A Curve-Based Mixed System Rating Method for Unitary Air Conditioners

W. Vance Payne Piotr A. Domanski

U.S. DEPARTMENT OF COMMERCE National Institute of Standards and Technology Building Environment Division Building and Fire Research Laboratory Gaithersburg, Maryland 20899-8631



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1.1: Coil 9 evaporator cooling capacity, confidenc	e and error
bands on the mean predicted value of the co	oling capacity
sampled at a particular evaporator saturation	temperature

Nomenclature

A	EVAP-COND air-side heat transfer coefficient correction factor
A-Test	refers to ARI Standard 210/240 steady-state test conditions of 35 °C (95 °F) outdoor air and 16.7 °C (80 °F) dry-bulb/ 19.4 °C (67 °F) wet-bulb indoor air conditions
B-Test	refers to ARI Standard 210/240 steady-state test conditions of 27.8 °C (82 °F) outdoor air and 16.7 °C (80 °F) dry-bulb/ 19.4 °C (67 °F) wet-bulb indoor air conditions
C _D	cyclic degradation coefficient as defined in ARI Standard 210/240-2003
C-B Method	curve-based method as presented in this report
CD Unit	condensing unit, the outdoor section of the split air-conditioner
CLF	Cooling Load Factor as defined in ARI Standard 210/240-2003
Diff	abbreviation for difference
DOF	degrees of freedom
EVAP-COND	refers to evaporator and condenser simulation software available from NIST
EER	Energy Efficiency Ratio as calculated in ARI Standard 210/240-2003, W/W (Btu/W·h)
ṁ	mass flow rate, kg/h (lb/h)
matched mixed	refers to a split air-conditioning system, an indoor section/condensing unit combination, which rated performance is determined by laboratory testing; also may refer to the evaporator which is used in the matched system. refers to a split air-conditioning system, an indoor section/condensing unit combination, which rated performance is not determined by laboratory
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mixed n <i>P</i> p(82)	combination, which rated performance is determined by laboratory testing; also may refer to the evaporator which is used in the matched system. refers to a split air-conditioning system, an indoor section/condensing unit combination, which rated performance is not determined by laboratory testing; also may refer to the evaporator which is used in the mixed system. number of tests or number of data points electrical power, W condensing unit power at B-Test condition (indoor fan power not included), W total power of air conditioner at B-Test condition (condensing unit power plus

Q	Cooling capacity, W (Btu/h)				
q(82)	cooling capacity at B-Test condition without accounting for indoor fan heat input, W (Btu/h)				
Q(82)	cooling capacity at B-Test conditions with the indoor fan heat input accounted for , W (Btu/h)				
<i>q</i> (95)	cooling capacity at A-Test conditions without accounting for indoor fan heat input, W (Btu/h)				
Q(95)	cooling capacity at A-Test conditions with the indoor fan heat input accounted for, W (Btu/h)				
ρ	correlation coefficient				
R	EVAP-COND refrigerant-side heat transfer coefficient correction factor				
scfm	standard cubic feet per minute, which is equal to the equivalent volumetric flowrate of air with a density of 0.075 lbm/ft ³				
SEER	Seasonal Energy Efficiency Ratio as defined in ARI Standard 210/240-2003, Btu/(W·h)				
SHR	sensible heat ratio; the ratio of sensible capacity to total capacity				
$\hat{\sigma}$	data standard deviation or fit standard error				
SSE	sum of squares of the error				
t or t-value	percentage points of the t-distribution (Ott 1984)				
ton	cooling or heating capacity equal to 12 000 Btu/h or 3.517 kW				
U	absolute value of a quantity's uncertainty				

Subscripts

- condensing unit of the split system air conditioner CD
- cyclic testing сус
- difference diff
- dry
- dry-coil testing refers to the indoor coil or evaporator at saturated refrigerant conditions evap
- refers to the indoor coil fan fan
- mixed refers to the evaporator coil alone with respect to a system
- refrigerant ref
- steady-state SS

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Abstract

The curve-based method was evaluated based on performance predictions and independent laboratory testing for nine mixed systems. Capacity predictions were within ± 5 % of the tested values for six of the mixed systems, and four of the SEER predictions were within ± 5 % of the tested SEERs. Predictions for SEER showed an under prediction bias due to the wide variation of possible values for the cyclic degradation coefficient (C_D) and the necessity of assuming a conservative value of C_D in mixed system rating calculations. This report includes detailed measurement data for the tested evaporators and an uncertainty analysis of the rating methodology.

Keywords: air conditioner, cooling capacity, cyclic degradation coefficient, mixed system, rating procedure, SEER

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^{*} Use of Non-SI Units in a NIST Publication: The policy of the National Institute of Standards and Technology is to use the International System of Units (metric units) in all of its publications. However, in North America in the heating, ventilation and air-conditioning industry, certain non-SI units are so widely used instead of SI units that it is more practical and less confusing to include some measurement values in customary units only.

1: INTRODUCTION

A given condensing unit (outdoor section consisting of a condenser, compressor, and associated tubing) is typically offered on the market in several air-conditioner models, which differ by the indoor sections they employ. For all models, the manufacturers must provide performance information, which consists of the Seasonal Energy Efficiency Ratio (SEER) and capacity at the 35 °C (95 °F) rating point, *Q*(95). Federal regulations require that only the highest sales volume indoor-section/outdoor-section combination, referred to as the matched system, be tested in a laboratory to obtain the ratings (CFR 2004a). For other combinations of indoor and outdoor sections, so called mixed systems, the federal regulations allow the use of simplified analytical methodologies upon approval by the U.S. Department of Energy (CFR 2004b).

The most commonly used simplified methodologies for rating mixed systems are those based upon publicly available *Q*(95) and SEER of the matched systems (e.g., Domanski 1989). The application of these methods requires the rater to predict the capacity of the matched evaporator, which is a major shortcoming because the rater is not often familiar with the matched system product line. Since an inaccurate prediction of the matched evaporator leads directly to inaccurate mixed system ratings, a different rating method that would not include this step, e.g. the performance curve-based method (C-B Method), has the inherent potential to be a better rating approach than the one currently used. Recently, both coil and condensing unit manufacturers expressed interest in using the C-B Method to predict mixed system performance.

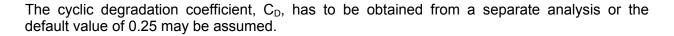
Figure 1.1 shows the application of the C-B Method in a graphical form. This method uses linear fits to the cooling capacity for the mixed coil, and cooling capacities, q(82) and q(95), and power, p(82), for the condensing unit (CD Unit). The lines are presented as a function of the compressor suction saturation temperature. Overlapping of the evaporator and CD Unit capacities provides mixed system capacities at 27.8 °C (82 °F) and 35.0 °C (95 °F) ambient temperatures. Projecting the saturation temperature corresponding with operation at the 27.8 °C (82 °F) ambient temperature on the CD Unit power chart provides the power requirement for the CD Unit at the 27.8 °C (82 °F) rating point. Figure 1.1 is convenient for explaining the C-B method. In real applications, this method is best implemented numerically using a computer.

It should be noted that the rating process explained above is exclusive of the indoor fan power. Before the rating of the mixed system is finalized, the indoor fan power must be added to the CD Unit power to produce the power for the system at the 27.8 °C (82 °F) rating point *P*(82) The indoor fan heat must also be included as heat reducing the cooling capacities *q*(95) and *q*(82) obtained from overlapping the capacity lines of the CD Unit and mixed evaporator to produce actual mixed system capacities, *Q*(82) and *Q*(95). The energy efficiency ratio at the 27.8 °C (82 °F) rating point (EER(82)) can then be calculated using the corrected values of capacity, *Q*(82), and power, *P*(82).

$$\mathsf{EER}(82) = \frac{\mathsf{Q}(82)}{\mathsf{P}(82)}$$
 1.1

To conclude with the SEER calculation, the value of the cyclic degradation coefficient, C_D , is required.

SEER =
$$(1 - 0.5 \cdot C_{D})$$
EER(82) 1.2



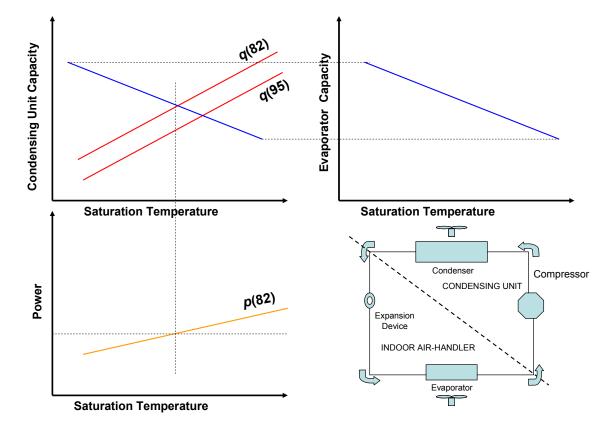


Figure 1.1: Graphical illustration of the curve-based rating procedure

The goal of this study was to evaluate the practicality and accuracy of the curve-based method through its application to nine mixed systems. In this effort, NIST assumed the role of an evaporator manufacturer and developed cooling capacity lines for nine mixed evaporator coils. After obtaining the needed condensing unit performance curves from the Air-Conditioning and Refrigeration Institute (ARI) database, NIST developed mixed system ratings, and then compared them to laboratory derived ratings obtained at an independent testing laboratory for the ARI Unitary Equipment Certification Program.

2: TESTED MIXED EVAPORATORS

Table 2.1 shows basic information on the tested mixed evaporators. They were manufactured by several different companies and had different capacities. All evaporators were of the finned-tube design. Three evaporators were inclined slabs, four coils were constructed in an A-shape configuration, and one in a semi-A-shape configuration. Three of the coils tested were equipped with a fan and required indoor fan power measurement. The remaining six coils were intended to have field-installed fans. Appendix A presents detailed design data, circuitry configuration, and pictures of the coils.

Coil	Coil	Coil	Airflow	Tube Outside	Expansion	Refrigerant
Number	Designation	Configuration	Direction	Diameter	Device	Reingerant
1	A01102	A	Horizontal	9.5 mm (0.375 in)	TXV	R22
2	A01070	Semi A	Horizontal	9.5 mm (0.375 in)	Piston	R22
3	A01148	A	Upflow	9.5 mm (0.375 in)	TXV	R22
4	A01138	A	Upflow	9.5 mm (0.375 in)	Piston	R22
5	A01060*	Inclined Slab	Upflow/ Horizontal	9.5 mm (0.375 in)	Piston	R22
6	A01125*	Inclined Slab	Horizontal	9.5 mm (0.375 in)	TXV	R22
7	H5326	A	Horizontal	9.5 mm (0.375 in)	Piston	R22
8	H5321	A	Upflow	9.5 mm (0.375 in)	Piston	R22
9	A01154*	Inclined Slab	Horizontal	9.5 mm (0.375 in)	TXV	R410A

Table 2.1: Tested mixed evaporators

*indoor fan included

3: MIXED EVAPORATOR CAPACITY DETERMINATION

3.1: Experimental setup

Figure 3.1.1 shows the experimental setup. The evaporator was installed in the indoor environmental chamber, where air conditions were controlled by a chiller/air handler system. Air was pulled through the evaporator by a centrifugal fan located at the outlet of the nozzle chamber ductwork. The adjacent outdoor chamber housed the water-cooled condensing unit and the laboratory water-chiller. Two different condensing units were used for R22 and R410A evaporators due to lubricant-related considerations. Each condensing unit was equipped with a variable-speed compressor, condenser, and subcooler. The water chiller control system manipulated the temperature and mass flow rate of the water delivered to the condensing unit. The chiller rejected heat to the in-house chilled water loop. Heat rejection was to water and did not require maintaining the outdoor chamber conditions.

The installation of the evaporator and test instrumentation conformed to ASHRAE Standard 37-1989. We used the air enthalpy method for the primary measurement of the evaporator capacity with the refrigerant enthalpy method providing the secondary measurement. Air dewpoint temperature was measured at the inlet of the evaporator ductwork and in the ductwork after the evaporator and several mixers. Twenty-five node thermocouple grids, located on each side of the evaporator, were used to verify that the air was well mixed at each point. A 25junction thermopile measured the air temperature change across the evaporator. Barometric pressure, evaporator air pressure drop, air temperature and pressure drop in the nozzle, and nozzle temperature were used along with the dew-point measurements to establish the thermodynamic state of the air. The refrigerant enthalpy method required measurement of the evaporator inlet and exit refrigerant temperatures and pressures in addition to mass flowrate. The agreement between the air-side and refrigerant-side methods was always within 4 %.

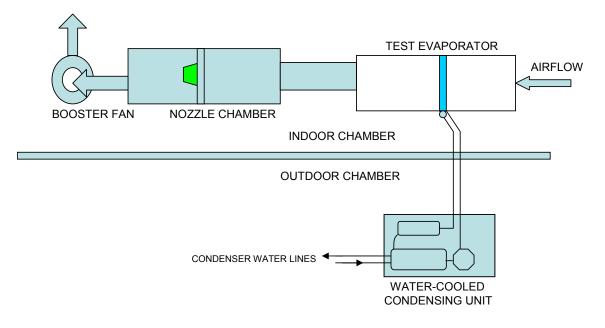


Figure 3.1.1: Evaporator test arrangement

3.2: Data acquisition and measurement uncertainty

The measurement points consisted of temperature, pressure, pressure difference, temperature difference, dew-point temperature, fan amps, fan volts, and fan power. Table 3.2.1 lists the measured quantities and their uncertainties for a 95 % confidence limit (two sigma on the mean value) (Taylor and Kuyatt 1994). The uncertainty for the evaporator capacity was calculated using a propagation of uncertainty technique, considering the uncertainty in each of the parameters associated with the capacity measurement. Appendix B explains the application of this technique in more detail.

Quantity	Range	Uncertainty
Pressure	0 kPa to 3447 kPa (0 psia to 500 psia)	±3.4 kPa (±0.5 psi)
Temperature	-26.1 °C to 93.3 °C (-15 °F to 200 °F)	±0.3 °C (±0.5 °F)
Temperature Difference	0 °C to 27.8 °C (0 °F to 50 °F)	±0.3 °C (±0.5 °F)
Barometric Pressure	0 mm Hg to 1270 mm Hg (0 in Hg to 50 in Hg)	±0.34 mm Hg (±0.0135 in Hg)
Dew-point Temperature	0 °C to 50 °C (32 °F to 122 °F)	±0.2 °C (±0.4 °F)
Pressure Difference	0 Pa to 1244 Pa (0 in H ₂ O to 5 in H ₂ O)	±24.4 Pa (±0.098 in H ₂ O)
Mass Flow	0 kg/h to 544.3 kg/h (0 lb/h to 1200.0 lb/h)	±1 %
Evaporator Capacity	5.56 kW to 14.4 kW (19 kBtu/h to 49 kBtu/h)	±3 % to ±7 %

Table 3.2.1: Measurement uncertainty

3.3: Tests conditions and procedure

Each evaporator coil was tested at the air volumetric flow rate that was used during mixed system tests carried out at an independent testing laboratory for the ARI certification program. For all tests, constant indoor conditions of 16.7 °C (80.0 °F) dry-bulb and 15.8 °C (60.4 °F) dewpoint temperatures were applied according to ARI Standard 210/240 (2003).

On the refrigerant side, the tests were constrained by the refrigerant inlet condition, defined by the liquid line temperature and subcooling, and the outlet condition, defined by the vapor line saturation temperature and superheat. The tests of each evaporator involved three vapor suction line saturation temperatures. The evaporator capacity line was generated as a function of the evaporator exit saturation temperature from these points. Table 3.3.1 lists the refrigerant conditions imposed during the evaporator tests for all coils.

Liquid line		Vapor line	
TemperatureSubcooling°C (°F)°C (°F)		Sat. temperature* °C (°F)	Superheat °C (°F)
40.6 ± 0.8 (105.0 ± 1.5)	5.6 to 8.3 (10.0 to 15.0)	4.4, 7.2, 10.0 (40.0, 45.0, 50.0)	5.6 to 8.3 (10.0 to 15.0)

Table 3.3.1: Refriger	ant conditions during	evaporator tests
rabio oror riteringor	and oonandonio aannig	, 0140014(01 (0000

*Three nominal conditions

The expansion devices supplied with the various evaporators were removed and replaced by precision needle valves. The liquid line temperature and subcooling, and evaporator superheat were controlled by adjusting the refrigerant charge and by changing the needle valve settings to produce the required superheat at the exit of the evaporator. In addition to compressor speed

control, an evaporator pressure regulating valve was used to produce the desired exit pressure. Liquid line temperature at the inlet to the expansion valves was also controlled by varying the water flow rates through the liquid cooled subcooler and condensing unit heat exchangers. At least five tests were performed for each evaporator. If the evaporator was equipped with a fan, its power was also measured and recorded for each test.

3.4: Evaporator capacity curve fits and characterization

Figures 3.4.1 through 3.4.9 present measured coil capacities, excluding fan heat when a fan was used, as a function of the coil outlet saturation temperature. The figures also include a linear fit to capacity data obtained for each evaporator and the fit coefficients. Examination of the figures indicates that a linear capacity fit is an adequate representation of the measured data. Table 3.4.1 summarizes the cooling capacity linear slopes and intercepts. Appendix C gives detailed data summaries of the tests performed for each coil.

We may note that the presented evaporator test data – including the performance lines – refers to the evaporator exit saturation temperature. The CD Unit curves also use the evaporator exit saturation temperature to calculate cooling capacity; i.e., they include the effect of refrigerant pressure drop and heat transfer in the suction line.

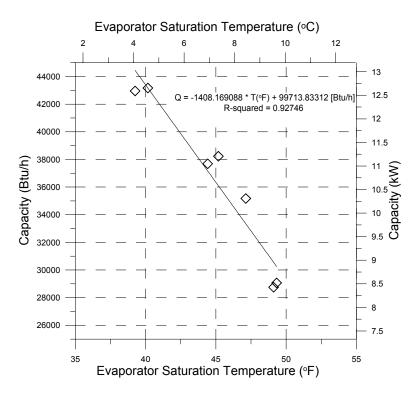


Figure 3.4.1: Coil 1 cooling capacity as a function of outlet saturation temperature

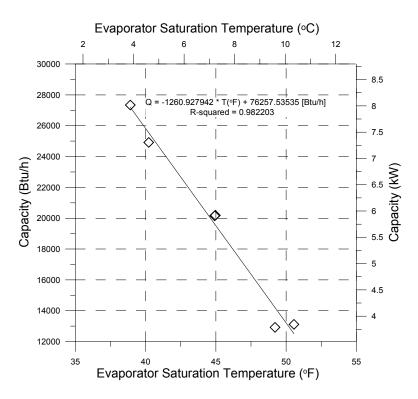


Figure 3.4.2: Coil 2 cooling capacity as a function of outlet saturation temperature

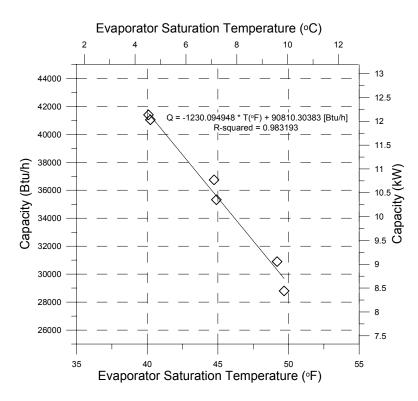


Figure 3.4.3: Coil 3 cooling capacity as a function of outlet saturation temperature

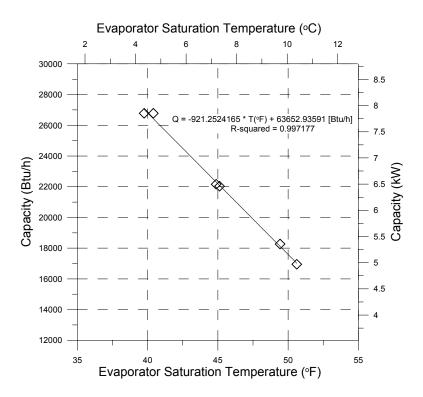


Figure 3.4.4: Coil 4 cooling capacity as a function of outlet saturation temperature

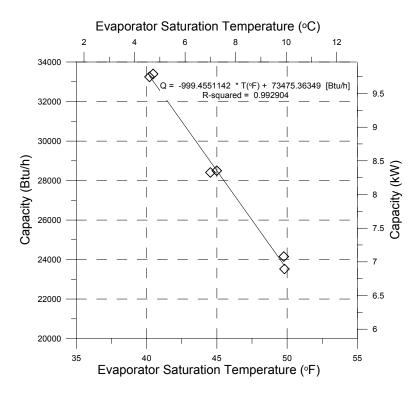


Figure 3.4.5: Coil 5 cooling capacity as a function of outlet saturation temperature

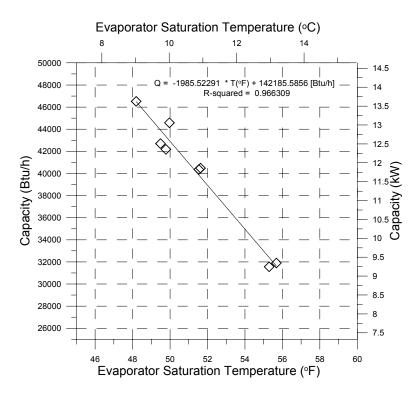


Figure 3.4.6: Coil 6 cooling capacity as a function of outlet saturation temperature

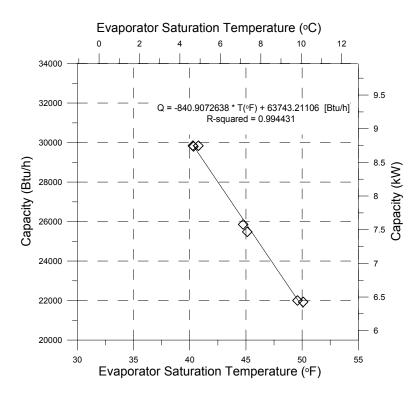


Figure 3.4.7: Coil 7 cooling capacity as a function of outlet saturation temperature

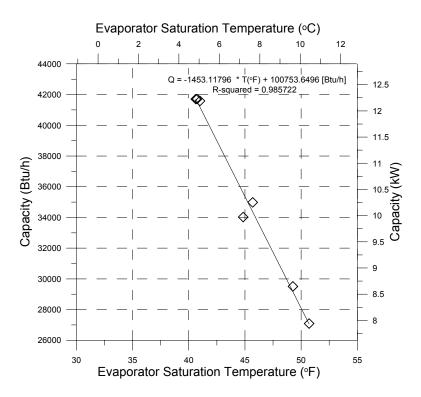


Figure 3.4.8: Coil 8 cooling capacity as a function of outlet saturation temperature

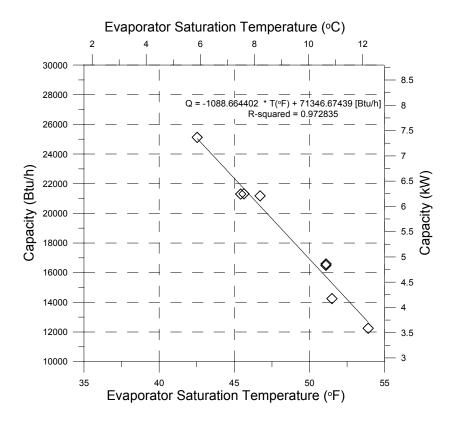


Figure 3.4.9: Coil 9 cooling capacity as a function of outlet saturation temperature

Coil	Evaporator	Evaporator Fan Cooling Capacity L		y Linear Coefficients
Number	Airflow	Power	Slope	Intercept
Number	m³/h (scfm)	W	W/⁰C (Btu/h·°F)	W (Btu/h)
1	1699 (1000)	0	-742.8 (-1408.17)	29223.85 (99713.83)
2	1368 (805)	0	-665.1(-1260.93)	22348.89 (76257.54)
3	1621 (954)	0	-648.9 (-1230.09)	26613.89 (90810.3)
4*	1342 (790)	0	-486.0 (-921.25)	18654.84 (63652.94)
5	1279 (753)	271	-527.2 (-999.46)	21533.51 (73475.36)
6	1954 (1150)	784	-1047.4 (-1985.52)	41670.51 (142185.6)
7	2047 (1205)	0	-443.6 (-840.91)	18681.3 (63743.21)
8	2360 (1389)	0	-766.6 (-1453.12)	29527.99 (100753.65)
9	849 (500)	364	-574.3 (-1088.66)	20909.65 (71346.67)
t Opil 4 sinflations to a bink and associate associate a second size other to ADI to sta				

Table 3.4.1: Mixed evaporator capacity linear fit coefficients and fan powers from NIST coil tests

* Coil 4 airflow was too high and results cannot be compared directly to ARI tests

Figures 3.4.10 thru 3.4.12 help to characterize and contrast the performance of the nine evaporators with respect to one another. Figure 3.4.10 shows the cooling capacity of each coil as a function of the evaporator saturation temperature generated from the capacity linear fits at an evaporator temperature of 7.2 °C (45 °F). The plot indicates the relative values of a change in capacity with respect to a change in evaporation temperature (slope) for each coil.

