.0198	2527.6	3507.5	152.47	23.13	39.48	190
142	1.99341	835	0.0192	2582.4	3585.7	153.02	22.95	38.73	193
144	1.94885	864	0.0187	2636.2	3662.5	153.56	22.80	38.07	195
146	1.90694	892	0.0181	2689.2	3738.0	154.08	22.66	37.49	197
148	1.86739	919	0.0177	2741.5	3812.5	154.59	22.55	36.97	199
152	1.79445	946	0.0172	2844.0	3958.6	155.56	22.35	36.10	201
154	1.76069	998	0.0164	2894.4	4030.4	156.03	22.27	35.72	205
156	1.72852	1024	0.0161	2944.4	4101.5	156.49	22.19	35.39	207
158 160	1.69781 1.66845	1049	0.0157 0.0154	2993.9 3043.1	4171.9 4241.8	156.94 157.38	22.13	35.08 34.80	209
165	1.60027	1133	0.0147	3104.5	4414.3	158.44	21.96	34.21	216
170	1.53855	1192	0.0140	3284.2	4584.1	159.45	21.88	33.73	220
175	1.48229	1248	0.0134	3402.5	4751.7	160.43	21.83	33.34	224
180	1.43069	1304	0.0129	3519.7	4917.6	161.36	21.78	32.77	228
190	1.33907	1411	0.0120	3751.8	5245.4	163,13	21.78	32.55	236
195	1.29811	1464	0.0116	3867.0	5407.7	163.98	21.80	32.38	239
200	1.25991	1515	0.0112	3981.8	5569.2	164.79	21.82	32.24	243
205 210	1.22415	1566 1617	0.0108	4096.4 4210.7	5890.5	165.59	21.85	32.13 32.04	246 249
215	1.15901	1666	0.0102	4324.9	6050.5	167.11	21.94	31.97	253
220	1.12924	1716	0.0099	4439.1	6210.2	167.85	22.00	31.91	256
225	1.10109	1765	0.0097	4553.3	6369.7	160.56	22.06	31.88	259
230	1.0/445	1813	0.0094	4782.0	6688.2	169-95	22.20	31-84	265
240	1.02514	1909	0.0089	4896.5	6847.4	170.62	22.27	31.84	268
245	1.00228	1956	0.0087	5011.2	7006.6	171.28	22.35	31.85	271
250	0.980490	2003	0.0085	5126.1	7165.9	171.92	22.43	31.86	274
255	0.939821	2090	0.0081	5356.7	7484.8	173.17	22.60	31.92	279
265	0.920809	2143	0.0080	5472.5	7644.5	173.78	22.68	31.95	282
270	0.902598	2189	0.0078	5588.5	7804.3	174.38	22.77	31.99	284
275	0.885136	2234	0.0076	5704.9	7964+4	175.50	22.95	32.08	207
285	0.852276	2325	0.0073	5938.6	8285.2	176.11	23.04	32.14	292
290	0.836793	2371	0.0072	6056.0	8446.1	176.67	23.13	32.19	295
295	0.821892	2416	0.0071	6173.7	8607.1	177.22	23.23	32.25	297
300	0.807540	2461	0.0069	6291.9	8768.5	1//.76	23.32	32.31	300

# 2.5 MN/m<sup>2</sup> ISOBAR

TEMPERATURE	OENSITY	ISOTHERM DERIVATIVE	I-SOCHORE OFRIVATIVE	INTERNAL	ENTHALPY	ENTROPY	Cv	Сp	VELOCITY OF SOUND
K	MOL/L	J/MOL	MN/m <sup>2</sup> - K	J/MOL	J/MOL	J/MOL-K	J / MC	ОL - К	M/S
* 53.726	44.9289	27738	4.3213	-6079.4	-6023.8	60.89	36.42	54.34	1044
56	44.5589	26937	4.3186	-5954.9	-5898.7	63.17	36.03	55.55	1044
58	44.2360	26391	4.2408	-5845.0	-5788.5	65.12	35.66	55.86	1043
60	43.9213	26155	4.1487	-5736.1	-5679.1	66.98	35.34	55.81	1043
62 64	43.5990 43.2689	25510 24412	4.0549 3.9587	-5625.9 -5514.8	-5568.6 -5457.0	68.79 70.57	35.08 34.72	56.11 56.66	1036 1024
66	42.9385	23410	3.8479	-5403.4	-5345.1	72.30	34.29	56.93	1011
68	42.6208	22933	3.6802	-5293.7	-5235.0	73.95	33.79	55.90	999
72	42.2900	21000	3.4251	+5070.9	-5011.4	77.15	33.01	56.50	959
74	41.6167	19883	3.3339	-4959.5	-4899.4	78.69	32.71	56.59	952
76	41.2751	19079	3.2166	-4847.2	-4786.7	80.20	32.28	56.48	937
78 80	40.9317 40.5827	18053	3.0918 2.9906	-4622.6	-4561.0	81.66 83.10	31.90 31.57	56.84	918 903
82	40.2204	16199	2.8818	-4508.3	-4446.2	84.52	31.19	57.18	884
84	39.8715	15540	2.6606	-4396.1	-4333+4	87.22	30.84	56.91	871
88	39.1440	13918	2.5480	-4168.1	-4104.2	88.54	30.14	56.93	832
90	38.7735	13093	2.4540	-4053.9	-3989.5	89.82	30.07	57.61	812
92	38.3937	12390	2.3687	-3938.4	-3873.2	91.10	29.90	58.17	796
96	37.6159	11032	2.1862	-3705.0	-3638.5	93.58	29.39	58.79	762
98	37.2150	10397	2.0962	-3587.0	-3519.8	94.80	29.29	59.19	744
100	36.8077	9724	2.0099	-3468.0	-3400.1	95.99	29.07	59.74	725
102	36.3889	9121	1.9260	+3347.7	-3279.0	97.18	28.94	60.27	707
104	35.5231	7908	1.7545	-3103.0	-3032.6	99.51	28.56	61.25	668
108	35.0730	7299	1.6704	-2978.4	-2907.1	100.66	28.40	61.96	647
110	34.6083	6721	1.5959	-2852.0	-2779.8	101.81	28.34	63.15	628
112	34.1242	5658	1.4410	-2591.8	-2517.5	102.96	28.2U	65.11	587
116	33.1069	5136	1.3632	-2457.6	-2382.1	105.24	27.99	66.29	566
118 120	32.5649 31.9922	4608 4111	1.2878 1.2116	-2320.6 -2179.4	-2243.8 -2101.2	106.38 107.54	27.92 27.85	67.97 69.71	543 520
122	31.3844	3638	1.1377	-2033.6	+1953.9	108.71	27.82	71.89	497
124	30.7376	3148	1.0644	-1882.7	-1801.3	109.90	27.83	75.06	473
126	30.0361	2694	0.9069	+1/24+/	-1641.5	111.12	27.89	79.09	448
* 128.076	29.2351	2231	0.9055	-1551.5	-1466.0	112.44	27.92	82.99	418
¥ 128.076	3.38107	4 38	0.0379	1971.5	2710.9	145.05	27.10	63.93	165
130	3.22908	490	0.0354	2053.9	2828.1	145.96	26.33	58.22	169
134	2.98026	583	0.0315	2205.8	3044.7	147.60	25.14	50.78	176
136	2.87857	625	0.0300	2275.1	3143.6	148.33	24.70	48.28	179
138 140	2.78763 2.70537	664 701	0.0286 0.0275	2341.3 2404.9	3238.1 3328.9	149.02 149.67	24.32 24.00	46.27 44.63	182 185
142	2.63030	7 36	0.0265	2466.3	3416.8	150.30	23.73	43.25	188
144	2.56126	770	0.0255	2526.0	3502.1	150.89	23.49	42.08	191
146	2.49737	802	0.0247	2584.2	3585.2	151.47	23.28	41.08	193
150	2.38240	865	0.0232	2696.7	3746.1	152.55	22.94	39.45	198
152	2.33029	894	0.0226	2751.5	3824.3	153.07	22.80	38.78	200
154	2.28124	923	0.0220	2805.4	3901.3	153.57	22.68	38.18	202
156	2.23491 2.19106	951	0.0209	2000.0	4051.9	154.00	22.48	37.18	204
160	2.14940	1006	0.0204	2962.7	4125.9	155.01	22.40	36.76	208
165	2.05378	1072	0.0193	3090.0	4307.3	156.12	22.23	35.86	213
175	1.96839	1135	0.0184	3214.7	4484.8	157.18	22.11	35.15	218
180	1.82147	1256	0.0168	3458.3	4830.8	159.16	21.97	34.12	227
185	1.75750	1313	0.0161	3578.0	5000.5	160.09	21.93	33.75	231
190	1.69867	1370	0.0155	3696.7	5168.4	160.99	21.92	33.44	235
200	1.59384	1480	0.0144	3931.7	5500.3	162.69	21.93	32.97	242
205 210	1.54683	1533 1586	0.0139 0.0135	4048.4 4164.8	5664.6 5828.2	163.50 164.29	21.96 21.99	32.79 32.65	245 249
215	1.46170	1638	0,0131	4280.8	5991.2	165.05	22.03	32.53	252
220	1.42298	1689	0.0127	4396.7	6153.6	165.80	22.09	32.44	256
225	1.38650	1739	0.0123	4512.5	6315.6	166.53	22.14	32.37	259
235	1.35204	1839	0.0120	4020.3	6638.8	167.93	22.27	32.27	265
240	1.28851	1888	0.0114	4859.9	6800.1	168.61	22.34	32.25	268
245	1.25915	1937	0.0111	4975.8	6961.3	169.28	22.42	32.23	271
255	1.20459	1986	0.0108	5208.2	7283.6	109.93	22.58	32.23	274
260	1.17920	2081	0.0103	5324.7	7444.8	171.19	22.66	32.25	279
265	1.15493	2129	0.0101	5441.5	7606.1	171.81	22.74	32.26	282
275	1.10950	2223	0.0097	5675.7	7929.0	173.00	22.92	32.32	287
280	1.08819	2269	0.0095	5793.3	8090.7	173.59	23.01	32.36	290
285	1.06775	2316	0.0093	5911.2	8252.6	174.16	23.10	32.40	292
290	1.04810	2362	0.0089	6148-0	8577-0	175.28	23.28	32.44	295
300	1.01104	2454	0.0088	6266.9	8739.6	175.83	23.38	32.54	300

\* TWO-PHASE BOUNDARY

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## 3.0 MN/m<sup>2</sup> ISOBAR

TEMPERATURE	DENSITY	ISOTHERM	ISOCHORE	INTERNAL	ENTHALPY	ENTROPY	Cv	Cp	VELOCITY
(IPIS 1968) K	MOL/L	J/MOL	MN/m <sup>2</sup> ~ K	J/MOL	J/MOL	J∕MOL-K	J / MO	рг – к	M/S
* 53+775	44.9390	27925	4.3233	-6089.9	-6023.1	60.90	36.41	54.23	1046
54	44.9026	27863	4.3230	-6077.6	-6010.8	61.13	36.37	54.33	1047
56	44.5774	27066	4.3204	-5968.3	-5901.0	63.13	36.02	55.45 55.83	1047
60	43.9404	26238	4.1547	-5749.9	-5681.6	66.93	32.34	55.78	1044
62	43.6186	25516	4.0556	-5640.0	-5571.2	68.75	35.11	56.12	1036
66	42.9598	23374	3.8513	-5417.9	-5348.0	72.25	34.33	57.02	1011
68	42.6426	22965	3.6874	-5308.3	-5238.0	73.90	33.82	55.96	1000
70	42.3189	21925	3.5487	-5198.3	-5127.4	75.51	33.40	55.85	982
74	41.6418	19850	3.3347	-4975.0	-4902.9	78.64	32.75	56.66	951
76	41.3013	19070	3.2203	-4863.0	-4790.4	80.15	32.33	56.56	937
78 80	40.9593 40.6118	17225	3.0948 2.9931	-4751.3 -4639.1	-4678.1 -4565.2	81.61 83.04	31.94 31.62	56.85 56.85	918 903
82	40.2513	16197	2.8853	-4525.1	-4450.6	84.46	31.24	57.25	884
84	39.9034	15688	2.7793	-4413.2	-4338.0	85.82	30.89	56.87	872
88	39.1798	13986	2.5559	-4186.0	-4109.4	88.48	30.17	56.94	834
90	38.8115	13198	2.4585	-4072.3	-3995.0	89.76	30.13	57.49	814
92	38.0493	12478	2.3720	~3841.1	-3879.1	91.03	29.98	58.33	798
96	37.6610	11129	2.1911	-3724.8	-3645.1	93.51	29.46	58.66	764
98	37.2629	10491	2.1012	-3607.3	-3526.8	94.72	29.38	59.08	745
100	76 1474	5025	4.0745	-340340	7207.0	07.40	23.10		700
104	36.0183	8620	1.8483	-3248.2	-3164.9	98.27	29.03	60.63	690
106	35.5858	8024	1.7630	-3126.0	-3041.7	99.43	28.63	61.05	671
108	35.1409	7425	1.6801	-3002.3	-2916.9	100.57	28.46	61.70 62.76	651 631
112	34.2042	6310	1.5273	-2748.6	-2660.9	102.85	28.26	63.64	612
114	33.7147	5799	1.4517	-2619.0	-2530.0	103.98	28.16	64.61	592
118	32.6716	4766	1.3010	-2350.6	-2258.8	106.25	27.96	67.22	549
120	32.1115	4270	1.2265	-2211.3	-2117.9	107.40	27.87	68.87	527
122	31.5191	3790	1.1527	-2067.7	-1972.5	108.55	27.85	70.90	504
124	30.2160	2864	1.0099	-1765.3	-1666.0	109.72	27.84	73.62	480
128	29.4801	2425	0.9286	-1602.8	-1501.0	112.16	27.85	80.21	429
130	28.6667	1962	0.8520	-1431.1	-1326.4	113.45	28.01	86.56	399
	4.22233	364	0.0495	1905.5	2616.0	143.30	28.17	78.05	163
132	4.20034	369	0.0491	1914.4	2628.6	143.39	28.07	76.97	163
134	3.96591	434	0.0451	2015.3	2771.7	144.47	27.05	66.96	168
138	3.61958	540	0.0394	2186.1	3015.0	146.26	25.63	55.93	176
140	3.48338	586	0.0373	2262.ů	3123.2	147.04	25.12	52.50	180
142	3.36358	629	0.0355	2333.6	3225.5	147.76	24.69	49.84	183
144	3.25662	569 Z 08	0.0339	2401.7	3322.9 3416.5	148.45	24.32	47.70	186
148	3.07197	744	0.0314	2530.3	3506.9	149.71	23.75	44.47	192
150	2.99109	779	0.0303	2591.6	3594.5	150.29	23.52	43.22	194
154	2.84682	846	0.0284	2709.4	3763.2	151.40	23.15	42.19	197
156	2.78193	877	0.0275	2766.5	3844.9	151.93	23.00	40.42	201
158 160	2.72110 2.66387	908 938	0.0268	2822.5 2877.6	3925.0 4003.7	152.44 152.94	22.86 22.75	39.70 39.07	204 206
165	2.53418	1010	0.0245	3011.9	4195.7	154.12	22.51	37.77	211
170	2.42018	1079	0.0231	3142.3	4381.9	155.23	22.34	36.76	216
180	2.22747	1208	0.0210	3395.0	4741.8	157.29	22.14	35.32	225
185	2.14475	1269	0.0200	3518.3	4917.1	158.25	22.09	34.81	229
190	2.06923	1329	0.0192	3640.2	5090.0	159.17	22.05	34.38	233
200	1.93587	1444	0.0178	3880.7	5430.4	160.92	22.04	33.74	241
205	1.87653	1500	0.0172	3999.7	5598.4	161.75	22.06	33.49	245
245	4 76 0 74	1555	0.0161	4110+6	5071	102.000	22.07	33.63	240
220	1.72139	1663	0.0156	4353.9	6096.7	164.09	22.13	32.99	252
225	1.67599	1715	0.0151	4471.4	6261.3	164.83	22.22	32.88	258
230	1.63322	1767	0.0147	4588.6	6425.5	165.55	22.28	32.79	262
240	1.55467	1869	0.0139	4823.0	6752.7	166.95	22.41	32.67	268
245	1.51847	1919	0.0135	4940.3	6915.9	167.62	22.48	32.63	271
250	1.48409	1969	0.0132	5057.6	7079.0	168.28	22.56	32.58	274
260	1.42025	2067	0.0126	5292.6	7404.9	169.56	22.72	32.58	279
265	1.39054	2116	0.0123	5410.3	7567.7	170.18	22.81	32.58	282
270	1.36216	2164	0.0120	5528.3	7893.7	171.38	22.98	32.59	285
280	1.30901	2259	0.0115	5765.0	8056.8	171.97	23.07	32.63	290
285	1.28409	2307	0.0113	5883.7	8220.0	172.55	23.16	32.66	293
295	1.23719	2401	0.0108	6122.1	8547.0	173.68	23.34	32.73	295
300	1,21510	2447	0.0106	6241.8	8710.7	174.23	23.43	32.77	300

#### TABLE 16. THERMOOYNAMIC PROPERTIES OF FLUORINE

#### 3.5 MN/m<sup>2</sup> ISOBAR

TEMPERATURE	DENSITY	ISOTHERM	ISOCHORE	INTERNAL	ENTHALPY	ENTROPY	Cv	Сp	VELOCITY
(IPIS 1968) K	MOL/L	J/MOL	MN/m <sup>2</sup> +K	J/MOL	J/MOL	J/MOL-K	J / M	οι <del>-</del> κ	OF SOUND M/S
* 53 823	66 969 <b>0</b>	28107	1. 725.2	-6100 6	-6022 E	60.01	76 70	6/ 12	1010
54	44.9205	28053	4.3250	-6090.8	-6012.9	61.09	36.39	54.20	1049
56 58	44.5959	27195	4.3222	-5981.7	-5903.2	63.09	36.01	55.35	1049
60	43.9594	26321	4.1613	-5763.7	-5684.0	66.89	35.34	55.76	1046
62	43.6382	25527	4.0570	-5654.0	-5573.8	68.71	35.14	56.13	1036
66	42.9813	23346	3.8543	~5432.4	-5351.0	72.21	34.38	57.11	1021
68	42.6644	22999	3.6940	-5323.0	-5240.9	73.86	33.84	56.01	1001
70	42.3416	21986	3.4319	-5213.2	-5130.5	77.06	33.42 33.06	56.53	983
74	41.6671	19827	3.3358	-4990.5	-4906.5	78.59	32.80	56.72	950
76 78	41.3275	19067	3.2238	-4878.8	-4794.1	80.10	32.38	56.63 56.58	937
80	40.6408	17260	2.9957	-4655.5	-4569.3	82.99	31.67	56.86	903
82	40.2822	16204	2.8888	-4541.9	-4455.1	84.41	31.29	57.32	884
86	39.5779	14894	2.6730	-4317.3	-4228.9	87.10	30.58	56.92	854
88	39.2154	14058	2.5635	-4203.8	-4114.5	88.42	30.20	56.95	835
92	38.4738	12568	2.3756	-3975.9	-3884.9	90.97	30.18	57.96	816 799
94	38.0915	11890	2.2846	-3860.3	-3768.4	92.22	29.82	58.26	782
96	37.7057	11227	2.1958	-3627.6	-3651.7	93.44	29.53	58.53	765
100	36.9095	9935	2.0190	-3509.8	-3415.0	95.84	29.24	59.36	729
102 104	36.4973 36.0760	9318 8714	1.9373 1.8545	-3390.8 -3270.3	-3294.9 -3173.3	97.02 98.19	29.11	59.95 60.49	711
106	35.6477	8140	1.7712	-3148.9	-3050.7	99.34	28.70	60.85	674
108	35.2077 34.7543	7550	1.6893	-3026.0	-2926.6	100.48	28.51	61.45	654
112	34.2827	6428	1.5374	-2774.3	-2672.2	102.75	28.32	63.36	615
114	33.7999	5937 5415	1.4621	-2645.7	-2542.1	103.87	28.22	64.15	596 576
118	32.7748	4918	1.3138	-2380.2	-2273.4	106.13	27.99	66.55	555
120	32.2265	4425	1.2408	-2242.6	-2134.0	107.26	27.90	68.10	533
122	31.0394 31.0394	3940 3480	1.1681	-1955.5	-1842.8	108.40	27.87	70.05	511 488
126	30.3858	3028	1.0259	-1804.3	-1689.1	110.74	28.01	75.43	463
130	28.9100	2150	0.8753	-1479.5	-1358.4	113.20	27.98	83.41	439
132	28.0436	1720	0.7956	-1301.1	-1176.3	114.52	27.91	89.67	381
134 * 135.161	27.0363	1290	0.7162	-1106.3	-976.8	115.95	28.24	101.14	349
* 135.161	5.18934	285	0.0638	1813.5	2487.9	141.54	29.36	101.00	161
136	5.01713 4.69405	321 394	0.0606	1870.4	2568.0	142.13	28.71	90.62 75.44	163
140	4.44564	455	0.0506	2086.5	2873.8	144.35	26.63	66.52	173
142	4.24282	510	0.0473	2175.6	3000.6	145.25	25.93	60.56	177
144	4.U/11U 3.92204	56U 606	0.0446	2257.4	3117.1	146.06	25.37	56.24	181
148	3.79033	649	0.0404	2406.0	3329.4	147.52	24.52	50.37	187
150 152	3.56549	728	0.0386	2474.9 2541.1	3428.U 3522.8	148.18	23.91	48.28	190
154	3.46789	765	0.0358	2605.1	3614.4	149.40	23.67	45.09	196
156	3.29497	8U1 835	0.0334	2667.2	3789.9	149.98	23.47	43.85	198
160	3.21764	868	0.0324	2786.7	3874.5	151.06	23.13	41.85	203
165 170	3.04517	947 1022	0.0302	2929.5	4078.8	152.32	22.82	39.98 38.58	209
175	2.76585	1093	0.0268	3199.7	4465.2	154.59	22.43	37.50	219
180	2.64983	1160	0.0255	3329.6	4650.4 4831.9	155.64	22.32	36.64	224
190	2.45130	1289	0.0232	3582.4	5010.2	157.58	22.19	35.39	233
195	2.36524	1350	0.0222	3706.2	5185.9 5359.6	158.50	22.17	34.93	237
205	2.21341	1468	0.0206	3950.2	5531.5	160.22	22.17	34.23	244
210	2.14591	1526	0.0198	4071.0	5702.0	161.05	22.19	33.96	248
220	2.02448	1637	0.0192	4191.U 4310.6	5871.2 6039.4	162.62	22.22	33.74	251
225	1.96956	1691	0.0180	4429.8	6206.8	103.37	22.30	33.28	258
235	1.86941	1798	0.0170	4667.4	6539.6	164.82	22.42	33.17	265
240	1.82357	1850	0.0165	4786.0	6705.3 6870.6	165.51	22.48	33.09	268
250	1.73909	1953	0.0156	5023.0	7035.5	166.86	22.62	32.97	274
255 260	1.70006 1.66294	2003 2054	0.0152 0.0149	5141.6 5260.2	7200.3 7364.9	167.51 168.15	22.70 22.78	32.94 32.91	277 279
265	1.62758	2103	0.0145	5379.0	7529.5	168.78	22.86	32.90	282
275	1.59384	2153	0.0142	5617.1	7858.4	170.00	23.04	32.89	285
280	1.53077	2250	0.0136	5736.5	8022.9	170.59	23.12	32.91	290
285	1.50125	2298 2346	0.0133	5856.1 5976.0	8187.5	1/1.1/ 171.75	23.21	32.92	293
295	1.44577	2394	0.0127	6096.1	8517.0	172.31	23.39	32.97	298
300	1.41967	2441	0.0125	6216.6	8681.9	172.86	23.49	33.01	300