Figure 3.4.11 presents the airflow rate per unit of capacity for all coils, which is an indication of air temperature change across the coil. These values are from NIST tests at an evaporator saturation temperature of 10 °C (50 °F). All NIST tests were intended to be performed at the ARI Test airflow rates. Inadvertently, Coil 4 airflow was 262 m³/h (154 scfm) higher than the ARI Tests. Consequently, NIST capacity measurements and predictions for Coil 4 were significantly higher (approximately 24 %) than would have been the case with correct lower airflow rate. The results for Coil 4 have been included in this report, but they cannot be directly compared with the ARI Tests. The airflow rates at the other tests differed from the ARI Test values on average by 0.14 % with a standard deviation of 1.8 %. The average airflow rate per unit cooling capacity was 0.1852 m³/W h (383.5 scfm/ton) with a standard deviation of 0.0518 m³/W h (107.1 scfm/ton). Coil 6 had the smallest airflow rate per unit capacity [0.1261 m³/W h (262 scfm/ton)] as well as the largest change in cooling capacity with respect to a change in evaporator saturation temperature (see Figure 3.4.10). Coil 6 also had the lowest sensible heat ratio (SHR) of 0.710 (Fig. 3.4.12). Fig. 3.4.12 shows a linear trend of SHR with respect to airflow rate per unit capacity, which is consistent with general experience. The high sensible heat ratios were due to the high evaporating temperature of 10 °C (50 °F). At the lowest evaporating temperatures tested at NIST, the highest SHR's occurred for Coils 2, 7, and 8 with values of 0.77, 0.81, and 0.78, respectively. All other coils had SHR's less than 75 % at the lowest tested evaporating temperature.

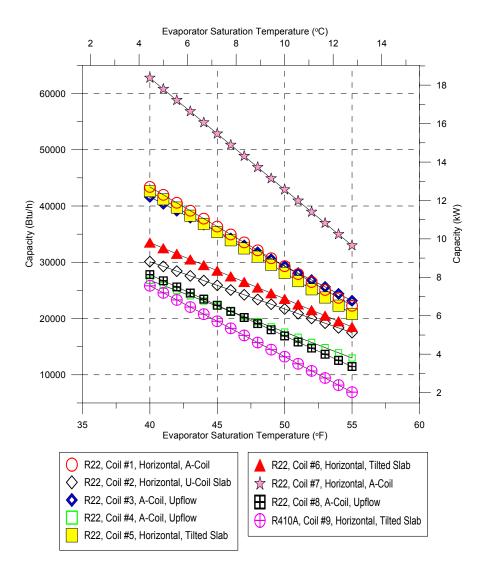


Figure 3.4.10: Cooling capacity, q(95), for all evaporators based on the NIST linear fit

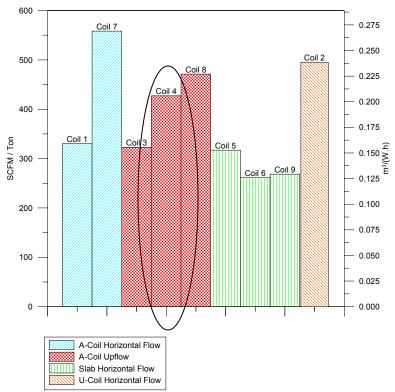


Figure 3.4.11: Airflow rate relative to cooling capacity from the NIST linear fit for all coils at an evaporation temperature of 7.2 °C (45 °F)

(Note: Coil 4 airflow was too high and results cannot be compared directly to ARI tests)

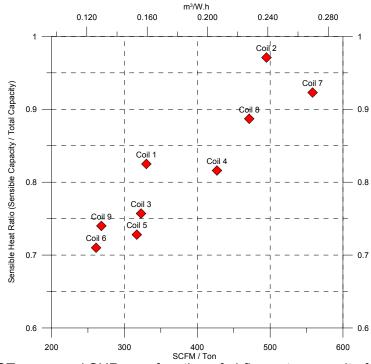


Figure 3.4.12: NIST measured SHR as a function of airflow rate per unit of cooling capacity at an evaporator exit saturation temperature of 16.2 °C (50.0 °F)

4: MIXED SYSTEM PERFORMANCE PREDICTION

4.1: Calculation of Q(95), Q(82) and EER(82)

With the coil capacity coefficients from Table 3.4.1 and CD Unit capacity coefficients from Table 4.1.1, the C-B Method was used to calculate cooling capacity and EER at 27.8 °C (82.0 °F), and cooling capacity at 35.0 °C (95.0 °F) for all coils.

				Trom ARI				
	q(8	32)	p	(82)	q(95)	p	(95)
Coil	Slope W/ºC (Btu/h ºF)	Intercept W (Btu/h)	Slope W/ºC (W/ºF)	Intercept W	Slope W/ºC (Btu/h ºF)	Intercept W (Btu/h)	Slope W/ºC (W/ºF)	Intercept W
1	312.7 (592.7)	2092.9 (7141.5)	7.38 (4.1)	2340.0	300.2 (569.1)	2217.7 (7567.0)	5.76 (3.2)	2717.1
2	184.7 (350.2)	2979.2 (10165.6)	31.14 (17.3)	1242.9	163.2 (309.3)	2785.3 (9503.9)	35.64 (19.8)	1289.6
3	312.7 (592.7)	2092.9 (7141.5)	7.38 (4.1)	2340.0	300.2 (569.1)	2217.7 (7567.0)	5.76 (3.2)	2717.1
4*	237.1 (449.5)	-622.6 (-2124.6)	22.14 (12.3)	880.9	232.2 (440.2)	-1253.0 (-4275.5)	26.1 (14.5)	877.7
5	266.2 (504.7)	674.2 (2300.5)	32.22 (17.9)	1177.1	263.3 (499.2)	22.7 (77.3)	38.7 (21.5)	1069.6
6	581.6 (1102.5)	3886.6 (13261.7)	28.98 (16.1)	3584.9	564.6 (1070.2)	2995.4 (10220.7)	32.94 (18.3)	4123.4
7	484.1 (917.6)	-148.4 (-506.2)	31.68 (17.6)	2253.8	508.6 (964.1)	-2569.6 (-8767.8)	38.34 (21.3)	2278.8
8	96.8 (735.5)	3140.6 (10716.2)	138.24 (76.8)	36.4	336.6 (638)	3420.9 (11672.7)	172.8 (96)	-697.3
9	286.6 (543.2)	984.7 (3359.9)	10.8 (6.0)	1692.8	278.5 (528.0)	423.0 (1443.2)	11.52 (6.4)	1990.9

Table 4.1.1: CD Unit linear coefficients for power and capacity at A-Test and B-Test conditions

*Coil 4 airflow was too high and results cannot be compared directly to ARI tests

The calculation procedure, which we illustrated graphically in Figure 1.1, was implemented computationally by solving the set of two linear equations for the evaporation temperature at which the cooling capacity of the mixed coil equals the cooling capacity of the CD Unit:

$$q_{\rm CD} = B_{\rm CD} + A_{\rm CD}T_{\rm evap} = q_{\rm mixed} = B_{\rm mixed} + T_{\rm evap}A_{\rm mixed}$$
 4.1.1

$$T_{\text{evap}} = \frac{(\mathsf{B}_{\text{mixed}} - \mathsf{B}_{\text{CD}})}{(\mathsf{A}_{\text{CD}} - \mathsf{A}_{\text{mixed}})}$$
4.1.2

In the equations above, B represents the intercept and A represents the slope for the CD Unit (CD subscript) and mixed evaporator (mixed subscript), respectively. Applying the obtained value of the saturation temperature into either capacity equation yields the capacity of the evaporator of the mixed system. The rated cooling capacity of the mixed system was obtained by reducing the evaporator capacity by the fan heat. For coils equipped with a fan, the fan heat was measured; for other coils it was calculated according to ARI Standard 210/240 (ARI 2003).

$$Q = q + Q_{fan}$$
 4.1.3

Similarly, the power of the mixed system was obtained by applying the value of the evaporator saturation temperature from equation 4.1.2 into the condensing unit power equation 4.1.4 and making adjustment for the indoor fan power as shown in equation 4.1.5.

$$p_{\rm CD} = b_{\rm CD} + a_{\rm CD} T_{\rm evap} \tag{4.1.4}$$

$$P_{CD} = p_{CD} + P_{fan} \tag{4.1.5}$$

Table 4.1.2 shows the results for A-Test mixed system capacities. Table 4.1.3 presents the results for B-Test capacity, power, and EER.

	Table 4.1.2:	Mixed system A	A- Lest capacity	from the C-B Meth	DOI		
Coil	<i>T_{evap}</i> °C (°F)	<i>q</i> (95) W (Btu/h)	Indoor Airflow m ³ /h (scfm)	Q _{fan} ⁽¹⁾ W (Btu/h)	Q(95) W (Btu/h)		
1	8.1 (46.6)	9990 (34089)	1699 (1000)	366.3 (1250.0)	9624 (32839)		
2	5.8 (42.5)	6639 (22653)	1368 (805)	294.9 (1006.3)	6344 (21647)		
3	7.9 (46.3)	9935 (33898)	1621 (954)	349.5 (1192.5)	9585 (32705)		
4*	9.9 (49.9)	5184 (17688)	1342 (790)	289.4 (987.5)	4894 (16700)		
5	9.4 (49.0)	7188 (24526)	1279 (753)	271.0 (925.5)	6917 (23601)		
6	6.2 (43.2)	16541 (56439)	1954 (1150)	784.0 (2677.5)	15756 (53761)		
7	4.5 (40.2)	8781 (29962)	2047 (1205)	441.5 (1506.3)	8340 (28456)		
8	5.9 (42.6)	11386 (38851)	2360 (1389)	507.0 (1736.3)	10877 (37115)		
9	6.2 (43.2)	7114 (24274)	849 (500)	364.0 (1243.1)	6749 (23030)		

Table 4.1.2: Mixed system A-Test capacity from the C-B Method

(1) For units with no fan Q_{fan} was calculated to be 1250 Btu/h per 1000 scfm of airflow (ARI 210/240-2003).
 *Coil 4 airflow was too high and results cannot be compared directly to ARI tests

		. IVIIACU Sys	SIGHT D-103	i capacity, po				ou
Coil	<i>T_{evap}</i> °C (°F)	q(82) W (Btu/h)	р _{сD} (82) W	Indoor Airflow, m ³ /h (scfm)	Q _{fan} (1) W (Btu/h)	P _{fan} ⁽²⁾ W	Q(82) W, (Btu/h)	EER(82) W/W (Btu/W h)
1	7.93 (46.3)	10192 (34563)	2530	1699 (1000)	365.0 (1250.0)	365.0	9763 (33313)	3.37 (11.51)
2	5.01 (41.0)	7190 (24532)	1953	1368 (805)	293.8 (1006.3)	293.8	6895 (23525)	3.07 (10.47)
3	7.72 (45.9)	10066 (34347)	2528	1621 (954)	348.2 (1192.5)	348.2	9717 (33155)	3.38 (11.53)
4*	8.88 (48.0)	5699 (19445)	1471	1342 (790)	288.4 (987.5)	288.4	5410 (18458)	3.07 (10.49)
5	8.51 (47.3)	7666 (26182)	2024	1279 (753)	271 (924.7)	271.0	7402 (25258)	3.27 (11.01)
6	5.42 (41.7)	17361 (59291)	4257	1954 (1150)	784 (2675.0)	784.0	16593 (56616)	3.29 (11.23)
7	2.52 (36.5)	9677 (33019)	2897	2047 (1205)	439.8 (1506.3)	439.8	9236 (31513)	2.77 (9.44)
8	5.11 (41.1)	12009 (40974)	3196	2360 (1389)	507.0 (1736.3)	507.0	11500 (39238)	3.11 (10.6)
9	5.37 (41.7)	7610 (25991)	1943	849 (500)	364 (1241.9)	364.0	7253 (24749)	3.14 (10.73)

Table 4.1.3: Mixed system B-Test capacity, power, and EER from the C-B Method

(1) For units with no fan Q_{fan} is calculated to be 1250 Btu/h per 1000 scfm of airflow (ARI 210/240-2003).

(2) For units with no fan P_{fan} is calculated to be 365 W per 1000 scfm of airflow (ARI 210/240-2003).

Coil 4 airflow was too high and results cannot be compared directly to ARI tests.

4.2: Calculation of SEER

The calculation of SEER involves the value of EER(82) and the cyclic degradation coefficient C_{D} .

SEER =
$$(1 - 0.5 \cdot C_{D})$$
EER(82) 1.2

For the tested systems, C_D was typically obtained by conducting dry-coil steady-state and cyclic tests (C and D tests of ARI Standard 210/240, (ARI 2003)). Alternatively, the rater may use the 0.25 default value instead of performing the tests. In practice, C_D values fall between 0.0 and 0.25. Since, by definition, the mixed system is not tested, the C_D value must be obtained from some engineering analysis or the default value of 0.25 must be taken.

Dougherty (2004), working with DOE and ARI, performed a statistical analysis of experimentally determined C_D values for a large sample of systems. He grouped the studied systems into four basic categories shown in Table 4.2.1. The analysis of C_D values for these four system categories produced the C_D percentiles shown in Table 4.2.2.

System Category	Equalize During Off Cycle	Indoor Fan Off Delay	System Components
A	Yes	No	Cap Tube Orifice Bleed TXV
B1	No	No	Non-Bleed TXV Electronic Expansion Device Liquid Line Solenoid
B2	Yes	Yes	Cap Tube Orifice Bleed TXV
С	No	Yes	Non-Bleed TXV Electronic Expansion Device Liquid Line Solenoid

Table 4.2.1: System classifications for cyclic degradation coefficient analysis

The range of C_D values is rather significant in each equipment category. In category A, for example, the classification for all nine mixed systems tested for this project, the difference between the 50th and 99th percentiles is 0.24-0.09=0.15. This means that assuming the 50th percentile value for the mixed system with an actual C_D of 0.24 will result in a SEER prediction error of 7.5%. For illustration in Table 4.2.3, we generated two SEER numbers for mixed systems using C_D values of 0.22 and 0.24, which correspond to the 95th and 99th percentiles, respectively. While both choices are conservative statistically, they still represent a risk of SEER overprediction by 1.5% and 0.5%, respectively, should the actual C_D value be the maximum of 0.25. We believe that the most accurate assignment of C_D for the mixed system would be that of the matched system if the changes implemented in the mixed system do not move it to a different equipment category, as defined in Table 4.2.1.

	Cyclic degradation		5 101 0111010111 3930	Sin categories
Percentile	A	B1	B2	С
99 th	0.24	0.16	0.22	0.15
95 th	0.22	0.14	0.14	0.12
90 th	0.16	0.14	0.12	0.10
85 th	0.14	0.12	0.11	0.09
80 th	0.12	0.12	0.10	0.08
75 th	0.12	0.11	0.10	0.07
70 th	0.11	0.11	0.09	0.06
60 th	0.10	0.9	0.08	0.05
50 th	0.09	0.07	0.07	0.04
Sample Size	77	58	109	78

Table 4.2.2: Cyclic degradation coefficient values for different system categories

		percentiles						
Coil		egradation cient, C _d	SEER (Btu/W·h)					
	95 th	99 th	95 th	99 th				
1	0.22	0.24	10.24	10.13				
2	0.22	0.24	9.32	9.22				
3	0.22	0.24	10.26	10.14				
4*	0.22	0.24	9.34	9.23				
5	0.22	0.24	10.08	9.97				
6	0.22	0.24	10.33	10.21				
7	0.22	0.24	8.41	8.31				
8	0.22	0.24	9.43	9.32				
9	0.22	0.24	9.89	9.78				

Table 4.2.3: Mixed system SEERs calculated using statistically determined C_D for 95th and 99th percentiles

Coil 4 airflow was too high and results cannot be compared directly to ARI tests.

5: NIST PREDICTIONS AND ARI DATABASE COMPARISON

5.1: A-Test capacity comparison

Table 5.1.1 and Figure 5.1.1 present mixed system capacities, Q(95), from the C-B Method and the ARI database for the A-Test conditions. Capacity predictions from the C-B Method were within ± 5 % of the ARI tests for five of eight coils. Among the three cases with poor predictions, the disagreement was as high as 17.6 %.

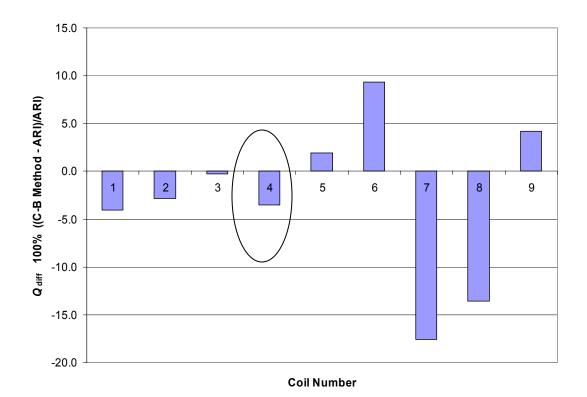
					pacilies no	III AIXI 103		Nethou
Coil	C-B Method 7 _{evap} °C (°F)	ARI Test <i>T</i> _{evap} °C (°F)	C-B Method q(95) W (Btu/h)	Indoor Airflow m ³ /h (scfm)	Q _{fan} W (Btu/h)	ARI Test Q(95) W (Btu/h)	C-B Method Q(95) W (Btu/h)	Q _{diff} 100%(NIST – ARI)/ARI
1	8.1 (46.6)	7.2 (45.0)	9991 (34089)	1699 (1000)	366.3 ⁽¹⁾ (1250.0)	10034 (34238)	9624 (32839)	-4.1
2	5.8 (42.5)	6.1 (43.0)	6639 (22653)	1368 (805)	294.9 ⁽¹⁾ (1006.3)	6529 (22278)	6344 (21647)	-2.8
3	7.9 (46.3)	7.6 (45.6)	9935 (33898)	1621 (954)	349.5 ⁽¹⁾ (1192.5)	9609 (32786)	9585 (32705)	-0.2
4*	9.9 (49.9)	8.4 (47.2)	5184 (17688)	1342 (790)	289.4 ⁽¹⁾ (987.5)	5073 (17311)	4894 (16700)	-3.5
5	9.4 (49.0)	10.5 (50.9)	7188 (24526)	1279 (753)	271.0 ⁽¹⁾ (925.5)	6787 (23157)	6917 (23601)	1.9
6	6.2 (43.2)	7.2 (44.9)	16541 (56439)	1954 (1150)	784.0 ⁽²⁾ (2677.5)	14407 (49159)	15756 (53761)	9.4
7	4.5 (40.2)	6.8 (44.3)	8781 (29962)	2047 (1205)	441.5 ⁽²⁾ (1506.3)	10122 (34537)	8340 (28456)	-17.6
8	5.9 (42.6)	5.7 (42.2)	11387 (38851)	2360 (1389)	507.0 ⁽¹⁾ (1736.3)	12591 (42963)	10878 (37115)	-13.6
9	6.2 (43.2)	4.1 (44.2)	7114 (24274)	849 (500)	364 ⁽²⁾ (1243.1)	6480 (22112)	6749 (23030)	4.2

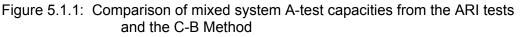
Table 5.1.1: Mixed system A-Test capacities from ARI Tests and C-B Method

⁽¹⁾ Coil without a fan; Q_{tan} was calculated to be 1250 Btu/h per 1000 scfm of airflow (ARI 210/240-2003)

⁽²⁾ Coil equipped with a fan; fan power measured by NIST

*Coil 4 airflow was too high and results cannot be compared directly to ARI tests.





(Note: Coil 4 airflow was too high and results cannot be compared directly to ARI tests)

Table 5.1.1 also shows evaporator saturation temperatures obtained from the C-B Method and measured during mixed system certification tests. Ideally, these temperatures should be the same or very close for good capacity predictions. One can rationalize that a saturation temperature from the C-B Method that is lower than that from the certification tests should result in an overprediction of capacity while a higher C-B Method saturation temperature should drive toward the opposite effect. This physical rationale holds somewhat for Coils 1, 5, and 6, while other coils do not conform. In particular, Coil 7, associated with the largest underprediction of Q(95) of 17.6 % has a 4.5 °C (40.2 °F) C-B Method saturation temperature versus a 6.8 °C (44.3 °F) saturation temperature measured during certification tests.

To further explore the reasons for inconsistent Q(95) predictions, we compared test-obtained mixed system Q(95) capacities with those calculated for mixed evaporators from NIST-developed capacity lines and those calculated for condensing units from condensing performance curves using the same evaporator saturation temperature as measured during the mixed system certification tests. Table 5.1.2 presents the data. It is desirable for these three capacities to be close, ideally equal, to each other. The table shows that NIST-calculated capacities agreed with the certification test capacities for Coils 1, 3, 6, and 9 within \pm 2.5 %, which is a remarkable agreement. The capacities for coils 2 and 5 are underpredicted within 6.5 %. The largest disagreement of -27.6 % is for Coil 7. For condensing unit capacities, the

agreement with mixed system data was within \pm 6.5 % for six cases. In the remaining cases, the deviations from mixed system capacities were as much as -14.2 %.

Looking back at the predicted Q(95) presented in Table 5.1.1, we can see that we obtained good predictions of Q(95) in every case where the capacities from three sources shown in Table 5.1.2 are in good agreement (Coils 1, 2, 3, and 9). Also good Q(95) predictions are for Coil 5 in Table 5.1.1; in this case the capacity calculated from evaporator and condensing unit correlations in Table 5.1.2 underpredicted and overpredicted the mixed system capacity by a similar percentage. The result is a good prediction of Q(95) at a somewhat different evaporator saturation temperature than that measured during a system test.

In the cases with the largest Q(95) prediction errors, Coils 6, 7 and 8, no offsetting of errors took place; even for Coil 8 where the C-B Method predicted the evaporator saturation temperature within 0.2 °C ($0.4 \, ^\circ$ F). Since evaporator capacity and mixed system capacity for Coil 6 in Table 5.1.2 agree within 2.5 % while the condensing unit capacity deviates by 13.1 %, a suggestion can be made that the condensing unit correlation could be faulted for the Q(95) underprediction. Using the same rationale, a case against the evaporator capacity correlation could be made for Coil 7. For Coil 8, the evaporator and condensing unit correlations yield similar capacities and disagree with the system test data by a similar capacity percentage, -12.2 % and -14.2 %, respectively, suggesting some testing irregularity or an error in data handling.

Table 5.1.3 allows additional analysis of capacity predictions from the NIST-developed capacity lines. The table shows the tested mixed system capacities and those calculated using capacity lines (adjusted for the indoor fan heat) as presented in Table 5.1.2, but it includes temperature and subcooling of the refrigerant entering the expansion valve and the refrigerant superheat at the evaporator exit. Since values of these parameters are different for most cases, it was of interest to assess the extent to which these differences could affect the evaporator capacity predictions. For this purpose, we used the EVAP-COND simulation package (NIST 2003) to simulate coil performance at different inlet refrigerant temperatures and outlet superheats.

For example, for Coil 7, the ARI superheat was 2.4 °C (4.3 °F) and the NIST superheat was 7.3 °C (13.2 °F); a difference of 4.9 °C (8.9 °F). Keeping the same evaporator saturation temperature and liquid temperature (inlet quality), and changing the superheat to the ARI value increased the predicted Coil 7 capacity by 494 W (1686 Btu/h) to 7818 W (26 675 Btu/h), thus reducing the percent difference from -27.6 % to -22.8 %. Changing the liquid temperature from 40.6 °C (105.1 °F) to the ARI value of 49.4 °C (120.9 °F) and keeping the same subcooling of 7.7 °C (13.8 °F), increased the capacity by an additional 222 W (758 Btu/h) to 8038 W (27 433 Btu/h), thus reducing the ARI-NIST percent difference to -20.5 %. It appears that some installation and test condition related factors are responsible for the remaining -20.5 % deviation in the Coil 7 results.

Table 5.1.2: Mixed system A-Test capacities from the ARI tests,	, condensing unit capacities from CD Unit curves, and evaporator
capacities from NIST-developed evaporator capacit	ty curves at the ARI-test evaporating temperature ^(1,2)

	Co	il 1	Coil 2		Coil 3		Co	Coil 4* Coil 5		Coil 6		Co	il 7	Co	Coil 8 C		il 9	
	W	Btu/h	W	Btu/h	W	Btu/h	W	Btu/h	W	Btu/h	W	Btu/h	W	Btu/h	W	Btu/h	W	Btu/h
ARI Value Q(95)	10034	34238	6529	22278	9609	32786	5073	17311	6787	23157	14407	49159	10122	34537	12591	42963	6480	22112
NIST Q(95)	10282	35083	6163	21029	9829	33536	5622	19183	6353	21679	14760	50363	7324	24989	11049	37702	6443	21984
CD Unit Q(95)	10338	35273	6388	21796	9475	32330	4548	15518	7198	24562	16294	55598	9508	32441	10804	36866	6899	23539
NIST/ARI %	2.5 -5.6		2	2.3 10.).8	-6	.4	2	.5	-2	7.6	-12	2.2	-0	.6		
CD Unit/ARI %			-2	.2	-1	-1.4		0.4	6	.1	13	3.1	-6	.1	-14	4.2	6	.5

⁽¹⁾Mixed system evaporating temperature, *T_{evap}*, is listed in Tables 5.1.1. ⁽²⁾ Indoor fan heat from the mixed system accounted for in all capacity calculations ⁽³⁾Q_{diff} = 100% (NIST – ARI)/ARI ⁽⁴⁾Q_{diff} = 100% (CD Unit – ARI)/ARI *Coil 4 airflow was too high and results cannot be compared directly to ARI tests

Table 5.1.3: Mixed system A-test capacities from ARI values and evaporator capacities from NIST-developed evaporator capacity
curves at the ARI-test evaporating temperature ⁽¹⁾

					-					<u> </u>								
	Co	il 1	Co	il 2	Co	il 3	Coi	4*	Co	il 5	Co	oil 6	Co	117	Co	il 8	Co	il 9
	ARI	NIST	ARI	NIST	ARI	NIST	ARI	NIST	ARI	NIST								
T _{liq} °C	37.2	40.7	41.1	40.5	35.2	40.5	42.2	40.7	40.3	40.4	40.3	40.4	49.4	40.6	39.1	40.9	40.8	40.6
(°F)	(99.0)	(105.3)	(106.0)	(104.9)	(95.4)	(104.9)	(108.0)	(105.3)	(104.6)	(104.8)	(104.6)	(104.8)	(120.9)	(105.1)	(102.4)	(105.7)	(105.4)	(105.0)
T _{sub} °C	6.9	6.2	11.8	6.6	7.7	7.7	13.8	7.6	7.7	7.7	6.4	7.7	6.7	7.7	11.1	7.1	5.9	7.6
(°F)	(12.5)	(11.1)	(21.2)	(11.9)	(13.8)	(13.9)	(24.9)	(13.6)	(13.9)	(13.9)	(11.6)	(13.9)	(12.0)	(13.8)	(19.94)	(12.8)	(10.6)	(13.6)
<i>T_{evap}</i> °C	7.2	7.2	6.1	6.1	7.6	7.6	8.4	8.4	10.5	10.5	7.2	7.2	6.8	6.8	5.7	5.7	6.8	6.8
(°F)	(45.0)	(45.0)	(43.0)	(43.0)	(45.6)	(45.6)	(47.2)	(47.2)	(50.9)	(50.9)	(44.9)	(44.9)	(44.3)	(44.3)	(42.2)	(42.2)	(44.2)	(44.2)
T _{suph} °C	6.2	7.1	4.7	8.1	11.6	7.4	2.1	7.4	0.8	7.8	7.1	7.6	2.4	7.3	3.9	7.4	6.2	7.8
(°F)	(11.2)	(12.8)	(8.5)	(14.6)	(20.9)	(13.4)	(3.8)	(13.3)	(1.5)	(14.0)	(12.7)	(13.6)	(4.3)	(13.2)	(7.1)	(13.4)	(11.2)	(14.0)
Q, W	10034	10282	6529	6163	9609	9829	5073	5622	6787	6353	14407	14760	10122	7324	12591	11049	6480	6443
(Btu/h)	(34238)	(35083)	(22278)	(21029)	(32786)	(33536)	(17311)	(19183)	(23157)	(21679)	(49159)	(50363)	(34537)	(24989)	(42963)	(37702)	(22112)	(21984)
$Q_{\text{diff}}(\%)^{(2)}$		2.5		-5.6		2.3		10.8		-6.4		2.5		-27.6		-12.2		-0.6

⁽¹⁾ Indoor fan heat from the mixed system accounted for in all capacity calculations ⁽²⁾ Q_{diff} = 100% (NIST – ARI)/ARI *Coil 4 airflow was too high and results cannot be compared directly to ARI tests

5.2: B-Test EER comparison

Table 5.2.1 shows EER values from the ARI tests and the C-B Method. Coils 5 and 7 show an agreement within ± 5 %. The C-B Method overpredicted the ARI values by more than 5 % in four cases. System power, fan power, Q(82), and EER(82) were compared in Figure 5.2.1 to illustrate the sources of disagreement between the C-B Method and the ARI tests.

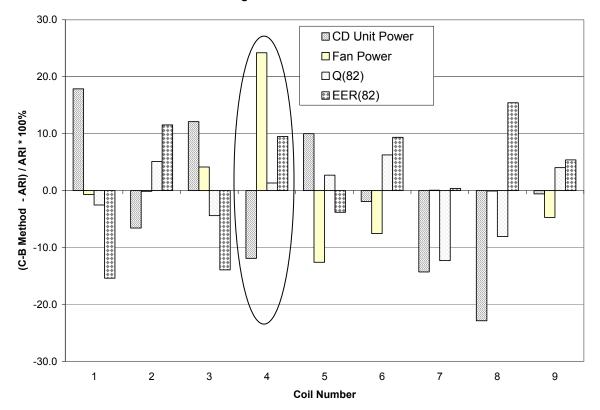


Figure 5.2.1: Percent differences between ARI Values and the C-B Method for the EER(82) calculation (Note: Coil 4 airflow was too high and results cannot be compared directly to ARI tests)

We may note that the largest EER disagreement was a 15.4 % underprediction and a 15.4 % over prediction for Coil 1 and Coil 8, respectively. For Coil 1 the 17.9 % higher power and the 2.5 % lower capacity caused the C-B Method EER(82) to be 15.4 % lower than the ARI Test EER(82). Since the evaporator saturation temperatures were equal for this coil, the 400 W difference in ARI Test and CD Unit linear fit power is the main contributor to the EER(82) difference. If the ARI Test CD Unit power were used in the C-B Method calculation of EER(82), the percent difference in EER(82) would only be -2.4 %.

Coil 8 had a 22.9 % under prediction in CD Unit power compared to the ARI Test results. The C-B Method's lower power was not completely mitigated by a lower capacity, resulting in the EER(82) being 15.4 % higher than the ARI Test EER(82). The lower evaporating temperature for the C-B Method would tend to produce a higher capacity than the ARI Test capacity, but this was not the case. According to the CD Unit capacity linear fit, a 1.3 °C (2.4 °F) lower evaporating temperature should increase capacity by 517 W (1765 Btu/h).

This does not equal the 1518 W (5179 Btu/h) difference between the C-B Method and ARI Test capacities. If the ARI Test value of power were used with the C-B Method capacity, the resulting EER(82) percent difference would be -8.1 %.

The C-B Method produced a 13.9 % underprediction of EER(82) for Coil 3. The ARI Test and C-B Method evaporating temperature were within 3.6 %. The CD Unit power and the ARI Test power differed by 12.1 %. The higher C-B Method power and the lower C-B Method capacity produced the 13.9 % lower EER(82). If the ARI Test power were used with the C-B Method capacity, the EER(82) difference would be -4.9 %.

From examining Table 5.2.1, the clear factor in EER(82) disagreement is the system power difference between actual tests and the power fits. This is true for all cases except Coil 7. For Coil 7, the evaporating temperatures differed by almost 19 %. The C-B Method's lower evaporating temperature should produce a higher capacity than the ARI Test evaporating temperature, but this was not the case. The lower evaporating temperature produced a 12.3 % lower capacity which was combined with a 14.3 % lower CD Unit power to produce an almost equivalent EER(82).

Coil		<i>T_{evap}</i> °C (°F)	CD Unit Power W				Fan Power W			Q(82) ^c W (Btu/h)		EER(82) W/W (Btu/W h)		
	C-B Method	ARI Test	Difference (C-B Method - ARI)	C-B Method	ARI Test	Percent Diff %	C-B Method	ARI Test	Percent Diff %	C-B Method	ARI Test	Percent Diff %	C-B Method	ARI Test	Percent Diff %
1	7.94 (46.3)	7.94 (46.3)	0.0 (0.0)	2530	2146	17.9	365	368	-0.7	9763 (33313)	10017 (34178)	-2.5	3.37 (11.51)	3.99 (13.60)	-15.4
2	5.0 (41.0)	6.50 (43.7)	-1.5 (-2.7)	1953	2090	-6.6	294	294	-0.1	6895 (23525)	6559 (22381)	5.1	3.07 (10.47)	2.75 (9.39)	11.5
3	7.72 (45.9)	6.83 (44.3)	0.9 (1.6)	2528	2255	12.1	348	334	4.1	9717 (33155)	10164 (34680)	-4.4	3.38 (11.53)	3.92 (13.39)	-13.9
4 ^d	8.89 (48.0)	9.72 (49.5)	-0.8 (-1.5)	1471	1670	-11.9	288	232	24.2	5410 (18458)	5338 (18215)	1.3	3.07 (10.49)	2.81 (9.58)	9.5
5	8.50 (47.3)	9.67 (49.4)	-1.2 (-2.1)	2024	1840	10.0	271	310	-12.6	7402 (25258)	7207 (24591)	2.7	3.23 (11.01)	3.35 (11.44)	-3.8
6	5.39 (41.7)	6.50 (43.7)	-1.1 (-2.0)	4257	4340	-1.9	784 ^a	848 ^b	-7.5	16593 (56616)	15613 (53274)	6.3	3.29 (11.23)	3.01 (10.27)	9.4
7	2.50 (36.5)	7.22 (45.0)	-4.7 (-8.5)	2897	3380	-14.3	440 ^a	439 ^b	0.1	9236 (31513)	10529 (35926)	-12.3	2.77 (9.44)	2.76 (9.41)	0.4
8	5.06 (41.1)	6.39 (43.5)	-1.3 (-2.4)	3196	4143	-22.9	507	507	-0.1	11500 (39238)	12508 (42680)	-8.1	3.11 (10.60)	2.69 (9.18)	15.4
9	5.39 (41.7)	5.89 (42.6)	-0.5 (-0.9)	1943	1954	-0.6	364 ^a	382 ^b	-4.7	7253 (24749)	6972 (23790)	4.0	3.14 (10.73)	2.98 (10.18)	5.4

Table 5.2.1: Mixed system B-Test comparison of ARI tested and C-B Method results

a) Fan power measured by NIST. b) Fan power measured by ARI contracted testing facility. c) *Q*(82) included the fan heat correction for coils with no fan. d) NIST airflow was 262 m³/h (154 scfm) higher than the ARI tested airflow for Coil 4.

5.3: SEER comparison

Table 5.3.1 presents SEER values from the ARI database and the C-B Method for the 99th percentile cyclic degradation coefficients. With the exception of Coil 6, where the predicted SEER exceeds the measured SEER by 0.6 %, the SEER values obtained from the C-B Method are lower than the measured values by as much as 27 %. Four C-B Method SEERs agreed to within ± 5 % of the measured SEERs. Figure 5.3.1 shows that this level of agreement can be attributed to offsetting errors between EERs and SEER/EER Multipliers, (1-0.5 C_D), especially considering the large differences in cyclic degradation coefficient between the NIST 99th percentile and ARI database. These large differences in degradation coefficient indicate that more information is needed to accurately determine a representative C_D value. Clearly, the use of a fixed value for the degradation coefficient cannot reliably reproduce ARI database values.

Table 5.3.1:	SEERs from ARI value and C-B Method
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Coil	SEER from ARI values Btu/(W·h)	SEER from C-B Method using 99 th percentile C _d	SEER ⁽¹⁾ Diff %	ARI SEER/EER Multiplier ⁽²⁾ (1-0.5 C _d)	NIST 99 th Percentile SEER/EER Multiplier (1-0.5 Cd)	(ARI - NIST 99 th) SEER/EER Multiplier
1	13.87	10.13	-27.0	0.931	0.880	0.051
2	9.63	9.22	-4.3	0.983	0.880	0.103
3	13.33	10.14	-23.9	0.964	0.880	0.084
4*	9.79	9.23	-5.7	0.980	0.880	0.100
5	10.01	9.68	-3.3	0.876	0.880	-0.004
6	9.82	9.88	0.6	0.976	0.880	0.096
7	9.56	8.31	-13.1	0.977	0.880	0.097
8	10.17	9.32	-8.4	0.949	0.880	0.069
9	9.78	9.44	-3.5	0.961	0.880	0.081

(1) SEER Diff = 100% (NIST – ARI)/ARI

⁽²⁾ARI SEER/EER multiplier was calculated from SEER = $(1-0.5 C_d)$ EER(82)

*Coil 4 airflow was too high and results cannot be compared directly to ARI tests.

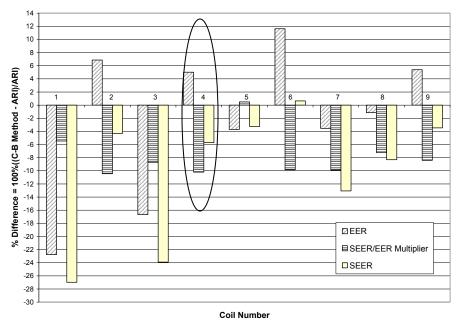


Figure 5.3.1: ARI Values and C-B Method SEER/EER Multiplier, EER, and SEER

6: GENERATING AN EVAPORATOR CAPACITY LINE USING EVAP-COND

In this study, we developed evaporator capacity lines based on measured capacities at several different evaporator exit saturation temperatures with constant superheat and inlet quality. Controlling these three parameters makes coil tests more time consuming than complete system tests. For this reason, we explored the possibility to minimize the laboratory effort by using an evaporator simulation model. A simulation model can be tuned to predict the measured capacity, which can then be used to provide capacities at other saturation temperatures needed to generate the evaporator capacity line. To demonstrate this approach, we used the EVAP-COND finned-tube heat exchanger simulation package (NIST 2003).

EVAP-COND uses coil design parameters (including refrigerant circuitry) and refrigerant and air parameters as input to calculate the capacity of the heat exchanger. The model allows the user to tune its prediction to experimental data by adjusting the correction factors for the air-side heat transfer coefficient, refrigerant-side heat transfer coefficient, and refrigerant-side pressure drop. In our case, we considered Coil 9 and selected appropriate values for these factors, shown in Table 6.1, so the model predictions agreed with the test results at the 7.4 °C (45.4 °F) saturation temperature. Simulations at additional saturation temperatures allowed generation of a linear capacity fit for the coil.

7 _{evap} ⁰C (⁰F)	R	ΔP	А	<i>q</i> Predicted W (Btu/h)	<i>q</i> Measured W (Btu/h)	$q_{ m diff}$ %	
7.4 (45.4)	1.15	2.00	1.30	6249 (21323)	6242 (21300)	0.1	

R - refrigerant-side heat transfer coefficient correction factor

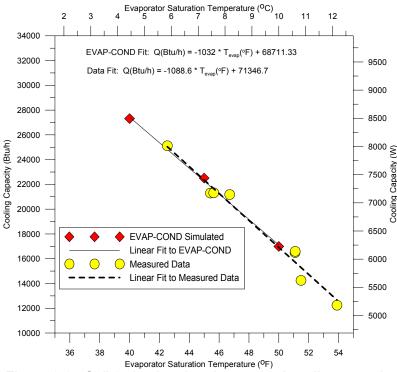
 ΔP - refrigerant pressure drop correction factor

A - air-side heat transfer coefficient correction factor

Figure 6.1 shows cooling capacities for Coil 9 from the laboratory measurements, the EVAP-COND simulations, and the corresponding capacity lines as a function of evaporating temperature. The capacity lines almost overlap. Consequently, the C-B Method performance predictions for mixed system using Coil 9 were within 0.5 % for the two capacity lines, as shown in Figure 6.2.

It is possible that the approach presented here could be extended to other evaporators that use the same air-side and refrigerant-side heat transfer surfaces; i.e., once EVAP-COND adjustable factors for air-side heat transfer, refrigerant-side heat transfer, and refrigerant pressure drop are determined for one coil, they could be applied to other coils using the same surfaces.

*q*diff = 100%(Predicted-Measured)/Measured





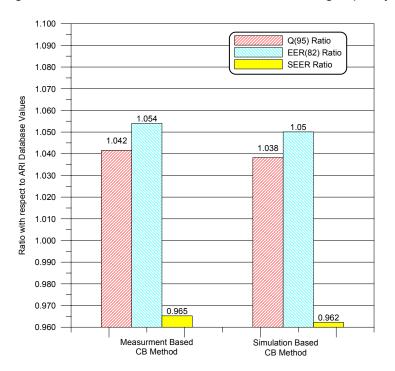


Figure 6.2: C-B Method Q(95), EER(82) and SEER ratio with respect to the ARI database using the measured and simulated Coil 9 capacity

7: UNCERTAINTY OF THE C-B METHOD

7.1: Uncertainty of the evaporator capacity linear fit

We used Coil 9 data as an example to evaluate the uncertainty of the evaporator capacity linear fit. This is the uncertainty that would result if someone used this linear fit to calculate capacity at a known evaporator temperature. The data set used to generate the linear fit consisted of 8 tests. A linear equation has two adjustable parameters; therefore, the fit had 6 degrees of freedom (DOF= n-2). Table 7.1.1 summarizes the linear fit parameters (slope and intercept) and related fit statistics.

Correlation Coefficient R ²	DOF Adjusted R ²	Fit Standard Error, W (Btu/h)	F-Value	n = 8 data	•			
0.972835	0.961969	226.28 (772.093)	214.872					
Parameter	Value	Standard Error	t-value	95 % Confidence Mean V Minimum				
B (intercept), W (Btu/h)	20909.6 (71346.5)	1058.35 (3611.22)	19.757	18309.1 (62473.4)	23510.1 (80219.6)			
A (slope), W/ºC (Btu/h ºF)	-574.32 (-1088.7)	39.18 (74.27)	-14.659	-670.56 (-1271.2)	-478.0 (-906.2)			
S _{xx}	108.0774							
Mean T _{evap}	9.2 (48.5)	Mean <i>q</i>	5440 (18562.8)					

Table 7.1.1: Coil 9 evaporator linear fit equation statistics

At a 95 % confidence level, the linear intercept is equal to 20909.6 ± 2600.45 W (71346.5 \pm 8873.1 Btu/h), and the linear slope is equal to -574.32 ± 39.18 W/°C (-1088.7 \pm 182.5 Btu/h °F). The confidence bands are determined by subtracting the minimum 95 % limit from the maximum 95 % limit and dividing by two (or taking the fit standard error and multiplying by the appropriate t-value). With confidence limits as a percentage value, the linear intercept is 20909.6 W (71346.5 Btu/h) \pm 12.4 %, and the linear slope is -574.32 W/°C (-1088.7 Btu/h °F) \pm 16.8 %.

For capacity predictions using the linear correlation, the confidence interval for the mean value at a particular point is given by (Ott 1984):

$$\pm t \cdot \hat{\sigma} \sqrt{\frac{1}{n} + \frac{(x - \overline{x})^2}{S_{xx}}}$$
 7.1.1

where $\hat{\sigma} = \sqrt{\frac{\text{SSE}}{n-2}}$ = fit standard error

$$S_{xx} = \sum (x^2) - \frac{(\sum x)^2}{n}$$

t - two tailed t-value for the appropriate confidence level with DOF = n - 2

 $\hat{\sigma}$ - estimated standard deviation equal to the fit standard error

- \overline{x} mean value of the x-variables or, in this case, the mean value of the evaporating temperatures used to generate the linear fit
- x independent variable or, in this case, the evaporator temperature

At a 95 % confidence level, the t-value for six DOF is 2.447 from a table of the percentage points of the t-distribution (Ott 1984). From Table 7.1.1, the fit standard error was 226.28 W (772.093 Btu/h), and S_{xx} was 33.36 °C² (108.08 °F²). Substituting these values into Equation 7.1.1 yields:

$$\pm 2.447 \cdot 772.093 \sqrt{0.125 + \frac{(x - 48.485)^2}{108.08}}$$
 7.1.2

Knowing the confidence interval for a given confidence level and the predicted value, we can calculate the upper and lower confidence bands for the mean value of the cooling capacity sampled multiple times at a particular value of the evaporator saturation temperature within the range of the evaporator saturation temperature data. Figure 7.1.1 plots the evaporator capacity line, 90 % and 95 % confidence bands, and 5 % offset lines for Coil 9. The figure shows that the 90% and 95% confidence lines are very close to each other; they are within the \pm 5 % offset lines for the majority of the saturation temperature range except the lowest and highest saturation temperatures due to the smaller number of data points associated with the end points of the temperature range.

Once the rater has used the C-B Method (Equation 4.1.2) to determine the evaporating temperature for the condensing unit and the mixed evaporator, the analysis of section 7.1 provides the uncertainty in the mean value of the cooling capacity sampled at that particular evaporator temperature. For Coil 9 and its CD Unit, the evaporating temperature was 6.2 °C (43.2 °F) which produced a cooling capacity, q(95), of 7114 W (24 273 Btu/h) with an uncertainty of ± 341 W (1164 Btu/h) or ± 4.8 % on the mean value at a 95 % confidence level. Subtracting the fan heat, which has a ± 3 % uncertainty, yields the numbers seen in Table 5.1.1 or a rated Q(95) of 6749 W (23 030 Btu/h) ± 341 W (1165 Btu/h) (± 5.1 %) at a 95 % confidence level. Table 7.1.2 summarizes the uncertainty results for the remaining evaporators.

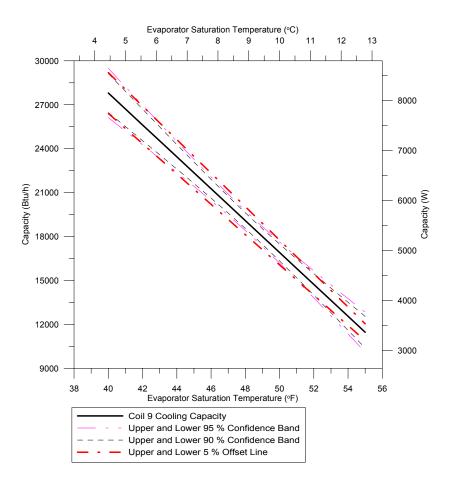


Figure 7.1.1: Coil 9 evaporator cooling capacity, confidence and error bands on the mean predicted value of the cooling capacity sampled at a particular evaporator saturation temperature

			(35) intear in uncertainty	
Coil	<i>T_{evap}</i> ℃ (°F)	Q(95) W (Btu/h)	95 % Confidence Level on the Mean, Uncertainty Q(95)	% Uncertainty
1	8.11 (46.60)	9624 (32839)	541 (1847)	5.6
2	5.84 (42.51)	6344 (21647)	334 (1138)	5.3
3	7.93 (46.27)	9585 (32705)	267 (910)	2.8
4*	9.94 (49.89)	4894 (16700)	127 (434)	2.6
5	9.43 (48.98)	6917 (23601)	192 (655)	2.8
6	6.2 (43.19)	15756 (53761)	939 (3205)	6.0
7	4.5 (40.17)	8340 (28456)	124 (424)	1.5
8	5.9 (42.6)	10878 (37115)	260 (886)	2.4
9	6.2 (43.24)	6749 (23030)	342 (1166)	5.1

Table 7.1.2: Evaporator Q(95) linear fit uncertainty

*Coil 4 airflow was too high and results cannot be compared directly to ARI tests.

7.2: Uncertainty of C-B Method Q(95) and EER

The ARI database, q(95), q(82) and p(82) linear fits of Table 4.1.1, NIST capacity linear fits of Table 3.4.1, Equation 4.1.2, and fan heat were used to calculate the uncertainty in the C-B Method Q(95) and EER.

$$q_{\rm CD} = A_{\rm CD}T_{\rm evap} + B_{\rm CD} = q_{\rm mixed} = A_{\rm mixed}T_{\rm evap} + B_{\rm mixed}$$

$$4.1.1$$

$$T_{evap} = \frac{B_{mixed} - B_{CD}}{A_{CD} - A_{mixed}}$$

$$4.1.2$$

$$p_{\rm CD} = b_{\rm CD} + a_{\rm CD} T_{\rm evap} \tag{4.1.4}$$

Substituting Equation 4.1.2 into Equation 4.1.1 and 4.1.4 yields an expression for the cooling capacity and CD Unit power of the mixed system.

$$q_{CD} = q_{mixed} = A_{CD} \left(\frac{B_{mixed} - B_{CD}}{A_{CD} - A_{mixed}} \right) + B_{CD}$$
 7.2.1

$$p_{\rm CD} = b_{\rm CD} + a_{\rm CD} \left(\frac{B_{\rm mixed} - B_{\rm CD}}{A_{\rm CD} - A_{\rm mixed}} \right)$$
 7.2.2

The fit standard errors for the CD Unit capacity and power linear coefficients are unknown. If we assume the fit standard error for the CD Unit capacity is similar (the same percentage) to that obtained for the evaporator tests, power coefficient uncertainties are 3 %, power and capacity fits have no covariance, and the covariance of the slope and intercept are equal for the CD Unit and evaporator tests, then we may calculate an uncertainty for the mixed system capacity and power.

In general the capacity is a function of the four linear fit coefficients and the power is a function of six linear fit coefficients:

$$q_{CD} = q_{mixed} = f(A_{CD}, B_{CD}, A_{mixed}, B_{mixed})$$
 7.2.3

$$q_{CD} = q_{mixed} = f(a_{CD}, b_{CD}, A_{CD}, B_{CD}, A_{mixed}, B_{mixed})$$
 7.2.4

Since the slope and intercept are not independent in Equations 7.2.1 and 7.2.2, we must include covariance in the form of a correlation coefficient (Coleman and Steele 1989). In general terms this becomes:

$$U_{q}^{2} = \left(\frac{\partial q}{\partial A_{CD}}U_{A_{CD}}\right)^{2} + \left(\frac{\partial q}{\partial B_{CD}}U_{B_{CD}}\right)^{2} + \left(\frac{\partial q}{\partial A_{mixed}}U_{A_{mixed}}\right)^{2} + \left(\frac{\partial q}{\partial B_{mixed}}U_{B_{mixed}}\right)^{2} + 2\left(\frac{\partial q}{\partial A_{CD}}U_{A_{CD}}U_{A_{CD}}U_{B_{CD}}\right)^{2} + 2\left(\frac{\partial q}{\partial A_{mixed}}U_{A_{mixed}}U_{A_{mixed}}U_{A_{mixed}}U_{A_{mixed}}U_{B_{mixed}}\right)^{2} + 2\left(\frac{\partial q}{\partial A_{CD}}U_{A_{CD}}U_{A_{CD}}U_{B_{CD}}\right)^{2} + 2\left(\frac{\partial q}{\partial A_{mixed}}U_{A_{mixed}}U_{A_{mixed}}U_{A_{mixed}}U_{A_{mixed}}U_{B_{mixed}}\right)^{2} + 2\left(\frac{\partial q}{\partial A_{mixed}}U_{A_{mi$$

Here the partial derivatives are taken from Equation 7.2.1 with respect to the various coefficients. A similar procedure is necessary for the CD Unit power equation with the addition of the two extra terms for the power equation linear fit coefficients. The fan power and resulting heat were assumed to have an uncertainty of ± 3 %. The fan heat must be

subtracted from the cooling capacity, and the fan power must be added to the CD Unit power with their variances added to produce the cooling capacity and total power final values and associated uncertainties.