## 4.0 MN/m<sup>2</sup> ISOBAR

TEMPERATURE	DENSITY	ISOTHERM	ISOCHORE	INTERNAL	ENTHALPY	ENTROPY	Cv	Cp	VELOCITY
(1PTS 1968) K	MOL/L	DERIVATIVE J/MOL	DERIVATIVE MN/m <sup>2</sup> -K	ENERGY J/MOL	J/MOL	J/MOL-K	J / MI	DL - K	OF SOUND M/S
* 53.871	44.9589	28285	4.3270	-6110.9	-6021.9	60.92	36.37	54.02	1051
54	44.9383	28241	4.3269	-6103.9	-6014.9	61.05	36.35	54.08	1052
58	44.2926	26653	4.2619	-5885.8	-5795.5	64.99	35.64	55.78	1048
60	43.9784	26403	4.1684	-5777.4	-5686.5	66.85	35.33	55.75	1047
62	43.6578	25544	4.0591	-5667.9	-5576.3	68.67	35.16	56.15	1036
64	43.3306	24255	3.9545	-5557.5	-5465.2	70.44	34.84	56.82	1020
68	43.0027	23326	3.0563	-5446.9	-5353.9	72.16	34.43	57.18	1010
70	42.3643	22049	3.5591	-5228.1	-5133.6	75.42	33.44	55.85	984
72	42.0269	20509	3.4373	-5116.7	-5021.5	77.01	33.08	56.57	961
74	41.3537	19071	3.2271	-4894.5	-4910.1	80.05	32.43	56.69	949
78	41.0145	18147	3.1021	-4783.4	-4685.9	81.51	32.02	56.60	919
8 D	40,6697	17380	2.9985	-4671.8	-4573.5	82.94	31.72	56.86	903
82	40.3130	16219	2.8921	-4558.7	-4459.5	84.35	31.35	57.37	884
84	39.9670	15792	2.7885	-4447.3	-4347.2	85.71	30.99	56.88	873
88	39.2509	14134	2.5708	-4221.5	-4119.6	88.36	34.23	56.94	837
90	38.8867	13407	2.4692	-4108.8	-4005.9	89.64	30.23	57.29	818
92	38.5134	12660	2.3795	-3994.6	+389ú.7	90.90	30.11	57.85	800
96	37.7501	11326	2.2006	-3764.1	-3658.1	93.37	29.60	58.40	767
98	37.3574	10684	2.1121	-3647.7	-3540.6	94.58	29.53	58.85	749
100	30.9595	10042	2.0237	-3530.5	-3422+3	95.77	29.31	59.17	730
102	36.5507	9419	1.9433	-3412.1	-3302.7	96.94	29.18	59.79	713
104	35.7087	8256	1.7790	-3171.6	-3059.5	99.25	28.77	60.63	677
108	35.2734	7674	1.6983	-30+9.5	-2936.1	100.39	28.57	61.19	658
110	34.8252	7112	1.6214	-2925.9	-2811.0	101.52	28.53	62.06	638
114	33.8832	6070	1.4723	-2672.1	-2554.0	102.05	28.27	63.73	600
116	33.3877	5551	1.3995	-2541.8	-2422.0	104.89	28.13	64.85	580
118	32.8750 32.3376	5065 4574	1.3262	-2409.2 -22/3.2	-2287.5 -2149.5	106.00 107.13	28.03 27.92	65.94 67.40	56U 539
122	31 7730	6.0.8.6	1 1920	- 2177 7	-2007 9	109 26	27 88	60.26	E 1 7
124	31.1799	3638	1.1128	-1990.4	-1862.1	109.40	27.88	71.29	495
126	30.5466	3188	1.0422	-1842.0	-1711.1	110.56	28.03	74.03	471
128	29.8661	2759	0.9713	-1686.7	-1552.8	111.75	27.85	76.92	448
132	28.3192	1910	0.8218	-1353.3	-1212.0	112.90	27.77	85.97	394
134	27.3957	1495	0.7446	-1168.5	-1022.5	115.59	28.13	94.34	363
136	26.2965	1087	0.6603	-951.0	-798.9	117.08	28.16	107.04	330
* 138.147	24.7511	614	0.5539	-703.4	-541.8	118.96	30.05	142.67	277
* 138.147	6.35753	205	0.0806	1684.9	2314.1	139.63	31.10	139.49	156
140	5.78681	294	0.0715	1844.3	2535.5	141.22	28.98	101.69	165
142	5.37988	372	0.0642	1973.4	2716.9	142.51	27.70	82.04	170
144	5.07587	438	0.0590	2081.2	2869.3	143.58	20.77	71.18	175
148	4.62739	547	0.0516	2252.8	3127.2	145.34	25.47	59.16	183
150	4.45142	595	0.0489	2343.0	3241.6	146.11	25.00	55.42	186
152	4.29688	640	0.0466	2418.5	3349.4	146.82	24.61	52.50	190
156	4.03491	723	0.0427	2558.9	3550.3	148.13	24.00	48.22	195
158	3.92182	761	0.0411	2625.2	3645.1	148.73	23.76	46.61	198
160	3.81808	798	0.0397	2689.3	3736.9	149.31	23.55	45.24	201
165	3.59123	884	0.0367	2842.3	3956.1	150.66	23.14	42.58	207
175	3.23465	965	0+0342	2907.44	4363.5	151+90	22.65	39.21	213
180	3.08977	1113	0.0303	3202.0	4556.6	154.15	22.50	38.09	223
185	2.96102	1182	0.0288	3393.9	4744.8	155.18	22.40	37.20	227
190	2.84541	1249	0.0262	3523.1	4928.9	156.16	22.34	36.48	232 23p
200	2.64524	1376	0.0251	3775.8	5287.9	158.00	22.27	35.40	240
205	2.55762	1437	0.0242	3900.0	5463.9	158.87	22.27	35.00	244
210	214/001	14,57	0.0200	402311	,	199111	22.20	54.00	240
215 220	2.40192 2.33226	1555 1612	0.0224	4145.3 4266.8	5810.6 5981.9	160.52	22.31 22.34	34.38 34.14	251 255
225	2.26721	1668	0.0210	4387.8	6152.1	162.07	22.38	33.94	258
230	2.20629	1724	0.0203	4508.4	6321.4	162.82	22.43	33.78	261
235	2.09517	1832	0.0197	4748.6	6657.8	164.25	22.55	33.52	265
245	2.04429	1885	0.0186	4868.5	6825.2	164.94	22.62	33.43	271
250	1.99616	1937	0.0182	4988.3	6992.1	165.61	22.69	33.36	274
260	1.90720	2041	0.0172	5227.8	7325.1	166.92	22.84	33.25	280
26.5	1.86598	2091	0.0168	5347.6	7491.3	167.55	22,92	33.22	282
270	1.82671	2142	0.0164	5467.6	7657.3	158.17	23.00	33.20	285
275	1.78924	2192	0.0161	5587.7	7823.3	168.78	23.09	33.19	288
285	1.71918	2241	0.0154	5828.4	8155.1	169.97	23.26	33.19	293
290	1.68637	2339	0.0150	5949.1	8321.1	170.55	23.35	33.20	296
295	1.65491	2388	0.0147	6070.1	8487.1	171.11	23.44	33.22	298
500	1:05411	2400	0.0144	01)1.0	000000	1.1.0.	20.04	00027	201

# TABLE 16. THERMODYNAMIC PROPERTIES OF FLUORINE

#### 4.5 MN/m<sup>2</sup> ISOBAR

TEMPERATURE	DENSITY	ISOTHERM	ISOCHORE	INTERNAL	ENTHALPY	ENTROPY	Cv	Сp	VELOCITY
K (1512-1969)	MOL/L	J/MOL	MN/m <sup>2</sup> -K	J/MOL	J/MOL	J/MOL-K	JIM	10L - K	M/S
* 53.920	44.9688	28458	4.3288	-6121.3	-6021.2	60.93	36.36	53.92	1054
54	44.9559	28429	4.3287	-6117.0	-6016.9	61.01	36.35	53.96	1054
56	44.6325	27451	4.3256	-6008.4	-5907.6	63.01	36.00	55.16	1052
58 60	44.3113 43.9973	26739 26485	4.2687 4.1761	-5899.3	-5797.8	54.95 66.81	35.63 35.33	55.76 55.74	1049 1049
62	43.6774	25566	4.0618	-5681.9	-5578.9	68.63	35.19	56.16	1036
64	43.3512	24222	3.9534	-5571.8	-5468.0	70.40	34.89	56.86	1019
68	42.7078	23075	3.7058	-5352.1	-5246.8	73.77	33.90	56.08	1009
70	42.3870	22114	3.5643	-5242.9	-5136.7	75.38	33.46	55.84	986
72	42.0513	20546	3.4428	-5131.9	-5024.9	76.96	33.11	56.59	961
74	41.779	19808	3.3393	-5021.5	-4913.6	78.50	32.88	56.82	949
78	41.0421	18188	3.1071	-4799.4	-4689.8	81.46	32.06	56.64	920
80	40.6986	17344	3.0014	-4688.2	-4577.6	82.89	31.77	56.86	904
82	40.3438	16242 ·	2.8954	-4575.4	-4463.9	84.30	31.40	57.40	884
86	39.6447	15034	2.6847	-4352.0	-4238.5	86.99	34.67	56.90	857
88	39.2862	14212	2.5778	-4239.2	-4124.7	88.30	30.27	56.93	839
90	38.9239	13511	2.4753	-4126.9	-4011.3	89.58	30.26	57.20	820
92	38.1750	12/54	2.2932	-401301	-3896.4	90.84	30.18	58.10	8U2 784
96	37.7940	11428	2.2053	-3783.6	-3664.5	93.31	29.66	58.26	769
98	37.4039	10783	2.1179	-3667.7	-3547.4	94.51	29.60	58.74	750
100	37.0090	10150	2.0287	-3551.0	-3429.4	95.69	29.39	58.99	732
102	36.6035	9522	1.9493	-3433.3	-3310.3	96.86	29.24	59.62	715
104	35.7688	8371	1.7867	-3194.0	-3068.2	99.17	28.83	60.42	680
108	35.3380	7798	1.7071	-3072.7	-2945.4	100.30	28.62	60.94	661
110	34.8949	7241	1.6302	-2950.0	-2821.1	101.43	28.58	61.74	642
112	34.4354 33.9647	6200	1.4824	-2698.2	-2694.1	102.55	28.43	62.75	622
116	33.4767	5685	1.4107	-2569.0	-2434.6	104.77	28.17	64.41	585
118	32.9724	5207	1.3382	-2437.7	-2301.2	105.88	28.06	65.39	565
422	71 0072	1.271	1 4 0 7 4	2465 6	2024 6	400 40	27.00	60.10	507
124	31.3145	4234	1.1278	-2024.4	-1880.7	100.12	27.89	76.31	523
126	30.6997	3344	1.0588	-1878.5	-1732.0	110.38	28.04	72.86	478
128	30.0423	2918	0.9891	-1726.3	-1576.5	111.56	27.89	75.44	456
130	29.3405	2499	0.9172	-1568.9	-1415.5	112.74	27.88	/8./1	431
134	27.7102	1687	0.7720	-1225.2	-1062.8	115.28	27.95	89.62	377
136	26.7183	1288	0.6934	-1003.7	-835.2	116.68	28.03	99.14	346
138	25.5267	899	0.6118	-800.0	-623.8	118.22	28.53	116.66	311
8 1/D 955	22 84.70	305	0.4507		- 20/ 6	124 22	70.07	246.05	202
* 140.855	7.87301	123	0.1055	1501.1	2072.6	137.39	34.06	240.05	151
142	7.14432	201	0.0927	1664.6	2294.5	138.96	31.32	149.90	159
144	6.44627	297	0.0800	1844.6	2542.7	140.70	28.95	103.66	167
146	5.64689	370	0.0725	1978.2	2887.5	141.98	26.71	73.82	174
150	5.37088	494	0.0619	2189.3	3027.2	144.00	26.00	66.34	182
152	5.14031	547	0.0582	2278.9	3154.3	144.84	25.44	61.04	186
154	4.94221	596	0.0551	2361.7	3272+2	145.61	24.99	57.08	189
158	4.61398	685	0.0501	2513.3	3488.6	147.00	24.29	51.51	195
160	4.47479	726	0.0481	2583.9	3589.5	147.63	24.02	49.47	198
165	4.17777	821	0.0439	2749.6	3826.7	149.09	23.50	45.67	205
170	3.72715	909	0.0379	2904.2	4040.2	150.42	22.88	43.05	211
180	3.54857	1067	0.0356	3192.2	4460.3	152.77	22.69	39.68	222
185	3.39168	1140	0.0337	3329.0	4655.8	153.84	22.57	38.55	226
190	3.25211	1210	0.0320	3462.4	4846.1	154.86	22.48	37.64	231
200	3.01301	1343	0.0291	3721.9	5215.4	156.75	22.39	36.30	239
205	2.90928	1407	0.0279	3848.9	5395.7	157.64	22.38	35.81	243
210	2.81406	1469	0.0268	3974.5	5573.6	158.50	22.38	35.39	247
215	2.72618	1529	0.0259	4099.0	5749.7 5924.1	159.33	22.40	35.04	251
225	2.56890	1646	0.0241	4345.5	6097.2	160.91	22.46	34.50	258
230	2.49819	1703	0.0233	4467.7	6269.1	161.67	22.51	34.29	261
235	2.43175	1759	0.0226	4589.6	6440.1	162.40	22.56	34.11	265
245	2.31068	1869	0.0213	4832.3	6779.8	163.82	22.68	33.84	271
250	2.25522	1923	0.0207	4953.4	6948.7	164.50	22.75	33.74	274
255 260	2.20274	1976 2028	0.0202	5074.3 5195.2	7117.2 7285.4	165.17 165.82	22.82	33.66 33.59	277 280
265	2.10570	2080	0.0192	5316.1	7453.2	166,46	22.98	33-54	283
270	2.06072	2132	0.0187	5437.1	7620.8	167.09	23.06	33.50	286
275	2.01785	2183	0.0183	5558.1	7788.2	167.70	23.14	33.48	288
280	1.97694	2233	0.0179	5679.3	7955.6	168.30	23.23	33.46	291
205	1.90041	2203	0.0175	5922.2	8290.1	169.48	23.40	33.45	296
295	1.86456	2382	0.0167	6043.9	8457.4	170.05	23.49	33.46	299
300	1.83017	2431	0.0164	6165.9	8624.7	170.61	23.58	33.47	301

## 5.0 MN/m² ISOBAR

TEMPERATURE	OENSITY	ISOTHERM	ISOCHORE	INTERNAL	ENTHALPY	ENTROPY	Cv	Cp	VELOCITY
(IPIS 1968) K	MOL/L	J/MOL	MN/m <sup>2</sup> - K	ENERGY J∕MOL	JZMOL	J∕MOL≁K	J / MC	)L – K	M/S
* 53,968	44.9785	28627	4.3305	-6131.8	=6020.6	50.94	36.35	53.82	1056
54	44.9734	28615	4.3305	-6130.0	-6018.9	60.98	36.34	53.84	1u56
56	44.6506	27577	4.3272	-6021.7	-5909.7	62.98	35.99	55.06	1054
60	44.0162	26567	4.1830	-5804.9	-5691.3	66.77	35.82	55.72	1051
62	43.6969	25594	4.0651	-5695.9	-5581.5	68.58	35.21	56.18	1037
66	43.0456	23307	3.8529	-5475.8	-5359.7	72.08	34.52	57.21	1019
68	42.7294	23117	3.7110	-5366.7	-5249.7	73.73	33.93	56.11	1003
70	42.4096	22181	3.5696	-5257.7	-5139.8	75.33	33.48	55.83	987
74	41.7428	19812	3.3416	-5036.9	-4917.1	78.45	32.92	56.86	949
76	41.4061	19097	3.2330	-4925.9	-4805+1	79.95	32.52	56.79	937
78 80	41.0695 40.7274	18234 17393	3.1119 3.0044	-4815.4 -4704.5	-4693.7 -4581.7	81.41 82.83	32.10 31.82	56.66 56.85	920 904
82	40.3746	16273	2.8986	-4592.1	-4468.3	84.24	31.45	57.43	884
84	40.0301	15907	2.7969	-4481.2	-4356.3	85.60	31.09	56.87	875
88	39.3213	14293	2.5845	-4256.9	-4129.7	88.24	30.30	56.90	840
90	38.9607	13615	2.4817	-4145.0	-4016.6	89.52	30.30	57.12	822
92	38.5918	12850	2.3891	+4031.6	-3902.0	90.78	30.23	57.67	803
96	37.8376	11529	2.2100	-3803.0	-3670.8	93.24	29.72	58.12	770
98 100	37.4501 37.0580	10883 10258	2.1239 2.0352	-3687.6 -3571.5	-3554.1 -3436.5	94.44 95.62	29.66 29.45	58.63 58.86	752 734
102	36.6557	9626	1.9553	-3454.3	-3317.9	96.79	29.31	59.46	717
104	36.2452	9012	1.8747	-3335.8	-3197.9	97.95	29.18	60.05	699
106	35.8282	8487	1.7941	-3216.3	-3076.8	99.09	28.89	60.69	682
110	34.9634	7369	1.6390	-2973.9	-2830.9	101.33	28.63	61.43	645
112	34.5097	6795	1.5660	-2849.6	-2704.7	102.45	28.48	62.43	626
114	34.0445	6328	1.4927	-2723.9	-2577.0	103.56	28.36	62,99	608
118	33.0671	5345	1.3504	-2465.8	-2314.6	105.77	28.09	64.91	570
122	72 0007	4001	1 2100	-2106 8	-2040 6	107 08	27 92	67 78	529
124	31.4438	3941	1.1422	-2057.5	-1898.5	109.09	27.90	69.42	508
126	30.8459	3497	1.0747	-1914.1	-1752.0	110.22	28.05	71.79	485
128	30.2092	3073	1.0059	-1/64+7	-1599.2	111.37	27.93	74+11	463
132	28.7990	2262	0.8672	-1448.5	-1274.9	113.74	27.67	80.57	416
134	27.9916	1868	0.7966	-1277.8	-1099.2	114.99	27.82	85.92	390
136	27.0801	1479	0.7227	-1049.4	-864.8	116.32	27.92	93.42	361
140	24.7137	743	0.5654	-644.3	-442.0	119.38	29.00	127.69	293 .
142	22.7963	357	0.4555	-360.7	-141.4	121.51	30.16	188.83	243
* 143.322	10.3573	37	0.1498	1179.1	1661.8	134.11	38.38	841.03	147
144	9.02334	108	0.1249	1416.2	1970.3	136.25	34.21	288.84	155
146	7.67269	229	0.0993	1699.3	2351.0	138.88	30.31	136.94	165
150	6.51104	387	0.0783	2002.3	2770.2	141.72	27.30	83.49	176
152	6.14910	449	0.0728	2114.4	2927.6	142.76	26.48	73.99	182
154	5.85075	506	0.0682	2214.7	3069.3	143.69	25.84	67.10	186
158	5.38845	559	0.0607	2389.8	3317.7	145.28	24.89	57.94	193
160	5.20038	653	0.0579	2468.9	3430.4	145.99	24.54	54.85	196
165	4.81132	758 853	0.0521	2650.6	3689.9	147.59	23.88	49.38 45.81	203
175	4.24553	940	0.0442	2972.0	4149.7	150.30	23.11	43.30	215
180	4.02757	1021	0.0413	3119.9	4361.3	151.49	22.89	41.44	221
185	3.67190	1172	0.0368	326202	4761.9	152.65	22.62	38.89	230
195	3.52342	1243	0.0350	3535.0	4954.1	154.65	22.55	37.99	235
200	3.38977	1311	0.0333	3667.1	5142.1	155.60	22.50	37.25	239
205 210	3.26850 3.15770	1377 1442	0.0319	3797.0 3925.3	5508.7	156.52	22.48	36.65 36.14	243 247
215	3.05588	1504	0.0294	4052.2	5688.4	158.24	22.49	35.72	251
220	2.96184	1565	0.0283	4177.9	5066+1	159.00	22.54	35.30	254
230	2.79335	1684	0.0264	4426.8	6216.8	160.62	22.58	34.81	261
235	2.71741	1741	0.0256	4550.3	6390.3	161.36	22.63	34.59	265
240	2.64623	1/98	0.0248	4013.3	6734.5	162.80	22.74	34.26	268
250	2.51622	1909	0.0234	4918.3	6905.4	163.49	22.81	34.13	274
255 260	2.45662 2.40020	1963 2017	0.0228 0.0222	5040.5 5162.5	7075.8 7245.7	164.16 164.82	22.88 22.95	34.02 33.94	277 280
265	2.34667	2070	0.0216	5284.5	7415.2	165.47	23.03	33.87	283
270	2.29581	2122	0.0211	5406.5	7584.4	166.10	23.11	33.81	286
275	2.24738	2174	0.0206	5650.6	7922.1	167.33	23.27	33.73	289
285	2.15714	2277	0.0196	5772.8	8090.7	167.92	23.36	33.71	294
290	2.11500	2327	0.0192	5895.2	8259.2	168.51	23.49	33.70	297
300	2.03600	2427	0.0184	6140.4	8596.2	169.65	23.63	33.70	302
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#### TABLE 16. THERMOOYNAMIC PROFERTIES OF FLUORINE

# 5.5 MN/m<sup>2</sup> ISOBAR

TEMPERATURE	OENSITY	ISOTHERM	ISOCHORE	INTERNAL	ENTHALPY	ENTROPY	Cv	Cp	VELOCITY
К К	MOL/L	J/MOL	MN/m <sup>2</sup> - K	J/MOL	J/MOL	J/MOL-K	J / M	о <b>с -</b> к	MIS
÷ 54.017	44.9882	28787	4.3322	-6142.2	-6019.9	60.96	36.33	53,73	1059
56	44.6687	27704	4.3287	-6035.0	-5911.9	62.94	35.99	54.97	1055
58 60	44.3486 44.0350	26912 26648	4.2823 4.1897	-5926.4 -5818.5	-5802.4 -5693.6	64.87 66.73	35.62 35.32	55.71 55.70	1053 1052
62	43.7164	25627	4.0690	-5709.8	-5584.0	68.54	35.23	56.19	1037
64	43.3925	24186	3.9516	-5600.2	-5473.4	70.31	34.97	56.91	1018
68	43.0670	23310	3.0919	-5381.2	-5252.6	72.03	34.51	56.14	1008
70	42.4321	22250	3.5748	-5272.5	-5142.9	75.29	33.49	55.82	988
72	42.0998	20638	3.4538	-5162.2	+5031.5	76.87	33.15	56.63	963
74	41.7680	19826	3.3443	-5052.3	-4920.7	78.40	32.96	56.89	949
78	41.0969	18284	3.1165	-4831.3	-4697.5	81.36	32.14	56.67	921
80	40.7561	17446	3.0076	-4720.7	-4585.8	82.78	31.86	56.84	905
82 84	40.4053 40.0614	16312 15969	2.9017 2.8008	-4608.8 -4498.1	-4472.7 -4360.8	84.19 85.54	31.50 31.14	57.43 56.85	885 876
86	39.7109	15183	2.6956	-4386.5	-4248.0	86.88	30.75	56.85	859
88	39.3562	143/9	2.5909	-4274.5	-4134.7	88.18	30.34	56.86	842
92	38.6306	12947	2.3947	-4050.0	-3907.6	90.72	30.29	57.60	805
94	38.2573	12233	2.3030	-3936.3	-3792.5	91.96	30.09	57.94	787
96	37.8808	11631	2.2148	-3822.3	-3677.1	93.17	29.77	57.99	772
100	37.1065	10367	2.0419	-3591.8	-3443.5	95.55	29.52	58.73	737
102	36.7074	9732	1.9614	-3475.2	-3325.4	96 <b>.7</b> 1 97.87	29.37	59.29	719
106	35.8867	8602	1.8015	- 3238.5	-3085.2	99.01	28.95	60.00	685
108	35.4643	8044	1.7239	-3118.6	-2963.5	100.13	28.72	60.44	668
110	35.0306	7496	1.6482	-2997.5	-2840.5	101.24	28.67	61.15	649
114	34.1227	6454	1.5032	-2749.4	-2588.2	102.36	28.40	62.68	612
116	33.6486	5947	1.4326	-2622.5	-2459.0	104.56	28.25	63.61	594
118 120	33.1595 32.6510	5480 5001	1.3624 1.2930	-2493.5	-2327.6	106.75	28.12	64.47 65.63	575
122	32.1216	4522	1.2247	-2227.5	-2056.3	107.85	27+93	67.15	535
124	31,9859	4087	1.1566	-2090.0 -1948.7	-1915.7	108.95	27.91	68.64 70.81	514
128	30.3680	3225	1.0223	-1801.8	-1620.7	111.20	27.96	72.93	471
130	29.7165	2823	0.9548	-1650.9	-1465.8	112.34	27.83	75.36	449
132	29.0123	2428	0.8192	-1492.7	-1303+1	113.52	27.73	18.51	426
136	27.3989	1661	0.7498	-1090.2	-889.4	116.01	27.81	89.13	374
138 140	26.4371 25.3035	1310 958	0.6793 0.6034	-912.6 -715.9	-704.5 -498.6	117.36 118.84	27.78 28.30	97.33 111.41	348 315
142	23.8512	604	0.5162	-483.2	-252.6	120.58	29.01	139.14	276
144	21.6567	267	0.4098	-171.2	82.8	122.93	30.95	223.92	226
148	9.04992	179	0.1215	1542.8	2150.5	132.03	31.35	180.35	165
150	8.04361	272	0.1028	1759.0	2442.7	139.07	29.07	119.29	171
152	7.41155	347	0.0925	1914.3	2656.4	140.49	27.74	95.99	178
156	6.57626	414	0.0782	2152.0	2988.4	142.65	26.13	72.73	186
158	6.27296	528	0.0737	22-0.9	3127.7	143.53	25.58	66.84	191
160	6.01379	579	0.0698	2341.8	3256.4	144.34	25.14	62.39	195
165 170	5.49979 5.10815	695 797	0.0614 0.0556	2544.5 2724.1	3544.5 3800.9	146.12 147.65	24.29	53.86 49.01	201 208
175	4.79212	890	0.0511	2889.5	4037.2	149.02	23.36	45.73	214
180	4.52814	977	0.0475	3045.0	4259.7	150.27	23.09	43.37	220
190	4.30220	1136	0.0445	3336.6	4471.9	152.53	22.90	41.60	225
195	3.93124	1209	0.0397	3475.5	4874.6	153,56	22.68	39.13	234
200	3.77567	1280	0.0378	3611.3	5068.0	154.54	22.62	38.25	239
205	3.50774	1349	0.0345	3875.5	5443.5	155.47	22.59	36.93	243
215	3.39099	1480		4004.9	5626.8	157.23	22.57	36.43	251
225	3.18423	1605	0.0307	4259.7	5987.0	158.87	22.62	35.65	258
230	3.09198	1665	0.0296	4385.6	6164.4	159.65	22.65	35.34	261
235	3.00598	1724	0.0287	4510.8	6340.5	160.41	22.70	35.09	265
245	2.85008	1839	0.0269	4759.4	6689.2	161.86	22.80	34.68	271
250	2.77907	1896	0.0261	4883.1	6862.2	162.56	22.87	34.53	274
255 260	2.71210 2.64879	1951 2006	0.0254 0.0247	5006.5 5129.7	7034.5 7206.2	163.24 163.91	22.93 23.00	34.39 34.28	278 280
265	2.58882	2060	0.0241	5252.8	7377.3	164.56	23.08	34.19	283
275	2.47778	2113	0.0229	5498.8	7718.5	165.82	23.24	34.06	289
280	2.42623	2219	0.0223	5621.8	7888.7	166.44	23.32	34.01	292
285	2.37706	2271	0.0218	5744.9	8058.7	167.04	23.40	33.97	295
295	2.28518	2322	0.0213	5991.4	8398.2	168.21	23.49	33.95	300
300	2.24216	2424	0.0204	6114.8	8567.8	168.73	23.66	33.92	302

## 6.0 MN/m<sup>2</sup> ISOBAR

TEMPERATURE	OENSITY	ISOTHERM	ISOCHORE	INTERNAL	ENTHALPY	ENTROPY	Cv	Сp	VELOCITY
(IPIS 1968) K	MOL/L	J/MOL	MN/m <sup>2</sup> -K	J/MOL	J/MOL	J/MOL-K	J / M	оц <del>-</del> к	M/S
* 54.065	44,9977	28915	4.3337	-6152.6	-6019.2	60.97	36.32	53.66	1060
56	44.6867	27829	4.3302	-6048.3	-5914.0	62.90	35.98	54.87	1057
58 60	44.3671 44.0537	26998 26730	4.2889 4.1963	-5939.9 -5832.2	-5804.7 -5696.0	64.83 66.69	35.61 35.31	55.69 55.68	1054 1053
62	43.7359	25665	4.0735	-5723.7	-5586.5	ő8.50	35.25	56.21	1038
64	43.4132	24183	3.9509	-5614.4	-5476+2	70.27	35.01	56.93	1017
66	43.0885	23320	3.8502	-5504.7	-5365.4	71.99	34.62	57.21	1007
70	42.4545	22321	3,5801	-5287.2	-5145.9	75.24	33.51	55.81	989
72	42.1240	20692	3.4594	-5177.3	-5034.9	76.82	33.17	56.64	964
74	41.7932	19849	3.3474	-5067.7	-4924.2	78.35	33.00	56.91	949
76	41.1242	19149	3+2382	-4957.2	-4812.4	79.85	32.62	56.67	922
80	40.7847	17504	3.0109	-4736.9	-4589.8	82.73	31.91	56.82	906
82 84	40.4359 40.0927	16359 16033	2.9047 2.8046	-4625.4 -4514.9	-4477.0	84.13 85.49	31.56 31.19	57.42 56.82	885 877
86	39.7437	15262	2.7008	-4403.7	-4252.7	86.82	30.80	56.82	861
88	39.3908	14466	2.5970	-4292.0	-4139.7	88.13	30.38	56.82	844
92	38.6691	13046	2.4008	-4068.4	-3913.2	90.65	30.34	57.52	807
94	38.2981	12326	2.3083	-3955.1	-3798.4	91.89	30.15	57.85	789
96	37.9236	11734	2.2197	-3841.4	-3683.2	93.11	29.83	57.86	756
100	37.1545	10476	2.0488	-3612.0	-3450.5	95.48	29.58	58.60	739
102	36.7585	98 <b>3</b> 9 9222	1.9675	-3496.0	-3332.8	96.64 97.79	29.42 29.30	59.12 59.76	721 704
106	35.9444	8718	1.8087	-3260.4	-3093.5	98.92	29.00	59.79	688
108	35.5260	8167	1.7323	-3141.3	-2972.4	100.05	28.76	60.20	671
112	34.6542	7049	1.5850	-2898.5	-2725.4	102.26	28.58	61.82	633
114	34.1995	6578	1.5134	-2774.5	-2599.1	103.36	28.43	62.37	616
116	33.7318	6077	1.4433	-2648.7	-2470.8	104.45	28.29	63.24	598
120	32.7497	5137	1.3053	-2390.5	-2207.3	106.63	28.02	65.13	>61
122	32.2305	4664	1.2379	-2257.6	-2071.5	107.72	27.95	66.54	541
124	31.6886	4231	1.1049	-2121.7	-1932.4	108.81	27.93	67.94 69.94	52U 499
128	30.5195	3374	1.0384	-1837+9	-1641.4	111.03	27.97	71.88	478
130	29.8889	2979	0.9716	-1689.7	-1489.0	112.15	27.83	73.95	456
132	29.2116	2589	0.9067	= 1535+0 = 1374+0	-1329.6	113.31	27.65	76.73	435
136	27.6849	1837	0.7743	-1127.1	-910.4	115.72	27.72	85.64	386
138 140	26.7941 25.7780	1493 1153	0.7035 0.6351	-957.6 -774.6	-733.7 -541.8	117.01 118.39	27.61 27.92	91.33 101.63	361 332
142	24.5584	817	0.5603	-568.2	-323.9	119.93	28.36	118.84	3 O U
144	22.9795	506	0.4742	-322.8	-61.7	121.77	29.06	150.33	262
146	14.2507	215	0.2125	814.0	1235.1	130.61	36.83	630.39	158
150	10.4630	154	0.1439	1395.2	1968.7	135.54	31.87	216.20	166
152	9.12224	244	0.1208	1653.2	2310.9	137.81	29.43	138.71	174
156	7.74012	389	0.0963	1973.3	2748.5	140.66	27.02	89.06	184
158	7.29777	450	0.0893	2093.6	2915.8	141.72	26.30	78.84	188
160	6.93624	507	0.0837	2200.4	3065.5	142.67	25.74	/1./0	193
165	6.25485 5.75736	632 744	0.0726	2429.6 2626.4	3388.9 3668.5	144.66	24.07	59.87 52.73	201 207
175	5.36932	843	0.0587	2803.3	3920.8	147.79	23.61	48.46	213
180	5.05161	934	0.0542	2967.5	4155.3	149.11	23.29	45.49	219
190	4.55267	1100	0.0505	3271.3	4589.3	151.46	22.92	41.65	229
195	4.35034	1177	0.0448	3414.9	4794.1	152.52	22.81	46.34	234
200	4.17079	1251	0.0424	3554.5	4993.1	153.53	22.74	39.30	239
210	3.86415	1390	0.0386	3825.1	5377.8	155.41	22.67	37.74	243
215	3.73147	1457	0.0370	3957.0	5565.0	156.29	22.66	37 • 15	251
225	3.49772	1585	0.0342	4216.3	5931.7	157.96	22.69	36.24	258
230	3.39390	1647	0.0330	4344.1	6112.0	158.75	22.72	35.89	262
235	3.29737	1708	0.0318	44/1.0	6290.7	159.52	22.81	35.33	265
245	3.12292	1826	0.0298	4722.7	6644.0	150.99	22.86	35.11	272
250	3.04370	1883	0.0289	4847.8	6819.1	161.70	22.92	34.92	275
255	2.96911 2.89870	1940 1996	0.0281	5096.9	7166.8	163.06	23.06	34.63	281
265	2.83208	2051	0.0266	5221.0	7339.6	163.72	23.13	34.52	284
270	2.70893	2105	0.0253	5469.0	7683.9	165.00	23.28	34.43	290
280	2.65190	2213	0.0246	5593.0	7855.5	165.61	23.36	34.29	292
285	2.59753	2265	0.0235	5/16.9	8197.9	166.81	23.53	34.24	295
295	2.49604	2369	0.0230	5965.0	8368.8	167.40	23.61	34.17	300
300	2,44858	2421	0.0225	6089.2	8539.6	167.97	23.70	34.15	303

## 6.5 MN/m<sup>2</sup> ISOBAR

TEMPERATURE (IPTS 1968)	DENSITY	ISOTHERM OERIVATIVE	ISOCHORE DERIVATIVE	INTERNAL ENERGY	ENTHALPY	ENTROPY	Cv	Сp	VELOCITY OF SOUNO
к	MOL/L	J/MOL	MN/m <sup>2</sup> - K	J/MOL	J/MOL	J/MOL-K	JZM	οL - Κ	M/S
* 54.113	45.0072	29041	4.3352	-6163.0	-6018.6	60.98	36.30	53.59	1062
56	44.7047	27955	4.3317	-6061.5	-5916.1	62.86	35.97	54.78	1058
58 60	44.3856 44.0724	27083 26811	4.2955 4.2029	-5953.4 -5845.9	-5807.0 -5698.4	64.79 66.65	35.61 35.31	55.66 55.66	1056
62	43.7554	25709	4.0786	-5737.6	-5589.1	68.46	35.27	56.22	1039
64	43.4339	24190	3.9504	-5628.5	-5478.9	70.22	35.05	56.93	1017
66	43.1099	23337	3.8490	-5519.1	-5368.3	71.94	34.66	57.21	1007
68	42 .7941	23254	3.1231	-5410.2	-5258.4	73.60	34.02	56.16	1005
70	42.4709	20753	3.2024	-5192.4	-5149.0	76.77	33.19	55.64	990
74	41.8184	19881	3.3508	-5083.1	-4927.7	78.30	33.03	56.93	950
76	41.4845	19185	3.2405	-4972.8	-4816.1	79.80	32.67	56.85	937
78	41.1514	18397	3.1248	-4863.1	-4705.1	81.26	32.22	56.67	923
80	40.8132	17566	3.0144	-4753.1	-4593.9	82.68	31.95	56.80	906
82	40.4664	16414	2.9076	-4642.0	-4481.3	84.08	31.61	57.40	886
86	39.7764	15342	2.7058	-4420.8	-4257.4	86.76	30.84	56.78	862
88	39.4253	14556	2.6028	-4309.5	-4144.6	88.07	30.42	56.77	846
90	39.0697	13926	2.5036	-4198.6	-4032.3	89.34	30.38	56.92	829
92	38.7073	13147	2.4072	-4086.6	-3918.7	90.59	30.39	57.46	809
94	38.3385	12422	2.3139	-3973.8	-3804.2	91.83	30.20	57.77	791
96	37.9660	11838	2 4 2 2 4 8	-3860.5	-3689.3	93.04	29.88	5/ 1/3	776
100	37.2020	10586	2.0558	-3632.0	-3457.3	95.41	29.64	58.48	750
	76 0000	001.0	4 0 7 7 7	7646 6	771.0.0	04 57	20 ( 7	50.05	70(
102	36.8090	9948	1 8966	-3516.6	-3340.0	96.97	29.47	50.95	724
104	36.0014	8833	1.8160	-3282.3	-3221.5	98.84	29.05	59.59	690
108	35.5867	82 89	1.7408	-3163.7	-2981.1	99.96	28.81	59.99	674
110	35.1618	7749	1.6671	-3044.2	-2859.3	101.07	28.74	60.65	656
112	34.7245	7178	1.5945	-2922.6	-2735.4	102.17	28.62	61.52	637
114	34.2748	6701	1.5234	-2799.5	-2609.8	103.26	28.47	62.08	620
116	33.8132	6205	1.4538	-26/4.6	-2482.3	104.35	28.32	62.88	602
120	32.8457	5271	1.3173	-2418.7	-2220.8	106.51	28.05	64.66	566
122	32.3361	4804	1.2507	-2287.2	-2086.2	107.59	27.97	65.96	546
124	31.8049	4372	1.1847	-2152.9	-1948.5	108.67	27.94	67.29	526
126	31.2497	3938	1.1194	-2015.4	-1807.4	109.76	28.07	69.13	505
128	30.6646	3521	1.0543	-1873.1	-1661.1	110.87	27.97	70.94	485
130	30.0526	3131	0.9877	-1/2/+3	-1511.0	111.98	27.84	72.70	464
134	29.3991	2745	0.8604	-15/5+/	=1192.1	114.26	27.59	78.36	444
136	27.9453	2006	0.7965	-1160.9	-928.3	115.45	27.64	82.71	398
138	27.1107	1667	0.7292	-998.0	-758.2	116.70	27.48	87.37	374
140	26.1804	1335	0.6633	-824.9	-576.6	118.00	27.66	94.96	347
142	25.1066	1012	0.5963	-635.4	-376.5	119.42	27.99	107.15	319
144	23.8061	(12	0.5196	-420.6	-147.6	121.02	28.30	124.64	287
140	19.5430	433	0.34070	-103.3	525.9	125.63	29.40	256.41	207
150	15.0599	94	0.2296	784.5	1216.1	130.26	33.98	403.14	172
152	11.7077	155	0.1658	1284.0	1839.2	134.39	31.54	228.35	172
154	10.1336	235	0.1382	1564.7	2206.1	136.79	29.43	151.22	178
156	9.18237	309	0.1199	1759.2	2467.0	138.47	28.07	114.20	182
158	8.51353 7.99852	376	0.1088 0.1004	1912.1 2041.4	2679.6	139.60	26.40	95.80 84.09	187
165	7 09629	5 <b>7</b> 2	0 0050	2705 2	7222 5	1/ 7 10	25 10	66 67	200
170	6.45711	690	0.0747	2522.3	3528.9	145.02	24.41	57.44	207
175	5.97947	797	0.0671	2713.3	3800.4	146.60	23.88	51.53	213
180	5.59919	893	0.0615	2887.3	4048.2	147.99	23.50	47.82	219
185	5.28338	982	0.0570	3050.0	4280.3	149.27	23.25	45.16	224
190	5.01438	1066	0.0533	3204.6	4500.9	150.44	23.07	43.17	229
195	4.78087	1146	0.0501	3353.1	4/12.7	151.54	22.94	41.62	234
205	4.39185	1296	0.0474	3637.0	5117.0	153.57	22.80	39.40	243
210	4.22687	1367	0.0429	3774.1	5311.8	154.51	22.77	38.56	247
215	4.07722	1435	0.0410	3908.8	5503.0	155.40	22.75	37.90	251
220	3.94054	1502	0.0393	4041.5	5691.0	156.27	22.75	37.33	255
225	3.81497	1567	0.0378	4172.6	5876.4	157.10	22.77	36.85	258
230	3.69902	1630	0.0364	4302.4	6059.6	157.91	22.80	36.44	262
239	3.49147	1753	0.0351	4431+1	6420.6	159.44	22.87	35.79	269
245	3.39775	1813	0.0328	4685.9	6598.9	160.18	22.92	35.54	272
250	3.31003	1872	0.0318	4812.4	6776.1	160.90	22.98	35.32	275
255	3.22755	1929	0.0309	4938.3	6952.2	- 161.59	23.04	35.14	278
260	3.14982	1986	0.0300	5063.9	7127.5	152.27	23.10	34.98	281
265	3.07638	2043	0.0292	5189.2	7302.1	162.94	23.17	34.85	284
275	3.00684	2098	0.0284	5430 2	7640	164 23	23.32	34.64	290
280	2.87817	2207	0.0270	5564.0	7822.4	164.85	23.40	34.56	293
285	2.81848	2261	0.0263	5688.8	7995.1	165.46	23.48	34.50	296
290	2.76156	2314	0.0257	5813.7	8167.4	166.06	23.56	34.44	298
295	2.70721	2366	0.0251	5938.5	8339.5	166.65	23.65	34.41	301
300	2.65523	2418	0.0246	6063.5	6511.5	167.23	23.73	34.38	304

\* TWO-PHASE BOUNDARY

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#### 7.0 MN/m<sup>2</sup> ISOBAR

TEMPERATURE (IPTS 1968) K	OENSITY MOL/L	ISOTHERM DERIVATIVE J/MOL	ISOCHORE OERIVATIVE MN/m²-K	INTERNAL ENERGY J/MOL	ENTHALPY J/MOL	ENTROPY J/MOL-K	C <sub>V</sub> J / M	С <sub>р</sub> оц. – к	VELOCITY OF SOUND M/S
* 54.102 56 58 60	45.0167 44.7225 44.4041 44.0910	29165 20079 27169 26892	4.3367 4.3331 4.3020 4.2094	-6173.4 -6074.7 -5966.9 -5859.5	-6017.9 -5918.2 -5809.2 -5700.7	60.99 62.82 64.75 66.61	36.29 35.97 35.60 35.30	53.53 54.69 55.64 55.64	1064 1060 1057 1056
62 64 68 70 72 74 76 78 80	$\begin{array}{c} 43.7748\\ 43.4545\\ 43.1313\\ 42.8156\\ 42.4992\\ 42.1722\\ 41.8435\\ 41.5105\\ 41.1786\\ 40.8416 \end{array}$	25758 24208 23363 23305 22469 20819 19923 19226 18461 17632	4.0842 3.9500 3.8480 3.7271 3.5907 3.4706 3.3546 3.2425 3.1286 3.0179	-5751.5 -5642.6 -5533.4 -5424.7 -5216.7 -5207.4 -5098.4 -4988.3 -4878.9 -4769.3	-5591.6 -5481.6 -5371.1 -5261.2 -5152.0 -5041.5 -4931.1 -4619.7 -4708.9 -4597.9	58.42 70.18 71.90 73.55 75.15 76.73 78.25 79.75 81.21 82.63	35.29 35.08 34.71 34.05 33.55 33.22 33.07 32.72 32.26 32.00	56.24 56.93 57.19 56.16 55.79 56.64 56.94 56.84 56.66 56.77	1039 1017 1007 992 967 950 938 924 907
82 84 86 90 92 94 96 98 100	40.4968 40.1548 39.8089 39.4595 39.1054 38.7451 38.3786 38.0080 37.6305 37.2490	16477 16170 15425 14649 14029 13249 12520 11942 11294 10696	2.9104 2.8117 2.7106 2.6084 2.5107 2.4140 2.3196 2.2302 2.1479 2.0630	-4658.5 -4548.4 -4437.8 -4326.9 -4216.4 -4104.8 -3992.4 -3766.1 -3652.0	-4485.6 -4374.1 -4262.0 -4149.5 -4037.4 -3924.1 -3810.0 -3695.4 -3580.1 -3464.1	84.02 85.38 86.71 88.01 89.28 90.53 91.76 92.97 94.16 95.34	31.06 31.28 30.89 30.46 30.41 30.44 30.25 29.87 29.87 29.69	57.37 56.75 56.74 56.71 56.86 57.39 57.68 57.68 57.61 58.14 58.37	886 879 864 847 831 811 793 778 761 744
102 104 106 108 110 112 114 116 118 120	36.8590 36.4621 36.0576 35.2258 34.7935 34.3487 33.8930 33.4238 32.9394	10057 9440 8948 8410 7874 7307 6823 6332 5871 5404	1.9800 1.9042 1.8242 1.7493 1.6762 1.6041 1.5331 1.4642 1.3963 1.3290	-3537.1 -3421.1 -3303.9 -3186.0 -3067.2 -2946.5 -2824.1 -2700.2 -2574.4 -2446.5	-3347.2 -3229.2 -3109.8 -2989.7 -2668.4 -2745.3 -2620.3 -2493.7 -2365.0 -2234.0	96.49 97.64 98.77 99.88 100.98 102.08 103.17 104.25 105.32 106.40	29.52 29.41 29.10 28.85 28.77 28.66 28.50 28.35 28.21 28.07	58.78 59.45 59.43 59.77 60.41 61.24 61.79 62.54 63.28 64.22	726 693 677 660 641 624 626 589 570
122 124 126 128 130 132 134 136 138 140	32.4387 31.9174 31.3744 30.8037 30.2086 29.5764 28.9052 28.1847 27.3965 26.5323	4943 4511 3666 3280 2898 2530 2171 1834 1509	1.2630 1.1980 1.1333 1.0694 1.0044 0.9421 0.8792 0.8173 0.7532 0.6880	-2316.3 -2183.4 -2047.7 -1907.4 -1763.8 -1615.0 -1461.3 -1192.2 -1034.7 -869.4	-2100.6 -1964.1 -1824.6 -1680.2 -1532.1 -1378.4 -1219.1 -943.9 -779.2 -605.5	107.47 108.54 109.62 110.71 111.81 112.92 114.05 115.21 116.41 117.66	27.98 27.95 28.08 27.97 27.86 27.56 27.55 27.55 27.38 27.45	65.40 66.67 68.37 70.06 71.68 73.77 76.56 80.25 84.25 89.85	551 532 511 492 471 452 430 408 385 360
142 144 146 150 152 154 156 158 160	25.5604 24.4278 23.0625 21.2920 18.7769 15.3569 12.6285 11.0175 9.98193 9.23686	1195 902 630 210 139 176 242 310 374	0.6272 0.5566 0.4856 0.4069 0.226 0.2358 0.1825 0.1825 0.1517 0.1335 0.1208	-691.8 -496.0 -275.0 -8.4 343.8 811.9 1222.8 1499.4 1700.7 1861.5	-417.9 -209.5 28.5 320.4 716.6 1267.7 1777.1 2134.8 2402.0 2619.3	118.99 120.45 122.09 124.07 126.73 130.38 133.71 136.02 137.72 139.09	27.73 27.94 28.51 29.63 30.85 31.54 30.62 29.10 27.95 27.08	99.29 110.87 131.24 167.69 241.94 288.55 213.05 151.07 151.07 19.21 100.34	336 307 276 241 208 183 180 182 186 186
165 170 175 180 185 190 195 200 205 210	8.00665 7.20996 6.62813 6.17322 5.80194 5.49060 5.22287 4.98879 4.78144 4.59580	516 640 750 851 947 1034 1117 1196 1271 1344	0.0993 0.0859 0.0766 0.0697 0.0639 0.0595 0.0557 0.0557 0.0525 0.0498 0.0498	2170.3 2411.9 2618.6 2834.1 2975.3 3136.4 3290.2 3438.4 3582.2 3722.5	3044.5 3382.7 3674.7 3938.0 4181.8 4411.3 4630.4 4841.5 5046.2 5245.6	141.71 143.73 145.43 146.91 148.25 149.47 150.61 151.68 152.69 153.65	25.65 24.75 24.15 23.72 23.42 23.22 23.07 22.97 22.90 22.86	74.81 62.51 55.31 50.64 47.14 44.77 42.96 41.53 40.38 39.44	199 206 213 219 224 239 234 239 243 243
215 220 225 230 235 240 245 250 255 260	4.42813 4.27556 4.13585 4.00721 3.88818 3.77760 3.67446 3.57794 3.48735 3.40208	1415 1483 1550 1615 1678 1740 1801 1861 1920 1978	0.0452 0.0432 0.0415 0.0309 0.0385 0.0371 0.0359 0.0348 0.0337 0.0337	3860.0 3995.3 4128.6 4260.4 4391.0 4520.4 4649.0 4776.8 4904.1 5030.9	5440.8 5632.5 5821.2 6007.3 6191.3 6373.4 6554.0 6733.3 6911.3 7088.4	154.57 155.45 156.30 157.12 157.91 158.67 159.42 160.85 161.54	22.84 22.85 22.87 22.90 22.93 22.98 23.03 23.03 23.09 23.15	38.66 38.01 37.47 37.00 36.60 36.27 35.98 35.73 35.51 35.33	251 255 262 269 269 272 276 279 282
265 270 275 280 285 290 295 300	3.32163 3.24554 3.17344 3.10498 3.03986 2.97782 2.91862 2.86205	2035 2091 2147 2202 2257 2311 2364 2417	0.0318 0.0310 0.0302 0.0294 0.0287 0.0280 0.0280 0.0274 0.0267	5157.3 5283.4 5409.3 5535.1 5660.7 5786.4 5912.0 6037.7	7264.7 7440.2 7615.1 7789.5 7963.5 8137.1 8310.4 8483.5	162.21 162.86 163.51 164.13 164.75 165.35 165.95 166.53	23.22 23.29 23.36 23.44 23.52 23.60 23.68 23.76	$35 \cdot 17$ $35 \cdot 04$ $34 \cdot 93$ $34 \cdot 83$ $34 \cdot 76$ $34 \cdot 69$ $34 \cdot 64$ $34 \cdot 64$	285 288 291 293 296 299 302 304