EER is the ratio of Q(82) and P(82).

$$EER = \frac{Q(82)}{P(82)}$$
 1.1

The propagation of the capacity uncertainty and the power uncertainty through Equation 1.1 produces a resulting uncertainty in the EER. We assumed no covariance between capacity and power. The resulting uncertainty in EER is shown below in Table 7.2.1.

Coil	T _{evap} (82)	T _{evap} (95)	Q(95) W (Btu/h)	*% U _{Q(95)}	Q(82) W (Btu/h)	^a % U _{Q(82)}	<i>P</i> (82) W	% U _{P(82)}	EER W/W (Btu/W h)	% U _{EER}
1	7.9 (46.3)	8.1 (46.6)	9624 (32839)	15.3	9763 (33313)	15.7	2895	3.7	3.37 (11.51)	16.1
2	5.0 (41.0)	5.8 (42.5)	6344 (21647)	4.4	6895 (23525)	4.5	2246	9.7	3.07 (10.47)	10.7
3	7.7 (45.9)	7.9 (46.3)	9585 (32705)	8.3	9717 (33155)	8.5	2876	2.8	3.38 (11.53)	9.0
4*	8.9 (48.0)	9.9 (49.9)	4894 (16700)	7.5	5410 (18458)	6.2	1760	3.4	3.07 (10.49)	7.1
5	8.5 (47.3)	9.4 (49.0)	6917 (23601)	8.2	7402 (25258)	7.0	2295	5.8	3.23 (11.01)	9.1
6	5.4 (41.7)	6.2 (43.2)	15756 (53761)	9.0	16593 (56616)	8.1	5041	4.1	3.29 (11.23)	9.1
7	2.5 (36.5)	4.5 (40.2)	8340 (28456)	6.3	9236 (31513)	4.6	3337	2.5	2.77 (9.44)	5.2
8	5.1 (41.1)	5.9 (42.6)	10877 (37115)	5.2	11500 (39238)	5.6	3703	16.9	3.11 (10.60)	17.8
9	5.4 (41.7)	6.2 (43.2)	6749 (23030)	10.8	7253 (24749)	9.3	2307	3.3	3.14 (10.73)	9.9

Table 7.2.1: C-B Method Q(95), Q(82), P(82), and EER uncertainty at the 95 % confidence level on the mean value

^a U: uncertainty

*Coil 4 airflow was too high and results cannot be compared directly to ARI tests.

The uncertainty values may be skewed higher by the assumption of equal percentage uncertainties for the evaporator and CD Unit linear fit capacity coefficients. It is likely that the manufacturers of the CD Units have much larger data sets than those collected in this work; therefore, the uncertainty percentages may be lower than those presented in Table 7.2.1.

8: CONCLUDING REMARKS

This report examines the application of the C-B Method to determine Q(95) and SEER of mixed air conditioners was studied on a sample of eight mixed systems. An independent certification laboratory performed mixed system tests and shipped the mixed evaporators to NIST for testing in NIST's environmental chambers. We implemented the C-B Method for

Q(95) and SEER ratings using condensing unit performance correlations obtained from ARI, the evaporator capacity correlations developed at NIST, and the 99th percentile value of cyclic degradation coefficients identified for the equipment studied. We compared the obtained Q(95) and SEER ratings to the test-obtained values from the certification laboratory (referred to as ARI values).

The C-B Method produced Q(95) results that were within ± 5 % of the ARI tested values for five of eight coils. Among the remaining cases, one Q(95) was overpredicted by 9.4 % and two Q(95) were underpredicted by 13.6 % and 17.6 %. In two of the five cases with ± 5 % agreement, the good Q(95) predictions were obtained as a result of error offsetting between evaporator and condensing unit performance correlations with respect to the system tested capacities, as evidenced by the misprediction of the evaporator saturation temperature by the C-B Method in these two cases.

The Q(82) values from the C-B method were within ± 5 % of the ARI tested values for four of eight coils with six of eight coils being within ± 7 %. Of all the factors contributing to the differences in EER(82), the CD Unit power had the largest effect. Using the CD Unit linear fits for power, the C-B Method predicted EER(82) to within ± 5 % for only two coils. Using the ARI Test values for CD Unit power, the C-B Method predicted EER(82) to within ± 5 % for four of eight coils and within ± 8 % for six of eight coils. Clearly good representations of CD Unit power must be attained to produce consistently correct values of EER(82).

Regarding SEER values, four of eight predictions were within ± 5 % of the ARI tested values, but offsetting of errors played a role in this agreement due to conservative (99th percentile) selection of the cyclic degradation coefficient used by the C-B Method. For the same reason seven of eight SEER predictions were below the test-derived SEERs.

The uncertainty analysis of the C-B Method showed that the 95 % confidence level on the mean predictions averaged 3.8 % for A-Test capacity and 10.4 % for EER. The analysis also showed the importance of careful collection of data; when the evaporator capacity linear fits had a lower standard error, the uncertainty in capacity and EER for a given evaporator temperature was also low.

We demonstrated that EVAP-COND can be used effectively in developing evaporator capacity correlations, which will facilitate the use of the C-B Method.

The C-B Method does not have any inherent features that would produce a bias in predicting Q(95) and EER(82) values. The values obtained in this study for Q(95) and EER(82), under predictions or over predictions, are caused by random deviations between the obtained system test results and evaporator and condensing unit performance correlations.

Predicted values of SEER have strong under predicting tendencies due to the conservative 99^{th} percentile selection of the cyclic degradation coefficient. The category of equipment involved in this study can have a C_D in the range from 0.09 to 0.25, with 0.24 being the 99^{th} percentile value that was used in our SEER calculations. It appears that there is no other way to improve SEER predictions other than providing the matched system C_D value along with condensing unit performance correlations for the application of the C-B Method. It is reasonable to assume that a mixed system would have a C_D very similar to that of the matched system if only the evaporator and indoor fan are the replaced system components.

As compared to the traditional approach for rating mixed systems that is based on the matched system Q(95) and SEER values and adjusting them using coil capacity ratios (or similar scaling parameters), the C-B Method is an inherently more accurate methodology; the selected prediction problems encountered in this study should be studied further to tighten this procedure.

Some of the procedural issues that must be stipulated before a working standard is produced include the following:

- 1) Standard superheats for evaporator curve development with a method to accommodate different superheat for evaporator capacity determination
- 2) Liquid line temperatures for evaporator curve development
- 3) Cyclic degradation coefficients for comparable systems with different expansion devices
- 4) Cyclic degradation coefficient for matched system provided to coil manufacturers, or a method developed to determine a default value
- 5) Procedure for developing CD Unit curves; it should include a method for accommodating different superheats at the evaporator exit

As an alternative to the C-B Method, the traditional method for testing mixed systems could be revisited if the evaporator saturation temperature from the Q(95) matched system test was made available for the mixed system rater. This would facilitate an accurate estimation of the capacity ratio of the mixed and matched coils, which is used as the most influential scaling factor in the traditional rating method. This methodology does not require the matched system C_D since it is included in the matched system SEER, which is available for rating.

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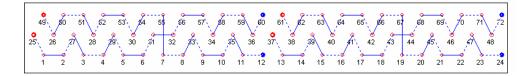
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APPENDIX A: EVAPORATOR COIL DESCRIPTIONS

Appendix A presents design information for the nine mixed evaporators tested at NIST. It includes a picture, design data, and refrigerant circuitry representation in the input format of the EVAP-COND simulation package. General information and name designation for the mixed evaporators is given in Table 2.1.

Coil 1

Data for a section No. of tubes in depth row #1: 24 No. of tubes in depth row #2: 24 No. of tubes in depth row #3: 24 No. of tubes in depth row #4: 0	A01102, Right Side
No. of tubes in depth row #5: 0 Tube data Tube length in 17 Inner diameter in 0.3125 Outer diameter in 0.375 Tube pitch in 1 Depth row pitch in 0.875 Inner surface Smooth I Thermal conductivity Btu/(ft.h.F) 216.671	SI Units British Units Fin data 0.004 Thickness in Pitch in Type Louver Thermal conductivity Btu/(ft.h.F) Volumetric flow rate ft²/min





il Design Data	
Data for a section No. of tubes in depth row #1: 16 No. of tubes in depth row #2: 0 No. of tubes in depth row #3: 0 No. of tubes in depth row #4: 0 No. of tubes in depth row #5: 0 Tube data Tube length in 0 Inner diameter in	3125 Pitch in 0.0416665 375 Type Louver T Thermal conductivity Btu/(ft.h.F) 132.891
Inner surface	Mooth Volumetric flow rate ft²/min 810.001 16.671 Cancel OK

Coil circuitry

o		- Q		o		- O		o		- O		o		- O	
1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	1



Design Data		
5		
Data for a section		A01148 R22 Right Side
No. of tubes in depth row #1: 18	3	
No. of tubes in depth row #2: 1	3	1
No. of tubes in depth row #3:	2	
· · · ·		
No. of tubes in depth row #4: 11	5	Units
No. of tubes in depth row #5: 0		🔲 SI Units 🛛 🔽 British Units
Tube data		🗆 Fin data
Tube length in	17	Thickness in 0.004
	0.3125	Pitch in 0.0625
Inner diameter in		j w
Outer diameter 🔰 in	0.375	Type Louver
Tube pitch in	1	Thermal conductivity Btu/(ft.h.F) 132.891
Depth row pitch	0.875	
Inner surface		Volumetric flow rate ft ^e /min 480.001
	Smooth 🗾	, ,
Thermal conductivity Btu/(ft.h.F) 216.671	Cancel OK
		00,000, 010

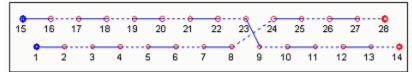
Coil Circuitry (left slab)

	55		56	57		58	59		60	61		62	63		64	65	5	66	67		68	6	9	70		71	;
7	•	- <mark>0</mark> 38		9 39	⇔ 40	41) 	0 42	4	3	∂ 44	$\frac{1}{\lambda}$	5	46	\geq	87	48	~	49	- 0 50		○ 51	52	-	○ 53	;	- 2 54
	19		0 20	21		22	23		- ⊘ 24	25		26	27	~	28	29)	30	31	_	32	:	33	34	_	35	
ľ		2		3	4	5		6		о 7	8		9 9	10		۵ 1	12		13	14		15	16		17		18



Design Data		
Data for a section No. of tubes in depth row No. of tubes in depth row	#2: 14	R22 A01138
No. of tubes in depth row No. of tubes in depth row No. of tubes in depth row	#4: 0	Units 🔽 SI Units 🔽 British Units
Tube data Tube length in Inner diameter in Outer diameter in Tube pitch in Depth row pitch in Inner surface Thermal conductivity Bt	16 0.3125 0.375 1 0.75 Smooth ▼ u/(ft.h.F) 216.671	Fin data in .004 Thickness in 0.0625 Type Louver Thermal conductivity Btu/(ft.h.F) 132.891 Volumetric flow rate ft²/min 395.0

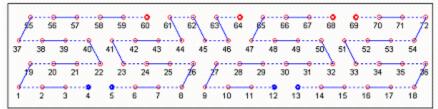
Coil Circuitry (right slab as seen below)





Design Data	
Data for a section No. of tubes in depth row #1: 18 No. of tubes in depth row #2: 18 No. of tubes in depth row #3: 18 No. of tubes in depth row #4: 18 No. of tubes in depth row #5: 0	A01060 Units SI Units ▼ British Units
Tube data Tube length in Inner diameter in Outer diameter in Tube pitch in Depth row pitch in Inner surface Thermal conductivity Btu/(ft.h.F)	17 Fin data 17 Thickness in 0.004 0.3125 Pitch in 0.0588228 0.375 Type Louver 1 1 Thermal conductivity Btu/(ft.h.F) 132.891 0.625 Volumetric flow rate ft²/min 753.0 216.671 Cancel OK

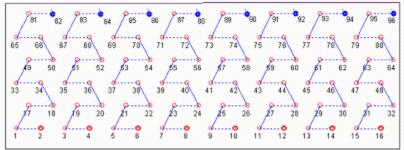
Coil circuitry





Design Data		
Data for a section		B22 A01125
No. of tubes in depth row	#1: 16	RZZ AUTIZS
No. of tubes in depth row	#2: 16	
No. of tubes in depth row	#3: 16	
No. of tubes in depth row	#4: 16	Units
No. of tubes in depth row	#5: 16	🔲 SI Units 🔽 British Units
No. of tubes in depth row	#6: 16	
Tube data		Fin data
Tube length in	29	Thickness in 0.004
Inner diameter in	0.3125	Pitch in 0.0666665
Outer diameter in	0.375	Type Louver 💌
Tube pitch in	1	Thermal conductivity Btu/(ft.h.F) 132.891
Depth row pitch in	0.625	
Inner surface	Smooth	▼ Volumetric flow rate ft [®] /min 575.001
Thermal conductivity Bt	u/(ft.h.F) 216.671	
		Cancel OK

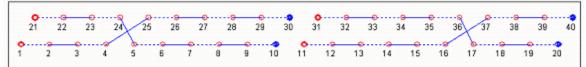
Coil circuitry





Design Data		
Data for a section No. of tubes in depth row #1: 20		R22 H5326
No. of tubes in depth row #2: 20 No. of tubes in depth row #3: 0 No. of tubes in depth row #4: 0 No. of tubes in depth row #5: 0		Units
Tube data Tube length in Inner diameter in Outer diameter in Tube pitch in Depth row pitch in Inner surface Thermal conductivity Btu/(ft.h.F)	16.125 0.3125 0.375 1 0.625 Smooth 216.671	Fin data Thickness in Pitch in Dures Louver Type Louver Thermal conductivity Btu/(ft.h.F) Volumetric flow rate ft*/min Cancel OK

Coil circuitry (left or right slab)





Design Data		
Data for a section		D00 U5001
No. of tubes in depth row #1: 20		R22 H5321
No. of tubes in depth row #2: 20		1
No. of tubes in depth row #3: 20		
No. of tubes in depth row #4: 0		Units
No. of tubes in depth row #5: 0		🗖 SI Units 🔽 British Units
Tube data Tube length in Inner diameter in Outer diameter in Tube pitch in Depth row pitch in Inner surface Thermal conductivity	16 0.3125 0.375 1 0.875 Smooth ▼ 216.671	Fin data 0.004 Thickness in Pitch in Type Louver ▼ Thermal conductivity Btu/(ft.h.F) Volumetric flow rate ft²/min Cancel OK

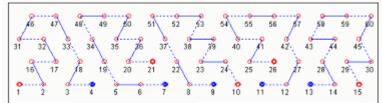
Coil circuitry (left slab)

	4	2	43	44		45	46		47	48		49	50	\ .	51	52	5	53	54		55	56		57	58	5	59	6
	o			o			o			·····			o	¥.		a		-	·····	-0	-	<u></u>		37		-0-		
4	21	22	2	3	24	2	5	26	27	ŗ	28		29	20	3	1	32	33)	34	3	5	36	37		38	39	1
۰.					2.22	0			0						b			0			0			0			o	
	0.00	2	3	4		5	6		7	8		9	10		11	12	1000	3	14		15	16		17	18	100	9	2



Design Data		
Data for a section		R410A, A01154
No. of tubes in depth row #1: 15		H410A, A01134
No. of tubes in depth row #2: 15		,
No. of tubes in depth row #3: 15		
No. of tubes in depth row #4: 15		- Units
No. of tubes in depth row #5: 0		🗖 SI Units 🔽 British Units
Tube data		Fin data
Tube length in	20.5	
Inner diameter in	0.3125	Pitch in 0.071428
Outer diameter in	0.375	Type Louver
Tube pitch in	1	Thermal conductivity Btu/(ft.h.F) 132.891
Depth row pitch	0.875	
Inner surface	Smooth 💌	Volumetric flow rate ft [®] /min 500
Thermal conductivity Btu/(ft.h.F)	216.671	Cancel OK

Coil circuitry





APPENDIX B: UNCERTAINTY ANALYSIS

A. 1 General Remarks

The uncertainty analysis was performed to gain knowledge about the uncertainty of the measured and calculated data. This Appendix presents the major equations used for the uncertainty analysis.

A. 2 Theory

The uncertainty of a quantity *R* calculated from *n* independent measurements x_i is a function of the individual uncertainty of each measurement.

$$R = f(x_1, x_2, x_3, \dots, x_n)$$
(A.1)

When each measurement, x_i , has a given uncertainty, dx_i , the maximum uncertainty of *R* is given by:

$$E_{\rm R} = \left| \frac{\partial f}{\partial x_1} dx_1 \right| + \left| \frac{\partial f}{\partial x_2} dx_2 \right| + \left| \frac{\partial f}{\partial x_3} dx_3 \right| + \dots + \left| \frac{\partial f}{\partial x_n} dx_n \right|.$$
(A.2)

However, using the maximum error to judge the uncertainty of a calculated quantity is not common. Usually the standard deviation (root sum square) is regarded to be a much better approach to a quantity's uncertainty.

$$\boldsymbol{E}_{\mathsf{R}} = \sqrt{\left(\frac{\partial f}{\partial x_1} dx_1\right)^2 + \left(\frac{\partial f}{\partial x_2} dx_2\right)^2 + \left(\frac{\partial f}{\partial x_3} dx_3\right)^2 + \dots + \left(\frac{\partial f}{\partial x_n} dx_n\right)^2}$$
(A.3)

The absolute error calculated with equation (A.3) is often converted to a relative error having the units of percent.

$$e_{\rm R} = \frac{E_{\rm R}}{R} 100 \tag{A.4}$$

A. 3 Temperature Measurements

Most of the temperature measurements performed for these tests were determined by thermocouples. Their voltage signals were measured with the data acquisition system and then converted into a temperature.

The equation used in the test rig's control program to convert the voltage signals into temperatures was a sixth degree polynomial of the form:

$$\mathcal{G} = f(V) = \frac{9}{5}(A + BV + CV^2 + DV^3 + EV^4 + FV^5 + GV^6) + 32$$
(A.5)

where:

$$\vartheta$$
 = temperature (°F)
V = measured voltage (μ V)

If one premises that the uncertainty of the equation itself can be neglected, only one derivation is needed to evaluate the uncertainty in the temperature measurements.

$$\frac{\partial \theta}{\partial V} = \frac{9}{5} \left(B + 2CV + 3DV^2 + 4EV^3 + 5FV^4 + 6GV^5 \right)$$
(A.6)

According to the manufacturer of the voltmeter, the 95 % uncertainty of the voltage measurement (*VM*) was: $E_{VM} = dV(VM) = \pm 0.007$ % of reading + 5 μ V.

The measurement of a temperature (\mathcal{G}) actually is the measurement of the difference to a reference temperature. The data acquisition system provided temperature compensation to 0 °C (32 °F) with a given uncertainty of: $E_{TC} = dTC = \pm 0.2236$ °C = ± 0.4025 °F.

Rewriting equation A.3 for the measurement of the absolute temperature gives:

$$\mathcal{G} = f(V) \tag{A.7}$$

$$\boldsymbol{E}_{\mathrm{T}} = \sqrt{\left(\frac{\partial \mathcal{G}}{\partial V} \mathrm{d} V \boldsymbol{M}\right)^{2} + \left(\mathrm{d} T \boldsymbol{C}\right)^{2}} \tag{A.8}$$

In addition to the common thermocouple measurements, the dew-point temperature in the air duct was measured to evaluate the humidity ratio of the moist air in the duct.

The manufacturer of the dew-point hygrometer specified the 95 % uncertainty in this measurement to be: $E_{T_{dew}} = dT_{dew} = \pm 0.05 \%$ of reading.

A. 4 Temperature Difference Measurements

The evaluation of the uncertainty of a temperature difference $(\Delta \vartheta)$ measurement using a thermopile is slightly more complicated than that for a normal temperature measurement. The uncertainty evaluation is presented using the air duct temperature difference as an example, because this shows the most complicated case. Again there are two independent uncertainties being part of the measurement uncertainty. The first is the uncertainty caused by the voltage signal measurement, discussed in section A.3. The cause for the second uncertainty influencing the measurement of a temperature difference is the nonlinear character of the temperature/voltage function (see equation A.5). The nonlinearity requires temperature at one end of the thermopile used for the temperature difference measurement to be known.

The temperature difference across the indoor coil was calculated using both the voltage signals of the temperature difference measurement (ΔV) and the average voltage signal

 $(V_{av.})$ of the entering temperature measurement of the air duct. The equation used to do so was:

$$\Delta \mathcal{G} = f(V_{\mathsf{av}} + \Delta V) - f(V_{\mathsf{av}})$$
(A.9)

The entering temperature was measured using 25 thermocouples equally distributed over the air duct's cross section. The average of the 25 temperature signals was considered to be the entering temperature. For the uncertainty in this average entering temperature the average voltage measurement uncertainty $E_{VM,av}$ of the 25 measurements was calculated.

$$E_{VM,av.} = dV_{av}(VM) = \sum_{x=1}^{25} \frac{dV_{av.}(VM_x)}{25}$$
(A.10)

All 25 thermocouples were connected to the same temperature compensation. This means the overall uncertainty of the air's average entering temperature voltage signal V_{av} was:

$$dV_{\rm av.} = \sqrt{E_{VM,\rm av.}^{2} + E_{TC}^{2}} = \sqrt{(dV_{\rm av.}(VM))^{2} + (dV_{\rm av.}(TC))^{2}}$$
(A.11)

To evaluate equation A.11 the uncertainty in the temperature compensation must be rewritten to have the unit of μV . Using equation A.5 one finds that an uncertainty of $E_{TC} = dTC = \pm 0.2236^{\circ}C = \pm 0.4025^{\circ}F$ in the temperature compensation to 0 °C (32 °F) is equivalent to a voltage signal uncertainty of $dV_{av.}(TC) = \pm 8.6264 \ \mu V$. As already mentioned, the uncertainty of the voltage signal measurement was given from manufacturer data.

The nonlinearity of the voltage/temperature function (A.5) causes an uncertainty *dslope* in the temperature difference that depends on the uncertainty in the entering temperature voltage signal $V_{av.}$.

$$E_{slope} = dslope = |(\mathscr{G}(V_{av.} + dV) - \mathscr{G}(V_{av.})) - (\mathscr{G}(V_{av.} + dV_{av.} + \Delta V) - \mathscr{G}(V_{av.} + dV_{av.}))|$$
(A.12)

where:

$$V_{av.}$$
 = entering temperature voltage signal (μV)
 $dV_{av.}$ = uncertainty of the entering temperature voltage signal (μV)
 ΔV = temperature difference voltage signal (μV)

Remembering that an additional uncertainty in the temperature difference is caused by the voltage measurement of the temperature difference voltage signal (ΔV), the uncertainty of the air duct temperature difference is given to be:

$$\boldsymbol{E}_{\Delta \mathcal{G}} = \boldsymbol{\mathsf{d}} \Delta \mathcal{G} = \left[\left(\frac{\partial \mathcal{G}}{\partial \boldsymbol{\mathsf{V}}} \boldsymbol{\mathsf{d}} \Delta \boldsymbol{\mathsf{V}} \right)^2 + \boldsymbol{\mathsf{d}} \boldsymbol{s} \boldsymbol{\mathsf{lope}}^2 \right]^{1/2}$$
(A.13)

A. 5 Uncertainty of the Air Side Capacity

The air side capacity of the heat pump was evaluated using the equation:

$$\dot{\mathbf{Q}}_{\mathrm{C}} = \dot{\mathbf{Q}}_{\mathrm{S}} + \dot{\mathbf{Q}}_{\mathrm{L}} \tag{A.14}$$

where:

$$\dot{Q}_{s}$$
 = sensible capacity, kW (*Btu/h*)
 \dot{Q}_{L} = latent capacity, kW (*Btu/h*)

The sensible capacity is the heat needed to cool or heat the moist air passing the heat pump's indoor coil. The latent capacity is the heat rejected by water vapor condensing on the air coil. Condensation does not occur in the heating mode.

The two different capacities were calculated separately and then added (A.14). Therefore the uncertainty of the air-side capacity can be written as:

$$\boldsymbol{E}_{\dot{\boldsymbol{Q}}_{C}} = \left[\left(\frac{\partial \dot{\boldsymbol{Q}}_{C}}{\partial \dot{\boldsymbol{Q}}_{S}} d\dot{\boldsymbol{Q}}_{S} \right)^{2} + \left(\frac{\partial \dot{\boldsymbol{Q}}_{C}}{\partial \dot{\boldsymbol{Q}}_{L}} d\dot{\boldsymbol{Q}}_{L} \right)^{2} \right]^{1/2} = \left(d\dot{\boldsymbol{Q}}_{S}^{2} + d\dot{\boldsymbol{Q}}_{L}^{2} \right)^{1/2}$$
(A.15)

The equations for both the sensible and latent capacities and their uncertainties are presented on the following pages.