# 7.5 MN/m<sup>2</sup> ISOBAR

TEMPERATURE	OENSITY	ISOTHERM	ISOCHORE	INTERNAL	ENTHALPY	ENTROPY	Cv	Cp	VELOCITY
K	MOL/L	J/MOL	MN/m <sup>2</sup> - K	J/MOL	J/MOL	J/MOL-K	J/M	0 <b>і -</b> К	M/S
* 54.210	45.0261	29286	4.3380	-6183.7	-6017.2	61.00	36.28	53.46	1066
56	44.7403	28203	4.3344	-6087.9	-5920.3	62.78	35.96	54.60	1062
58	44.4224	27254	4.3084	-5980.3	-5811.5	64.71	35.60	55.62	1059
60	44.1095	26972	4.2158	-5873.1	-5703.1	66.57	35.30	55.62	1058
62	43.7942	25812	4.0905	-5765.4	-5594.1	68.37 70.14	35.30	56.26	1040
66	43.1527	23396	3.8471	-5547.8	-5374.0	71.85	34.75	57.17	1016
68	42.8370	23357	3.7299	-5439.2	-5264.1	73.51	34.09	56.16	1006
70	42.5214	22545	3.5971	-5331.4	-5155.0	75.11	33.57	55.79	993
72	42.1962	20891	3.4762	-5222.5	-5044.7	76.68	33.24	56.63	968
74	41.8686	19973	3.3588	-5113.7	-4934.6	78.21	33.10	56.94	951
76	41.5365	19274	3.2446	-5003.9	-4823.3	79.71	32.77	56.84	938
78 80	41.2056 40.8699	18528	3.1322 3.0216	-4894.7 -4785.3	-4712.7 -4601.8	81.16 82.58	32.31 32.04	56.63 56.74	925 908
82	40.5271	16548	2.9139	-4675.0	-4489.9	83.97	31.72	57.33	887
84	40.1857	16242	2.8151	-4565.1	-4378.5	85.33	31.33	56.71	880
86	39.8412	15509	2.7153	-4454.9	-4260.6	86.65	30.93	56.69	865
88	39.4935	14744	2.6136	-4344.3	-4154.4	87.95	30.50	56.64	849
90	39.1409	14132	2.5176	-4234.1	-4042.5	89.22	30.44	56.79	833
92	38.7827	13353	2.4210	-4122.9	-3929.5	90.47	30.48	57.33	813
94	38.4183	12621	2.3256	-4010.9	-3815.7	91.70	30.30	57.59	795
90	30.0497	114.00	2 1540	-3090.5	-3701.3	92.91	29.97	57.51	760
100	37.2955	10807	2.0702	=3671.8	-3470.7	95.27	29.74	58.25	763
100	76 0005	10000						50.25	
102	36.9085	10168	1.9864	-3507.5	-3354.3	96.42	29.56	58.61	728
104	30.2140	9551	1.8325	= 3442.1	-3230.7	97.50	29.45	59.30	696
108	35.7057	8531	1.7576	-3208.2	-2998.1	99.80	28.88	59.56	680
110	35.2888	7998	1.6852	-3090.0	-2877.4	100.90	28.80	60.17	663
112	34.8613	7437	1.6137	-2970.1	-2754.9	101.99	28.69	60.96	645
114	34.4214	6944	1.5426	-2848.5	-2630.7	103.07	28.54	61.51	628
116	33.9712	6458	1.4744	-2725.5	-2504.7	104.15	28.38	62.21	610
118	33.5080	5998	1.4070	-2600.7	-2376.8	105.22	28.23	62.92	593
120	33.0308	5535	1.3406	-2473.9	-2246.8	106.28	28.09	63,80	575
122	32.5385	5080	1.2752	-2345.0	-2114.5	107.35	28.00	64.89	557
124	32.0266	4649	1.2110	-2213.5	-1979.3	108.41	27.96	66.10	538
126	31.4949	4222	1.1468	-2079.4	-1841.3	109.48	28.09	67.65	517
128	30.9376	38 08	1.0840	-1940.9	-1698.5	110.50	27.98	69.24	498
132	29 7446	3420	1.0200	-1653 1	-1000 9	112 74	27.54	72 47	4/0
134	29.0971	2684	0.8973	-1502.3	-1244.6	113.85	27.52	75.00	439
136	28.4069	2331	0.8368	-1221.4	-957.4	114.98	27.50	78.13	417
138	27.6577	1996	0.7751	-1068.5	-797.4	116.15	27.31	81.62	396
140	26.8465	1675	0.7125	-909.4	-630.0	117.35	27.30	86.16	373
142	25.9508	1369	0.6547	-740+8	-451.8	118.62	27.52	93.54	350
144	24.9334	1080	0.5886	-558.3	-257.5	119.97	27.70	102.01	323
146	23.7582	813	0.5237	-358.6	-42.9	121.45	27.97	115.20	297
150	22.3394	773	0.4000	-131.7	204.0	125.13	20.57	170 02	200
152	18.1998	272	0.3055	472.2	884.3	127.66	30.24	213.70	208
154	15.5117	185	0.2391	854.7	1338.3	130.63	30.42	228.52	191
156	13.2735	209	0.1938	1199.0	1764.0	133.38	29.65	188.48	187
158	11.7458	263	0.1649	1458.3	2096.8	135.50	28.60	147.03	189
160	10.6819	322	0.1457	1659.0	2361.1	137.16	27.69	120.06	192
165	9.02682	466	0.1159	2024.2	2855.0	140.21	26.10	84.43	199
1/0	8.02101	594	0.0985	2295.0	3230.0	142.45	25.10	68.25	206
1/5	7.31360	709	0.0308	2519.9	3545.3	144.28	24.43	59.18	213
185	6 3/ 003	014	0.0716	2809 1	3022.1 1.091 2	147.05	23.95	53.40	224
190	5,981.37	1004	0.0661	3066.7	4320.6	148.53	23.37	46.46	229
195	5.67627	1089	0.0617	3226.1	4547.4	149.71	23.20	44.35	234
200	5.41151	1170	0.0580	3379.0	4764.9	150.81	23.09	42.71	239
205	5.17841	1248	0.0548	3526.7	4975.0	151.85	23.01	41.39	243
210	4.97078	1323	0.0520	3670.4	5179.3	152.84	22.96	40.33	247
215	4.78405	1395	0.0495	3810.9	5378.6	153.77	22.93	39.45	251
220	4.61476	1465	0.0473	3948.7	5574.0	154.67	22.92	38.71	255
225	4.46023	1533	0.0454	4084.4	5765.9	155.54	22.92	38.09	259
230	4.31833	1600	0.0436	4218.3	5955.1	156.37	22.93	37.57	263
235	4.18/37	1005	0.0419	4350.7	0141.8	157.05	22.90	31.12	200
240	4.00090	1720	0.0701	4401.8	6509 7	158 70	22.04	36 41	273
250	3.84735	1851	0.0391	4011.9	6690-6	159.43	23.04	36-13	276
255	3.74840	1911	0.0366	4869.8	6870.6	160.15	23.14	35.89	279
260	3.65539	1970	0.0356	4997.8	7049.5	150.84	23.20	35.68	282
265	3.56775	2028	0.0345	5125.3	7227.5	161.52	23.26	35.50	285
270	3.48497	2085	0.0336	5252.5	7404.6	162.18	23.33	35.35	288
275	3.40660	2142	0.0327	5379.4	7581.0	162.83	23.40	35.22	291
280	3.33225	2198	0.0318	5506.1	7756.8	163.46	23.47	35.11	294
285	3.26160	2253	0.0311	5632.6	7932.1	164.08	23.55	35.01	297
290	3.19434	2308	0.0303	5/59.0	8106.9	164.69	23.03	34.93	300
300	3.06898	2416	0.0289	6011.9	8455.7	165.87	23.79	34.82	305

\* TWO-PHASE BOUNDARY

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## 8.0 MN/m² ISOBAR

TEMPERATURE	OENSITY	ISOTHERM	ISOCHORE	INTERNAL	ENTHALPY	ENTROPY	Cv	Cp	VELOCITY
(1PTS 1968) K	MOL/L	J/MOL	MN/m <sup>2</sup> - K	J/MOL	J/MOL	J/MOL-K	J / M	оц – к	M/S
* 54.259	45.0354	29405	4.3393	-6194.1	-6016.5	61.02	36.26	53.40	1067
56	44.7580	28327	4.3357	-6101.1	-5922.4	62.74	35.96	54.51	1063
58 60	44.4408 44.1281	27338 27053	4.3148 4.2222	-5993.7 -5886.7	-5813.7 -5705.4	64.67 66.53	35.59 35.29	55.59 55.60	1060 1059
62	43.8136	25871	4.0972	-5779.2	-5596.6	68.33	35.31	56.27	1042
64	43.4958	24272	3.9495	-5670.8	-5486.9	70.10	35.16	56.90	1017
66	43.1741	23436	3.8463	-5562.1	-5376.8	71.81	34.80	57.15	1006
58	42.0504	23412	3.7324	-5453.6	-5266.9	75.47	34.13	56.15 CC 70	1007
72	42.2201	20969	3.4818	-5237.5	-5158.0	76.63	33.26	56.61	969
74	41.8936	20032	3.3632	-5129.0	-4938.1	78,16	33.13	56.94	952
76	41.5624	19328	3 . 2471	-5019.4	-4826.9	79.66	32.82	56.82	938
78	41.2325 40.8981	18600	3.1356 3.0254	-4910.5 -4801.4	-4716.4 -4605.8	81.11 82.52	32.35 32.08	56.60 56.71	925
82	40.5572	16626	2.9175	-4691.4	-4494.2	83.92	31.77	57.29	888
84	40.2164	16317	2.8184	-4581.7	-4382.8	85.27	31.38	56.67	881
88	39.5273	148.42	2.6192	-4361.6	-4271+2	87.90	30.54	56.57	851
90	39.1762	14234	2.5241	-4251.7	-4047.5	89.16	30.47	56.72	835
92	38.8200	13458	2.4282	-4140.9	-3934.9	90.41	30.52	57.27	815
94	38.4578	12724	2.3317	-4029.3	-3821.3	91.64	30.34	57.50	797
96	38.0910	12154	2.2432	-3917.3	-3707.3	92.85	30.02	57.41	782
100	37.3415	10918	2.0774	-3691.6	-3477.3	95.20	29.79	58.13	749
102	36.9574	10280	1.9930	-3577.8	-3361.3	96.35	29.60	58.45	731
104	36,1680	9664	1.8409	-33463.0	-3244+2	97+40	29.49	59.13	699
108	35.7639	8651	1.7659	-3230.1	-3006.4	99.72	28.92	59.35	684
110	35.3509	8121	1.6939	-3112.6	-2886.3	100.81	28.83	59.93	667
112	34.9280	7566	1.6232	-2993.5	-2764.5	101.90	28.72	60.69	649
114	34+4928	7065	1.0807	-2872.7	-2640.8	102.98	28.57	61.23	031 615
118	33.5905	6123	1.4180	-2626.7	-2388.5	105.11	28.26	62.60	597
120	33.1201	5664	1.3523	-2500.9	-2259.4	106.17	28.11	63.42	580
122	32,6356	5216	1.2875	-2373.2	-2128.1	107.23	28.02	64.42	562
124	32.1326	4785	1.2239	-2243.0	-1994.0	108.29	27.97	65.57	543
128	31.0665	4361	1.0083	=2110+4	-1057.4	109+34	28.09	67+U4 68.49	523
130	30.5007	3569	1.0362	-1834.1	-1571.8	111.48	27.87	69.90	485
132	29.9048	3194	0.9729	-1690.0	-1422.5	112.56	27.53	71.26	467
134	29.2783	2835	0.9150	-1542.0	-1268.8	113.65	27.49	73.67	447
136	28.6145	2487	0.8555	-12+8.8	-969.2	114.76	21.44	76.32	427
138	27.0900	1836	0.7350	-946.0	-651.1	117.07	27.25	83.14	365
142	26.2953	1536	0.6795	-784.5	-480.2	118.28	27.35	89.08	363
144	25.3633	1250	0.6170	-611.9	-296.5	119.57	27.52	95.70	338
146	24.3151	986	0 4910	-426.6	-97.6	120.94	27.68	105.05	314
150	21.6605	536	0.4293	-220+0 6+6	375.9	124.13	28.80	138.70	261
152	19.8936	371	0.3594	273.3	675.5	126.12	29.28	163.15	233
154	17.8008	266	0.2944	579.3	1028.8	128.43	29.72	187.79	210
156	15.5979	231	0.2430	904.3	1417.2	130.93	29.78	193.61	199
160	12.3220	292	0.1755	1199.4 1438.4	2087.6	133.26	28.82 28.08	139.23	195
165	10.1513	426	0.1350	1867.3	2655.3	138.68	26.50	95.10	200
170	8.89257	554	0,1126	2171.8	3071.4	141.16	25.43	74.58	207
180	8.U38U2 7.40156	572	0.0876	2628.9	3412.3	143+14	24+18	63.38 56.48	213
185	6.89938	880	0.0797	2819.5	3979.0	146.29	23.80	51.82	225
190	6.48823	973	0.0733	2995.4	4228.4	147.63	23.53	48.42	230
195	6.14150	1062	0.0682	3161.0	4463.6	148.85	23.33	45.95	235
200	5.84310	1147	0.0637	3318.8	4688.0	149.98	23.20	43.92	239
210	5.35159	1303	0.0568	3617.9	5112.8	152.06	23.05	41.23	243
215	5.14477	1377	0.0540	3761.4	5316.4	153.02	23.01	40.24	252
220	4.95794	1449	0.0493	3991+9	5515.5 5710.8	153.93	22.99	39.42	256
230	4.63224	1586	0.0473	4176.0	5903.0	155.65	23.00	38.14	. 263
235	4.48889	1652	0.0455	4310.2	6092.4	156.47	23.02	37.65	267
240	4.35627	17 17	0.0439	4443.1	6279.6	157.26	23.05	37.22	270
245	4.23305	1780	0.0423	4574.8	6464.7	158.02	23.09	36.85	273
250	4.11013	1903	0.0396	4835.4	6830-1	159,48	23.18	36.26	277
260	3.90967	1963	0.0384	4964.7	7010.9	160.18	23.24	36.03	283
265	3.81467	2022	0.0373	5093.3	7190.5	160.87	23.30	35.83	286
275	3.64026	2138	0.0353	5349.4	7547.1	162,19	23.43	35.50	209
280	3.55993	2194	0.0343	5477.0	7724.3	162.83	23.50	35.38	295
285	3.48364	2251	0.0335	5604.4	7900.9	163.45	23.58	35.27	298
290	3.41108	2306	0.0327	5731.7	8077.0	164.07	23.65	35.18	300
295	3.34195	2361	0.0319	5986.0	8428.0	165.26	23.81	35.04	303

## TABLE 16. THERMOOYNAMIC PROPERTIES OF FLUORINE

## 8.5 MN/m<sup>2</sup> ISDBAR

TEMPERATURE (IPTS 1968) K	DENSITY MOL/L	ISOTHERM DERIVATIVE J/MOL	ISOCHORE DERIVATIVE MN/m <sup>2</sup> <del>-</del> K	INTERNAL ENERGY J∕MOL	ENTHALPY J/MOL	ENTROPY J/MOL-K	C <sub>V</sub> J Z Mi	С <sub>р</sub> DL - К	VELOCITY OF Sound M/S
* 54.306 56 58 60	45.0449 44.7756 44.4590 44.1465	29524 28446 27423 27133	4.3405 4.3369 4.3211 4.2285	-6204.5 -6114.3 -6007.1 -5900.3	-6015.8 -5924.4 -5816.0 -5707.7	61.03 62.70 64.63 66.49	36.25 35.95 35.59 35.29	53.33 54.42 55.57 55.58	1069 1065 1062 1060
62 64 68 70 72 74 76 78 80	43.8329 43.5164 43.1954 42.8798 42.5656 42.2439 41.9185 41.5883 41.2594 40.9262	25936 24319 23484 23469 22704 21052 20101 19388 18677 17857	4.1045 3.9520 3.8457 3.7344 3.6086 3.4875 3.3680 3.2500 3.1387 3.0293	-5793.1 -5684.9 -5576.4 -5468.0 -5360.6 -5252.4 -51+4.3 -5034.9 -4926.2 -4817.4	-5599.1 -5489.6 -5379.6 -5269.7 -5160.9 -5051.2 -4941.5 -4830.5 -4720.2 -4609.7	68.29 70.05 71.76 73.43 75.02 76.59 78.11 79.61 81.06 82.47	35.33 35.20 34.84 34.16 33.61 33.28 33.16 32.87 32.40 32.12	56.29 56.90 57.12 56.14 55.77 56.59 56.92 56.81 56.56 56.56 56.67	1043 1017 1007 996 971 953 939 926 911
82 84 86 90 92 94 96 98 100	40.5872 40.2469 39.9053 39.5609 39.2112 38.8570 38.4969 38.1320 37.7615 37.3871	16712 16394 15685 14943 14336 13564 12830 12261 11614 11030	2.9212 2.8216 2.7241 2.6247 2.5303 2.4355 2.3380 2.2501 2.1664 2.0846	-4707.8 -4598.3 -4488.7 -4378.8 -4269.2 -4158.9 -4047.7 -3935.0 -3824.0 -3711.2	-4498.4 -4387.1 -4275.7 -4164.0 -4052.5 -3940.2 -3826.9 -3713.1 -3598.9 -3483.9	83.86 85.22 86.54 89.11 90.35 91.58 92.78 93.97 95.13	31 • 82 31 • 43 31 • 0 3 30 • 58 30 • 51 30 • 56 30 • 38 30 • 06 29 • 99 29 • 8 3	57.24 56.52 56.58 56.65 57.21 57.40 57.76 57.76 58.02	889 882 868 852 837 817 799 784 767 751
102 104 106 108 110 112 114 116 118 120	37.0057 36.6183 36.2221 35.8213 35.4120 34.9935 34.5629 34.1231 33.6714 33.2074	10394 9779 9292 8771 8244 7696 7185 6709 6248 5792	1.9999 1.9264 1.8494 1.7742 1.7026 1.6327 1.5621 1.4951 1.4288 1.3636	-3597.9 -3483.7 -3368.0 -3251.9 -3135.0 -3016.7 -2896.7 -2775.4 -2652.3 -2527.6	-3368.2 -3251.6 -3133.3 -3014.6 -2895.0 -2773.8 -2650.8 -2526.3 -2399.9 -2271.6	96.28 97.41 98.53 99.64 100.73 101.81 102.89 103.95 105.01 106.07	29.63 29.53 29.23 28.94 28.86 28.74 28.60 28.42 28.28 28.12	58.29 58.96 58.97 59.15 59.70 60.42 61.00 61.62 62.29 63.06	734 717 702 687 670 653 635 619 602 585
122 124 126 128 130 132 134 136 138 140	32.7303 32.2357 31.7243 31.1909 30.6381 30.0579 29.4502 28.8096 28.1231 27.3927	5350 4919 4498 3711 3339 2982 2640 2306 1993	1.2995 1.2363 1.1740 1.1122 1.0512 0.9880 0.9319 0.8731 0.8149 0.7561	-2401.0 -2272.1 -2140.9 -2005.8 -1867.9 -1725.9 -1580.4 -1274.7 -1129.4 -979.8	-2141.3 -2008.4 -1873.0 -1733.3 -1590.5 -1443.1 -1291.8 -979.6 -827.1 -669.5	107.12 108.17 109.21 110.27 111.33 112.40 113.47 114.56 115.67 116.81	28.03 27.98 28.10 27.98 27.86 27.52 27.47 27.39 27.20 27.08	63.97 65.06 66.46 67.80 69.11 70.24 72.45 74.71 77.45 80.61	567 529 511 492 475 435 435 416 395
142 144 148 150 152 154 156 158 160	26.6048 25.7392 24.7834 23.7066 22.4757 21.0305 19.3626 17.5018 15.6483 14.0501	1697 1413 1152 911 697 518 385 304 279 292	0.6987 0.6427 0.5843 0.5231 0.4669 0.4026 0.3413 0.2909 0.2442 0.2094	-824.0 -659.2 -484.5 -296.6 -91.0 139.0 394.3 674.0 957.2 1215.1	-504.5 -329.0 -141.5 62.0 287.2 543.1 833.3 1159.7 1500.4 1820.1	117.98 119.20 120.50 121.88 123.39 125.09 126.98 129.09 131.26 133.27	27.19 27.36 27.49 27.79 28.29 28.69 29.03 29.31 29.31 29.34 28.17	84.91 90.91 97.91 106.89 121.16 136.31 153.40 170.89 167.43 149.83	373 352 329 304 280 254 231 216 205 202
165 170 175 180 185 190 195 200 205 210	11.3697 9.82304 8.80079 8.05570 7.47702 7.00898 6.61782 6.28390 5.99350 5.73797	398 522 640 750 852 947 1038 1124 1207 1285	0.1568 0.1283 0.1102 0.0976 0.0883 0.0808 0.0749 0.0655 0.0619	1701.9 2042.8 2310.5 2537.3 2738.7 2922.9 3094.9 3257.9 3414.1 3565.0	2449.5 2908.2 3276.3 3592.4 3875.5 4135.6 4379.3 4610.6 4832.3 5046.3	137.15 139.89 142.02 143.81 145.36 146.75 148.01 149.18 150.28 151.31	26.81 25.73 24.95 24.40 23.99 23.69 23.47 23.32 23.21 23.14	105.68 81.26 67.83 59.66 54.24 50.32 47.51 45.32 43.50 42.15	203 208 214 220 225 230 235 240 244 244
215 220 225 230 235 240 245 250 255 260	5.51006 5.30489 5.11876 4.94876 4.79260 4.64841 4.51469 4.39019 4.27385 4.16480	1361 1434 1505 1573 1641 1706 1771 1834 1896 1957	0.0587 0.0559 0.0535 0.0492 0.0492 0.0473 0.0457 0.0441 0.0427 0.0424	3711.6 3854.9 3995.3 4133.5 4269.7 4404.3 4537.6 4669.8 4801.0 4931.5	5254.2 5457.2 5655.9 5851.1 6043.3 6232.9 6420.4 6605.9 6789.9 6772.4	152.29 153.22 154.12 154.97 155.80 156.60 157.37 158.12 158.85 159.56	23.10 23.07 23.07 23.08 23.11 23.14 23.18 23.23 23.23 23.28	41.05 40.14 39.37 38.72 38.17 37.70 37.29 36.94 36.64 36.38	252 256 264 267 271 274 277 281 284
265 270 275 280 285 290 295 300	4.06228 3.96566 3.87437 3.78793 3.70592 3.62798 3.55376 3.48299	2017 2076 2134 2192 2248 2305 2360 2415	0.0491 0.0390 0.0369 0.0359 0.0350 0.0350 0.0342 0.0334	5061.3 5190.6 5319.4 5448.0 5576.2 5704.3 5832.2 5960.1	7153.7 7334.0 7513.3 7691.9 7869.8 8047.2 8224.0 8400.5	160.25 160.92 161.58 152.23 162.86 163.47 164.08 164.67	23.34 23.40 23.46 23.53 23.60 23.68 23.75 23.83	36.15 35.96 35.65 35.65 35.52 35.42 35.33 35.25	287 290 293 296 298 301 304 307