A. 5. 1 Uncertainty of the Sensible Capacity

According to ASHRAE Standard 116-1993 the sensible capacity $Q_{\rm S}$ is given by:

$$\dot{Q}_{\rm S} = 3600 C_{\rm D} A_{\rm n} (0.24 + 0.444 W_{\rm av.}) (\vartheta_{\rm l} - \vartheta)_{\rm e} \left[\frac{2g_{\rm C} \Delta p_{\rm n} \rho_{\rm nact}}{144 (1 - \beta^2)} \right]^{1/2}$$
(A.16)

where:

144 = unit conversion factor from
$$in^2$$
 to ft^2
 β = area relation factor (0.250723)

The partial derivatives required for the uncertainty analysis of $\mathcal{Q}_{\rm S}$ are:

$$\frac{\partial \dot{\mathbf{Q}}_{\mathrm{S}}}{\partial \mathsf{A}_{\mathrm{n}}} = 3600 C_{\mathrm{D}} \left(0.24 + 0.444 W_{\mathrm{av.}} \right) \left(\mathcal{G}_{\mathrm{I}} - \mathcal{G}_{\mathrm{e}} \right) \left[\frac{2g_{\mathrm{C}} \Delta p_{\mathrm{n}} \rho_{\mathrm{nact}}}{144 \left(1 - \beta^{2} \right)} \right]^{1/2}$$
(A.17)

$$\frac{\partial \dot{\mathbf{Q}}_{\mathrm{S}}}{\partial W_{\mathrm{e}}} = 1800 C_{\mathrm{D}} A_{\mathrm{n}} 0.444 \left(\beta_{\mathrm{I}} - \beta_{\mathrm{e}} \right) \left[\frac{2g_{\mathrm{C}} \Delta p_{\mathrm{n}} \rho_{\mathrm{nact}}}{144 \left(1 - \beta^{2} \right)} \right]^{1/2}$$
(A.18)

$$\frac{\partial \dot{\mathbf{Q}}_{\mathrm{S}}}{\partial W_{\mathrm{I}}} = 1800 C_{\mathrm{D}} A_{\mathrm{n}} 0.444 \left(\vartheta_{\mathrm{I}} - \vartheta_{\mathrm{e}} \right) \left[\frac{2g_{\mathrm{C}} \Delta p_{\mathrm{n}} \rho_{\mathrm{nact}}}{144 \left(1 - \beta^{2} \right)} \right]^{1/2}$$
(A.19)

$$\frac{\partial \dot{\mathbf{Q}}_{\mathrm{S}}}{\partial (\boldsymbol{\beta}_{\mathrm{I}} - \boldsymbol{\beta}_{\mathrm{e}})} = 3600 C_{\mathrm{D}} A_{\mathrm{n}} (0.24 + 0.444 W_{\mathrm{av.}}) \left[\frac{2g_{\mathrm{C}} \Delta p_{\mathrm{n}} \rho_{\mathrm{nact}}}{144 (1 - \beta^2)} \right]^{1/2}$$
(A.20)

$$\frac{\partial \dot{\mathbf{Q}}_{\mathrm{S}}}{\partial \Delta \boldsymbol{p}_{\mathrm{n}}} = 1800 C_{\mathrm{D}} A_{\mathrm{n}} (0.24 + 0.444 W_{\mathrm{av.}}) (\beta_{\mathrm{I}} - \beta_{\mathrm{e}}) \left[\frac{2g_{\mathrm{C}} \rho_{\mathrm{nact}}}{144 (1 - \beta^{2}) \Delta \boldsymbol{p}_{\mathrm{n}}} \right]^{1/2}$$
(A.21)

$$\frac{\partial \dot{Q}_{\rm S}}{\partial \rho_{\rm nact}} = 1800 C_{\rm D} A_{\rm n} (0.24 + 0.444 W_{\rm av.}) (\vartheta_{\rm l} - \vartheta_{\rm e}) \left[\frac{2g_{\rm C} \Delta p_{\rm n}}{144 (1 - \beta^2) \rho_{\rm nact}} \right]^{1/2}$$
(A.22)

$$\frac{\partial \dot{\mathbf{Q}}_{\mathrm{S}}}{\partial \beta} = 3600 C_{\mathrm{D}} A_{\mathrm{n}} (0.24 + 0.444 W_{\mathrm{av.}}) (\beta_{\mathrm{I}} - \beta_{\mathrm{e}}) \beta \left[\frac{2g_{\mathrm{C}} \Delta p_{\mathrm{n}} \rho_{\mathrm{nact}}}{144 (1 - \beta^{2})^{3}} \right]^{1/2}$$
(A.23)

Using the above partial derivatives for rewriting equation A.3 gives:

$$E_{Q_{S}} = \left[\left(\frac{\partial \dot{Q}_{S}}{\partial A_{n}} dA_{n} \right)^{2} + \left(\frac{\partial \dot{Q}_{S}}{\partial W_{e}} dW_{e} \right)^{2} + \left(\frac{\partial \dot{Q}_{S}}{\partial W_{l}} dW_{l} \right)^{2} + \left(\frac{\partial \dot{Q}_{S}}{\partial \Delta \rho_{n}} d\Delta \rho_{n} \right)^{2} + \left(\frac{\partial \dot{Q}_{S}}{\partial (\beta_{l} - \beta_{e})} d(\beta_{l} - \beta_{e}) \right)^{2} + \left(\frac{\partial \dot{Q}_{S}}{\partial \rho_{nact}} d\rho_{nact} \right)^{2} + \left(\frac{\partial \dot{Q}_{S}}{\partial \beta} d\beta \right)^{1/2}$$
(A.24)

Equation A.24 can be evaluated to give the uncertainty of $\dot{Q}_{\rm s}$ if each of the individual uncertainties is known. However, *A*, β , *W*_e, *W*_l and $\rho_{\rm nact}$ are calculated quantities, so their uncertainties were not known, but had to be calculated using equation A.3.

The flow in the air duct was measured using a venturi tube measurement. The nozzle throat area A_n , which is part of equation A.16, was calculated from the throat diameter. Thus its uncertainty can be evaluated very easily.

$$A_{\rm n} = \frac{\pi d_{\rm n}^2}{4} \tag{A.25}$$

$$\boldsymbol{E}_{A_{n}} = \frac{\partial A_{n}}{\partial d_{n}} \mathrm{d}d_{n} = \frac{\pi d_{n}}{2} \mathrm{d}d_{n}$$
(A.26)

The uncertainty of the throat diameter was given to be: $E_{dn} = dd_n = \pm 0.254$ mm = ± 0.01 in.

The area ratio factor β was calculated using the equation:

$$\beta = \frac{A_{\rm n}}{A_{\rm en}} = \frac{d_{\rm n}^{2}}{d_{\rm en}^{2}}$$
(A.27)

Again, both areas were calculated using their diameter given by the manufacturer of the venturi tube. The partial derivatives used to evaluate the uncertainty in β were:

$$\frac{\partial \beta}{\partial d_{\rm n}} = 2 \frac{d_{\rm n}}{d_{\rm en}^2} \tag{A.28}$$

$$\frac{\partial \beta}{\partial d_{\rm en}} = -2 \frac{d_{\rm n}^2}{d_{\rm en}^3} \tag{A.29}$$

Using these derivatives to rewrite A.3 gives:

$$\boldsymbol{E}_{\beta} = \left[\left(2 \left(\frac{\boldsymbol{d}_{n}}{\boldsymbol{d}_{en}^{2}} \right) d\boldsymbol{d}_{n} \right)^{2} + \left(-2 \left(\frac{\boldsymbol{d}_{n}^{2}}{\boldsymbol{d}_{en}^{3}} \right) d\boldsymbol{d}_{en} \right)^{2} \right]^{1/2}$$
(A.30)

The required uncertainty in the inlet diameter was also $E_{d_{en}} = dd_{en} = \pm 0.254 \text{ mm} = \pm 0.01 \text{ in}$.

The humidity ratios W_e and W_l are a function of the water vapor pressure p_w and the atmospheric pressure *p*.

$$W = 0.62198 \frac{p_{\rm w}}{p - p_{\rm w}}$$
 (A.31)

The factor 0.62198 comes from the ratio of the mole weights of the two components, water and air.

The required partial derivatives of equation A.31 are:

$$\frac{\partial W}{\partial p} = 0.62198 \frac{p_{\rm w}}{\left(p - p_{\rm w}\right)^2} \tag{A.32}$$

$$\frac{\partial W}{\partial p_{w}} = 0.62198 \frac{p}{\left(p - p_{w}\right)^{2}}$$
(A.33)

They lead to the uncertainty in *W*:

$$\boldsymbol{E}_{W} = \boldsymbol{d}W = \left[\left(\frac{\partial W}{\partial \boldsymbol{p}} d\boldsymbol{p} \right)^{2} + \left(\frac{\partial W}{\partial \boldsymbol{p}_{w}} d\boldsymbol{p}_{w} \right)^{2} \right]^{1/2}$$
(A.34)

Unfortunately the water saturation pressure is a calculated quantity itself, which means its uncertainty had to be calculated.

The equation that was used to calculate the saturation pressure from the dew-point temperature, T_{dew} , (°R), is given below. The equation was assumed to cause no additional uncertainties.

$$p_{\rm w} = EXP\left[\frac{C_8}{T_{\rm dew}} + C_9 + C_{10}T_{\rm dew} + C_{11}T_{\rm dew}^2 + C_{12}T_{\rm dew}^3 + C_{13}\ln T_{\rm dew}\right]$$
(A.35)

The partial derivative of equation A.35 with respect to T_{dew} is:

$$\frac{\partial p_{w}}{\partial T_{dew}} = \left[\frac{-C_{8}}{T_{dew}^{2}} + C_{10} + 2C_{11}T_{dew} + 3C_{12}T_{dew}^{2} + \frac{C_{13}}{T_{dew}}\right]p_{w}$$
(A.36)

The uncertainty in $p_{\rm W}$ is now given by:

$$E_{\rho_{w}} = d\rho_{w} = \frac{\partial \rho_{w}}{\partial T_{dew}} dT_{dew}$$
(A.37)

As already mentioned in section A.3, the uncertainty of the dew-point temperature measurement was given to be: $E_{T_{dew}}=dT_{dew}=\pm\,0.05$ % of reading .

Finally, the uncertainty in the moist air's density ρ_{nact} had to be evaluated. The density was calculated using the ideal gas equation and the humidity ratio.

$$\rho_{\text{nact}} = \frac{p_{\text{n}} 144(1+W)}{R_{\text{a}} T_{\text{n}} (1+1.6078W)}$$
(A.38)

The factor 1.6078 is the ratio of the molar weights of air and water.

The partial derivatives of the A.38 are:

$$\frac{\partial \rho_{\text{nact}}}{\partial p_{\text{n}}} = \frac{144(1+W)}{RT_{\text{n}}(1+1.6078W)}$$
(A.39)

$$\frac{\partial \rho_{\text{nact}}}{\partial T_{\text{n}}} = \frac{-p_{\text{n}} 144(1+W)}{R T_{\text{n}}^{2} (1+1.6078W)}$$
(A.40)

$$\frac{\partial \rho_{\text{nact}}}{\partial W} = \frac{-0.6078 \, \rho_{\text{n}} \, 144}{R T_{\text{n}} \left(1 + 1.6078 W\right)^2} \tag{A.41}$$

Rewriting equation A.3 with the above partial derivatives gives:

$$\boldsymbol{E}_{\rho_{\text{nact}}} = \left[\left(\frac{\partial \rho_{\text{nact}}}{\partial \boldsymbol{p}_{\text{n}}} d\boldsymbol{p}_{\text{n}} \right)^{2} + \left(\frac{\partial \rho_{\text{nact}}}{\partial \boldsymbol{T}_{\text{n}}} d\boldsymbol{T}_{\text{n}} \right)^{2} + \left(\frac{\partial \rho_{\text{nact}}}{\partial \boldsymbol{W}} d\boldsymbol{W} \right)^{2} \right]$$
(A.42)

The pressure p_n in the nozzle throat was calculated as the difference of atmospheric pressure and nozzle pressure drop. The uncertainty of the nozzle pressure can be derived as follows:

$$\boldsymbol{p}_{n} = \boldsymbol{p}_{atm} - \Delta \boldsymbol{p} \tag{A.43}$$

$$E_{p_{n}} = dp_{n} = \left[(dp_{atm})^{2} + (d\Delta p)^{2} \right]^{1/2}$$
(A.44)

The uncertainties of the pressure measurements were given from manufacturer data: $E_{p_{atm}} = dp_{atm} = \pm 0.3429 \text{mmHg} = \pm 0.0135 \text{ in Hg}$ and $E_{Dp_n} = dDp_n = \pm 2.489 \text{ mmH}_2O = \pm 0.098 \text{ in H}_2O$.

A. 5. 2 Uncertainty of the Latent Capacity

The latent cooling capacity (ASHRAE Standard 116-1983) is given by:

$$\dot{Q}_{L} = 6360060C_{D}A_{n}(W_{e} - W_{I})\left[\frac{2g_{C}\Delta p_{n}\rho_{nact}}{144(1-\beta^{2})}\right]^{1/2}$$
(A.44)

where:

$$\rho_{nact} = density of the moist air (lb / ft3)$$
144 = unit conversion factor from in² to ft²
 β = area relation factor (0.250723)

The partial derivatives of this equation are:

$$\frac{\partial \dot{\mathbf{Q}}_{\mathrm{L}}}{\partial A_{\mathrm{n}}} = 6360060 C_{\mathrm{D}} \left(W_{\mathrm{e}} - W \right)_{\mathrm{I}} \left[\frac{2g_{\mathrm{C}} \Delta p_{\mathrm{n}} \rho_{\mathrm{nact}}}{144 \left(1 - \beta^{2} \right)} \right]^{1/2}$$
(A.45)

$$\frac{\partial \dot{Q}_{L}}{\partial W_{e}} = 6360060 C_{D} A_{n} \left[\frac{2g_{C} \Delta p_{n} \rho_{nact}}{144 \left(1 - \beta^{2}\right)} \right]^{1/2}$$
(A.46)

$$\frac{\partial \dot{Q}_{\rm L}}{\partial W_{\rm I}} = -6360060C_{\rm D}A_{\rm n} \left[\frac{2g_{\rm C}\Delta p_{\rm n}\rho_{\rm nact}}{144(1-\beta^2)}\right]^{1/2}$$
(A.47)

$$\frac{\partial \dot{\mathbf{Q}}_{\mathrm{L}}}{\partial \Delta \boldsymbol{p}_{\mathrm{n}}} = 3180060 C_{\mathrm{D}} A_{\mathrm{n}} (W_{\mathrm{e}} - W_{\mathrm{I}}) \left[\frac{2g_{\mathrm{C}} \rho_{\mathrm{nact}}}{144(1 - \beta^{2}) \Delta \boldsymbol{p}_{\mathrm{n}}} \right]^{1/2}$$
(A.48)

$$\frac{\partial \dot{\mathbf{Q}}_{\mathrm{L}}}{\partial \rho_{\mathrm{nact}}} = 3180060 C_{\mathrm{D}} A_{\mathrm{n}} (W_{\mathrm{e}} - W)_{\mathrm{I}} \left[\frac{2g_{\mathrm{C}} \Delta p_{\mathrm{n}}}{144(1 - \beta^2)\rho_{\mathrm{nact}}} \right]^{1/2}$$
(A.49)

$$\frac{\partial \dot{\mathbf{Q}}_{\mathrm{L}}}{\partial \beta} = 6360060 C_{\mathrm{D}} A_{\mathrm{n}} (W_{\mathrm{e}} - W_{\mathrm{I}}) \beta \left[\frac{2g_{\mathrm{C}} \Delta p_{\mathrm{n}} \rho_{\mathrm{nact}}}{144 (1 - \beta^2)^3} \right]^{1/2}$$
(A.50)

If the above derivatives are used to rewrite equation A.3, one obtains the uncertainty of the latent capacity:

$$E_{Q_{L}} = \left[\left(\frac{\partial \dot{Q}_{L}}{\partial A_{n}} dA_{n} \right)^{2} + \left(\frac{\partial \dot{Q}_{L}}{\partial W_{e}} dW_{e} \right)^{2} + \left(\frac{\partial \dot{Q}_{L}}{\partial W_{l}} dW_{l} \right)^{2} + \left(\frac{\partial \dot{Q}_{L}}{\partial A_{n}} d\Delta p_{n} \right)^{2} + \left(\frac{\partial \dot{Q}_{L}}{\partial \Delta p_{n}} d\rho_{nact} \right)^{2} + \left(\frac{\partial \dot{Q}_{L}}{\partial \beta} d\beta \right)^{2} \right]^{1/2}$$
(A.51)

In this equation, all the needed uncertainties are known. Either because the quantities are directly measured or their uncertainties have already been calculated in Appendix A.4.1.

The final step was calculating the uncertainty of the air side capacity by using the now known uncertainties of sensible and latent capacity in equation A.15.

APPENDIX C: COOLING MEASUREMENT SUMMARY SHEETS

Coil 1 R22, A01102, No Fan

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a031216a.dat SUMMARY FILENAME: a031216a.sum Range Range Total Air-Side Capacity: 35172.37 1870.22 Air-Side Conditions

 Indoor Dry-Bulb : 79.847
 0.35
 Sensible Cap (Btu/h): 27501.92
 541.05

 Indoor Inlet Dew (F): 60.414
 0.55
 Latent Cap (Btu/h): 7670.45
 1669.75

 Indoor Exit Dry-Bulb: 57.177
 0.59
 EvapAir Delta T (F): 24.64
 0.44

 Indoor Exit Dew (F): 56.227 0.95 Air/Ref Cap Prcnt Diff: 3.16 7.82 Sensible Heat Ratio: 0.782 0.0357 SCFM per Ton: 345.94 Indoor Airflow (CFM): 995.24 7.59 Indoor Airflow (SCFM): 1013.97 7.68 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011194 Evap Exit Humidity Ratio (16H2O/1bAir): 0.009608 Parametric Pressure (in HG): 29.96 Nozzle Temp (F): 56.87 0.55 Air Chamber Nozzle Pressure Drop (in Water): 1.332 0.020 Evaporator Coil Air Pressure Drop (in Water): 0.200 0.007 _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 258.17 Upstream Temp (F): 106.25 Ref-side Cap (Btu/h) : 36280.23 2439.34 3.898 0.476 Ref-side Cap (tons): 3.02 0.20 Refrigerant Mdot (lbm/h): 575.01 39.17 Coriolis Density (lbm/ft3): 82.26 0.77 Upstream R22 Tsat (F): 115.23 1.159 Average Subcooling (F): 8.98 1.231 1.213 4.189 Evap Exit Pressure (psia): 94.11 Evap Exit Avg Temp : 57.64 Exit Superheat (F): 10.52 3.862 Evap Exit Tsat (F): 47.13 0.761

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a031218a.dat SUMMARY FILENAME: a031218a.sum Range Air-Side Conditions Range Total Air-Side Capacity: 38226.98 1139.85 735.90 Indoor Dry-Bulb : 80.193 0.40 Sensible Cap (Btu/h): 29108.93 Indoor Inlet Dew (F): 60.613 0.63 Indoor Exit Dry-Bulb: 55.959 1.09 Latent Cap (Btu/h): 9118.05 EvapAir Delta T (F): 26.11 921.08 0.66 Indoor Exit Dew (F): 55.653 0.55 Air/Ref Cap Pront Diff: 4.70 2.57 Sensible Heat Ratio: 0.761 SCFM per Ton: 317.85 0.0210 Indoor Airflow (CFM): 1001.86 17.80 Indoor Airflow (SCFM): 1012.53 17.34 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011395 Wap Infect Humidity Ratio (15H20/15H17):0.009507Evap Exit Humidity Ratio (15H20/15Air):0.009507Barometric Pressure (in HG):29.65Nozzle Temp (F):55.660.92 Air Chamber Nozzle Pressure Drop (in Water): 1.339 0.046 Evaporator Coil Air Pressure Drop (in Water): 0.211 0.006 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 269.72 2.680 Upstream Temp (F): 104.33 0.781 Ref-side Cap (Btu/h) : 40021.38 1132.54 0.09 Ref-side Cap (tons): 3.34 Refrigerant Mdot (lbm/h): 628.23 17.22 Coriolis Density (lbm/ft3): 81.73 0.52 Upstream R22 Tsat (F): 118.61 0.771 Average Subcooling (F): 14.27 0.991 1.456 2.244 Evap Exit Pressure (psia): 91.05 Evap Exit Avg Temp : 56.59 Exit Superheat (F): 11.41 1.933 Evap Exit Tsat (F): 45.18 0.937

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a031218b.dat SUMMARY FILENAME: a031218b.sum Range Range Total Air-Side Capacity: 28751.99 1236.15 Air-Side Conditions Indoor Dry-Bulb : 80.040 0.64 Sensible Cap (Btu/h): 23904.52 675.89 Indoor Inlet Dew (F): 60.201 0.85 Indoor Exit Dry-Bulb: 60.446 0.55 Latent Cap (Btu/h): 4847.46 1439.20 EvapAir Delta T (F): 21.55 0.65 Indoor Exit Dew (F): 57.614 0.40 Air/Ref Cap Pront Diff: 1.70 10.06 Sensible Heat Ratio: 0.831 SCFM per Ton: 420.26 0.0432 Indoor Airflow (CFM): 1004.88 19.23 Indoor Airflow (SCFM): 1006.94 18.75 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011227 Evap Exit Humidity Ratio (lbH20/lbAir): 0.010217 Barometric Pressure (in HG): 29.65 Nozzle Temp (F): 59.90 0.78 Air Chamber Nozzle Pressure Drop (in Water): 1.336 0.050 0.006 Evaporator Coil Air Pressure Drop (in Water): 0.186 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 263.16 3.898 Upstream Temp (F): 106.15 0.476 Ref-side Cap (Btu/h) : 29238.19 2647.34 Ref-side Cap (tons): 2.44 0.22 Refrigerant Mdot (lbm/h): 463.18 41.95 Coriolis Density (lbm/ft3): 82.34 0.44 Upstream R22 Tsat (F): 116.70 1.142 Average Subcooling (F): 10.55 1.129 1.092 Evap Exit Pressure (psia): 97.30 Evap Exit Avg Temp : 60.43 4.243 Exit Superheat (F): 11.32 4.689 Evap Exit Tsat (F): 49.11 0.668

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040105a.dat SUMMARY FILENAME: a040105a.sum Range Air-Side Conditions Range Total Air-Side Capacity: 42951.53 1660.25 Indoor Dry-Bulb : 80.221 0.58 Sensible Cap (Btu/h): 31907.84 1084.17 Indoor Inlet Dew (F): 60.321 0.90 Latent Cap (Btu/h): 11043.69 1769.65 Indoor Exit Dry-Bulb: 53.609 0.78 EvapAir Delta T (F): 28.59 0.88 Indoor Exit Dew (F): 54.113 0.58 Air/Ref Cap Pront Diff: 4.12 6.78 Sensible Heat Ratio: 0.743 SCFM per Ton: 283.38 0.0319 Indoor Airflow (CFM): 994.75 11.31 Indoor Airflow (SCFM): 1014.32 11.62 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011218 Evap Exit Humidity Ratio (lbH2O/lbAir): 0.008935 Barometric Pressure (in HG): 29.80 Nozzle Temp (F): 53.84 1.11 Air Chamber Nozzle Pressure Drop (in Water): 1.332 0.030 Evaporator Coil Air Pressure Drop (in Water): 0.233 0.010 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 247.77 Upstream Temp (F): 103.08 3.289 0.651 Ref-side Cap (Btu/h) : 44718.18 2028.31 Ref-side Cap (tons): 3.73 Refrigerant Mdot (lbm/h): 697.60 0.17 32.61 Coriolis Density (lbm/ft3): 81.39 0.58 Upstream R22 Tsat (F): 112.09 1.010 9.01 Average Subcooling (F): 1.335 1.334 4.586 Evap Exit Pressure (psia): 82.17 Evap Exit Avg Temp : 55.72 Exit Superheat (F): 16.47 4.310 Evap Exit Tsat (F): 39.25 0.928

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040106a.dat SUMMARY FILENAME: a040106a.sum Range Range Total Air-Side Capacity: 29066.22 1028.82 Air-Side Conditions Indoor Dry-Bulb : 80.127 0.53 Sensible Cap (Btu/h): 23807.89 1479.10 Indoor Inlet Dew (F): 60.3911.19Latent Cap (Btu/h): 5258.331463.71Indoor Exit Dry-Bulb: 60.6180.78EvapAir Delta T (F): 21.401.30 Indoor Exit Dew (F): 57.586 0.55 Air/Ref Cap Pront Diff: -0.33 7.26 Sensible Heat Ratio: 0.819 SCFM per Ton: 417.11 0.0450 Indoor Airflow (CFM): 1003.02 11.71 Indoor Airflow (SCFM): 1010.32 11.26 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011239 Wap Infect Humidity Ratio (15H20/15Air):0.010148Evap Exit Humidity Ratio (15H20/15Air):0.010148Barometric Pressure (in HG):29.82Nozzle Temp (F):60.170.69 Air Chamber Nozzle Pressure Drop (in Water): 1.337 0.030 0.006 Evaporator Coil Air Pressure Drop (in Water): 0.205 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 277.93 Upstream Temp (F): 106.41 2.680 1.016 Ref-side Cap (Btu/h) : 28969.38 2550.83 Ref-side Cap (tons): 2.41 Refrigerant Mdot (lbm/h): 459.52 0.21 39.02 Coriolis Density (lbm/ft3): 82.58 0.25 Upstream R22 Tsat (F): 120.95 0.754 Average Subcooling (F): 14.53 1.221 1.092 Evap Exit Pressure (psia): 97.68 Evap Exit Avg Temp : 60.34 6.253 Exit Superheat (F): 11.01 5.661 Evap Exit Tsat (F): 49.33 0.666

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040106b.dat SUMMARY FILENAME: a040106b.sum Range Air-Side Conditions Range Total Air-Side Capacity: 43160.68 1322.97 Indoor Dry-Bulb : 80.200 0.56 Sensible Cap (Btu/h): 31693.62 1212.47 Indoor Inlet Dew (F): 60.615 0.79 Latent Cap (Btu/h): 11467.06 1103.23 0.82 EvapAir Delta T (F): 28.28 Indoor Exit Dry-Bulb: 53.835 0 88 Indoor Exit Dew (F): 54.234 0.88 Air/Ref Cap Pront Diff: 3.83 7.30 Sensible Heat Ratio: 0.734 SCFM per Ton: 283.18 0.0240 Indoor Airflow (CFM): 998.32 8.90 Indoor Airflow (SCFM): 1018.50 9.47 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011330 Evap Exit Humidity Ratio (lbH2O/lbAir): 0.008969 Barometric Pressure (in HG): 29.82 Nozzle Temp (F): 53.90 0.79 Air Chamber Nozzle Pressure Drop (in Water): 1.342 0.024 Evaporator Coil Air Pressure Drop (in Water): 0.227 0.006 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 256.74 6.334 Upstream Temp (F): 105.66 1.212 Ref-side Cap (Btu/h) : 44811.32 2412.50 Ref-side Cap (tons): 3.73 Refrigerant Mdot (lbm/h): 708.12 0.20 37.74 Coriolis Density (lbm/ft3): 82.23 0.65 Upstream R22 Tsat (F): 114.80 1.885 1.941 Average Subcooling (F): 9.14 1.698 6.429 Evap Exit Pressure (psia): 83.48 55.55 Evap Exit Avg Temp : Exit Superheat (F): 15.39 6.523 Evap Exit Tsat (F): 40.16 1.166

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040106c.dat SUMMARY FILENAME: a040106c.sum Range Range Total Air-Side Capacity: 37684.76 2294.76 Air-Side Conditions Indoor Dry-Bulb : 80.306 0.53 Sensible Cap (Btu/h): 29012.99 1198.92 Latent Cap (Btu/h): 8671.77 1663.84 EvapAir Delta T (F): 25.92 0.88 Indoor Inlet Dew (F): 60.153 1.06 Indoor Exit Dry-Bulb: 56.339 0.90 Indoor Exit Dew (F): 55.373 0.66 Air/Ref Cap Pront Diff: 1.68 6.76 Sensible Heat Ratio: 0.770 SCFM per Ton: 323.93 0.0305 Indoor Airflow (CFM): 1001.35 10.45 Indoor Airflow (SCFM): 1017.26 9.57 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011142 Evap Exit Humidity Ratio (lbH2O/lbAir): 0.009355 Barometric Pressure (in HG): 29.82 Nozzle Temp (F): 55.99 0.88 Air Chamber Nozzle Pressure Drop (in Water): 1.344 0.027 Evaporator Coil Air Pressure Drop (in Water): 0.217 0.005 _____ _____ _____ Refrigerant Side Conditions Expansion Valve 2.680 1.061 Upstream Pressure (psia): 261.11 Upstream Temp (F): 105.03 Ref-side Cap (Btu/h) : 38311.76 1857.38 Ref-side Cap (tons): 3.19 0.15 Refrigerant Mdot (lbm/h): 603.49 30.41 Coriolis Density (lbm/ft3): 82.11 0.52 Upstream R22 Tsat (F): 116.10 0.790 Average Subcooling (F): 11.07 0.938 1.456 3.112 Evap Exit Pressure (psia): 89.86 Evap Exit Avg Temp : 57.73 Exit Superheat (F): 13.31 2.874 Evap Exit Tsat (F): 44.42 0.945

Coil 2 R22, A01070, No Fan

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040116a.dat SUMMARY FILENAME: a040116a.sum Range Air-Side Conditions Range Total Air-Side Capacity: 20154.12 719.94 Indoor Dry-Bulb : 79.789 0.60 Sensible Cap (Btu/h): 17010.06 488.46
 Indoor Inlet Dew (F): 60.417
 0.50
 Latent Cap (Btu/h): 3144.06

 Indoor Exit Dry-Bulb: 62.508
 0.74
 EvapAir Delta T (F): 19.09
 761.03 0.44 Indoor Airflow (CFM): 809.55 6.98 SCFM per Ton: 481.49 Indoor Airflow (SCFM): 808.66 7.38 (0.075 lb/f+3 c+c-1) 3.74 0.0335 (0.075 lb/ft3 standard air) Air Chamber Nozzle Pressure Drop (in Water): 0.866 0.015 Evaporator Coil Air Pressure Drop (in Water): 0.075 0.005 Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 262.38 1.340 Upstream Temp (F): 103.41 0.677 Ref-side Cap (Btu/h) : 20429.82 535.58 Ref-side Cap (tons): 1.70 0.04 Refrigerant Mdot (lbm/h): 319.23 9.16 Coriolis Density (lbm/ft3): 81.95 0.16 Upstream R22 Tsat (F): 116.47 0.394 Average Subcooling (F): 13.06 0.505 Evap Exit Pressure (psia): 90.62 0.485 Evap Exit Avg Temp : 59.63 1.905 Exit Superheat (F): 14.72 2.148 Evap Exit Tsat (F): 44.91 0.313

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040116a.dat SUMMARY FILENAME: a040116a.sum Range Range Total Air-Side Capacity: 20154.12 Air-Side Conditions 719.94 Indoor Dry-Bulb : 79.789 0.60 Sensible Cap (Btu/h): 17010.06 488.46 Latent Cap (Btu/h): 3144.06 EvapAir Delta T (F): 19.09 Indoor Inlet Dew (F): 60.417 0.50 761.03 Indoor Exit Dry-Bulb: 62.508 0.74 0.44 Indoor Exit Dew (F): 58.360 0.40 Air/Ref Cap Pront Diff: 1.37 3.74 Sensible Heat Ratio: 0.844 SCFM per Ton: 481.49 0.0335 Indoor Airflow (CFM): 809.55 6.98 Indoor Airflow (SCFM): 808.66 7.38 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011315 Wap Infect Humidity Ratio (15H20/15H17):0.010499Evap Exit Humidity Ratio (15H20/15Air):0.010499Barometric Pressure (in HG):29.65Nozzle Temp (F):61.600.91 Air Chamber Nozzle Pressure Drop (in Water): 0.866 0.015 Evaporator Coil Air Pressure Drop (in Water): 0.075 0.005 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 262.38 1.340 Upstream Temp (F): 103.41 0.677 Ref-side Cap (Btu/h) : 20429.82 535.58 Ref-side Cap (tons): 1.70 Refrigerant Mdot (lbm/h): 319.23 0.04 9.16 Coriolis Density (lbm/ft3): 81.95 0.16 Upstream R22 Tsat (F): 116.47 0.394 Average Subcooling (F): 13.06 0.505 0.485 1.905 Evap Exit Pressure (psia): 90.62 Evap Exit Avg Temp : 59.63 Exit Superheat (F): 14.72 2.148 Evap Exit Tsat (F): 44.91 0.313

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040116b.dat SUMMARY FILENAME: a040116b.sum Range Range Total Air-Side Capacity: 12918.77 Air-Side Conditions 789.67 Indoor Dry-Bulb : 79.796 0.56 Sensible Cap (Btu/h): 12648.04 554.30 0.84 Latent Cap (Btu/h): 270.73 0.86 EvapAir Delta T (F): 14.26 Indoor Inlet Dew (F): 60.435 Latent Cap (Btu/h): 270.73 1125.53 Indoor Exit Dry-Bulb: 67.321 0.65 Indoor Exit Dew (F): 60.263 0.66 Air/Ref Cap Pront Diff: 1.07 6.01 Sensible Heat Ratio: 0.979 SCFM per Ton: 747.34 0.0856 Indoor Airflow (CFM): 813.14 9.68 Indoor Airflow (SCFM): 804.56 9.01 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011322 Evap Exit Humidity Ratio (lbH2O/lbAir): 0.011251 Barometric Pressure (in HG): 29.65 Nozzle Temp (F): 66.36 1.64 Air Chamber Nozzle Pressure Drop (in Water): 0.866 0.020 0.005 Evaporator Coil Air Pressure Drop (in Water): 0.066 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 264.15 Upstream Temp (F): 104.96 0.731 0.542 Ref-side Cap (Btu/h) : 13054.22 511.78 Ref-side Cap (tons): 1.09 Refrigerant Mdot (lbm/h): 205.56 0.04 8.43 Coriolis Density (lbm/ft3): 82.60 0.32 Upstream R22 Tsat (F): 116.99 0.214 Average Subcooling (F): 12.03 0.614 1.092 1.224 Evap Exit Pressure (psia): 97.48 Evap Exit Avg Temp : 65.53 Exit Superheat (F): 16.32 1.741 Evap Exit Tsat (F): 49.21 0.666

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040119a.dat SUMMARY FILENAME: a040119a.sum Range Air-Side Conditions Range Total Air-Side Capacity: 24917.81 718.96 Indoor Dry-Bulb : 79.836 0.39 Sensible Cap (Btu/h): 19597.48 514.71 Indoor Exit Dry-Bulb: 59.747 0.72 Indoor Exit Dry-Bulb: 59.747 0.72 Latent Cap (Btu/h): 5320.33 EvapAir Delta T (F): 21.91 650.76 0.44 Indoor Exit Dew (F): 56.767 0.50 Air/Ref Cap Pront Diff: 2.24 3.20 Sensible Heat Ratio: 0.787 SCFM per Ton: 391.26 0.0238 Indoor Airflow (CFM): 808.89 8.66 Indoor Airflow (SCFM): 812.44 8.25 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011277 Wap Infect Humidity Ratio (15H20/15H17):0.009905Evap Exit Humidity Ratio (15H20/15Air):0.009905Barometric Pressure (in HG):29.65Nozzle Temp (F):58.930.65 Air Chamber Nozzle Pressure Drop (in Water): 0.869 0.018 Evaporator Coil Air Pressure Drop (in Water): 0.078 0.006 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 267.30 Upstream Temp (F): 105.31 0.974 0.610 Ref-side Cap (Btu/h) : 25473.46 406.33 0.03 Ref-side Cap (tons): 2.12 Refrigerant Mdot (lbm/h): 401.83 6.23 Coriolis Density (lbm/ft3): 82.41 0.36 Upstream R22 Tsat (F): 117.91 0.282 Average Subcooling (F): 12.60 0.661 0.485 2.180 Evap Exit Pressure (psia): 83.58 Evap Exit Avg Temp : 54.97 Exit Superheat (F): 14.74 2.108 Evap Exit Tsat (F): 40.22 0.333

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040119b.dat SUMMARY FILENAME: a040119b.sum Range Range Total Air-Side Capacity: 20189.62 1211.57 Air-Side Conditions Indoor Dry-Bulb : 79.724 0.56 Sensible Cap (Btu/h): 16949.08 903.59 Latent Cap (Btu/h): 3240.53 1052.94 EvapAir Delta T (F): 19.01 0.87 Indoor Inlet Dew (F): 60.387 1.22 Indoor Exit Dry-Bulb: 62.620 0.61 Indoor Exit Dew (F): 58.265 0.66 Air/Ref Cap Pront Diff: 0.36 7.19 Sensible Heat Ratio: 0.840 SCFM per Ton: 481.09 0.0486 Indoor Airflow (CFM): 810.32 9.82 Indoor Airflow (SCFM): 809.42 9.70 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011302 Evap Exit Humidity Ratio (lbH2O/lbAir): 0.010463 Barometric Pressure (in HG): 29.65 Nozzle Temp (F): 61.61 0.55 Air Chamber Nozzle Pressure Drop (in Water): 0.868 0.021 Evaporator Coil Air Pressure Drop (in Water): 0.075 0.004 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 265.97 Upstream Temp (F): 105.55 1.462 0.519 Ref-side Cap (Btu/h) : 20258.54 775.30 Ref-side Cap (tons): 1.69 Refrigerant Mdot (lbm/h): 319.95 0.06 11.72 Coriolis Density (lbm/ft3): 82.53 0.56 Upstream R22 Tsat (F): 117.52 0.425 Average Subcooling (F): 11.97 0.670 0.607 1.869 Evap Exit Pressure (psia): 90.71 Evap Exit Avg Temp : 59.55 Exit Superheat (F): 14.58 1.791 Evap Exit Tsat (F): 44.97 0.391

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040121a.dat SUMMARY FILENAME: a040121a.sum Range Range Total Air-Side Capacity: 13113.32 Air-Side Conditions 956.28 Indoor Dry-Bulb : 80.145 0.30 Sensible Cap (Btu/h): 12617.08 431.95 Indoor Exit Dry-Bulb: 67.736 0.55 Indoor Exit Dry-Color 67.736 0.55 Latent Cap (Btu/h): 496.25 EvapAir Delta T (F): 14.16 974.54 0.44 Indoor Exit Dew (F): 60.395 0.53 Air/Ref Cap Pront Diff: -3.01 8.47 Sensible Heat Ratio: 0.963 SCFM per Ton: 739.70 0.0714 Indoor Airflow (CFM): 809.05 8.27 Indoor Airflow (SCFM): 808.33 8.12 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011319 Wap Infect Humidity Ratio (15H20/15H17):0.011190Evap Exit Humidity Ratio (15H20/15Air):0.011190Barometric Pressure (in HG):29.95Nozzle Temp (F): Air Chamber Nozzle Pressure Drop (in Water): 0.865 0.017 0.006 Evaporator Coil Air Pressure Drop (in Water): 0.066 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 259.38 1.218 Upstream Temp (F): 104.33 0.435 Ref-side Cap (Btu/h) : 12712.62 464.37 0.04 Ref-side Cap (tons): 1.06 Refrigerant Mdot (lbm/h): 199.55 7.33 Coriolis Density (lbm/ft3): 82.36 0.16 Upstream R22 Tsat (F): 115.59 0.361 Average Subcooling (F): 11.26 0.607 0.607 0.892 Evap Exit Pressure (psia): 99.70 Evap Exit Avg Temp : 65.65 Exit Superheat (F): 15.10 1.143 Evap Exit Tsat (F): 50.56 0.365

Coil 3 R22, A01148, No Fan

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040205a.dat SUMMARY FILENAME: a040205a.sum Range Air-Side Conditions Range Total Air-Side Capacity: 41040.73 1364.36 Indoor Dry-Bulb : 79.463 0.23 Sensible Cap (Btu/h): 27659.16 873.81 Indoor Inlet Dew (F): 60.632 0.44 Indoor Exit Dry-Bulb: 55.072 0.38 Indoor Exit Dry (T) Latent Cap (Btu/h): 13381.57 655.21 EvapAir Delta T (F): 26.26 0.44 Indoor Exit Dew (F): 52.370 0.41 Air/Ref Cap Pront Diff: 2.87 4.66 Sensible Heat Ratio: 0.674 SCFM per Ton: 280.16 0.0119 Indoor Airflow (CFM): 929.07 19.21 Indoor Airflow (SCFM): 958.17 19.81 ((0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011184 Evap Exit Humidity Ratio (lbH2O/lbAir): 0.008256 Barometric Pressure (in HG): 30.22 Nozzle Temp (F): 55.25 0.88 Air Chamber Nozzle Pressure Drop (in Water): 1.175 0.048 Evaporator Coil Air Pressure Drop (in Water): 0.358 0.016 _____ Refrigerant Side Conditions Expansion Valve Ref-side Cap (Btu/h) : 42213.99 Upstream Pressure (psia): 273.51 2.193 Upstream Temp (F): 105.26 0.520 650.68 Ref-side Cap (tons): 3.52 Refrigerant Mdot (lbm/h): 665.74 0.05 10.62 Coriolis Density (lbm/ft3): 82.17 0.33 Upstream R22 Tsat (F): 119.69 0.625 0.947 Average Subcooling (F): 14.43 83.57 0.728 Evap Exit Pressure (psia): Evap Exit Avg Temp : 57.45 Exit Superheat (F): 17.24 2.513 2.347 Evap Exit Tsat (F): 40.22 0.498

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040209a.dat SUMMARY FILENAME: a040209a.sum Range Range Total Air-Side Capacity: 30896.46 694.06 Air-Side Conditions Indoor Dry-Bulb : 79.728 0.51 Sensible Cap (Btu/h): 22952.69 764.15 Indoor Exit Dry-Bulb: 59.655 0.39 Indoor Exit Dry-CD Latent Cap (Btu/h): 7943.77 EvapAir Delta T (F): 22.04 517.21 0.86 Indoor Exit Dew (F): 55.835 0.32 Air/Ref Cap Prcnt Diff: -1.06 2.84 Sensible Heat Ratio: 0.743 SCFM per Ton: 367.48 0.0153 Indoor Airflow (CFM): 925.27 13.65 Indoor Airflow (SCFM): 946.16 13.96 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011135 Evap Exit Humidity Ratio (lbH20/lbAir):0.009375Barometric Pressure (in HG):30.26Nozzle Temp (F):60.010.28 Air Chamber Nozzle Pressure Drop (in Water): 1.156 0.034 Evaporator Coil Air Pressure Drop (in Water): 0.348 0.012 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 267.52 Upstream Temp (F): 104.48 0.731 0.480 Ref-side Cap (Btu/h) : 30568.21 436.20 0.04 Ref-side Cap (tons): 2.55 7.69 Refrigerant Mdot (lbm/h): 480.19 Coriolis Density (lbm/ft3): 81.94 0.38 Upstream R22 Tsat (F): 117.97 0.212 Average Subcooling (F): 13.49 0.586 0.485 2.736 Evap Exit Pressure (psia): 97.44 Evap Exit Avg Temp : 60.39 Exit Superheat (F): 11.20 2.884 0.297 Evap Exit Tsat (F): 49.19

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040209b.dat SUMMARY FILENAME: a040209b.sum Range Range Total Air-Side Capacity: 41393.85 883.37 Air-Side Conditions Indoor Dry-Bulb : 80.019 0.52 Sensible Cap (Btu/h): 27938.72 683.02 Indoor Inlet Dew (F): 60.502 0.30 Indoor Exit Dry-Bulb: 55.085 0.39 Indoor Exit Dev (D) 50.11 Latent Cap (Btu/h): 13455.14 489.03 EvapAir Delta T (F): 26.72 0.44 Indoor Exit Dew (F): 52.064 0.34 Air/Ref Cap Pront Diff: -0.24 2.76 Sensible Heat Ratio: 0.675 SCFM per Ton: 275.80 0.0102 Indoor Airflow (CFM): 920.26 12.52 Indoor Airflow (SCFM): 951.37 12.85 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011116 Evap Exit Humidity Ratio (lbH2O/lbAir): 0.008151 Barometric Pressure (in HG): 30.26 Nozzle Temp (F): 54.73 0.65 Air Chamber Nozzle Pressure Drop (in Water): 1.156 0.031 Evaporator Coil Air Pressure Drop (in Water): 0.349 0.014 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 274.99 1.340 Upstream Temp (F): 105.87 0.909 Ref-side Cap (Btu/h) : 41292.35 720.00 Ref-side Cap (tons): 3.44 Refrigerant Mdot (lbm/h): 653.21 0.06 10.26 Coriolis Density (lbm/ft3): 82.34 0.60 Upstream R22 Tsat (F): 120.11 0.380 Average Subcooling (F): 14.24 1.163 0.971 4.966 Evap Exit Pressure (psia): 83.38 Evap Exit Avg Temp : 53.47 Exit Superheat (F): 13.38 4.716 Evap Exit Tsat (F): 40.09 0.667

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040210a.dat SUMMARY FILENAME: a040210a.sum Range Air-Side Conditions Range Total Air-Side Capacity: 35323.45 1001.75 Indoor Dry-Bulb : 79.862 0.41 Sensible Cap (Btu/h): 24841.59 604.71 Indoor Exit Dry-Bulb: 57.472 0.54 Indoor Exit Dry-Bulb: 57.472 0.54 Latent Cap (Btu/h): 10481.86 1001.13 EvapAir Delta T (F): 24.22 0.65 Indoor Exit Dew (F): 54.086 0.29 Air/Ref Cap Pront Diff: 3.52 4.05 Sensible Heat Ratio: 0.703 SCFM per Ton: 316.85 0.0216 Indoor Airflow (CFM): 906.77 6.99 Indoor Airflow (SCFM): 932.67 7.17 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011150 Evap Exit Humidity Ratio (lbH20/lbAir):0.008794Barometric Pressure (in HG):30.24Nozzle Temp (F):56.840.75 Air Chamber Nozzle Pressure Drop (in Water): 1.117 0.017 0.007 Evaporator Coil Air Pressure Drop (in Water): 0.334 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 268.66 Upstream Temp (F): 104.33 0.974 0.498 Ref-side Cap (Btu/h) : 36563.86 598.74 0.05 Ref-side Cap (tons): 3.05 Refrigerant Mdot (lbm/h): 573.95 9.71 0.36 Coriolis Density (lbm/ft3): 81.89 Upstream R22 Tsat (F): 118.30 0.281 Average Subcooling (F): 13.97 0.508 0.485 2.837 Evap Exit Pressure (psia): 90.59 Evap Exit Avg Temp : 59.09 Exit Superheat (F): 14.20 2.837 0.313 Evap Exit Tsat (F): 44.89

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040211a.dat SUMMARY FILENAME: a040211a.sum Range Range Total Air-Side Capacity: 28797.52 635.22 Air-Side Conditions Indoor Dry-Bulb : 79.830 0.53 Sensible Cap (Btu/h): 22212.84 940.77 0.50 Latent Cap (Btu/h): 6584.67 EvapAir Delta T (F): 21.15 Indoor Inlet Dew (F): 60.172 551.13 Indoor Exit Dry-Bulb: 60.467 0.86 Indoor Exit Dew (F): 56.318 0.29 Air/Ref Cap Pront Diff: 0.04 2.65 Sensible Heat Ratio: 0.771 SCFM per Ton: 397.62 0.0215 Indoor Airflow (CFM): 936.15 14.99 Indoor Airflow (SCFM): 954.21 15.48 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011025 Evap Exit Humidity Ratio (lbH2O/lbAir): 0.009579 Barometric Pressure (in HG): 30.15 Nozzle Temp (F): 59.73 0.65 Air Chamber Nozzle Pressure Drop (in Water): 1.180 0.038 Evaporator Coil Air Pressure Drop (in Water): 0.340 0.010 _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 266.91 Upstream Temp (F): 104.74 0.853 0.367 Ref-side Cap (Btu/h) : 28808.32 546.01 Ref-side Cap (tons): 2.40 Refrigerant Mdot (lbm/h): 453.13 0.05 8.79 Coriolis Density (lbm/ft3): 82.05 0.40 Upstream R22 Tsat (F): 117.80 0.247 Average Subcooling (F): 13.06 0.367 0.607 2.732 Evap Exit Pressure (psia): 98.26 Evap Exit Avg Temp : 62.18 Exit Superheat (F): 12.49 2.732 0.369 Evap Exit Tsat (F): 49.69

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040211b.dat SUMMARY FILENAME: a040211b.sum Range Range Total Air-Side Capacity: 36747.94 789.39 Air-Side Conditions Indoor Dry-Bulb : 80.029 0.45 Sensible Cap (Btu/h): 25913.75 926.16 Indoor Inlet Dew (F): 60.367 Latent Cap (Btu/h): 10834.19 457.19 0.36 Indoor Exit Dry-Bulb: 57.210 0.23 EvapAir Delta T (F): 24.69 0.65 Indoor Exit Dew (F): 53.785 0.32 Air/Ref Cap Pront Diff: -0.41 3.06 Sensible Heat Ratio: 0.705 SCFM per Ton: 311.64 0.0118 Indoor Airflow (CFM): 930.35 10.67 Indoor Airflow (SCFM): 954.35 12.08 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011103 Evap Exit Humidity Ratio (lbH2O/lbAir): 0.008723 Barometric Pressure (in HG): 30.15 Nozzle Temp (F): 56.70 0.60 Air Chamber Nozzle Pressure Drop (in Water): 1.172 0.028 Evaporator Coil Air Pressure Drop (in Water): 0.343 0.012 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 269.10 Upstream Temp (F): 104.40 0.974 0.520 Ref-side Cap (Btu/h) : 36596.26 594.50 0.05 Ref-side Cap (tons): 3.05 Refrigerant Mdot (lbm/h): 574.65 9.71 Coriolis Density (lbm/ft3): 81.89 0.19 Upstream R22 Tsat (F): 118.43 0.281 Average Subcooling (F): 14.03 0.731 0.728 3.573 Evap Exit Pressure (psia): 90.35 Evap Exit Avg Temp : 56.66 Exit Superheat (F): 11.93 3.494 Evap Exit Tsat (F): 44.73 0.471