#### TABLE 16. THERMODYNAMIC PROPERTIES OF FLUORINE

9.0 MN/m² ISOBAR

IEMPERATURE (IPTS 1968)	OENSITY	ISOTHERM DERIVATIVE	ISOCHORE OERIVATIVE MN/m <sup>2</sup> =K	INTERNAL ENERGY	ENTHALPY	ENTROPY	C <sub>V</sub>	С <sub>р</sub>	VELOCITY OF SOUNO
N.	110272	07 HOL	into in .N	SVIICE	OTHOL	STRUE R	0 7 1		117 3
8 EL 7EL	45 0543	20670	1. 71.4.7	6.244 0	6.045.4	64 04	76 24	57 0 <b>7</b>	4071
56	44.7931	28569	4.3381	-6127.4	-5926.5	62.67	35.95	54.34	1066
58	44.4772	27507	4.3273	-6020.5	-5818.2	64.59	35.58	55.54	1063
60	44.1649	27213	4.2347	-5913.8	-5710.0	66.45	35.29	55.56	1062
62	43,8521	260.05	4.1123	-5806.9	=5601.6	68.25	32.34	56.30	1044
64	43.5369	24375	3.9558	-5698.9	-5492.2	70.01	35.23	56.91	1018
66	43.2166	23539	3.8452	-5590.7	-5382.4	71.72	34.89	57.08	1007
68	42.9010	23528	3.7360	-5482.4	-5272.6	73.38	34.20	56.12	1008
72	42.2676	21140	3.4931	-5267.4	~5054.4	76.54	33.30	56.56	972
74	41.9433	20178	3.3731	-5159.5	-4944.9	78.06	33.19	56.91	954
76	41.6140	19454	3.2531	-5050.3	-4834.0	79.56	32.92	56.79	940
80	41.2001	17940	3.0333	-4941.8	-4613.6	82.42	32.16	56.63	927
82	40.6170	16805	2.9251	-4724.1	-4502.6	83.81	31.87	57.18	891
36	40+2774	15776	2.7282	-4614.9	-4391.4	05.17	31.07	56.51	869
88	39.5943	15046	2.6300	-4396.0	-4168.7	87.79	30.62	56.43	854
90	39.2459	14438	2.5363	-4286.7	-4057.4	89.05	30.54	56.57	839
92	38.8938	13672	2.4428	-4176.8	-3945.4	90.29	30.60	57.14	820
96	38.1726	12369	2.2570	-3954.7	-3718.9	92.72	30.09	57.23	787
98	37.8043	11723	2.1729	-3843.1	-3605.1	93.90	30.02	57.64	770
100	37.4322	11142	2.0917	-3730.8	-3490.3	95.06	29.87	57,90	754
102	37.0536	10508	2.0083	-3617.9	-3375.1	96.21	29.66	58.18	736
104	36.6691	9896	1.9338	-3504.3	-3258.8	97.34	29.56	58.79	720
106	36.2756	9406	1.8579	-3389.1	-3141.0	98.46	29.26	58.82	705
108	35.6779	8366	1.7111	-3273.6	-3022.07	99.55	28.89	50.96 59.48	673
112	35.0579	7826	1.6423	-3039.7	-2783.0	101.72	28.76	60.17	656
114	34.6319	7306	1.5722	-2920.4	-2660.6	102.80	28.62	60.78	639
116	34.1969	6833	1.5052	-2799.9	-2536.7	103.86	28.44	61.33	623
120	33.2928	5920	1.3747	-2554.0	-2283.6	105.96	28.14	62.70	589
	70								
122	32.8226	5484	1.3111	-2428.5	-2154.3	107+00	28.04	63.54	572
126	31.8338	4635	1.1869	-2170.9	-1888.1	109.08	28.10	65.90	535
128	31.3112	4226	1.1257	-2037.3	-1749.8	110.13	27.98	67.14	517
130	30.7704	3851	1.0657	+1901.1	-1608.6	111.18	27.86	68.36	499
134	29.6139	31.28	1.9473	-1617.7	=1313.8	112+24	27.44	71.29	401
136	28.9939	2789	0.8895	-1299.2	-988.7	114.36	27.35	73.24	443
138	28.3332	2456	0.8335	-1157.0	-839.4	115.45	27.15	75.78	425
140	27.6345	2145	0.7760	-1011.2	-685+5	116.56	27.02	18.48	405
142	26.8866	1853	0.7200	-860.2	-525.5	117.70	27.07	82.01	384
144	26.0745	1571	0.6664	-701+8	-356.6	118.88	27.22	87.09	364
146	25.1097	1312	0.5515	-358.7	-178.0	120.11	27.53	92.55	342
150	23.1225	8 5 4	0.4992	-169.5	219.7	122.80	27.91	109.82	297
152	21.8797	666	0.4391	37.4	448.7	124.31	28.23	120.16	273
154	20.4020	516	0.3332	201+4 504+4	980.0	127.76	28.80	147.35	234
158	17.2698	346	0.2846	760.1	1281.3	129.68	28.98	153.03	219
160	15.6841	326	0.2450	1011.1	1585.0	131.59	28.96	148.73	210
165	12.6482	387	0.1810	1533.1	2244.7	135.65	27.01	114.27	208
170	10.8045	499	0.1456	1909.6	2742.6	138.63	25.98	87.83	211
175	9.59903	614	0.1235	2200.7	3138.3	140.92	25.18	72.39	216
180	8.07290	724	0.1085	2443+4	3473.8	142+82	24+60	56.73	221
190	7.54341	924	0.0887	2849.1	4042.2	145.89	23.84	52.26	231
195	7.10468	1016	0.0819	3027.9	4294.6	147.20	23.60	49.10	236
200	6.73297	1104	0.0762	3196.3	4533.0	148.41	23.43	46.61	240
210	6.13016	1267	0.0673	3511.6	4979.7	150.59	23.23	43.22	249
215	5.87963	1345	0.0636	3661.5	5192+2	151.59	23.18	41.87	253
225	5.45252	1492	0.0577	3950.5	5601.1	153.45	23.14	40.02	261
230	5.26771	1562	0.0552	4090.9	5799.4	154.32	23.13	39.31	264
235	5.09832	1630	0.0530	4229.1	5994.4	155.16	23.14	38.70	268
245	4.79773	1763	0.0491	4500.4	6376.3	156.75	23.19	37.73	275
250	4.66339	1827	0.0474	4634.0	6564.0	157.51	23.23	37.35	278
255	4.53804	1889	0.0458	4706.6	6749.9	158.25	23.27	37.02	281
260	4.42070	1951	0.0443	4898.3	6934.2	158,96	23.32	36.73	284
265	4.31051	2012	0.0430	5029.3	7117.2	159.66	23.37	36.48	287
270	4.20676	2072	0.0417	5159.6	7299.0	160.34	23.43	36.26	291
275	4.10883	2131	0.0406	5289.5	7479.9	161.65	23.49	36.07	293
285	3.92837	2247	0.0384	5548.0	7839.0	162.29	23.62	35.77	299
290	3.84496	2304	0.0375	5676.9	8017.6	162.91	23.70	35.65	302
295	3.76560	2360	0.0366	5805.5 5934.1	8195.6	163.52	23.77	35.55	305

#### TABLE 16. THERMODYNAMIC PROPERTIES OF FLUORINE

#### 9.5 MN/m<sup>2</sup> ISOBAR

TEMPERATURE (IPTS 1968)	DENSITY	ISOTHERM DERIVATIVE	ISOCHORE DERIVATIVE	INTERNAL ENERGY	ENTHALPY	ENTROPY	Cv	Cp	VELOCITY OF SOUNO
к	MOL/L	J/MOL	MN/m <sup>2</sup> - K	J/MOL	J/MOL	J/MOL-K	JZM	о <b>г -</b> к	M/S
* 54.402	45.0634	29753	4.3428	-6225.2	-6014.4	61.05	36.23	53.21	1072
56	44.8106	28691	4.3392	-6140.5	-5928.5	62.63	35.95	54.25	1067
58 60	44.1833	27292	4.2408	-5927.4	-5712.3	66.41	35.28	55.54	1064
62	43.8713	26080	4.1207	-5820.6	-5604.1	68.21	35.34	56.32	1046
64	43.5574	24442	3.9602	-5713.0	-5494.9	69.97	35.26	56.91	1019
68	43+23/8	23602	3.8448	-5604.9	-5385.2	77 74	34.93	57+04	1007
70	42.6095	22870	3.6181	-5389.8	+5166.8	74.94	33.65	55.72	998
72	42.2912	21234	3.4988	-5282.3	-5057.6	76.49	33.32	56.53	974
74	41.9680	20263	3.3785	-5174.6	-4948.3	78.01	33.21	56.88	956
76	41.6397	19526	3.2567	-5065.7	-4837.6	79.51	32.96	56.77	941
80	41.3127 40.9819	18028	3.0374	-4957.5	-4727.5	80.96	32.49	56.58	928
82	40.6467	16905	2.9290	-4740.4	-4506.7	83.76	31.92	57.11	892
84	40.3076	16555	2.8276	-4631.3	-4395.7	85.11	31.53	56.50	884
86	39.9687	15869	2.7322	-4522.3	-4284.7	86.44	31.12	56.44	870
88	39.6274	15151	2.6351	-4413.1	-4173.4	87.73	30.67	56.35	856
90	39.2005	14540	2.0502	-4304.1	-4062.3	00.23	30.63	56.49	841
94	38.5742	13049	2.3534	-4084.2	-3837.9	91.46	30.44	57.26	804
96	38.2128	12477	2.2642	-3973.3	- 3724.6	92.66	30.12	57.14	789
98	37.8468	11832	2.1795	-3862.1	-3611.1	93.84	30.05	57.52	772
100	37.4768	11254	2.0988	-3750.2	-3496.7	95.00	29.91	57.78	756
102	37.1009	10623	2.0166	-3637.9	-3381.8	96.14	29.70	58.06	739
104	36.3284	9520	1.8665	-3410.0	-3148.5	98.38	29.29	58.68	708
108	35.9338	9009	1.7908	-3295.0	-3030.7	99.48	28.99	58.77	693
110	35.5315	8488	1.7199	-3179.4	-2912.0	100.57	28.91	59.28	677
112	35.1213	7955	1.6517	-3062.5	-2792.0	101.64	28.78	59.92	660
114	34.6998	7426	1.5823	-2944.0	-2670.2	102.71	28.64	60.56	643
118	33.8284	64.94	1.4500	-2024+2 +27i12-9	-2422.1	104.81	28.32	61.70	610
120	33.3764	6046	1.3855	-2580.0	-2295.4	105.86	28.16	62.36	594
122	32.9127	5616	1.3225	-2455.5	-2166.9	106.89	28.06	63.13	577
124	32.4337	5184	1.2601	-2328.9	-2036.0	107.93	28.00	64.11	559
128	31.4277	4/70	1 1388	-2068 2	-1902.9	110.00	27 99	66 51	540
130	30.8979	3989	1.0796	-1933.5	-1626.0	111.04	27.86	67.65	505
132	30.3454	3621	1.0196	-1795.1	-1482.0	112.08	27.51	68.67	488
134	29.7702	3270	0.9618	-1653.9	-1334.8	113.12	27.42	70.18	469
136	29.1686	2935	0.9066	-1322.5	-996.8	114.18	27.31	72.07	452
138 140	28.5309 27.8598	2603 2294	0.8511 0.7949	-1183.2 -1040.7	-856.2	115.25	27.10 26.96	74.28 76.64	433
142	27.1458	2006	0.7400	-893.7	-543.8	117.44	26.97	79.59	395
144	26.3781	1724	0.6883	-740.6	-380.5	118.58	27.10	83.95	375
146	25.5500	1466	0.6331	-580.7	-208.9	119.76	27.20	88.34	354
148	24.6486	1224	0.5773	-412.9	-27.5	121.00	27.33	93.64	332
150	23.0011	1006	0.5279	-235.6	105.9	123 69	27.00	101.01	290
154	21.3418	652	0.4156	158.5	603.6	125.17	28.09	117.59	268
156	20.0006	526	0.3700	375.7	850.7	126.77	28.32	129.81	252
158	18.5566	438	0.3217	605.5	1117.5	128.47	28.55	136.94	235
160	17.0944	389	0.2799	839.0	1394.7	130.21	28.65	138.89	223
165	13.9297	396	0.2070	1368.3	2050.3	134.25	27.08	119.02	214
175	10.4270	595	0.1379	2088.6	2999.7	139.85	25.39	76.84	218
180	9.43619	703	0.1201	2347.7	3354.5	141.85	24.78	66.24	222
185	8.68538	806	0.1072	2572.5	3666.2	143.56	24.33	59.25	227
190	8.09043	904	0.0971	2774.2	3948.4	145.06	23.98	54.24	232
195	7.60131	998	0.0893	2960.1	4209.9	146.42	23.73	50.71	237
205	6.83645	1171	0.0772	3234.1	4455.5	147.00	23.04	47.93	241
210	6.52703	1253	0.0728	3457.9	4913.4	149.90	23.32	44.18	250
215	6.25403	1331	0.0687	3611.1	5130.1	150.92	23.26	42.73	254
220	6.00936	1407	0.0653	3760.1	5341.0	151.89	23.23	41.71	258
225	5.78897	1481	0.0621	3905.6	5546.6	152.81	23.21	40.07	261
235	5.40588	1621	0.0593	4040.2	5945.7	154.55	23.20	39.23	269
240	5.23757	1669	0.0546	4326.6	6140.4	155.37	23.22	38.66	272
245	5.08201	1755	0.0526	4463.1	6332.5	156.16	23.24	38.17	275
250	4.93761	1820	0.0507	4598.3	6522.3	156.93	23.27	37.75	279
255	4.80306	1884 1947	0 • 0 4 9 0 0 • 0 4 7 4	4732.2 4865.1	6710.1 6896.2	157.67 158.40	23.31 23.35	37.39	282
265	4.55925	2008	0.0459	4997.2	7080.9	159.10	23.40	36.80	288
270	4.44825	2069	0.0446	5128.6	7264.3	159.79	23.46	36.56	291
275	4.34358	2129	0.0433	5259.5	7446.6	160.45	23.52	36.36	294
280	4.24465	2188	0.0421	5389.8	7627.9	161.11	23.58	36.18	297
285	4.15093	2246	0.0410	5519.8	7808.4	161.75	23.64	35.89	300
290	3,97740	2304	0.0400	5778 8	7988.2	162.98	23.79	35.78	303
300	3.89684	2418	0.0380	5908.1	8346.0	163.58	23.86	35.68	308

## 10 MN/m<sup>2</sup> ISOBAR

TEMPERATURE	DENSITY	ISOTHERM	ISOCHORE	INTERNAL	ENTHALPY	ENTROPY	Cv	Cp	VELOCITY
K	MOL/L	J/MOL	MN/m <sup>2</sup> - K	J/MOL	J/MOL	J∕MOL-K	J / M	ОL – К	M/S
* 54.450	45.0727	29864	4.3439	-6235.6	-6013.7	61.06	36.22	53.15	1074
56	44.8280	28812	4.3403	-6153.6	-5930.5	62.59	35.94	54.16	1069
58 60	44.5135 44.2016	27675 27372	4.3358 4.2469	-6047.3 -5940.9	-5822.6 -5714.6	54.51 66.37	35.58 35.28	55.46 55.51	1066 1065
62	43.8905	26159	4.1295	-5834.4	-5606.6	68.17	35.35	56.33	1047
64	43.5778	24518	3.9651	-5727.0	-5497.5	69.92	35.30	56.91	1020
66	43.2590	23672	3.8445	-5619.1	-5388.0	71.63	34.97	56.99	1008
68	42.9434	23652	3.7379	-5511.0	-5278.2	73.30	34.28	56.07	1009
70	42.0313	22950	3.50/1	-5404.3	-5169.7	74.89	33.01	55.69	1000
74	41.9926	20357	3.3842	-5189.8	- 4951.6	77.97	33.24	56.85	957
76	41.6652	19603	3.2605	-5081.1	-4841.1	79.46	33.00	56.75	942
78 80	41.3392 41.0096	18930 18119	3.1467 3.0415	-4973.1 -4865.2	-4731.1 -4621.3	80.91	32.53	56.41 56.53	929 914
82	40.6762	17012	2.9331	-4756.7	~4510.8	83.71	31.97	57.03	894
84	40.3378	16639	2.8304	-4647.8	-4399.9	85.06	31.58	56.44	885
86	40.0001	15964	2.7360	-4539+1	-4289.1	86.38	31.17	56.37	872
88	39.6603	15259	2.6401	-4430.2	-4178.0	87.68	30.71	56.26	858
90	39.3147	14642	2.5473	-4321.5	-4057+1	88.94	30.66	55.41	843
94	38.6124	13161	2.3613	-4212.4	- 3843.3	90.17	30.48	57.19	806
96	38.2527	12586	2.2714	-3991.8	-3730.3	92.60	30.16	57.05	792
98	37.8889	11943	2.1864	-3881.0	-3617.1	93.77	30.08 29.95	57.41	774
102	37 1477	10739	2 0 24 9	= 365.7 7	- 3388 5	96.07	20 73	57 05	74.2
104	36.7690	10133	1.9492	-3545.1	-3273.1	97.19	29.61	58.45	726
106	36.3807	9634	1.8750	-3430.8	-3156.0	98.31	29.32	58.55	712
108	35.9889	9127	1.7992	-3316.4	-3038.5	99.41	29.02	58.59	696
110	35.5900	8608	1.7289	-3201.3	-2920+4	100.49	28.93	59.09	680
114	32.1030	8003 7547	1.5924	= 3 0 0 5 + 1	-2679.7	102 62	28.66	59.00	647
116	34.3407	7080	1.5249	-2848.3	-2557.1	103.67	28.48	60.78	631
118	33.9046	6617	1.4604	-2727.8	-2432.8	104.72	28.33	61.42	614
120	33.4582	6172	1.3961	-2605.8	-2306.9	105.76	28.17	62.02	598
122	33.0007	5746	1.3336	-2482.2	-2179.2	106.79	28.07	62.74	581
124	32.5289	5314	1.2718	-2356.7	-2049.3	107.81	28.01	63.67	564
120	32:0435	4903	1 + 2117	-2628 5	-1917.5	100.04	27 00	66 94	546
130	31.0212	4125	1.0931	-1965.3	-1642.9	110.90	27.86	66.99	511
132	30.4809	3759	1.0344	-1828.5	-1500.4	111.93	27.50	67.94	494
134	29.9199	3411	0.9756	-1689.2	-1355.0	112.96	27.39	69.16	476
136	29.3349	3079	0.9228	-1344.7	-1003.8	114.00	27.28	70.99	459
138	28.0711	2440	0.8678	-1208.0 -1068.4	-859.8	115.05 116.11	27.05 26.92	72.92 75.03	441 423
142	27.3863	2154	0.7588	-925.0	-559.8	117.20	26.88	77.49	404
144	26.6562	1874	0.7068	-776.4	-401.3	118.30	26.99	81.01	385
146	25.8746	1616	0.6547	-622.0	-235.5	119.45	27.08	84.93	365
148	25.0337	1375	0.6012	-461.1	-61.7	120.63	27.17	89.27	345
153	24.1243	1156	0.5537	-292.9	121.6	121.86	27.40	95.79	326
154	22.0374	79ú	0.4463	74.3	528.0	124.53	27.77	107.76	284
156	20.8539	651	0.4025	2/3.3	752.8	125.98	27.92	117.21	268
158	19.5802	544	0.3551	482.6	993.3	127.52	28.14	123.59	251
160	18.2618	473	0.3127	697.8	1245.4	129.10	28.28	127.47	237
165	15.1513	426	0.2339	1214.6	1874.6	132.97	27:03	119.38	222
175	11.2755	585	0.1534	1975.6	2862.5	138.80	25.56	80.92	221
180	10.1555	688	0.1324	2250.8	3235.5	140.90	24.95	69.44	225
185	9.31210	790	0.1175	2487.6	3561.5	142.69	24.48	61.75	229
190	8.64851	888	0.1059	2698.5	3854.8	144.25	24.12	56.22	233
195	8.10665	982	0.0971	2891.6	4125.1	145.66	23.85	52.32	238
205	7.26606	1157	0.0834	3241.4	4370+1	148.12	23.50	49.20	246
210	6.92832	1240	0.0785	3404.0	4847.3	149.23	23.40	45.15	251
215	6.63141	1319	0.0739	3560.5	5068.5	150.27	23.33	43.57	255
220	6.36613	1396	0.0666	3712.5	5283.3 5492 3	151+26	23.29	42.45	259
230	5.91205	1543	0.0635	4005.4	5696.9	153.10	23.26	40.47	266
235	5.71508	1613	0.0608	4147.7	5897.4	153.96	23.26	39.76	269
240	5.53425	1682	0.0584	4287.7	6094.6	154.79	23.27	39.14	273
245	5.36739	1749	0.0561	4425.9	6289.0	155.59	23.29	38.61	276
250	5.21272	1815	0.0541	4562.5	6480.9	150.37	23.31	38.16	280
260	4.93436	1943	0.0505	4832.0	6858.6	157.85	23.39	37.42	285
265	4.80841	2005	0.0489	4965.2	7044.9	158.56	23.43	37.12	289
270	4.69005	2067	0.0475	5097.7	7229.8	159.25	23.48	36.86	292
275	4.57854	2127	0.0461	5229.5	7413.6	159.93	23.54	36.64	295
285	4.4/322	2187	0.0448	5491.5	7778.0	161.23	23.66	36.27	298
290	4.27896	2305	0.0425	5622.U	7959.0	161.86	23.73	36.12	304
295	4.18911	2362	0.0414	5752.1	8139.3	162.47	23.80	36.00	307
300	4.10357	2420	0.0404	5882.1	8319.0	163.08	23.87	35.89	309

#### TABLE 16. THERMOOYNAMIC PROPERTIES OF FLJORINE

## 11 MN/m<sup>2</sup> ISOBAR

TEMPERATURE	OENSITY	ISOTHERM OFRIVATIVE	ISOCHORE	INTERNAL ENERGY	ENTHALPY	ENTROPY	Cv	Cp	VELOCITY OF SOUND
К	MOL/L	J/MOL	MN/m <sup>2</sup> - K	J/MOL	J/MOL	J∕MOL-K	J / M	)L - K	M/S
* 54.546	45.0911	30082	4.3458	-6256.3	-6012.3	61.09	36.19	53.04	1077
56	44.8626	29054	4.3423	-6179.7	-5934.5	62.52	35.94	53.99	1072
58 60	44.5495 44.2380	27842 27530	4.3376 4.2589	-6073.9 -5967.8	-5827.0 -5719.2	64.43 66.29	35.57 35.27	55.32 55.47	1067 1067
62	43.9286	26333	4.1486	-5861.9	-5611.5	68.08	35.36	56.36	1051
64	43.6185	24698	3.9767	-5754.9	-5502.8	69.84	35.36	56.89	1023
66	43.3011	23833	3.8443	-5647.5	-5393.5	71.55	35.05	56.88	1009
70	42.6747	23132	3.6290	-5433.2	-5175.5	74.81	33.72	55.61	1002
72	42.3613	21546	3.5157	-5326.8	-5067.1	76.36	33.38	56.40	979
74	42.0415	20570	3.3957	~5219.9	-4958.3	77.87	33.28	56.75	961
78	41.3917	19119	3.1510	-5004.1	-4738.4	80.82	32.62	56.27	944
80	41.0645	18312	3.0490	-4896.8	-4628.9	82.22	32.32	56.40	917
82	40.7346	17246	2.9414	-4789.0	-4519.0	83.60	32.06	56.85	897
84	40.3976	16814	2.8357	-4680.5	-4408.2	84.96	31.68	56.29	887
86	40.0624	16159	2.7431	-4572.4	-4297.8	86.28	31.26	56.08	874
90	39.3826	14844	2.5573	-4356.0	-4076.7	88.82	30.68	56.24	846
92	39.0377	14116	2.4711	-4247.7	-3965.9	90.06	30.71	56.83	829
94	38.6877	13392	2.3773	-4138.4	-3854.0	91.28	30.54	57.04	811
98	37.9718	12166	2.2003	-3918.6	-3628.9	92.47	30.21	57.19	797
100	37.6081	11593	2.1202	-3807.9	-3515.4	94.80	30.01	57.42	764
102	37.2398	10973	2.0412	-3696.9	-3401.6	95.94	29.78	57.71	748
104	36.4832	10375	1.8920	-3585.4 -3472.1	-3287.U	97.05	29.04	58.27	732
108	36.0971	9363	1.8179	-3358.6	-3053.9	99.26	29.05	58.30	703
110	35.7046	8848	1.7471	-3244.8	-2936.7	100.33	28.96	58.73	687
112	35.3054	8338	1.6792	-3129.7	-2818.1	101.39	20.03	59.22	671
114	34.8970	7.790	1.5441	-2895.7	-2576.7	102.45	28.51	59.94	638
118	34.0530	6861	1.4810	-2776.8	-2453.8	104.53	28.35	60.89	623
120	33.6171	6421	1.4177	-2656.5	-2329.3	105.56	28.19	61.43	607
122	33.1709	6005	1.3560	-2534.7	-2203.1	106.58	28.09	62.04	591
124	32.7127	5573	1.2952	-2411.2	-2074.9	107.59	28.02	62.90	574
128	31.7566	4764	1.1771	-2157.7	-1811.3	109.62	27.99	64.91	539
130	31.2560	4394	1.1195	-2027.1	-1675.2	110.63	27.86	65.81	523
132	30.7377	4031	1.0624	-1893.4	-1535.5	111.64	27.50	66.62	507
134	30.2018	3686	1.0053	~1757.3	-1393.1	112.65	27.35	67.62	490
138	29.0644	3029	0.8994	-1254.3	-875.8	114.69	26.96	70.59	473
140	28.4585	2725	0.8473	-1119.7	-733.2	115.71	26.84	72.37	440
142	27.8219	2442	0.7945	-982.0	-586.6	116.75	26.76	74.19	422
144	27.1521	2164	U = 7 4 4 U D = 6 9 6 1	-840.8	-435.6	117.81	20.02	76.79	404
148	25.6934	1664	0.6444	-544.8	-116.7	119.99	26.95	82.90	367
150	24.8962	1 4 4 4	0.5994	-389.6	52.2	121.13	27.05	87.25	350
152	24.0386	1240	0.5489	-227.6	230.0	122.30	27.25	91.16	330
156	22.1503	907	0.4580	115.6	612.2	124.78	27.37	100.94	297
158	21.1127	777	0.4130	297.3	818.3	126.10	27.45	105.24	280
160	20.0302	675	0.3711	484.0	1033.1	127.45	27.59	108.90	265
165	17.2601	537	0.2869	954.4	1591.7	130.89	26.64	111.52	243
175	12.9850	592	0.1867	1753.0	2600.1	136.83	25.80	86.96	229
180	11.6239	678	0.1593	2056.8	3003.1	139.10	25.23	75.07	231
185	10.5950	772	0.1398	2316.7	3354.9	141.03	24.74	66.43	234
190	9.13804	867 960	0.1136	2545.9	3009.5	142.71	24.36	60.07 55.47	237
200	8.59705	1050	0.1043	2945.1	4224.6	145.56	23.84	51.90	245
205	8.13875	1136	0.0966	3124.8	4476.3	146.80	23.67	49.09	249
210	7.74183	1220	0.0905	3295.5	4/16.4	147.96	23.55	47.08	253
215 220	7.39508 7.08696	1301	0.0849	3459.0 3616.9	4946.5 5169.0	149.04 150.06	23.47	45.23	257 261
225	6.81183	1456	0.0761	3770.1	5385.0	151.03	23.38	42.65	264
230	6.56294	1530	0.0726	3919.7	5595.8	151.96	23.36	41.75	268
235	6.13058	1602	0.0691	4066.1	5801.8	152.85	23.36	40.80	271
245	5.94082	1739	0.0635	4351.4	6203.0	154.52	23.37	39.48	278
250	5.76506	1807	0.0611	4491.0	6399.1	155.31	23.39	38.95	281
255 260	5.60189 5.44982	1873 1938	0.0590	4629.1 4765.7	6592.7 6784.1	156.08 156.82	23.42 23.45	38.50 38.10	285 288
265	5.30762	2002	0.0551	4901.3	6973.8	157.55	23.48	37.75	291
270	5.17423	2065	0.0534	5035.8	7161.7	158.25	23.53	37.45	294
275	5.04875	2127	0.0518	5169.6	7348.3	158.93	23.58	37.19	297
285	4.93042	2100	0.0503	5435.1	7717.9	160,25	23.68	36.75	303
290	4.71261	2308	0.0476	5567.1	7901.3	160.89	23.75	36.58	306
295	4.61204	2367	0.0464	5698.7	8083.8	161.51	23.81	36.43	309
31111	4,21641	14/5	1.455	20.11.	0(05.0	10/11	(3.88	10 + 11	317
## 12 MN/m<sup>2</sup> ISOBAR

TEMPERATURE	OENSITY	ISOTHERM	ISOCHORE	INTERNAL	ENTHALPY	ENTROPY	Cv	Cp	VELOCITY
(1F12 1900)	MOL/L	J/MOL	MN/m <sup>2</sup> ~ K	J/MOL	J/MOL	J/MOL-K	J / M	0L <del>-</del> K	M/S
* 54.641	45.1093	30291	4.3474	=6276.9	=6010.9	61.11	36.17	52.93	10.80
56	44.8968	29293	4.3441	-6215.7	-5938.5	62.44	35.93	53.83	1075
58	44.5853	28008	4.3392	-6100.5	-5831.3	64.36	35.57	55.18	1069
60	44.2742	27687	4.2707	-5994.7	-5723.7	66.21	35.27	55.43	1070
62 64	43.9664	26526	4.1695	-5889.2	-5616.3	68.00 69.75	35.37	56.39 56.87	1055
66	43.3429	24022	3.8445	-5675.7	-5398.9	71.46	35.13	56.75	1011
68	43.0275	23925	3.7371	-5568.1	-5289.2	73.13	34.46	55.90	1011
70	42.7177	23315	3.6341	-5462.1	-5181.2	74.72	33.78	55.51	1004
72	42.4075	21779	3.5269	-5356.3	-5073.3	76.27	33.42	56.29	983
74	42.0899	20815	3.4072	-5250.0	-4964.9	77.78	33.33	56.63	965
78	41.4437	19370	3.1544	-5142+3	= 4 8 9 9 • U	/ 9. 2/ 80. <b>7</b> 2	33.10	56.10	947
80	41.1188	18520	3.0556	-4928.2	-4636.4	82.13	32.40	56.25	920
82	40.7922	17505	2.9500	-4821.1	-4526.9	83.50	32.15	56.65	901
84	40.4567	16361	2 7/06	-4/13+0	-4416.4	84.80	31.78	56.14	889
88	39.7895	15711	2.6580	-4605.5	-4196.2	87.46	30.88	55.87	865
90	39.4495	15046	2.5663	-4390.3	-4086.1	88.71	30.75	56.06	850
92	39.1080	14344	2.4830	-4282.7	-3975.9	89.94	30.77	56.62	833
94	38.7617	13631	2.3930	-4174.1	-3864.5	91.16	31.60	56.89	817
96	38.4089	13028	2.3015	-4064.9	-3752.5	92.35	30.25	56.71	802
100	37.6936	11821	2.1355	-3845.9	-3527.6	93.92	30.05	57.20	770
102	37.3300	11211	2.0569	-3735.8	-3414.4	95.80	29.83	57.46	754
104	36.9617	10622	1.9816	-3625.2	-3300.5	96.91	29.66	57.81	738
106	30.5835	10088	1.9090	-3512.9	-3184.9	98.02	29.40	58.U1 58.0/	724
110	35.8161	90.85	1.7656	- 3287.6	-2952.5	100.18	28.98	58.40	n94
112	35.4236	8589	1.6971	-3173.7	-2834.9	101.23	28.85	58.78	079
114	35.0234	8036	1.6319	-3058.7	-2716.1	102.28	28.72	59.52	662
116	34.6138	7572	1.5648	-2942.4	-2595.7	103.32	28.53	59.84	647
118	34.1963 33.7699	6669	1.5014	-2824.9	-2474.0 -2350.8	104.34 105.36	28.37 28.21	60.89	631 615
122	33.3340	6259	1.3775	-2586.0	-2226.0	106.38	28.10	61.39	60 ũ
124	32.8881	5829	1.3176	-2464.4	-2099.5	107.38	28.04	62.18	583
126	32.4309	5428	1.2586	-2341.2	-1971.2	108.38	28.14	63.10	500
130	31.4770	5020	1.1443	-2046.9	-1705.7	110.37	27.86	64.74	534
132	30.9779	4297	1.0885	-1955.8	-1568.4	111.37	27.49	65.42	519
134	30.4636	3955	1.0333	-1822.5	-1428.6	112.36	27.33	66.31	503
136	29.9318	3631	0.9794	-1425.2	-1024.3	113.35	27.17	67.27	486
138 140	29.3804 28.8079	3302 3001	0.9295 0.8787	-1296.7 -1166.3	-888.3 -749.7	114.35 115.34	26.89 26.76	68.71 70.16	471 455
142	28.2097	2719	0.8276	-1033.2	-607.8	116.35	26.68	71.64	438
144	27.5867	2442	0.7779	-897.6	-462.6	117.37	26.69	73.57	421
146	26.9333	2183	0.7303	-758.6	-313.1	118.40	26.78	75.96	404
148	26.2489	1942	0.6831	-616.2	-159.0	119.45	20.80	78.42	387
152	24.7671	1513	0.5915	-319.3	165.2	121.61	26.93	84.24	353
154	23.9657	1327	0.5447	-164.1	336.6	122.73	27.06	86.99	335
156	23.1215	1163	0.5049	- 4 + 4	514.6	123.88	27.06	91.04	321
158	22.2335	1019	J.4619	159.8	699.5	125.05	27.04	93.95	305
160	21.3108	833	0.4212	327.5	890.6	126.26	27.08	96.61	291
165	18.8976	697	0.3361	754.0	1389.0	129.32	26.18	101.06	266
175	14.6206	638	0.2222	1545.1	2365.9	135.07	25.87	89.22	240
180	13.0825	698	0.1884	1868.4	2/85.7	137.44	25.40	78.91	239
185	11.8889	777	0.1640	2147.8	3157.1	139.48	24.95	70.25	240
190	10.9470	864	0.1457	2393.8	3490.0	141.25	24.56	63.49	242
195	10.1855	952	0.1315	2615.3	3793.4	142.83	24.25	58.38	246
200	9.55495	1040	0.1202	2818.6	4074.5	144.25	24.01	54.43	249
210	8.56537	1210	0.1033	3186.9	4587.9	145.55	23.69	48.95	256
215	8.16703	1291	0.0965	3357.3	4826.6	147.88	23.59	46.85	260
220	7.81458	1370	0.0911	3521.3	5279 5	148.94	23.52	45.35	264
230	7.21846	1522	0.0819	3834-0	5495.4	150.90	23.45	42.89	271
235	6.96302	1596	0.0778	3984.5	5707.8	151.81	23.44	41.84	274
240	6.72961	1667	0.0745	4132.0	5915.2	152.68	23.44	41.09	277
245	6.51569	1738	0.0714	4276.9	6118.6	153.52	23.45	40.36	281
250	6.31819	1806	0.0686	4419.7	6319.0	154.33	23.46	39.80	284
255	5.96618	1936	0.0636	4500.0	6711.1	155.87	23.50	38.77	290
265	5.80733	2001	0.0615	4837.5	690'3.9	156.60	23.53	38.37	293
270	5.65857	2065	0.0595	4974.2	7094.8	157.32	23.56	38.02	296
275	5.51883	2129	0.0577	5109.8	7284.2	158.01	23.60	31.72	299
285	5.26298	2253	0.0560	5378.7	7658-8	159.35	23.70	37.23	305
290	5.14541	2314	0.0529	5512.3	7844.4	159.99	23.75	37.02	308
295	5.03394	2374	0.0516	56+5.3	8029.1	160.63	23.81	36.85	311
300	4.92804	2434	0.0503	5777.9	8213.0	161.24	23.87	36.69	314

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## TABLE 16. THERMOOYNAMIC PROPERTIES OF FLUORINE

#### 13 MN/m<sup>2</sup> ISOBAR

TEMPERATURE (IPTS 1968)	OENSITY	ISOTHERM DERIVATIVE	ISOCHORE OERIVATIVE	INTERNAL ENERGY	ENTHALPY	ENTROPY	Cv	Сp	VELOCITY OF SOUND
к	MOL/L	J/MOL	MN∕m <sup>2</sup> <del>-</del> K	J/MOL	J/MOL	J/MOL-K	J / M	IOL - K	M/S
* 54.737	45.1275	30494	4.3488	-6297.6	-6009.5	61.13	36.15	52.82	1083
56	44.9308	29530	4.3457	-6231.7	-5942.3	62.37	35.93	53.67	1077
58	44.6209	28172	4.3407	-6126.9	-5835.6	64.28	35.56	55.04	1071
60	44.3102	27844	4.2822	-6021.6	+5728.2	66.13	35.26	55.39	1073
62	44.0040	26737	4.1909	-5916.5	-5621.1	67.92	35.37	56.40	1059
64	43.6987	25168	4.0001	-5703.8	-5513.1	59.67 71.38	35.21	56.60	1030
68	43.0692	24074	3.7363	-5596.5	-5294.7	73.04	34.54	55,80	1012
70	42.7605	23504	3.6374	-5490.8	-5186.8	74.64	33.84	55.39	1006
72	42.4531	22031	3.5381	-5385.7	-5079.5	76.18	33.46	56.16	986
74	42.1376	21090	3.4186	-5279.8	-4971.3	77.69	33.38	56.47	969
76	41.8161	20185	3.2900	-51/2.6	-4861.8	79.18	33.23	56.54	951
80	41.1725	18743	3.0612	-4959.5	-4643.7	82.03	32.48	56.07	923
82	40.8488	17789	2,9589	-4853.0	-4534.7	83.40	32.23	56.42	905
84	40.5152	17189	2.8461	-4745.4	-4424.5	84.75	31.87	55.99	891
86	40.1847	16569	2.7557	-4638.4	-4314.9	86.07	31.45	55.85	880
88	39.8526	15949	2.6659	-4531.2	-4205.0	87.35	30.96	55.65	869
90	39.5155	15247	2.5747	-4424.4	-4095.4	88.61	30.83	55.89	853
92	39.1772	14577	2.4937	-4317.4	-3985.6	89.83	30.83	56.40	838
96	38.4850	13252	2.3170	-4101.1	-3763.3	92.23	30.28	56.54	807
98	38.1332	12620	2.2342	-3992.7	-3651.8	93.40	30.18	56.84	791
100	37.7773	12049	2.1517	-3883.6	-3539.5	94.55	30.08	57.01	775
102	37.4183	11451	2.0718	-3774.3	-3426.9	95.67	29.88	57.19	759
104	37.0548	10873	1.9992	-3664.6	-3313.8	96.78	29.68	57.52	745
106	36.6815	10313	1.9266	-3553.2	-3198.8	97.88	29.41	57.70	730
110	35.9248	9320	1.7846	-3329.8	-2968.0	100.03	28.98	58.10	701
112	35.5384	8836	1.7154	-3217.0	-2851.2	101.08	28.87	58.40	686
114	35.1460	8284	1.6510	-3103.4	-2733.5	102.12	28.73	59.10	670
116	34.7438	7817	1.5854	-2988.2	-2614.1	103.15	28.54	59.44	655
118	34.3346	7349	1.5213	-2872.2	-2493.6	104.17	28.38	59.90	639
120	33.91/1	0919	1.4600	-2194.0	-2371.5	105.10	20.22	60.30	624
122	33.4907	6509	1.3984	-2636.2	-2248.0	106.18	28.11	60.79	609
124	33.0560	6063	1 281 7	-2516.3	-1996 3	107.17	28 14	62 76	593
128	32,1548	5287	1.2243	-2270.9	-1866.6	109.15	28.01	63.10	560
130	31.6859	4918	1.1687	-2144.8	-1734.5	110.13	27.86	63.82	545
132	31.2038	4558	1.1139	-2016.0	-1599.4	111.11	27.48	64.39	530
134	30.7984	4218	1.0598	-1885.4	-1462.0	112.09	27.31	65.16	515
136	30.1977	3895	1.0072	-1461.2	-1030.7	113.06	27.10	65.95	499
138 140	29.6715 29.1270	3570 3270	0.9571	-1336.0	-762.8	114.03 115.00	26.84 26.69	67.06 68.32	485
142	28.5604	2987	0.8582	-1079.8	-624.6	115.98	26.63	69.56	453
144	27.9750	2712	0.8094	-948.8	-484.1	116.97	20.60	71.05	437
146	27.3653	2451	0.7632	-815.2	-340.1	117.96	26.67	73.00	420
148	26.7310	2211	0.7175	-678.7	-192.4	118.97	26.71	74.95	404
150	26.0691	1989	0.6744	-539.4	-40.8	119.98	26.70	77.17	389
152	25.3760	1778	0.684.7	-396.9	115.4	121.02	20.14	79.31	373
156	23.8996	1415	0.5460	-101.9	442.1	123.14	26.83	84.35	342
158	23.1137	1262	0.5045	50.4	612.9	124.23	26.78	86.45	327
160	22.3016	1129	0.4650	205.1	788.0	125.33	26.77	88.37	313
155	20.1717	883	0.3806	597.4	1241.9	128.12	25.83	92.33	288
170	10.0384	755	0.3114	1759.0	2467 /	130.92	25.97	93.04	267
180	10.0997	767	0.2189	1692.2	2590.5	135.95	25.45	80.57	255
185	13.1561	805	0.1897	1985.2	2973.3	138.05	25.06	72.82	248
190	12.0963	879	0.1677	2245.1	3319.8	139.90	24.70	66.22	249
195	11.2329	960	0.1505	2479.1	3636.4	141.54	24.39	60.88	251
200	10.5158	1043	0.1371	2693.3	3929.5	143.03	24.15	56.72	254
205 210	9.91192 9.39274	1127 1209	0.1258 0.1169	2891.9 3078.8	4203.5 4462.8	144.38 145.63	23.96 23.81	53,24 50,70	257 260
24 5	8 0/2/4	1200	0 4000	7056 4	6700 0	146 80	27 70	1.8.70	267
215	0.94241	1290	0.1020	3626.1	4109.8	140.00	23.62	40.39	263
225	8,19270	1446	0.0964	3589.7	5176.5	148.92	23.57	45.14	270
230	7.87584	1521	0.0916	3748.5	5399.1	149.90	23.54	43.99	274
235	7.59002	1595	0.0869	3903.1	5615.9	150.83	23.52	42.85	277
240	7.32949	1668	0.0831	4054.4	5828.0	151.72	23.51	42.01	280
245	7.09113	1739	0.0795	4202.7	6035.9	152.58	23.52	41.22	283
250	6.66889	1809	0.0783	4348.9	6441.5	154,20	23.54	39.94	289
260	6.48050	1943	0.0707	4634.0	6640.0	154.98	23.56	39.47	293
265	6.30509	2009	0.0681	4774.2	6836.0	155.72	23.58	38.98	296
270	6.14092	2074	0.0659	4912.9	7029.9	156.45	23.60	38.60	299
275	5.98814	21 33	0.0638	5050.3	7221.3	157.15	23.62	38.24	302
280	5.84306	2197	0.0619	5186.9	7411.7	157.84	23.65	37.95	305
205	5.57690	2200	0.0501	5457.6	7788.6	159.16	23.74	37.45	310
295	5.45438	2383	0.0569	5592.0	7975.4	159.80	23.80	37.25	313
300	5.33809	2444	0.0554	5725.8	8161.2	160.42	23.85	37.08	316

## 14 MN/m<sup>2</sup> ISOBAR

TEMPERATURE	DENSITY	ISOTHERM OFRIVATIVE	ISOCHORE DERIVATIVE	INTERNAL	ENTHALPY	ENTROPY	Cv	Cp	VELOCITY OF SOUND
ĸ	MOL/L	J/MOL	MN/m <sup>2</sup> -K	J/MOL	J/MOL	J/MOL-K	J / MC	)L – К	M/S
* 54.832	45.1455	30689	4.3500	-6318.2	+6008.1	61.16	36.13	52.72	1086
56	44.9646	29766	4.3470	-6257.5	-5946.2	62.30	35.92	53.51	1080
58 60	44.6563 44.3460	28336 27999	4.3419 4.2934	-6153.3 -6048.3	-5839.8 -5732.6	64.20 66.06	35.56 35.26	54.91 55.35	1073 1075
62	44.0412	26967	4.2025	-5943.7	-5625.8	67.84	35.36	56.30	1063
64	43,7382	25454	4.0237	-5838.2	-5518.2	69.58	35.50	56.78	1035
66	43.4254	24480	3.8460	-5731.8	-5409.4	71.29	35.29	56.43	1015
68	43.1106	24230	3.7359	+5624.8	-5300.0	72.96	34.63	55.70	1013
70	42.8028	23699	3.6391	-5519.4	-5192.3	74.55	33.90	55.25	1008
74	42.1847	21394	3.4300	-5309.5	+4977.7	77.60	33.42	56.29	974
76	41.8654	20421	3.3020	-5202.9	-4868.5	79.08	33.29	56.44	955
78	41.5461	19773	3.1651	-5096.3	-4759.3	80.53	32.90	55.80	939
80	41.2255	18978	3.0659	-4990.5	+4650.9	81.93	32.56	55.87	926
82	40.9046	18095	2.9681	-4884.7	-4542.4	83.30	32.31	56.17	910
84	40.5731	17389	2.8546	-4777.5	-4432.4	84.65	31.97	55.88	894
88	40.2446	16784	2.6731	-4671.U	-4323.1	85.97	31.54	55.66	883
9.0	39.5806	15447	2.5840	-4904.4	-4213.0	88.50	30.91	55.74	85 b
92	39.2452	14813	2,5034	-4351.9	- 3995 . 2	89.72	34.89	56.17	842
94	38.9058	14130	2.4224	-4244 * 7	-3884.9	90.93	30.72	56.51	827
96	38.5599	13478	2.3339	-4136.9	-3773.9	92.12	30.30	56.40	812
98	38.2118	12851	2.2514	-4029.3	-3662.9	93.28	30.20	56.67	797
100	37.8596	12278	2.1691	-3920.9	+3551.1	94.42	30.10	50.83	/81
102	37.5047	11693	2.0859	-3812.4	-3439.1	95.54	29.92	56.90	765
104	31.1451	11127	2.0165	-3703.5	-3320.0	90.65 07 7/	29.69	57.23	751
108	36.4061	10057	1.8733	-3482.4	-3097.8	98.82	29.10	57.54	723
110	36.0308	9552	1.8043	-3371.6	-2983.0	99.88	28.97	57.85	709
112	35.6500	9078	1.7352	-3259.8	-2867.1	100.93	28.87	58.10	693
114	35.2649	8537	1.6698	-3147.4	-2750.4	101.96	28.74	58.68	677
116	34.8697	8061	1.6056	-3033.4	-2631.9	102.98	28.55	59.06	662
120	34.0592	7161	1.4806	-2802.6	-2391.6	105.00	28.22	59.89	632
122	33.6414	6756	1.4200	-2685.3	-2269.2	105.99	28.11	60.29	617
124	33.2171	6334	1.3610	-2567.0	-2145.6	106.98	28.05	60.92	602
126	32.7830	5938	1.3034	-2447.3	-2020.3	107.95	28.15	61.69	585
128	32.3394	5544	1.2469	-2325.2	-1892.3	108.93	28.01	62.33	570
130	31.88841	5174	1.1780	-2201.1	-1/62+0	109.90	27.680	62.95	555
134	30.9385	4015	1.0848	=1945.1	-1493.6	111.83	27.30	64.12	526
136	30.4463	4152	1.0327	-1495.1	-1035.2	112.79	27.07	64.75	511
138	29.9419	38 31	0.9840	-1372.7	-905.1	113.74	26.77	65.67	497
140	29.4212	3532	0.9393	-1240+7	-772.9	114.69	20.03	00.09	402
142	28.8814	3247	0.8703	-1122.8	-638.0	115.64	26.59	67.91	467
146	27.7530	2711	0.7938	-866.3	-361.8	117.56	26.57	70.63	436
148	27.1585	2472	0.7494	-734.7	-219.2	118.53	20.64	72.23	420
150	26.5415	2249	0.7050	-600.7	-73.2	119.51	26.63	73.70	405
152	25.9012	2035	0.6633	-464.4	76.1	120.50	26.61	75.60	390
154	25.2379	1840	0.6205	-325.8	228.9	121.50	26.65	77.24	375
158	23.8389	1503	0.5426	= 104+2	546.5	123.54	20.00	79.51	361
160	23.1070	1361	0.5042	104.6	710.4	124.57	26.55	82.52	334
165	21.1933	1083	0.4209	471.0	1131.6	127.16	25.58	85.66	309
170	19.2435	913	0.3503	841.1	1568.6	129.77	25.78	87.51	286
175	17.3910	835	0.2935	1199.5	2004.5	132.30	25.75	85.45	270
185	14.3621	857	0.2163	1832.3	2807.1	136.76	25.44	74.05	258
190	13,2135	914	0.1907	2102.4	3161.9	138.65	24.77	68.07	257
195	12.2630	984	0.1706	2346.7	3488.3	140.35	24.49	62.84	258
200	11.4677	1060	0.1548	2570.5	3791.3	141.88	24.25	58.64	260
205	10.7954	1139	0.1416	2777.6	4074.5	143.28	24.06	55.01	262
210	10.21/2	1210	0.1311	29/201	4342.0	144.07	23.91	22:30	200
215	9.71597	1297	0.1218	3156.0	4596.9	145.77	23.80	49.83	267
225	8.88330	1452	0.1074	3500.5	5076.5	147.95	23.65	46.30	273
230	8.53228	1527	0.1018	3663.8	5304.7	148.96	23.61	45.04	277
235	8.21601	1601	0.0964	3822.5	5526.5	149.91	23.59	43.82	280
240	7.92825	1673	0.0920	3977.3	5743.2	150.82	23.58	42.90	283
245	7.66541	1745	0.0879	4128.9	5955.3	151.70	23.58	42.04	286
250	7.20085	1615	0.0843	4611.0	6368 /	152.54	23.60	41.35	289
260	6.99409	1951	0.0778	4568.6	6570.2	154.14	23.61	40.03	295
265	6.80179	2018	0.0750	4711.1	6769.4	154.89	23.63	39.59	298
270	6.62204	2083	0.0725	4852.0	6966.2	155.63	23.65	39.17	301
275	6.45388	2148	0.0700	4991.6	7160.8	156.34	23.67	38.73	304
280	6.29576	2212	0.0677	5129.8	7353.5	157.04	23.69	38.34	307
205	6.00640	2336	0.0638	5403.1	7733.9	158-37	23.73	37.71	313
295	5.87295	2395	0.0623	5538.8	7922.6	159.02	23.77	37.64	316
300	5.74618	2457	0.0607	5673.9	8110.3	159.65	23.82	37.45	319