Coil 4 R22, A01138, No Fan

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040219x.dat SUMMARY FILENAME: a040219x.sum Range Indoor Dry-Bulb : 79.733 0.75 Sensible Cap (Btu/h): 18268.01 480.03 Air-Side Conditions Indoor Inlet Dew (F): 60.591 0.85 Indoor Exit Dry-Bulb: 60.736 0.27 Indoor Exit Dry (T) Latent Cap (Btu/h): 8515.73 1438.99 EvapAir Delta T (F): 20.89 0.44 Indoor Exit Dew (F): 54.512 0.22 Air/Ref Cap Pront Diff: -3.06 7.01 Sensible Heat Ratio: 0.682 SCFM per Ton: 356.16 0.0356 Indoor Airflow (CFM): 784.16 9.68 Indoor Airflow (SCFM): 794.93 10.13 ((0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011259 Evap Exit Humidity Ratio (lbH2O/lbAir): 0.009013 Barometric Pressure (in HG): 29.98 Nozzle Temp (F): 60.11 0.55 Air Chamber Nozzle Pressure Drop (in Water): 0.825 0.020 Evaporator Coil Air Pressure Drop (in Water): 0.103 0.005 _____ Refrigerant Side Conditions Expansion Valve
 Upstream Pressure (psia):
 272.62
 0.974
 Ref-side Cap (Btu/h):
 25954.80

 Upstream Temp (F):
 106.07
 0.198
 Ref-side Cap (tons):
 2.16
 364.19 0.03 Ref-side Cap (tons): 2.16 Refrigerant Mdot (lbm/h): 410.99 Coriolis Density (lbm/ft3): 82.36 0.16 Upstream R22 Tsat (F): 119.44 0.278 0.301 Average Subcooling (F): 13.37 82.89 0.485 Evap Exit Pressure (psia): Evap Exit Avg Temp : 53.49 Exit Superheat (F): 13.74 3.640 0.335 Evap Exit Tsat (F): 39.75

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040223a.dat SUMMARY FILENAME: a040223a.sum Range Range Total Air-Side Capacity: 22035.41 717.30 Air-Side Conditions Indoor Dry-Bulb : 79.831 0.38 Sensible Cap (Btu/h): 16037.57 564.10 Latent Cap (Btu/h): 5997.85 EvapAir Delta T (F): 18.31 Indoor Inlet Dew (F): 60.757 0.25 366.03 Indoor Exit Dry-Bulb: 63.300 0.29 0.43 Indoor Exit Dew (F): 56.680 0.24 Air/Ref Cap Pront Diff: -1.11 3.19 Sensible Heat Ratio: 0.728 SCFM per Ton: 433.12 0.0115 Indoor Airflow (CFM): 797.03 14.29 Indoor Airflow (SCFM): 795.33 14.25 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011454 Wap Infect Humidity Ratio (15H20/15H17):0.009873Evap Exit Humidity Ratio (15H20/15Air):0.009873Barometric Pressure (in HG):29.65Nozzle Temp (F):62.300.82 Air Chamber Nozzle Pressure Drop (in Water): 0.839 0.030 Evaporator Coil Air Pressure Drop (in Water): 0.102 0.008 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 271.21 Upstream Temp (F): 104.30 0.731 0.520 Ref-side Cap (Btu/h) : 21790.52 420.49 0.04 Ref-side Cap (tons): 1.82 Refrigerant Mdot (lbm/h): 342.00 6.96 Coriolis Density (lbm/ft3): 82.11 0.16 Upstream R22 Tsat (F): 119.04 0.209 Average Subcooling (F): 14.73 0.614 0.243 4.399 Evap Exit Pressure (psia): 90.96 Evap Exit Avg Temp : 56.93 Exit Superheat (F): 11.80 4.399 0.156 Evap Exit Tsat (F): 45.12

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040225a.dat SUMMARY FILENAME: a040225a.sum Range Range Total Air-Side Capacity: 18269.45 1171.80 Air-Side Conditions Indoor Dry-Bulb : 80.022 0.51 Sensible Cap (Btu/h) : 14746.16 529.64

 Indoor Inlet Dew (F): 60.413
 0.20
 Latent Cap (Btu/h): 3523.29

 Indoor Exit Dry-Bulb: 64.826
 0.28
 EvapAir Delta T (F): 16.93

 695.37 0.43 Indoor Exit Dew (F): 58.000 0.61 Air/Ref Cap Pront Diff: -3.42 5.96 Sensible Heat Ratio: 0.807 SCFM per Ton: 519.44 0.0264 Indoor Airflow (CFM): 782.66 8.87 Indoor Airflow (SCFM): 790.82 9.75 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011122 Wap Infect Humidity Ratio (15H20/15H17):0.010188Evap Exit Humidity Ratio (15H20/15Air):0.010188Barometric Pressure (in HG):30.15Nozzle Temp (F): Air Chamber Nozzle Pressure Drop (in Water): 0.819 0.019 Evaporator Coil Air Pressure Drop (in Water): 0.101 0.006 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 267.89 Upstream Temp (F): 104.71 0.487 0.520 Ref-side Cap (Btu/h) : 17640.72 256.55 0.02 Ref-side Cap (tons): 1.47 Refrigerant Mdot (lbm/h): 277.43 4.21 Coriolis Density (lbm/ft3): 82.22 0.16 Upstream R22 Tsat (F): 118.08 0.141 Average Subcooling (F): 13.37 0.590 0.243 0.682 Evap Exit Pressure (psia): 97.83 Evap Exit Avg Temp : 62.27 Exit Superheat (F): 12.84 0.694 Evap Exit Tsat (F): 49.43 0.148

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040226x.dat SUMMARY FILENAME: a040226x.sum Range Range Total Air-Side Capacity: 22162.66 746.55 Air-Side Conditions Indoor Dry-Bulb : 79.824 0.48 Sensible Cap (Btu/h): 16293.07 683.39 Indoor Inlet Dew (F): 60.511 0.30 Indoor Exit Dry-Bulb: 62.849 0.23 Latent Cap (Btu/h): 5869.59 EvapAir Delta T (F): 18.75 264.85 0.65 Indoor Exit Dew (F): 56.419 0.24 Air/Ref Cap Pront Diff: -2.32 4.07 Sensible Heat Ratio: 0.735 SCFM per Ton: 427.28 0.0134 Indoor Airflow (CFM): 783.74 11.71 Indoor Airflow (SCFM): 789.14 11.92 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011249 Wap Infect Humidity Ratio (15H20/15H17):0.009689Evap Exit Humidity Ratio (15H20/15Air):0.009689Barometric Pressure (in HG):29.92Nozzle Temp (F):62.38 Air Chamber Nozzle Pressure Drop (in Water): 0.819 0.024 Evaporator Coil Air Pressure Drop (in Water): 0.102 0.006 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 269.24 Upstream Temp (F): 105.78 0.731 0.649 Ref-side Cap (Btu/h) : 21646.36 359.14 0.03 Ref-side Cap (tons): 1.80 Refrigerant Mdot (lbm/h): 342.26 5.68 0.22 Coriolis Density (lbm/ft3): 82.45 Upstream R22 Tsat (F): 118.47 0.211 Average Subcooling (F): 12.69 0.511 0.243 0.975 Evap Exit Pressure (psia): 90.58 Evap Exit Avg Temp : 59.46 Exit Superheat (F): 14.58 1.131 Evap Exit Tsat (F): 44.88 0.157

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: b040225b.dat SUMMARY FILENAME: b040225b.sum Range Air-Side Conditions Range Total Air-Side Capacity: 26781.23 822.37 Indoor Dry-Bulb : 80.166 0.54 Sensible Cap (Btu/h): 18704.64 613.34 Latent Cap (Btu/h): 8076.59 EvapAir Delta T (F): 21.40 Indoor Inlet Dew (F): 60.286 0.36 Indoor Exit Dry-Bulb: 60.610 0.30 295.67 0.44 Indoor Exit Dew (F): 54.447 0.26 Air/Ref Cap Pront Diff: -2.53 4.62 Sensible Heat Ratio: 0.698 SCFM per Ton: 356.06 0.0098 Indoor Airflow (CFM): 779.61 15.74 Indoor Airflow (SCFM): 794.65 16.13 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011071 Wap fillet Humidity Ratio (lbH20/lbAir):0.008940Barometric Pressure (in HG):30.15Nozzle Temp (F):60.230.76 Air Chamber Nozzle Pressure Drop (in Water): 0.820 0.033 Evaporator Coil Air Pressure Drop (in Water): 0.105 0.009 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 270.17 Upstream Temp (F): 106.27 0.974 0.609 Ref-side Cap (Btu/h) : 26102.18 1283.93 Ref-side Cap (tons): 2.18 0.11 Refrigerant Mdot (lbm/h): 413.75 20.15 Coriolis Density (lbm/ft3): 82.51 0.32 Upstream R22 Tsat (F): 118.74 0.280 Average Subcooling (F): 12.47 0.542 0.485 3.049 Evap Exit Pressure (psia): 83.86 Evap Exit Avg Temp : 54.70 3.049 Exit Superheat (F): 14.28 Evap Exit Tsat (F): 40.41 0.332

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: b040226b.dat SUMMARY FILENAME: b040226b.sum Range Air-Side Conditions Range Total Air-Side Capacity: 16953.69 572.29 Indoor Dry-Bulb : 80.011 0.45 Sensible Cap (Btu/h): 14077.80 482.68 Latent Cap (Btu/h): 2875.89 EvapAir Delta T (F): 16.19 Indoor Inlet Dew (F): 60.711 0.16 Indoor Exit Dry-Bulb: 65.498 0.29 368.36 0.43 Indoor Exit Dew (F): 58.787 0.25 Air/Ref Cap Pront Diff: -2.57 4.27 Sensible Heat Ratio: 0.830 SCFM per Ton: 558.45 0.0187 Indoor Airflow (CFM): 788.03 16.16 Indoor Airflow (SCFM): 788.99 15.66 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011330 Evap Exit Humidity Ratio (lbH2O/lbAir): 0.010566 Barometric Pressure (in HG): 29.92 Nozzle Temp (F): 65.08 0.69 Air Chamber Nozzle Pressure Drop (in Water): 0.823 0.033 Evaporator Coil Air Pressure Drop (in Water): 0.099 0.005 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 271.82 Upstream Temp (F): 104.56 0.487 0.366 Ref-side Cap (Btu/h) : 16516.48 372.06 Ref-side Cap (tons): 1.38 Refrigerant Mdot (lbm/h): 259.56 0.03 5.68 Coriolis Density (lbm/ft3): 82.29 0.10 Upstream R22 Tsat (F): 119.21 0.139 Average Subcooling (F): 14.65 0.463 0.485 0.685 Evap Exit Pressure (psia): 99.80 Evap Exit Avg Temp : 63.23 Exit Superheat (F): 12.61 0.938 Evap Exit Tsat (F): 50.62 0.291

Coil 5 R22, A01060, Fan: 273 Watts

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040302a.dat SUMMARY FILENAME: a040302a.sum Range Air-Side Conditions Range Total Air-Side Capacity: 27580.34 853.16 Indoor Dry-Bulb : 80.145 0.29 Sensible Cap (Btu/h): 18827.50 513.83 Indoor Inlet Dew (F): 60.357 0.36 Indoor Exit Dry-Bulb: 59.345 0.23 Latent Cap (Btu/h): 8752.84 EvapAir Delta T (F): 22.72 468.87 0.44 Indoor Exit Dew (F): 53.644 0.22 Air/Ref Cap Prcnt Diff: -1.58 4.17 Sensible Heat Ratio: 0.683 SCFM per Ton: 327.76 0.0121 Indoor Airflow (CFM): 740.22 7.76 Indoor Airflow (SCFM): 753.31 7.78 ((0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011164 Evap Exit Humidity Ratio (lbH2O/lbAir): 0.008728 Barometric Pressure (in HG): 29.98 Nozzle Temp (F): 58.15 0.32 Air Chamber Nozzle Pressure Drop (in Water): 0.739 0.015 Evaporator Coil Air Pressure Drop (in Water): 0.124 0.028 _____ Refrigerant Side Conditions Expansion Valve
 Upstream Pressure (psia):
 268.54
 0.731
 Ref-side Cap (Btu/h) :
 27142.87

 Upstream Temp (F):
 105.08
 0.584
 Ref-side Cap (tons):
 2.26
 616.61 Ref-side Cap (tons): 2.26 Refrigerant Mdot (lbm/h): 427.67 0.05 9.16 Coriolis Density (lbm/ft3): 82.27 0.29 Upstream R22 Tsat (F): 118.27 0.211 0.661 Average Subcooling (F): 13.19 0.485 2.420 90.74 Evap Exit Pressure (psia): Evap Exit Avg Temp : 59.50 Exit Superheat (F): 14.52 2.420 Evap Exit Tsat (F): 44.99 0.313

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040303a.dat SUMMARY FILENAME: a040303a.sum Range Air-Side Conditions Range Total Air-Side Capacity: 32329.27 833.92 Indoor Dry-Bulb : 80.024 0.52 Sensible Cap (Btu/h): 20840.09 612.93 Indoor Inlet Dew (F): 60.435 Latent Cap (Btu/h): 11489.18 0.21 334.36 Indoor Exit Dry-Bulb: 56.983 0.27 EvapAir Delta T (F): 24.98 0.44 Indoor Exit Dew (F): 51.431 0.18 Air/Ref Cap Pront Diff: -0.37 2.91 Sensible Heat Ratio: 0.645 SCFM per Ton: 281.75 0.0055 Indoor Airflow (CFM): 745.45 9.82 Indoor Airflow (SCFM): 759.07 9.93 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011245 Wap Infect Humidity Ratio (15H20/15H17):0.008071Evap Exit Humidity Ratio (15H20/15Air):0.008071Barometric Pressure (in HG):29.85Nozzle Temp (F):55.800.42 Air Chamber Nozzle Pressure Drop (in Water): 0.749 0.020 Evaporator Coil Air Pressure Drop (in Water): 0.136 0.041 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 269.50 1.218 Upstream Temp (F): 104.63 0.910 Ref-side Cap (Btu/h) : 32208.02 435.83 Ref-side Cap (tons): 2.68 Refrigerant Mdot (lbm/h): 506.34 0.04 6.41 Coriolis Density (lbm/ft3): 81.99 0.30 Upstream R22 Tsat (F): 118.55 0.351 Average Subcooling (F): 13.91 1.170 0.607 Evap Exit Pressure (psia): 83.54 Evap Exit Avg Temp : 52.65 6.498 Exit Superheat (F): 12.45 6.498 Evap Exit Tsat (F): 40.20 0.416

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040304a.dat SUMMARY FILENAME: a040304a.sum Range Range Total Air-Side Capacity: 27488.36 891.82 Air-Side Conditions Indoor Dry-Bulb : 79.846 0.71 Sensible Cap (Btu/h): 18592.08 788.83 Indoor Inlet Dew (F): 60.399 0.31 Latent Cap (Btu/h): 8896.27 Indoor Exit Dry-Bulb: 59.306 0.39 EvapAir Delta T (F): 22.46 337.31 0.87 Indoor Exit Dew (F): 53.625 0.36 Air/Ref Cap Pront Diff: -1.74 3.39 Sensible Heat Ratio: 0.676 SCFM per Ton: 328.46 0.0109 Indoor Airflow (CFM): 746.16 7.72 Indoor Airflow (SCFM): 752.41 7.79 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011269 Evap Exit Humidity Ratio (lbH20/lbAir):0.008790Barometric Pressure (in HG):29.75Nozzle Temp (F):58.880.37 Air Chamber Nozzle Pressure Drop (in Water): 0.744 0.015 Evaporator Coil Air Pressure Drop (in Water): 0.140 0.024 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 269.51 1.096 Upstream Temp (F): 104.56 0.520 Ref-side Cap (Btu/h) : 27008.54 440.01 0.04 Ref-side Cap (tons): 2.25 Refrigerant Mdot (lbm/h): 424.44 6.59 Coriolis Density (lbm/ft3): 82.02 0.38 Upstream R22 Tsat (F): 118.55 0.316 Average Subcooling (F): 13.99 0.598 0.243 Evap Exit Pressure (psia): 90.05 Evap Exit Avg Temp : 59.41 5.210 5.052 Exit Superheat (F): 14.87 Evap Exit Tsat (F): 44.54 0.157

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: b040303b.dat SUMMARY FILENAME: b040303b.sum Range Range Total Air-Side Capacity: 23217.01 Air-Side Conditions 492.17 Indoor Dry-Bulb : 79.842 0.67 Sensible Cap (Btu/h): 16981.94 465.27

 Indoor Inlet Dew (F): 60.418
 0.12
 Latent Cap (Btu/h): 6235.07

 Indoor Exit Dry-Bulb: 61.269
 0.35
 EvapAir Delta T (F): 20.49

 176.50 0.43 Indoor Exit Dew (F): 55.823 0.20 Air/Ref Cap Pront Diff: -1.71 2.83 Sensible Heat Ratio: 0.731 SCFM per Ton: 389.23 0.0106 Indoor Airflow (CFM): 747.39 4.97 Indoor Airflow (SCFM): 753.05 5.01 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011238 Evap Exit Humidity Ratio (lbH2O/lbAir):0.009502Barometric Pressure (in HG):29.85Nozzle Temp (F):60.810.64 Air Chamber Nozzle Pressure Drop (in Water): 0.745 0.010 Evaporator Coil Air Pressure Drop (in Water): 0.146 0.014 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 272.97 Upstream Temp (F): 104.56 0.853 0.416 Ref-side Cap (Btu/h) : 22818.98 413.37 Ref-side Cap (tons): 1.90 Refrigerant Mdot (lbm/h): 358.60 0.03 6.78 Coriolis Density (lbm/ft3): 82.08 0.37 Upstream R22 Tsat (F): 119.54 0.243 Average Subcooling (F): 14.98 0.448 0.485 1.260 Evap Exit Pressure (psia): 98.39 Evap Exit Avg Temp : 64.17 Exit Superheat (F): 14.40 1.260 0.294 Evap Exit Tsat (F): 49.77

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040305a.dat SUMMARY FILENAME: a040305a.sum Range Range Total Air-Side Capacity: 32479.54 1003.87 Air-Side Conditions Indoor Dry-Bulb : 79.740 0.52 Sensible Cap (Btu/h): 20659.92 970.81 Indoor Inlet Dew (F): 60.443 0.46 Latent Cap (Btu/h): 11819.62 Indoor Exit Dry-Bulb: 56.551 0.39 EvapAir Delta T (F): 24.94 Latent Cap (Btu/h): 11819.62 344.26 1.08 Indoor Exit Dew (F): 51.099 0.32 Air/Ref Cap Pront Diff: -0.93 3.45 Sensible Heat Ratio: 0.636 SCFM per Ton: 278.47 0.0130 Indoor Airflow (CFM): 743.16 7.82 Indoor Airflow (SCFM): 753.71 7.68 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011286 Wap Infect Humidity Ratio (15H20/15Air):0.007999Evap Exit Humidity Ratio (15H20/15Air):0.007999Barometric Pressure (in HG):29.75Nozzle Temp (F):56.130.55 Air Chamber Nozzle Pressure Drop (in Water): 0.742 0.015 Evaporator Coil Air Pressure Drop (in Water): 0.151 0.028 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 269.37 Upstream Temp (F): 104.35 0.853 0.967 Ref-side Cap (Btu/h) : 32175.10 333.48 Ref-side Cap (tons): 2.68 Refrigerant Mdot (lbm/h): 505.11 0.03 5.68 Coriolis Density (lbm/ft3): 81.88 0.33 Upstream R22 Tsat (F): 118.51 0.246 Average Subcooling (F): 14.16 1.177 0.364 3.954 Evap Exit Pressure (psia): 83.93 Evap Exit Avg Temp : 54.32 Exit Superheat (F): 13.86 3.954 Evap Exit Tsat (F): 40.46 0.249

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040308a.dat SUMMARY FILENAME: a040308a.sum Range Range Total Air-Side Capacity: 22605.73 521.66 Air-Side Conditions Indoor Dry-Bulb : 79.710 0.39 Sensible Cap (Btu/h): 16356.36 502.56 Latent Cap (Btu/h): 6249.36 EvapAir Delta T (F): 19.86 Indoor Inlet Dew (F): 60.687 0.30 290.00 0.11 Indoor Exit Dry-Bulb: 61.590 0.43 Indoor Exit Dew (F): 56.086 0.16 Air/Ref Cap Prcnt Diff: -1.31 2.36 Sensible Heat Ratio: 0.724 SCFM per Ton: 397.08 0.0103 Indoor Airflow (CFM): 742.04 6.90 Indoor Airflow (SCFM): 748.02 6.88 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011336 Wap Infect Humidity Ratio (15H20/15Air):0.009585Barometric Pressure (in HG):29.88Nozzle Temp (F):61.040.10 Air Chamber Nozzle Pressure Drop (in Water): 0.735 0.013 Evaporator Coil Air Pressure Drop (in Water): 0.161 0.015 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 270.28 Upstream Temp (F): 105.69 0.731 0.237 Ref-side Cap (Btu/h) : 22309.53 298.84 0.02 Ref-side Cap (tons): 1.86 Refrigerant Mdot (lbm/h): 352.58 4.76 Coriolis Density (lbm/ft3): 82.32 0.18 Upstream R22 Tsat (F): 118.77 0.210 Average Subcooling (F): 13.08 0.386 0.364 0.793 Evap Exit Pressure (psia): 98.45 Evap Exit Avg Temp : 63.73 Exit Superheat (F): 13.92 0.657 Evap Exit Tsat (F): 49.81 0.221

Coil 6 R22, A01125, Fan: 768 Watts

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: c040406c.dat SUMMARY FILENAME: c040406c.sum Range
 Kange

 ir-Side Conditions
 Range Total Air-Side Capacity: 37805.35

 Indoor Dry-Bulb:
 79.347

 3.97
 Sensible Cap (Btu/h): 26735.16

 4315.08

 Door Tplet Dew (F):
 60.944

 0.45
 Total Air-Side Capacity: 37805.35
 Air-Side Conditions
 Indoor Inlet Dew (F): 60.944
 0.45
 Latent Cap (Btu/h): 11070.19

 Indoor Exit Dry-Bulb: 60.804
 1.28
 EvapAir Delta T (F): 20.91
 Latent Cap (Btu/h): 11070.19 1947.82 3.44 Indoor Exit Dew (F): 55.682 1.19 Air/Ref Cap Pront Diff: -0.44 13.23 Sensible Heat Ratio: 0.707 SCFM per Ton: 368.71 0.0418 Indoor Airflow (CFM): 1149.21 25.49 Indoor Airflow (SCFM): 1161.61 28.57 ((0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011438 Evap Exit Humidity Ratio (lbH2O/lbAir): 0.009440 Barometric Pressure (in HG): 29.89 Nozzle Temp (F): 60.06 1.13 Air Chamber Nozzle Pressure Drop (in Water): 0.918 0.043 Evaporator Coil Air Pressure Drop (in Water): 1.700 0.000 _____ Refrigerant Side Conditions Expansion Valve
 Upstream Pressure (psia):
 266.79
 3.350
 Ref-side Cap (Btu/h) :
 37608.27

 Upstream Temp (F):
 104.78
 1.051
 Ref-side Cap (tons):
 3.13
 993.66 Ref-side Cap (tons): 3.13 0.08 Refrigerant Mdot (lbm/h): 591.66 13.92 Coriolis Density (lbm/ft3): 81.51 0.28 Upstream R22 Tsat (F): 117.76 0.973 1.617 12.98 Average Subcooling (F): Evap Exit Pressure (psia): 101.49 1.630 5.368 1.638 Evap Exit Avg Temp : 65.58 Exit Superheat (F): 13.95 4.545 Evap Exit Tsat (F): 51.63 0.974

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040407a.dat SUMMARY FILENAME: a040407a.sum Range Air-Side Conditions Range Total Air-Side Capacity: 43850.60 5098.57 Indoor Dry-Bulb : 79.491 3.63 Sensible Cap (Btu/h): 29605.56 5146.04 Indoor Inlet Dew (F): 60.528 0.70 Indoor Exit Dry-Bulb: 58.585 1.12 Latent Cap (Btu/h): 14245.04 1882.32 EvapAir Delta T (F): 23.15 3.89 Indoor Exit Dew (F): 53.483 1.08 Air/Ref Cap Pront Diff: 0.37 13.50 Sensible Heat Ratio: 0.675 SCFM per Ton: 318.18 0.0485 Indoor Airflow (CFM): 1144.88 18.17 Indoor Airflow (SCFM): 1162.70 18.00 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011283 Wap Infect Humidity Ratio (15H20/15Air):0.008714Evap Exit Humidity Ratio (16H20/1bAir):0.008714Barometric Pressure (in HG):29.85Nozzle Temp (F):57.151.38 Air Chamber Nozzle Pressure Drop (in Water): 0.915 0.029 0.000 Evaporator Coil Air Pressure Drop (in Water): 1.700 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 268.66 2.741 Upstream Temp (F): 105.44 1.872 Ref-side Cap (Btu/h) : 43985.34 1308.50 Ref-side Cap (tons): 3.67 Refrigerant Mdot (lbm/h): 694.28 0.11 21.62 Coriolis Density (lbm/ft3): 81.89 0.33 Upstream R22 Tsat (F): 118.30 0.791 Average Subcooling (F): 12.87 1.662 1.395 4.507 Evap Exit Pressure (psia): 95.81 Evap Exit Avg Temp : 62.16 Exit Superheat (F): 13.98 3.719 Evap Exit Tsat (F): 48.19 0.864