## 15 MN∕m² ISOBAR

TEMPERATURE (IPTS 1968)	DENSITY	ISOTHERM DERIVATIVE	ISOCHORE Derivative	INTERNAL ENERGY	ENTHALPY	ENTROPY	Cv	Сp	VELOCITY OF SOUND
К	MOL/L	J/MOL	MN/m <sup>2</sup> -K	J/MOL	J/MOL	J∕MOL∸K	J/M	DL - К	M/S
* 54.927	45.1635	3ù877	4.3510	-6338.8	-6006.6	61.18	36.11	52.62	1088
58	44.9980	28499	4.3482	-6179.6	-5950.0	64.12	35.56	53.35	1083
60	44.3817	28154	4.3044	-6075.0	-5737.0	65.98	35.26	55.31	1078
62 64	44.0781 43.7773	27213 25774	4.2139 4.0430	-5970.8 -5865.8	-5630.5	67.76 69.50	35.36	56.18 56.71	1067
66	43.4660	24748	3.8472	-5759.7	-5414.6	71.21	35.36	56.25	1018
68	43.1517	24394	3.7358	-5652.9	-5305.3	72.88	34.71	55.60	1014
70	42.8449	23901	3.6558	=5547.9 +5404 0	-5197.8	74.47	33.97	55.10	1010
74	42.2311	21725	3.4412	-5339.1	-4983.9	77.51	33.46	56.08	979
76	41.9141	20676	3.3150	-5232.9	-4875.0	78.99	33.35	56.34	959
80	41.2778	19226	3.0698	-5021.4	-4658.0	81.84	32.99	55.69 55.65	943
82	40.9593	18422	2.9774	-4916.1	-4549.9	83.20	32.39	55.91	915
84	40.6302	17590	2.8634	-4809.4	-4440.3	84.55	32.00	55.46	898 886
88	39.9761	16447	2.6797	-4597.3	-4222.1	87.15	31.14	55.18	876
90	39.6450	15646	2.5927	-4491.8	-4113.4	88.39	30.99	55.59	859
92	39.3122	15053	2.4355	-4386.1 -4279.6	-4004.5	89.61	30.96	55.92	846
96	38.6334	13706	2.3505	-4172.5	-3784.2	92.00	30.33	56.26	818
98 100	38.2889 37.9403	13084 12507	2.2687 2.1876	-4065.6 -3957.9	-3673.8 -3562.6	93.16 94. <b>30</b>	30.21 30.10	56.51 56.68	803 787
102	37.5893	11938	2.1034	-3850.1	-3451.1	95.42	29.95	56.71	771
104	37.2346	11384	2.0328	-3742.1	-3339.2	96.52	29.70	56.93	758
106	36.5044	10761	1.9639	-3632.7	-3225.8	97.61	29.41	57.29	743
110	36.1342	9783	1.8242	-3412.8	-2997.7	99.74	28.96	57.61	716
112	35.7588	9315	1.7555	-3302.0	-2882.5	100.78	28.86	57.84	701
114	35.3803 34.9919	8794	1.6253	-3190.7	-2/66./	101.80	28.74	58.69	685
118	34.5981	7842	1.5616	-2964.3	-2530.8	103.83	28.38	59.03	055
120	34.1966	7406	1.5010	-2849.6	-2411.0	104.82	28.22	59.43	641
122	33.7869	6998	1.4411	-2733.6	-2289.7	105.81	28.11	59.83	626
126	32.9480	6189	1.3247	-2498+6	-2043.4	107.75	28.15	61.06	594
128	32.5158	5799	1.2689	-2378.1	-1916.8	108.72	28.01	61.63	579
130	32.0728	5427	1.2138	-2255.8	-1788.1	109.68	27.86	62.17	565
134	31.1559	4728	1.1090	-2131+2	-1523.4	111.58	27.29	63.21	551
136	30.6801	4404	1.0575	-1527.0	-1038.1	112.53	27.05	63.75	523
138 140	30.1945 29.6944	4088 3789	1.0099 0.9620	-1407.0 -1285.7	-910.3 -780.6	113.46 114.39	26.69 26.58	64.46 65 <b>.3</b> 6	510 495
142	29.1778	3501	0.9149	-1162.7	-648.6	115.33	26.55	66.42	480
144	28.6493	3230	0.8674	-1038.5	-515.0	116.26	26.53	67.39	465
146	28.1055	2966	0.8220	-913.0	-379.3	117.20	26.52	68.63	449
150	26.9629	2501	0.7358	-655.8	-99.5	119.09	20.58	71.26	420
152	26.3646	2285	0.6944	-524.5	44.4	120.04	26.54	72.68	406
154	25.7477	2087	0.6532	-391.5	191.1	121.00	26.53	74.01	391
158	24.4566	1740	0.5773	-119.3	494.0	122.94	26.51	77.09	365
160	23.7856	1592	0.5398	19.0	649.6	123.92	26.40	78.16	352
165	22.0389	1289	0.4576	365.6	1046.2	126.36	25.41	80.58	328
175	18.5028	971	0.3273	1061.6	1872.3	131.22	25.70	82.13	286
180	16.8950	926	0.2803	1389.0	2276.9	133.50	25.44	78.96	275
185	15.4831	931	0.2433	1691.5	2660.3	135.60	25.11	74.16	269
190	14.2781	10.24	0.2144	2219.7	3350.9	139.24	24.54	64.21	266
200	12.3991	1090	0.1732	2451.3	3661.1	140.81	24.32	60.11	266
205 210	11.6652 11.0322	1163 1238	0.1580 0.1459	2666.1 2867.4	3952.0 4227.0	142.25 143.58	24.13 23.99	56.50 53.68	268 270
215	10.4825	1314	0.1352	3057.4	4488.4	144.81	23.88	51.12	272
220	9.99820	1390	0.1266	3238.7	4738.9	145.96	23.79	49.19	275
230	9.18492	1539	0.1123	3580.1	5213.2	148.07	23.68	46.02	281
235	8.83866	1612	0.1063	3742.7	5439.8	149.04	23.65	44.74	283
240	8.52394	1685	0.1013	3901.1	5660.9	149.97	23.64	43.75	286
250	7.97303	1826	0.0925	4055.9	6089.0	151.72	23.64	42.00	292
255	7.73022	1895	0.0885	4356.8	6297.2	152.55	23.65	41.30	295
260	7.50510	1963	0.0852	4503.7	6502.3	153.34	23.67	40.73	298
265	7.29596	2030	0.0820	4648.5	6704.4	154.11	23.68	40.17	301
275	6.91806	2161	0.0764	4933.2	7101.4	155.58	23.72	39.25	307
280	6.74656	2225	0.0739	5073.3	7296.7	156.29	23.74	38.83	310
285	6.58533	2289	0.0717	5212.2	7490.0	156.97	23.76	38.51	312
295	6.28937	2413	0.0675	5486.7	7871.7	158.29	23.79	37.88	318
300	6.15331	2474	0.0657	5622.3	8060.0	158.92	23.81	37.63	321

## 16 MN∕m² ISOBAR

TEMPERATURE	DENSITY	ISOTHERM DERIVATIVE	ISOCHORE	INTERNAL	ENTHALPY	ENTROPY	Cv	Сp	VELOCITY OF SDUND
К	MOL/L	J/MDL	MN/m <sup>2</sup> - K	J/MOL	J/MOL	J/MOL-K	J / MC	L <del>-</del> K	M/S
* 55.022	45.1813	31058	4.3518	-6359.3	-6005.2	61.21	36.10	52.53	1091
56	45.0312	30232	4.3492	-6309.0	-5953.7	62.15	35.92	53.20	1086
58 60	44.7265 44.4171	28661 28308	4.3439 4.3152	-6205.9 -6101.6	-5848.1 -5741.4	64.05 65.90	35.55 35.26	54.64 55.26	1077 1081
62	44.1147	27477	4.2249	~5997.8	-5635.2	67.68	35.36	56.06	1071
64	43.8158	26124	4.0639	-5893.3	-5528.1	69.42	35.56	56.64	1046
66	43.5062	25039	3.8508	-5787.4	-5419.7	71.13	35.43	56.08	1021
70	42.8865	24565	3.6378	-5576.3	-5310.0	74.39	34.79	55.93	1012
72	42.5868	22892	3.5604	-5473.0	-5097.3	75.91	33.58	55.57	998
74	42.2767	22082	3.4523	-5368.5	-4990.0	77.42	33.51	55.85	984
76	41.9621	20950	3.3289	-5262.8	-4881.5	78.90	33.41	56.24	963
80	41.8460	19486	3.0727	-5052.1	-4665.0	81.75	32.73	55.42	932
82	41.0131	18768	2.9858	-4947.4	-4557.2	83.11	32.46	55.62	920
86	40.0007	17231	2.7711	-4041.2	-4440.0	84.40	31.72	55.25	901
88	40.0365	16706	2.6857	-4630.1	-4230.4	87.04	31.22	54.93	879
90	39.7085	15845	2.6007	-4525.2	-4122.2	88.29	31.07	55.43	863
92	39.3781	15296	2.5198	-4420.0	-4013.7	89.51	31.03	55.66	850
94	38.7058	13935	2.3661	-4314.2	-3904.4	90.71	30.37	56.11	823
98	38.3646	13319	2.2860	-4101.6	-3684.6	93.04	30.22	56.34	808
100	38.0195	12737	2.2072	-3994.6	-3573.8	94.18	30.09	56.55	794
102	37.6722	12184	2.1220	-3887.5	-3462.8	95.29	29.97	56.53	778
104	36.9634	10984	1.9837	-3671.8	-3238.9	90.39	29.39	57.18	750
108	36.6006	10512	1.9107	-3562.6	-3125.5	98.55	29.10	57.10	737
110	36.2353	10011	1.8435	-3453.7	-3012.1	99.59	28.94	57.38	723
112	35.8648	9546	1.7765	-3343.7	-2897.6	100.63	28.84	57.02	709
116	35.1106	8551	1.6446	-3121.8	-2666.0	102.66	28.55	58.32	678
118	34.7236	8091	1.5822	-3009.3	-2548.5	103.66	28.37	58.65	663
120	34.3294	7651	1.5211	-2895.8	-2429.7	104.65	28.21	59.00	649
122	33.9274	7238	1.4618	-2781.1	-2309.5	105.63	28.10	59.40	634
126	33.1064	6437	1.3460	-2548.8	-2065.5	107.56	28.15	60.50	603
128	32.6846	6050	1.2907	-2429.9	-1940.4	108.51	28.01	61.00	589
130	32.2530	5676	1.2361	-2309.2	-1813.2	109.47	27.86	61.50	574
132	31.8122	5317	1.1832	-2180.4	-1683.4	110.41	27.47	61.81	561
134	31.3620	4976	1.1323	-1557.3	-1039.5	112.28	27.04	62.86	533
138	30.4319	4339	1.0328	-1439.4	-913.6	113.20	26.65	63.27	521
140	29.9499	4041	0.9892	-1320.5	-786.3	114.11	26.50	64.31	508
142	29.4537	3750	0.9398	-1200.0	-656.8	115.03	26.51	65.07	492
144	28.9474	3481	0.8948	-1078.6	- 525 .8	115.95	20.53	66.07	478
148	27.8943	2976	0.8063	-831.9	- 258.3	117.78	26.53	68.08	448
150	27.3443	2746	0.7649	-706.0	-120.9	118.70	26.56	69.31	434
152	26.7803	2529	0.7233	-578.8	18.7	119.62	26.50	70.34	420
154	25.6058	2329	0.6671	= 450 + 2	304.7	120.55	20.40	72.92	407
158	24.9955	1975	0.6091	-188.4	451.7	122.42	26.45	73.97	381
160	24.3725	1821	0.5724	-55.7	600.7	123.36	26.36	74.84	369
165	22.7580	1498	0.4913	275.3	978.3	125.68	25.25	76.58	346
175	19.4611	1122	0.3596	942.7	1764.9	130.31	25.65	78.87	301
180	17.9117	1047	0.3101	1262.9	2156.2	132.51	25.45	76.99	289
185	16.5081	1025	0.2702	1563.5	2532.7	134,58	25.11	73.47	281
190	19.2760	1040	0.2127	2099.3	3225.1	138.22	24.56	65.01	276
200	13.2996	1134	0.1919	2336.9	3540.0	139.82	24.35	61.10	274
205 210	12.5132 11.8312	1198 1267	0.1751 0.1613	2558.U 2765.4	3836.7 4117.7	141.28 142.64	24.18 24.04	57.67 54.84	274 276
215	11.2368	1339	0.1492	2961.0	4384.9	143.90	23.93	52.24	277
220	10.7124	1412	0.1394	3147.3	4640.9	145.07	23.85	50.24	280
225	10.24//	1485	0.1232	3365.1	400/.0	146.18	23.74	40.35	282
235	9.45564	1630	0.1165	3664.0	5356.1	148.22	23.71	45.59	287
240	9.11462	1702	0.1108	3825.9	5581.3	149.17	23.70	44.54	290
245	8.80411	1772	0.1054	3983.8	5801.1	150.08	23.69	43.50	293
250	8.25593	1841	0.1009	4138.5	6228.2	150.95	23.69	42.74	296
260	8.01259	1979	0.0928	4439.5	6436.3	152.59	23.71	41.33	301
265	7.78678	2046	0.0892	4586.5	6641.3	153.37	23.73	40.73	304
275	7.37912	2112	0.0861	4875.3	7043.6	154.86	23.77	40.25	307
280	7.19429	2242	0.0802	5017.3	7241.3	155.58	23.78	39.30	312
285	7.02069	2306	0.0777	5157.9	7436.9	156.27	23.80	38.95	315
290	6.85688	2369	0.0753	5297.3	7630.8	156.94	23.82	38.60	318
300	6.55600	2493	0.0711	5572.7	8013.2	158.24	23.85	38.02	323

\* TWO-PHASE BDUNOARY

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#### TABLE 16. THERMODYNAMIC PROPERTIES OF FLUORINE

## 17 MN/m<sup>2</sup> ISOBAR

TEMPERATURE	DENSITY	ISOTHERM	ISOCHORE	INTERNAL	ENTHALPY	ENTROPY	Cv	Сp	VELOCITY
(IPTS 1968) K	MOL/L	DERIVATIVE J/MOL	DERIVATIVE MN/m <sup>2</sup> + K	ENERGY J/MOL	J/MOL	J/MOL-K	J / MC	)L - К	OF SOUNO M/S
* 55 11C	4E 1001	71373	1. 7527	-6770 0	-6007 8	64 37	7 0.9	E2 //	1007
56	45.0642	30462	4.3500	-6334.6	-5957.4	62.08	35.92	53.05	1093
58	44.7613 44.4523	28822 28461	4.3446	-6232.0	-5852.2	63.97 65.82	35.55	54.51	1078
62	44.1509	27756	4.2357	-6024.8	-5639.7	67,60	35,36	55.92	1075
64	43.8538	26503	4.0864	-5920.6	-5533.0	69.34	35.59	56.56	1053
66	43.5459	25353	3.8666	-5815.0	-5424.6	71.05	35.49	56.02	1026
70	43.2331	24743	3.6350	-5709.0	-5315.7	74.31	34+87	55.40	1017
72	42.6302	23210	3.5633	-5501.8	-5103.0	75.83	33.63	55.30	1002
74	42.3216	22462	3.4632	-5397.7	-4996.0	77.33	33.55	55.61	990
76	42.0095	21240	3.3429	-5292.6	-4887.9	78.81	33.45	56.11	968
80	41.3805	19758	3.0749	-5082.6	-4671.8	81.65	32.81	55.17	935
82	41.0659	19132	2.9907	-4978.4	-4564.4	83.01	32.53	55.26	925
86	40.4199	17463	2.7753	-4767.7	-4347.1	85.67	31.81	55.03	892
88	40.0959	16970	2.6913	-4662.6	-4238.6	86.95	31.31	54.67	883
90	39.7712	16043	2.6081	-4558.3	-4130.9	88.18	31.15	55.27	866
92	39.4430	15542	2.5265	-4453.7	-4022.7	89.40	31.10	55.39	854
96	38.7770	14165	2.3803	-4242.8	-3804.4	91.77	30.41	55.94	828
98	38.4391	13555	2.3032	-4137.3	-3695.1	92.92	30.22	56.17	814
100	38.0973	12968	2.2261	-4031.0	-3584.8	94.06	30.08	56.41	800
102	37.7535	12432	2.1418	+3924.6	-3474.3	95.17	29.97	56.38	785
104	37.4063	11907	2.0024	-3817.9	-3363.5	96+27	29.73	56.98	770
108	36.6947	10736	1.9310	-3602.2	-3138.9	98.41	29.08	56.94	744
110	36.3340	10237	1.8623	-3494.0	-3026.1	99.45	28.92	57.15	730
112	35.9683	9771	1.7983	+3385.0	-2912.4	100.49	28.80	57.45	716
116	35.2259	8796	1.6639	-3165.0	-2682.4	102.51	28.55	57.97	686
118	34.8453	8342	1.6023	-3053.6	-2565.8	103.50	28.36	58.27	672
120	34.4580	7897	1.5410	-2941.3	-2447.9	104.48	28.19	58.58	657
122	34.0633	7474	1.4823	-2827.7	-2328.7	105.46	28.09	59.00	643
124	33.2589	6683	1.3671	-2713+4	-2086.9	106.42	28.14	59.39	612
128	32.8465	6300	1.3118	-2480.6	-1963.0	108.32	28.00	60.41	598
130	32.4254	5924	1.2578	-2361.4	-1837.2	109.26	27.86	60.88	584
132	31.9960	5564	1.2039	-2240.2	-1708.9	110.20	27.47	61.06	570
136	31.1107	4891	1.1046	-1586.1	-1039.6	112.04	27.03	62.08	554
138	30.6560	4587	1.0558	-1470.0	-915.5	112.94	26.63	62.32	532
140	30.1901	4288	1.0131	-1353.4	-790.3	113.85	26.42	63.18	520
142	29.7121	3993	0.9668	-1235.1	-662.9	114.75	26.47	64.12	505
144	29.2250	3726	0.9196	-1116.0	-534.3	115.65	20.54	64.80	489
148	28.2172	3221	0.8316	-874.9	-272.4	117.44	26.52	66.42	461
150	27.6934	2985	0.7914	-752.2	-138.3	118.34	26.56	67.59	447
152	27.1581	2768	0.7509	-628.4	-2.4	119.24	26.50	68.49	434
154	26.0484	2565	0.6759	-503.6	275.1	120.14	26.41	69.35 70.55	421
158	25.4744	2205	0.6387	-250.2	417.1	121.95	26.40	71.45	396
160	24.8902	2047	0.6028	-122.1	560.9	122.85	26.34	72.18	384
165	23.3829	1707	0.5225	196.2	923.2	125.08	25.14	73.38	362
170	21.8354	1456	0.4514	518•4 830 3	1296.9	127.31	25.53	75.42	336
180	18.8112	1182	0.3388	1151.2	2054.9	131.65	25.43	74.82	303
185	17.4364	1134	0.2966	1448.2	2423.1	133.67	25.07	72.26	293
190	16.2005	1127	0.2621	1726.6	2776.0	135.55	24.82	68.92	287
200	15.1107	1150	U • 2341 0 • 2111	1986+4	3111.4	137.29	24.38	61.68	284
205	13.3327	1245	0.1925	2454.1	3729.2	140.38	24.21	58.53	261
210	12.6089	1307	0.1770	2666.5	4014.8	141.76	24.08	55.76	282
215	11.9746	1373	0.1636	2867.1	4286.8	143.04	23.97	53.18	283
220	11.4134	1443	0.1526	3058.1	4547.5	144.24	23.89	51.15	285
230	10.4678	1513	0.1344	3416.6	5040.7	146.43	23.79	49.23	289
235	10.0648	1654	0.1269	3586.6	5275.7	147.44	23.76	46.36	291
240	9.69849	1725	0.1206	3751.8	5504.7	148.41	23.75	45.27	294
245	9.36532	1793	0.1144	3912.7	5727.9	149.33	23.74	44.14	296
255	8.77685	1930	0.1047	4224.4	6161.3	151.06	23.75	42.55	302
260	8.51561	1998	0.1006	4376.1	6372.4	151.88	23.76	41.90	305
265	8.27341	2065	0.0965	4525.3	6580.1	152.67	23.77	41.25	307
270	8.04746	2131	0.0931	4672.6	6785.0	153.44	23.79	40.75	310
280	7.63843	2262	0.0866	4961.9	7187-4	154.90	23.83	39.75	315
285	7.45260	2325	0.0839	5104.2	7385.3	155.60	23.85	39.38	318
290	7.27732	2389	0.0814	5245.2	7581.2	156.28	23.87	39.04	321
295	7.11175	2453	0.0790	5385.1	7775.5	156.95	23.88	38.71	323
500	0. 00004	2919	0.0101	112300	1 201+1	1 - 1 + 00	20.90	00.41	520

#### 18 MN/m<sup>2</sup> ISOBAR

TEMPERATURE	OENSITY	ISOTHERM OFRIVATIVE	ISOCHORE	INTERNAL	ENTHALPY	ENTROPY	Cv	Ср	VELOCITY OF SOUND
к	MOL/L	J/MOL	MN/m <sup>2</sup> -K	J/MOL	J/MOL	J/MOL-K	J / MO	)L - K	M/S
* 55,211	45.2168	31 399	4.3527	-6400.4	-6002.3	61.25	36.06	52.36	1095
56	45.0969	30690	4.3505	-6360.2	-5961.0	62.01	35.92	52,90	1091
58	44.7959	28982	4.3452	-6258.1	-5856.3	63.90	35.55	54.38	1080
60	44.4873	28613	4.3361	-6154.6	-5750.0	65.75	35.26	55.18	1086
62	44.1868	28051	4.2463	-6051.6	-5644.2	67.52	35.36	55.77	1079
66	43.5851	25689	3,8842	-5842.6	-5429.6	70.97	35.55	55.95	1032
68	43.2734	24928	3.7381	-5736.8	-5320.8	72.63	34.94	55.30	1019
70	42.9688	24539	3.6307	-5632.6	-5213.7	74.23	34.19	54.55	1015
72	42.6729	23543	3.5646	-5530.4	-5108.6	75.75	33.68	55.02	1006
74	42.3658	22864	3.4740	-5426.8	-5001.9	77.25	33.59	55.35	996
78	42.0903	208.26	3.2102	-5217.0	-4094.2	80.17	33.22	55.37	973
80	41.4307	20039	3.0763	-5112.9	-4678.5	81.56	32.89	54.90	938
82	41.1177	19512	2.9946	-5009.1	-4571.4	82.92	32.60	54.90	930
86	40.79768	17699	2.7791	-4799.5	-4354.8	85.57	31.90	54.81	895
88	40.1543	17241	2.6964	-4694.8	-4246.5	86.85	31.40	54.41	887
90	39.8332	16240	2.6149	-4591.3	-4139.4	88.08	31.23	55.11	868
92	39.5068	15791	2.5327	-4487.1	-4031.5	89.30	31.17	55.12	857
94	39.1789	15195	2.4637	-4382.6	-3923.1	90.49	30.94	55.40	846
96	38.5122	13794	2.3202	-4277.5	-3705.4	92.81	30.21	55.00	820
100	38.1737	13199	2.2450	-4067.2	-3595.7	93.94	30.06	56.26	806
102	37.8331	12681	2.1629	-3961.4	-3485.6	95.05	29.96	56.25	792
104	37.1419	11426	2.0190	-3748.9	-3264.3	97.21	29.33	56.75	763
108	36.7869	10959	1.9520	-3641.3	-3152.0	98.28	29.05	56.80	751
110	36.4307	10461	1.8805	-3534.0	-3039.9	99.32	28.90	56.92	736
112	36.0696	9991	1.8193	-3425.8	-2926.8	100.35	28.75	57.27	724
114	35.7070	9590	1.6831	-3317.2	-2613.1	101.35	28.69	57.63	/10
118	34.9634	8595	1.6216	-3097.3	-2582.5	103.34	28.35	57.88	680
120	34.5827	8143	1.5615	-2986.1	-2465.6	104.32	28.17	58.21	666
122	34.1951	7707	1.5029	-2873.7	-2347.3	105.29	28.07	58.65	651
124	33.8037	7324	1.4451	-2760.5	-2228.0	106.24	28.02	58.96	637
128	33.4050	6547	1.3320	-2630.2	-2107+6	107.19	20.13	59.85	607
130	32.5908	6168	1.2791	-2412.5	-1860.2	109.06	27.85	60.32	593
132	32.1719	5807	1.2259	-2292.8	-1733.3	109.99	27.47	60.48	580
134	31.7454	5462	1.1757	-2171.8	-1664.8	110.90	27.27	60.93	567
136	31.3103	5128	1.1271	-1613.6	-1038.7	111.81	27.02	61.39	554
138	30.8684	4831 4531	1.0787	-1499.2	-916.U -792.6	112.71	26.62	62.02	542
142	29.9553	4231	0.9949	-1268.4	-667.5	114.48	26.38	63.40	517
144	29.4851	3967	0.9440	-1151.2	-540.8	115.37	26.52	63.73	501
146	29.0084	3701	0.8981	-1033.7	-413.2	116.25	26.59	64.41	486
148	28.5165	3462	0.8550	-914.8	-283.5	11/.13	26.52	64.95	472
152	27.5049	3001	0.7763	-674.1	+19.7	118.89	26.55	66.90	446
154	26.9829	2797	0.7374	-552.4	114.7	119.77	26.41	67.53	434
156	26.4497	2608	0.7029	-429.9	250.6	120.64	26.33	68.58	423
158	25.9060	2432	0.6665	-306.3	388.6	121.52	26.35	69.35	410
100	29.3930	2270	0.0312	-101.9	920+1	122.40	20.32	70.00	399
165	23.4807	1916	U.5515 0.4807	125.9	1237.7	124.55	25.47	70.78	377
175	21.0251	1454	0.4188	748.0	1604.1	128.82	25.59	73.35	331
180	19.6093	1328	0.3663	1052.0	1969.9	130.89	25.37	72.66	316
185	18.2743	1257	0.3223	1344.1	2329.1	132.85	25.00	70.79	306
190	17.0504	1229	0.2857	1620.6	2676.3	134.71	24.68	68.06	299
200	17:9512	1253	0.2306	2125.6	3327.4	138.05	24.39	61.93	293
205	14.1181	1304	0.2102	2355.0	3630.0	139.54	24.24	59.09	289
210	13.3604	1356	0.1931	2571.4	3918.7	140.93	24.12	56.46	289
215	12.6919	1417	0.1783	2776.2	4194.5	142.23	24.02	53.96	289
220	12.0979	1481	0.1660	2971.3	4459.1	143.45	23.93	51.92	291
225	11.5687	1548	0.1551	315/ ./	4/13./	144.59	23.84	49.99	292
235	10.6640	1684	0.1377	3510.8	5198.7	146.70	23.81	47.06	296
240	10.2738	1753	0.1306	3679.1	5431.1	147.68	23.79	45.93	298
245	9.91883	1821	0.1238	3842.8	5657.5	148.62	23.78	44.73	300
250	9.59269	1888	0.1182	4002.8	5879.3	149.51	23.79	43.90	303
260	9.29179	2025	0.1131	4313.6	6310.7	151.20	23.80	43.12	308
265	8.75496	2089	0.1041	4465.0	6520.9	152.01	23.82	41.75	310
270	8.51421	2155	0.1003	4614.2	6728.3	152.78	23.83	41.21	313
275	8.28936	2220	0.0966	4761.4	6932.9	153.53	23.85	40.68	316
280	0.07845	2284	0.0932	4907.0 5051 0	7135.2	154.26	23.87	40.17	318
200	7.69402	2411	0.0875	5193-7	7533-1	155-66	23.91	39.47	321
295	7.51762	2475	0.0849	5335.0	7729.4	156.33	23.93	39.13	326
300	7.35106	2539	0.0824	5475.0	7923.6	156.98	23.94	38.81	329

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## TABLE 16. THERMODYNAMIC PROPERTIES OF FLUORINE

## 19 MN/m<sup>2</sup> ISOBAR

TEMPERATURE	DENSITY	ISOTHERM	ISOCHORE	INTERNAL	ENTHALPY	ENTROPY	Cv	Сp	VELOCITY
(TEL2 1968)	MOL/L	J/MOL	MN/m <sup>2</sup> - K	J/MOL	J/MOL	J∕MOL-K	J / MC	DL - К	M/S
* 55.305	45.2344	31560	4.3528	-6420.9	-6000.9	61.28	36.05	52.27	1097
56	45.1294	30917	4.3509	-6385.7	-5964.6	61.94	35.92	52.76	1093
58 60	44.8303 44.5222	29142 28764	4.3455 4.3400	-6284.1 -6181.0	-5860.3 -5754.3	63.82 65.67	35.55 35.26	54.25 55.08	1082 1087
62	44.2222	28361	4.2565	-6078.3	-5648.7	67.45	35.36	55.62	1083
64	43.9281	27343	4.1353	-5975.0	-5542.5	69 <b>.18</b>	35.63	56.37	1067
68	43.3134	25120	3.7395	-5764.6	+5325.9	72.55	35.02	55.20	1021
70	43.0093	24762	3.6266	-5660.7	-5218.9	74.15	34.27	54.37	1017
72	42.7151	23890	3.5643	-5558.8	-5114.0	75.66	33.73	54.72	1010
74	42.4091	23287	3.4845	-5455.7	-5007.7	78.64	33.54	55.08	1002
78	41.7910	21117	3.2237	-5246.9	-4792.2	80.08	33.29	55.27	961
80	41.4803	20331	3.0769	-5143.1	-4685.0	81.48	32.98	54.63	941
82 84	41.1684 40.8521	19908	2.9976	-5039.7 -4935.5	-4578.1 -4470.4	82.83	32.68	54.52 55.30	935
86	40.5329	17941	2,7861	-4831.1	-4362.3	85.48	31.99	54.64	898
88	40.2119	17516	2.7011	-4726.8	-4254.3	86.75	31.48	54.15	890
90	39.5696	16042	2.5405	-4520.3	-4040.1	89.20	31.25	54.89	861
94	39.2441	15473	2.4710	-4416.3	-3932.2	90.39	31.00	55.09	851
96	38.9159	14629	2.4039	-4312.0	-3823.8	91.55	30.50	55.53	837
100	38.2488	13430	2.2637	-4103.0	-3606.3	93.83	30.04	56.12	813
102	37.9112	12931	2.1853	-3997.9	-3496.7	94.93	29.93	56.14	799
104	37.2285	12437	2.0939	-3892.3	-3386.6	96.02	29.76	55.73	783
108	36.8772	11181	1.9739	-3680.2	-3164.9	98.15	29.01	56.68	758
110	36.5253	10683	1.8992	-3573.5	-3053.3	99.18	28.87	56.71	743
112	35.8098	10204	1.8390	-3466.3	-2940.9	100.21	28.65	56.98	731
116	35.4472	9288	1.7023	-3249.8	-2713.8	102.21	28.51	57.31	701
118 120	35.0781 34.7037	8851 8389	1.6410 1.5818	-3140.4 -3030.2	-2598.8 -2482.7	103.19 104.16	28.34 28.14	57.51 57.86	688 674
122	34.3229	7937	1.5233	-2918.9	-2365.4	105.12	28.05	58.32	659
124	33.9380	7569	1.4656	-2806.8	-2247.0	106.07	28.00	58.55	645
126	33.5477	7169	1.4086	-2693.9	-2127.5	107.01	28.11	59.10	630
130	32.7498	6411	1.2999	-2462.6	-1882.4	108.87	27.85	59.79	602
132	32.3406	6048	1.2475	-2344.3	-1756.8	109.79	27.47	59.94	589
134	31.9246	5699	1.1957	-2224.8	-1629.6	110.69	27.01	60.25	576
138	31.0704	5072	1.1007	-1526.9	-915.4	112.48	26.61	60.75	552
140	30.6320	4771	1.0542	-1413.8	-793.5	113.35	26.35	61.11	540
142	30.1854	4465	1.0166	-1300.0	-670.6	114.22	26.29	62.36	528
144	29.2702	4203	0.9721	-1104.0	-545.5	115.10	26.65	63.45	497
148	28.7959	3700	0.8776	-952.0	-292.2	116.83	26.59	63.75	483
150	28.3160	3448	0.8388	-834.9	-163.9	117.70	26.58	64 • 76 65 - 52	470
154	27.3266	3024	0.7617	-597.6	97.7	119.42	26.48	66.04	446
156	26.8174	2833	0.7263	-478.0	230.5	120.27	26.30	66.69	435
158	25.7742	2490	0.6579	-236.4	500.7	121.13	26.28	68.17	424
165	24.4308	2124	0.5786	62.6	840.3	124.07	25.02	68.59	391
170	23.0549	1840	0.5082	364.2	1188.3	126.15	25.45	70.35	366
180	20.3219	1482	0.3927	963.1	1898.0	130.21	25.20	70.55	330
185	19.0312	1390	0.3472	1249.7	2248.1	132.13	24.89	69.20	319
190	17.8290	1343	0.3088	1523.2	2588.9	133.94	24.45	64.51	311 304
200	15.7433	1350	0.2508	2029.5	3236.4	137.27	24.35	61.97	301
205	14.8654	1375	0.2280	2261.1	3539.3	138.76	24.25	59.33 56.92	298
215	13.3855	1469	0.1932	2688.7	4108.2	141.47	24.07	54.56	296
220	12.7632	1527	0.1798	2887.2	4375.9	142.70	23.98	52.57	297
225	12.2063	1590	0.1678	3077.2	4633.7	143.86	23.92	50.67	298
235	11.2516	1721	0.1486	3436.5	5125.2	146.00	23.85	47.68	301
240	10.8390	1787	0.1409	3607.9	5360.8	146.99	23.84	46.53	303
245	10.4527	1857	0.1336	3774.4	5590.3	147.94	23.83	45.33	305
255	9.79938	1986	0.1217	4095.9	6034.8	149.72	23.83	43.63	309
260	9.50426	2052	0.1167	4252.1	6251.2	150.56	23.85	42.94	312
265	9.23036	2119	0.1119	4405.6	6464.0 6673.6	151.37	23.86	42.24	314 317
275	8.73711	2248	0.1036	4705.7	6880.3	152.91	23.89	41.11	319
280	8.51369	2312	0.0999	4852.9	7084.6	153.65	23.91	40.59	321
290	8.10649	2438	0.0937	5142.6	7486.4	155.06	23.95	39.84	327
295	7.91959	2500	0.0909	5285.5	7684.6	155.74	23.97	39.51	329
300	1.14346	(504	0.0003	2470.44	(000.4)	170+40	63.33	17017	332

#### TABLE 16. THERMOOYNAMIC PROPERTIES OF FLUORINE

## 20 MN/m<sup>2</sup> ISOBAR

TEMPERATURE	OENSITY	ISOTHERM	ISOCHORE	INTERNAL	ENTHALPY	ENTROPY	Cv	Сp	VELOCITY
(IPIS 1968) K	MOL/L	J/MOL	MN/m <sup>2</sup> ~K	ENERGY J/MOL	J/MOL	J/MOL-K	J / MC	IL - К	M/S
* 55 700	45 2520	71714	1. 7529	-6444	- 5000 /	61 70	76 07	62 10	1100
56	45.1616	31142	4.3511	-6411.1	-5968.2	61.88	35.92	52.61	1096
58	44.8645	29300	4.3457	-6310.0	-5864.2	63.75	35.55	54.13	1083
00	44.5565	20912	4.3401	-0207.5	-2120+2	02:23	39.20	54.95	1009
62 64	44.2573 43.9644	286 <b>8</b> 5 27800	4.2665 4.1616	-6104.9 -6002.0	-5653.0 -5547.1	67.37 69.10	35.37 35.64	55.45 56.26	1088
66	43.6619	26421	3.9238	-5897.3	-5439.3	70.81	35.65	55.83	1043
68	43.3530	25318	3.7413	-5792.2	-5330.9	72.47	35.09	55.09	1023
70	43.0495	24990	3.6273	-5688.6	-5224.0	74.07	34.34	54.23	1019
72	42.4516	24249	3.5625	-5587.1	-5119.4	75.58	33.66	54.40	1014
76	42.1477	22207	3.3764	-5380.9	-4906.4	78.55	33.59	55.55	983
78	41.8380	21417	3.2381	-5276.5	-4798.5	79.99	33.35	55.17	966
80	41.5291	20633	3.0840	-5173.1	-4691.5	81.39	33.07	54.45	946
82 84	41.2181 40.9058	20317 18730	2.9998 2.9115	-5070.0 -4966.5	-4584.8	82.75 84.08	32.75 32.46	54.13 55.18	940 915
86	40.5882	18186	2.7956	-4862.5	-4369.8	85.38	32.08	54.51	902
88	40.2685	17796	2.7053	-4758.6	-4262.0	86.66	31.56	53.88	894
90	39.9548	16532	2.5477	-4656.5	-4155.9	87+88	31.39	54.65	8/4
94	39.3082	15754	2.4773	-4449.8	-3941.0	90.28	31.06	54.76	855
96	38.9837	14863	2.4129	-4346.3	-3833.3	91.45	30.54	55.29	841
98 100	38.6547 38.3227	14274 13661	2.3500 2.2821	-4242.8 -4138.6	-3725.4 -3616.8	92.59 93.71	30.21 30.01	55,59 55,97	831 819
102	37.9878	13183	2.2091	-4034.1	-3507.6	94.82	29.90	56.06	807
104	37.6502	12704	2.1156	-3929.1	-3397.8	95.90	29.75	55.60	790
106	37.3136	11864	2.0479	-3824.6	-3288.6	96.96	29.30	56.21	774
108	36.9658	11401	1.9966	-3/18.6	-3177.6	98.U2 99.05	28.95	56.62	751
112	36.2656	10410	1.8580	-3506.3	-2954.8	100.07	28.66	56.90	738
114	35.9098	10145	1.7967	-3399.1	-2842.1	101.08	28.59	56.72	728
116	35.5534	9534	1.7236	-3291.5	-2728.9	102.06	28.48	57.08	709
120	34.8212	8635	1.6013	-3073.7	-2499.4	104.01	28.12	57.51	682
122	34.4471	8165	1.5436	-2963.6	-2383.0	104.96	28.02	58.02	667
124	34.0681	7812	1.4860	-2852.5	-2265.4	105.91	27.97	58.18	654
128	33.2968	7400	1.3741	+2626.8	-2146.9	100.04	27.97	58.95	625
130	32.9029	6651	1.3199	-2511.7	-1903.9	108.68	27.84	59.29	611
132	32.5028	6286	1.2685	-2394.7	-1779.4	109.59	27.46	59.45	598
134	32.0966	5934	1.2163	-2276.6	-1653.5	110.49	27.27	59.70	585
138	31.2630	5309	1.1225	-1553.5	-913.7	112.26	26.60	60.11	562
140	30.8366	5007	1.0761	-1441.9	-793.3	113.12	26.34	60.39	550
142	30.4037	4695	1.0341	-1330.0	-672.2	113.98	26.24	61.22	537
144	29.9615	4436	1.0010	-1216.5	-549.0	114.64	26.59	62.52	526
148	29.0579	3935	0.8967	-987.0	-298.7	116.56	26.75	62.57	492
150	28.5970	3671	0.8602	-872.4	-173.0	117.40	20.61	63.57	480
152	28.1255	3453	0.8228	-756.3	-45.2	118.25	26.66	64.33	468
156	27.1572	3055	0.7479	-522.5	21.3.9	119.09	26.36	65.08	450
158	26.6611	2875	0.7172	-405.0	345.1	120.77	26.20	65.97	436
160	26.1592	2708	0.6832	-286.7	477.8	121.60	26.25	66.56	425
165	24.8801	2330	0.6041	5.0 298.4	808.8	123.64	24.98	66.73	405
175	22.2581	18 04	0.4718	592.7	1491.3	127.65	25.48	69.06	359
180	20.9627	1642	0.4180	882.7	1836.8	129.60	25.07	68.67	344
185	19.7170	1530	0.3712	1163.8	2178.1	131.47	24.66	67.51	332
190	17.4571	1400	0.2977	1691.1	2836.7	133.29	23.95	63.45	316
200	16.4585	1450	0.2719	1939.2	3154.4	136.55	24.17	61.81	312
205 210	15.5720 14.7716	1458 1487	0.2459	2172.4 2394.0	3456.7 3747.9	138.04 139.44	24.20	59.24 57.15	307 304
215	14.0530	1529	0.2083	2604.8	4028.0	140.76	24.11	54.98	303
220	13.4071	1581	0.1937	2806.3	4298.0	142.00	24.05	53.08	303
225	12.8261	1638	0.1807	2999.2	4558.5	143.17	23.98	51.25	304
230	12.3013	1700	0.1598	3184.8	4810.7	144+28	23.93	49.70	305
240	11.3927	1827	0.1513	3538.0	5293.5	146.34	23.87	47.05	308
245	10.9949	1903	0.1441	3707.5	5526.6	147.30	23.88	46.01	311
250	10.6322	1968	0.1368	3872.4	5753.5	148.22	23.88	44.91	312
260	9.98757	2088	0.1250	4191.6	6194.1	149.95	23.88	43.38	316
265	9.69830	2157	0.1201	4347.2	6409.4	150.77	23.90	42.75	319
270	9.42947	2221	0.1153	4500.2	6621.2	151.56	23.92	42.10	321
280	8.94333	2345	0.1069	4799.8	7036.1	153.07	23,95	41.03	325
285	8.72223	2408	0.1033	4946.8	7239.8	153.79	23.97	40.56	328
290	8.51401	2471	0.0997	5092.3	7441.4	154.49	23.98	40.08	330
295	8.13115	2528	0.0968	5379.2	7838.9	155.84	24.00	39.53	332

.

#### TABLE 16. THERMOOYNAMIC PROPERTIES OF FLUORINE

## 21 MN/m<sup>2</sup> ISOBAR

TEMPERATURE	DENSITY	ISOTHERM	ISOCHORE	INTERNAL	ENTHALPY	ENTROPY	Cv	Сp	VELOCITY
(IPIS 1968) K	MOL/L	J/MOL	MN/m <sup>2</sup> -K	J/MOL	J/MOL	J/MOL-K	J / MC	н - к	M/S
¥ 55 493	45 2694	71861	1. 3526	-6/61 9	-5998 0	61 72	76 0 2	F2 12	1102
56	45.1936	31366	4.3512	-6436.4	-5971.7	61.81	35.92	52.47	1098
58	44.8985	29458	4.3458	-6335.9	-5868.1	63.68	35.56	54.00	1085
6.2	44.2010	200.22	1. 2762	-6171 6	-5657 /	67 30	35 77	54.02	1007
64	44.0001	28279	4.1890	-6028.9	-5551.7	69.02	35.64	56.15	1083
66	43.6994	26815	3.9457	-5924.6	-5444.0	70.73	35.70	55.76	1050
68	43.3924	25522	3.7434	-5819.7	-5335.8	72.39	35.16	54.99	1025
70	43.0894	25223	3.6283	-5716.4	-5229.0	73.99	34.42	54.10	1021
72	42.7976	24620	3.5593	-5615.3	-5124.6	75.51	33.85	54.07	1017
74	42.4934	24187	3.5051	-5513.0	-5010.0	77.00	33.70	54.52	1015
78	41.8844	21728	3,2531	-5306.0	-4804.7	79.91	33.41	55.06	971
80	41.5772	20943	3.0966	-5202.9	-4697.8	81.30	33.15	54.34	951
82	41.2668	20739	3.0012	-5100.1	-4591.2	82.66	32.82	53.74	945
86	40.6429	18436	2.8054	-4893.8	-4377.1	85.29	32.16	54.38	906
88	40.3243	18081	2.7090	-4790.2	-4269.4	86.56	31.65	53.61	898
90	40.0146	16826	2.6321	-4688.8	-4164.0	87.78	31.48	54.62	877
92	39.6924	16551	2.5543	~4585.9	-4056.9	89.00	31.39	54.41	869
94	39.3711	16039	2.4829	-4483.0	-3949.6	90.18	31.13	54.43	859
96	39.0909	14516	2.3621	-4300.5	-3042.5	91.34	30.23	55.35	836
100	38.3953	13892	2.3003	-4174.0	-3627.0	93.60	29.99	55.83	825
102	38.0629	13435	2.2297	-4070.0	-3518.3	94.70	29.85	55.91	814
104	37.3971	12973	2.1307	-3965.5	-3300.3	95.79	29.74	55.92	798
108	37.0527	11619	2.0153	-3756.8	-3190.0	97.89	28.90	56.40	773
110	36.7087	11121	1.9442	-3651.6	-3079.6	98.92	28.79	56.54	758
112	36.3607	10611	1.8763	-3545.9	-2968.4	99.94	28.61	56.72	744
114	36.0070	10428	1.8207	-3439.3	-2856.1	100.94	28.52	56.48	737
116	35.0570	9781	1.6803	-3332.1	-2630 0	101.92	28.44	56.83	718
120	34.9354	8883	1.6201	-3116.7	-2515.6	103.86	28.10	57.15	690
122	34.5679	8390	1.5639	-3007.6	-2400.1	104.81	27.98	57.74	675
124	34.1941	8055	1.5067	-2897.4	-2283.3	105.75	27.95	57.83	662
126	33.8178	704/	1.4502	-2677 8	-2165.6	105.67	28.07	58.37	647
130	33.0506	6890	1.3400	-2560.0	-1924.6	108.50	27.83	58.84	619
132	32,6590	65 22	1.2890	-2444.2	-1801.2	109.41	27.45	58.98	607
134	32.2619	6166	1.2377	-2327.4	-1676.5	110.29	27.27	59.26	594
136	31.8591	5815	1.1884	-1689.5	-1030.3	111.17	27.00	59.55	581
138 140	31.4473 31.0318	5544 5240	1.1434 1.0970	-1578.9 -1468.7	-911.2 -792.0	112.04 112.90	26.59 26.33	59.50 59.72	571 559
142	30.6117	4922	1.0530	-1358.5	-672.5	113.75	26.22	60.36	546
144	30.1812	4666	1.0205	-1246.9	-551.1	114.60	26.30	61.58	536
146	29.7499	4408	0.9779	-1134.3	-428.4	115.44	26.60	62.39	522
148	29.3048	4167	0.9227	-1020.1	-303.5	116.29	26.86	62.07	503
150	28.8615	3891	0 8/55	-907.4	-179.8	117.12	26.70	67 30	488
154	27.9436	3466	0.8059	-678.8	72.7	118.78	26.72	63.68	466
156	27.4733	3273	0.7658	-563.8	200.6	119.61	26.52	63.56	454
158	26.9964	3092	0.7357	-448.9	329.0	120.43	26.22	64.17	446
160	26.5146	2922	0.7107	-333.5	458.6	121.24	26.13	65.47	439
165	25.2914	2534	0.6281	-48.1	782.2	123.23	24.96	65.12	417
175	22.7867	1982	0.4962	526.1	1447.7	127.15	25.62	67.49	371
180	21.5434	1805	0.4423	809.4	1784.2	129.05	24.93	66,95	357
185	20.3414	1676	0.3942	1084.3	2116.7	130.87	24.19	65.64	346
190	19.1955	1597	0.3538	1351.3	2445.3	132.62	23.94	64.37	336
195	18.1268	1553	0.3186	1605.8	2764.3	134.28	23.54	62.31	329
200	16 2766	1565	0.2944	1823.1	3079.0	135.87	23+62	58.81	321
210	15.4267	1568	0.2421	2311.4	3672.7	138.77	24.10	57.08	313
215	14.6927	1599	0.2234	2524.6	3953.9	140.09	24.13	55.21	310
220	14.0279	1642	0.2077	2728.5	4225.5	141.34	24.10	53.46	310
225	12,8812	1094	0.1810	2924+1	4400.1	142.92	24.00	50.21	310
235	12.3854	1812	0.1713	3294-0	4989.5	144.70	23.95	48.77	312
240	11.9334	1873	0.1620	3469.9	5229.7	145.72	23.91	47.52	313
245	11.5130	1960	0.1559	3642.2	5466.2	146.69	23.90	46.83	318
250	11.1334	2026	0.1471	3809.6	5695.9	147.62	23.92	45.46	318
255 260	10.7857 10.4617	2077 2132	0.1394 0.1334	3972.8 4132.6	5919.8 6140.0	148.51 149.36	23.93	44.43	319
265	10.1572	2204	0.1289	4290.0	6357.5	150.19	23.93	43.31	324
270	9.87520	2268	0.1234	4444.8	6571.3	150.99	23.95	42.54	326
275	9.61271	2327	0.1183	4597.2	6781.8	151.76	23.97	41.87	327
280	9.36628	2386	0.1144	4747.6	6989.7	152.51	23.99	41.50	330
200	9.13407	2449	0.1052	4090.2	7398 4	153.24	24.02	40.35	332
295	8.71066	2558	0.1025	5188.3	7599.1	154.63	24.04	40.00	335
300	8.51548	2615	0.0997	5332.2	7798.3	155.30	24.06	39.79	337

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# APPENDIX A - TEMPERATURE SCALE DIFFERENCES

Given below are temperature scale differences from References [13] (T, IPTS 1968 - T, NBS 1955) and [14] (T, IPTS 1968-T, IPTS 1948) for temperatures below and above 90 K, respectively.

T, IPTS	T, IPTS 1968 -	T, IPTS	T, IPTS 1968 -
1968 - K	T, old - K	1968 <b>-</b> K	T, old - K
50.0	0.0131	83.0	-0.0064
51.0	0.0124	84.0	-0.0049
52.0	0.0116	85.0	-0.0029
53.0	0.0104	86.0	-0.0005
54.0	0.0089	87.0	0.0022
55.0	0.0071	88.0	0.0049
56.0	0.0052	89.0	0.0074
57.0	0.0034	90.0	0.0096
58.0	0.0017	,	,.
59.0	0.0003	93.15	0.012
60.0	-0.0008	103.15	0.007
61.0	-0.0014	113.15	-0,005
62.0	-0.0015	123.15	-0.013
63.0	-0.0012	133.15	-0.013
64.0	-0.0007	143.15	-0.006
65.0	-0.0001	153.15	0.003
66.0	0.0005	163.15	0.013
67.0	0.0009	173.15	0.022
68.0	0.0011	183.15	0.029
69.0	0.0009	193.15	0.033
70.0	0.0003	203.15	0.034
71.0	-0.0006	213.15	0.032
72.0	-0.0017	223.15	0.029
73.0	-0.0030	233.15	0.024
74.0	-0.0043	243.15	0.018
75.0	-0.0056	253.15	0.012
76.0	-0.0068	263.15	0.006
77.0	-0.0078	273.15	0.000
78.0	-0.0086	283.15	-0.004
79.0	-0.0090	293.15	-0.007
80.0	-0.0090	303.15	-0.009
81.0	-0.0086	313.15	-0.010
82.0	-0.0077	323.15	-0.010

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