DATA FILENAME: d040406d.dat SUMMARY FILENAME: d040406d.sum	
Range	
Air-Side Conditions Range Total Air-Side Capacity: 37704.09 1035.50	
Indoor Dry-Bulb : 79.017 0.79 Sensible Cap (Btu/h): 26399.92 873.21	
Indoor Inlet Dew (F): 61.007 0.41 Latent Cap (Btu/h): 11304.17 631.67	
Indoor Exit Dry-Bulb: 60.679 0.43 EvapAir Delta T (F): 20.73 0.76	
Indoor Exit Dew (F): 55.613 0.34 Air/Ref Cap Pront Diff: -0.30 3.53	
Sensible Heat Ratio: 0.700 0.0088	
Indoor Airflow (CFM): 1143.97 24.09 SCFM per Ton: 368.25 Indoor Airflow (SCFM): 1157.04 24.16 (0.075 lb/ft3 standard air)	
Evap Inlet Humidity Ratio (lbH20/lbAir): 0.011464	
Evap Exit Humidity Ratio (lbH2O/lbAir): 0.009416	
Barometric Pressure (in HG): 29.89 Nozzle Temp (F): 59.74 0.64	
Air Chamber Nozzle Pressure Drop (in Water): 0.910 0.038	
Evaporator Coil Air Pressure Drop (in Water): 1.700 0.000	
Refrigerant Side Conditions	
Expansion Valve	
±	26.25
<u>-</u>	
Upstream Pressure (psia): 266.07 0.670 Ref-side Cap (Btu/h) : 37587.47 5	0.04
Upstream Pressure (psia): 266.07 0.670 Ref-side Cap (Btu/h): 37587.47 5 Upstream Temp (F): 104.36 0.401 Ref-side Cap (tons): 3.13	0.04 7.69
Upstream Pressure (psia): 266.07 0.670 Ref-side Cap (Btu/h): 37587.47 5 Upstream Temp (F): 104.36 0.401 Ref-side Cap (tons): 3.13 Refrigerant Mdot (lbm/h): 590.11	0.04 7.69
Upstream Pressure (psia): 266.07 0.670 Ref-side Cap (Btu/h) : 37587.47 5 Upstream Temp (F): 104.36 0.401 Ref-side Cap (tons): 3.13 Refrigerant Mdot (lbm/h): 590.11 Coriolis Density (lbm/ft3): 81.47	0.04 7.69
Upstream Pressure (psia): 266.07 0.670 Ref-side Cap (Btu/h) : 37587.47 5 Upstream Temp (F): 104.36 0.401 Ref-side Cap (tons): 3.13 Refrigerant Mdot (lbm/h): 590.11 Coriolis Density (lbm/ft3): 81.47 Upstream R22 Tsat (F): 117.55 0.195	0.04 7.69
Upstream Pressure (psia): 266.07 0.670 Ref-side Cap (Btu/h) : 37587.47 5 Upstream Temp (F): 104.36 0.401 Ref-side Cap (tons): 3.13 Refrigerant Mdot (lbm/h): 590.11 Coriolis Density (lbm/ft3): 81.47 Upstream R22 Tsat (F): 117.55 0.195	0.04 7.69
Upstream Pressure (psia): 266.07 0.670 Ref-side Cap (Btu/h) : 37587.47 5 Upstream Temp (F): 104.36 0.401 Ref-side Cap (tons): 3.13 Refrigerant Mdot (lbm/h): 590.11 Coriolis Density (lbm/ft3): 81.47 Upstream R22 Tsat (F): 117.55 0.195 Average Subcooling (F): 13.19 0.542	0.04 7.69
Upstream Pressure (psia): 266.07 0.670 Ref-side Cap (Btu/h) : 37587.47 5 Upstream Temp (F): 104.36 0.401 Ref-side Cap (tons): 3.13 Refrigerant Mdot (lbm/h): 590.11 Coriolis Density (lbm/ft3): 81.47 Upstream R22 Tsat (F): 117.55 0.195 Average Subcooling (F): 13.19 0.542 Evap Exit Pressure (psia): 101.34 0.485	0.04 7.69

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040402.dat SUMMARY FILENAME: a040402.sum Range Range Total Air-Side Capacity: 40037.46 1134.23 Air-Side Conditions Indoor Dry-Bulb : 79.643 0.37 Sensible Cap (Btu/h): 28653.79 899.47 Indoor Inlet Dew (F): 60.353 0.49 Indoor Exit Dry-Bulb: 59.392 0.35 Latent Cap (Btu/h): 11383.68 598.35 EvapAir Delta T (F): 22.52 0.55 Indoor Exit Dew (F): 54.835 0.37 Air/Ref Cap Pront Diff: 0.26 3.31 Sensible Heat Ratio: 0.716 SCFM per Ton: 346.57 0.0107 Indoor Airflow (CFM): 1150.15 21.70 Indoor Airflow (SCFM): 1156.30 21.69 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011288 Wap Infect Humidity Ratio (15H20/15Air):0.009225Barometric Pressure (in HG):29.65Nozzle Temp (F):58.740.46 Air Chamber Nozzle Pressure Drop (in Water): 0.915 0.034 Evaporator Coil Air Pressure Drop (in Water): 1.715 0.000 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 269.74 1.157 Upstream Temp (F): 104.20 0.668 Ref-side Cap (Btu/h) : 40140.11 525.17 0.04 Ref-side Cap (tons): 3.35 Refrigerant Mdot (lbm/h): 629.67 7.24 Coriolis Density (lbm/ft3): 81.40 0.19 Upstream R22 Tsat (F): 118.61 0.333 Average Subcooling (F): 14.41 0.720 0.667 0.965 Evap Exit Pressure (psia): 97.93 Evap Exit Avg Temp : 63.23 Exit Superheat (F): 13.74 0.708 Evap Exit Tsat (F): 49.49 0.406

			R TEST SUMMARY SHEET		
DATA FILENAME: a04	0406a.dat	SUMMARY	FILENAME: a040406a.sum		
				Range	
	2		Side Capacity: 28898.20		
1			e Cap (Btu/h): 23756.23		
Indoor Inlet Dew (F): 60.35					
Indoor Exit Dry-Bulb: 63.43					
Indoor Exit Dew (F): 57.96	3 1.02		-		
		Sensib	le Heat Ratio: 0.822	0.0644	
Indoor Airflow (CFM): 1149	.71 20.1	.3	SCFM per Ton: 480.72		
Indoor Airflow (SCFM): 1157					
Evap Inlet Humidity Ratio (
Evap Exit Humidity Ratio (
Barometric Pressure (in HG	,		1 . ,	46	
Air Chamber Nozzle Press					
Evaporator Coil Air Press	ure Dron	(in Motor)	• 1 700 0 000		
- <u>1</u>	are prop	(III Water)	. 1.700 0.000		
		(III water)			
Refrigerant Side Conditions		(III water)			
Refrigerant Side Conditions Expansion Valve		······			
Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia):	274.96	1.279	Ref-side Cap (Btu/h)		
Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia):	274.96	1.279	Ref-side Cap (Btu/h) Ref-side Cap (tons)	: 2.39	0.08
Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia):	274.96	1.279 0.511	Ref-side Cap (Btu/h) Ref-side Cap (tons) Refrigerant Mdot (lbm/h)	: 2.39 : 452.28	0.08 14.65
Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): Upstream Temp (F):	274.96 105.07	1.279 0.511	Ref-side Cap (Btu/h) Ref-side Cap (tons)	: 2.39 : 452.28	0.08 14.65
Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): Upstream Temp (F): Upstream R22 Tsat (F):	274.96 105.07 120.10	1.279 0.511 0.363	Ref-side Cap (Btu/h) Ref-side Cap (tons) Refrigerant Mdot (lbm/h)	: 2.39 : 452.28	0.08 14.65
Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): Upstream Temp (F):	274.96 105.07 120.10	1.279 0.511 0.363	Ref-side Cap (Btu/h) Ref-side Cap (tons) Refrigerant Mdot (lbm/h)	: 2.39 : 452.28	0.08 14.65
Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): Upstream Temp (F): Upstream R22 Tsat (F): Average Subcooling (F):	274.96 105.07 120.10 15.04	1.279 0.511 0.363 0.649	Ref-side Cap (Btu/h) Ref-side Cap (tons) Refrigerant Mdot (lbm/h)	: 2.39 : 452.28	0.08 14.65
Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): Upstream Temp (F): Upstream R22 Tsat (F): Average Subcooling (F): Evap Exit Pressure (psia):	274.96 105.07 120.10 15.04 107.81	1.279 0.511 0.363 0.649 0.303	Ref-side Cap (Btu/h) Ref-side Cap (tons) Refrigerant Mdot (lbm/h)	: 2.39 : 452.28	0.08 14.65
Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): Upstream Temp (F): Upstream R22 Tsat (F): Average Subcooling (F): Evap Exit Pressure (psia): Evap Exit Avg Temp :	274.96 105.07 120.10 15.04 107.81 70.32	1.279 0.511 0.363 0.649 0.303 0.946	Ref-side Cap (Btu/h) Ref-side Cap (tons) Refrigerant Mdot (lbm/h)	: 2.39 : 452.28	0.08 14.65
Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): Upstream Temp (F): Upstream R22 Tsat (F): Average Subcooling (F): Evap Exit Pressure (psia):	274.96 105.07 120.10 15.04 107.81 70.32 15.03	1.279 0.511 0.363 0.649 0.303 0.946 0.948	Ref-side Cap (Btu/h) Ref-side Cap (tons) Refrigerant Mdot (lbm/h)	: 2.39 : 452.28	0.08 14.65

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: b040402b.dat SUMMARY FILENAME: b040402b.sum Range Air-Side Conditions Range Total Air-Side Capacity: 39504.41 778.58 Indoor Dry-Bulb : 79.763 0.63 Sensible Cap (Btu/h): 28482.79 688.71 Indoor Exit Dry-Bulb: 59.632 0.26 Indoor Exit Dry-CE Latent Cap (Btu/h): 11021.62 799.76 EvapAir Delta T (F): 22.39 0.43 Indoor Exit Dew (F): 55.021 0.24 Air/Ref Cap Pront Diff: 0.42 1.91 Sensible Heat Ratio: 0.721 SCFM per Ton: 351.11 0.0173 Indoor Airflow (CFM): 1150.36 15.38 Indoor Airflow (SCFM): 1155.87 15.45 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011287 Wap Infect Humidity Ratio (15H20/15Air):0.009288Evap Exit Humidity Ratio (15H20/15Air):0.009288Barometric Pressure (in HG):29.65Nozzle Temp (F):59.010.32 Air Chamber Nozzle Pressure Drop (in Water): 0.915 0.024 Evaporator Coil Air Pressure Drop (in Water): 1.715 0.000 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 269.24 0.974 Upstream Temp (F): 104.51 0.652 Ref-side Cap (Btu/h) : 39670.12 616.85 0.05 Ref-side Cap (tons): 3.31 Refrigerant Mdot (lbm/h): 623.27 9.62 Coriolis Density (lbm/ft3): 81.43 0.27 Upstream R22 Tsat (F): 118.47 0.281 Average Subcooling (F): 13.96 0.793 0.485 0.929 Evap Exit Pressure (psia): 98.41 Evap Exit Avg Temp : 63.64 Exit Superheat (F): 13.86 0.709 0.294 Evap Exit Tsat (F): 49.78

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: b040407b.dat SUMMARY FILENAME: b040407b.sum Range Range Total Air-Side Capacity: 29255.90 822.80 Air-Side Conditions Indoor Dry-Bulb : 79.329 0.59 Sensible Cap (Btu/h): 22885.70 580.88 Indoor Inlet Dew (F): 60.954 0.52 Indoor Exit Dry-Bulb: 63.454 0.37 Indoor Exit Dov (D) Latent Cap (Btu/h): 6370.21 EvapAir Delta T (F): 18.12 425.88 0.22 Indoor Exit Dew (F): 58.003 0.42 Air/Ref Cap Pront Diff: 1.42 2.38 Sensible Heat Ratio: 0.782 SCFM per Ton: 470.27 0.0113 Indoor Airflow (CFM): 1140.82 24.11 Indoor Airflow (SCFM): 1146.51 24.02 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011457 Evap Exit Humidity Ratio (lbH2O/lbAir):0.010293Barometric Pressure (in HG):29.85Nozzle Temp (F):62.100.62 Air Chamber Nozzle Pressure Drop (in Water): 0.900 0.038 Evaporator Coil Air Pressure Drop (in Water): 1.700 0.000 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 273.21 1.340 Upstream Temp (F): 104.45 0.510 Ref-side Cap (Btu/h) : 29670.07 566.32 0.05 Ref-side Cap (tons): 2.47 Refrigerant Mdot (lbm/h): 466.02 8.15 Coriolis Density (lbm/ft3): 81.61 0.36 Upstream R22 Tsat (F): 119.61 0.382 Average Subcooling (F): 15.15 0.739 0.607 1.244 Evap Exit Pressure (psia): 108.49 Evap Exit Avg Temp : 67.60 Exit Superheat (F): 11.92 1.107 Evap Exit Tsat (F): 55.68 0.342

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040410a.dat SUMMARY FILENAME: a040410a.sum Range Range Total Air-Side Capacity: 41868.75 1269.75 Air-Side Conditions Indoor Dry-Bulb : 80.137 0.67 Sensible Cap (Btu/h): 29034.75 990.29 Indoor Inlet Dew (F): 60.569 0.12 Latent Cap (Btu/h): 12834.01 529.88 Indoor Exit Dry-Bulb: 59.695 0.12 EvapAir Delta T (F): 22.68 0.54 Indoor Exit Dew (F): 54.315 0.11 Air/Ref Cap Pront Diff: 0.57 5.66 Sensible Heat Ratio: 0.693 SCFM per Ton: 333.47 0.0079 Indoor Airflow (CFM): 1148.39 30.81 Indoor Airflow (SCFM): 1163.50 31.34 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011299 Wap Infect Humidity Ratio (15H20/15Air):0.008987Evap Exit Humidity Ratio (15H20/15Air):0.008987Barometric Pressure (in HG):29.85Nozzle Temp (F):58.290.44 Air Chamber Nozzle Pressure Drop (in Water): 0.919 0.049 Evaporator Coil Air Pressure Drop (in Water): 1.635 0.000 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 271.76 1.218 Upstream Temp (F): 105.80 0.768 Ref-side Cap (Btu/h) : 42104.06 1447.15 Ref-side Cap (tons): 3.51 0.12 Refrigerant Mdot (lbm/h): 665.81 23.54 Coriolis Density (lbm/ft3): 82.00 0.58 Upstream R22 Tsat (F): 119.19 0.349 Average Subcooling (F): 13.39 0.856 0.303 1.047 Evap Exit Pressure (psia): 98.72 Evap Exit Avg Temp : 62.09 Exit Superheat (F): 12.13 1.002 Evap Exit Tsat (F): 49.97 0.184

Coil 7 R22, H5326, No Fan

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040506a.dat SUMMARY FILENAME: a040506a.sum Range ir-Side ConditionsRange Total Air-Side Capacity: 29842.95Indoor Dry-Bulb : 80.4780.22Sensible Cap (Btu/h): 24549.15 Air-Side Conditions 280.91 294.40 Indoor Inlet Dew (F): 60.104 0.10 Latent Cap (Btu/h): 5293.80 140.99 Indoor Exit Dry-Bulb: 64.374 0.12 EvapAir Delta T (F): 18.49 Indoor Exit Dew (F): 57.725 0.07 Air/Ref Cap Prcnt Diff: -1.65 Sensible Heat Ratio: 0.823 0.11 2.38 0.0044 Indoor Airflow (CFM): 1203.06 9.21 Indoor Airflow (SCFM): 1205.86 9.40 SCFM per Ton: 484.88 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011097 Evap Exit Humidity Ratio (lbH2O/lbAir): 0.010177 Barometric Pressure (in HG): 29.88 Nozzle Temp (F): 63.84 0.46 Air Chamber Nozzle Pressure Drop (in Water):0.9970.015Evaporator Coil Air Pressure Drop (in Water):0.2240.010 _____ Refrigerant Side Conditions Expansion Valve Ref-side Cap (Btu/h) : 29350.36 597.02 Upstream Pressure (psia): 269.40 0.487 Upstream Temp (F): 104.63 0.304 Ref-side Cap (tons): 2.45 0.05 Refrigerant Mdot (lbm/h): 461.40 8.79 Coriolis Density (lbm/ft3): 81.70 0.33 0.140 Upstream R22 Tsat (F): 118.51 Average Subcooling (F): 13.89 0.363 Evap Exit Pressure (psia): 84.38 0.303 Evap Exit Avg Temp : 1.624 52.33 Exit Superheat (F): 11.56 1.537 0.206 Evap Exit Tsat (F): 40.77

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040507a.dat SUMMARY FILENAME: a040507a.sum Range Range Total Air-Side Capacity: 25857.20 551.41 Air-Side Conditions Indoor Dry-Bulb : 79.848 0.35 Sensible Cap (Btu/h): 22239.56 436.75 Indoor Inlet Dew (F): 60.543 0.10 Indoor Exit Dry-Bulb: 65.465 0.23 Latent Cap (Btu/h): 3617.64 EvapAir Delta T (F): 16.75 217.35 0.00 Indoor Exit Dew (F): 58.962 0.11 Air/Ref Cap Pront Diff: -1.85 2.08 Sensible Heat Ratio: 0.860 SCFM per Ton: 559.05 0.0073 Indoor Airflow (CFM): 1206.00 22.60 Indoor Airflow (SCFM): 1204.62 23.63 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011289 Evap Exit Humidity Ratio (lbH2O/lbAir): 0.010659 Barometric Pressure (in HG): 29.85 Nozzle Temp (F): 64.90 0.46 Air Chamber Nozzle Pressure Drop (in Water): 0.999 0.038 Evaporator Coil Air Pressure Drop (in Water): 0.221 0.010 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 272.58 0.731 Upstream Temp (F): 105.77 0.300 Ref-side Cap (Btu/h) : 25378.56 556.29 0.05 Ref-side Cap (tons): 2.11 Refrigerant Mdot (lbm/h): 401.25 8.61 Coriolis Density (lbm/ft3): 82.11 0.16 Upstream R22 Tsat (F): 119.43 0.209 Average Subcooling (F): 13.66 0.282 0.364 0.960 Evap Exit Pressure (psia): 90.38 Evap Exit Avg Temp : 56.10 Exit Superheat (F): 11.35 0.862 0.235 Evap Exit Tsat (F): 44.75

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040510a.dat SUMMARY FILENAME: a040510a.sum Range Air-Side Conditions Range Total Air-Side Capacity: 22002.44 704.07 Indoor Dry-Bulb : 79.966 0.46 Sensible Cap (Btu/h): 20601.59 599.35 Indoor Exit Dry-Bulb: 66.622 0.23 Indoor Exit Dew (F): 50.55 Latent Cap (Btu/h): 1400.84 EvapAir Delta T (F): 15.54 220.96 0.43 Indoor Exit Dew (F): 59.592 0.06 Air/Ref Cap Pront Diff: -4.94 3.95 Sensible Heat Ratio: 0.936 SCFM per Ton: 656.15 0.0094 Indoor Airflow (CFM): 1210.01 17.49 Indoor Airflow (SCFM): 1203.07 17.29 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011188 Evap Exit Humidity Ratio (lbH2O/lbAir): 0.010943 Barometric Pressure (in HG): 29.75 Nozzle Temp (F): 65.48 0.59 Air Chamber Nozzle Pressure Drop (in Water): 1.001 0.029 Evaporator Coil Air Pressure Drop (in Water): 0.215 0.008 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 266.78 2.071 Upstream Temp (F): 104.31 0.680 Ref-side Cap (Btu/h) : 20914.67 485.59 Ref-side Cap (tons): 1.74 Refrigerant Mdot (lbm/h): 328.26 0.04 7.24 Coriolis Density (lbm/ft3): 81.79 0.31 Upstream R22 Tsat (F): 117.76 0.601 Average Subcooling (F): 13.45 0.686 0.546 1.807 Evap Exit Pressure (psia): 98.08 Evap Exit Avg Temp : 63.42 Exit Superheat (F): 13.85 1.659 0.332 Evap Exit Tsat (F): 49.58

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040513a.dat SUMMARY FILENAME: a040513a.sum Range Range Total Air-Side Capacity: 29846.20 Air-Side Conditions 378.77 Indoor Dry-Bulb : 79.918 0.24 Sensible Cap (Btu/h): 24101.01 316.28 Indoor Inlet Dew (F): 60.550 0.10 Indoor Exit Dry-Bulb: 64.014 0.17 Latent Cap (Btu/h): 5745.19 EvapAir Delta T (F): 18.08 232.49 0.11 Indoor Exit Dew (F): 58.012 0.08 Air/Ref Cap Pront Diff: -0.50 3.91 Sensible Heat Ratio: 0.808 SCFM per Ton: 486.62 0.0063 Indoor Airflow (CFM): 1207.72 16.23 Indoor Airflow (SCFM): 1210.32 15.90 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011291 Evap Exit Humidity Ratio (lbH2O/lbAir): 0.010296 Barometric Pressure (in HG): 29.85 Nozzle Temp (F): 63.29 0.62 Air Chamber Nozzle Pressure Drop (in Water): 1.005 0.027 Evaporator Coil Air Pressure Drop (in Water): 0.219 0.010 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 272.31 0.487 Upstream Temp (F): 104.46 0.455 Ref-side Cap (Btu/h) : 29695.17 974.02 Ref-side Cap (tons): 2.47 Refrigerant Mdot (lbm/h): 466.43 0.08 15.02 Coriolis Density (lbm/ft3): 81.86 1.27 Upstream R22 Tsat (F): 119.35 0.139 Average Subcooling (F): 14.89 0.525 0.485 1.583 Evap Exit Pressure (psia): 83.66 Evap Exit Avg Temp : 55.15 Exit Superheat (F): 14.88 1.532 Evap Exit Tsat (F): 40.28 0.333

DATA FILENAME: b04 Air-Side Conditions	Range 4 0.18 7 0.15 4 0.24 2 0.08 .24 18.3 .31 18.2	SUMMAR Total Air Sensib Late EvapA Air/Ref Sensi 2 1 (0	ir Delta T (F): 15.32 Cap Prcnt Diff: -5.72 ble Heat Ratio: 0.923 SCFM per Ton: 656.24 .075 lb/ft3 standard air)	243.13 0.33 3.59	
Evap Exit Humidity Ratio (lbH2O/lbA	ir): 0.	011055	1.4	
Barometric Pressure (in HG Air Chamber Nozzle Press Evaporator Coil Air Press	ure Drop	(in Water): 0.995 0.030	14	
Refrigerant Side Conditions					
Expansion Valve					
Upstream Pressure (psia):					
Upstream Temp (F):	105.77	0.454	Ref-side Cap (tons) Refrigerant Mdot (lbm/h)		
			Coriolis Density (lbm/ft3)		
Upstream R22 Tsat (F):					
Average Subcooling (F):	12.56	0.584			
Evap Exit Pressure (psia):					
Evap Exit Avg Temp :					
Exit Superheat (F):					
Evap Exit Tsat (F):	50.09	0.110			

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: b040511b.dat SUMMARY FILENAME: b040511b.sum Range Range Total Air-Side Capacity: 25476.71 Air-Side Conditions 634.85 Indoor Dry-Bulb : 80.144 0.24 Sensible Cap (Btu/h): 21755.04 534.33 Latent Cap (Btu/h): 3721.67 EvapAir Delta T (F): 16.35 Indoor Inlet Dew (F): 60.483 0.06 Indoor Exit Dry-Bulb: 65.840 0.17 200.30 0.22 Indoor Exit Dew (F): 58.853 0.03 Air/Ref Cap Pront Diff: -3.61 2.99 Sensible Heat Ratio: 0.854 SCFM per Ton: 568.77 0.0060 Indoor Airflow (CFM): 1207.11 13.97 Indoor Airflow (SCFM): 1207.54 13.81 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011245 Evap Exit Humidity Ratio (lbH2O/lbAir): 0.010599 Barometric Pressure (in HG): 29.90 Nozzle Temp (F): 65.02 0.19 Air Chamber Nozzle Pressure Drop (in Water): 1.002 0.023 Evaporator Coil Air Pressure Drop (in Water): 0.213 0.009 _____ _____ _____ Refrigerant Side Conditions Expansion Valve 0.731 0.354 Upstream Pressure (psia): 271.40 Upstream Temp (F): 106.02 Ref-side Cap (Btu/h) : 24555.06 415.26 Ref-side Cap (tons): 2.05 Refrigerant Mdot (lbm/h): 388.73 0.03 6.59 Coriolis Density (lbm/ft3): 82.22 0.41 Upstream R22 Tsat (F): 119.09 0.209 Average Subcooling (F): 13.07 0.224 0.303 1.001 Evap Exit Pressure (psia): 90.93 Evap Exit Avg Temp : 58.19 Exit Superheat (F): 13.08 1.080 0.195 Evap Exit Tsat (F): 45.11

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: b040513b.dat SUMMARY FILENAME: b040513b.sum Range Air-Side Conditions Range Total Air-Side Capacity: 29800.83 455.45 Indoor Dry-Bulb : 79.832 0.30 Sensible Cap (Btu/h): 24060.94 441.52 0.05 Latent Cap (Btu/h): 5739.89 EvapAir Delta T (F): 18.06 Indoor Inlet Dew (F): 60.562 112.39 Indoor Exit Dry-Bulb: 63.937 0.21 Indoor Exit Dew (F): 58.025 0.05 Air/Ref Cap Pront Diff: -1.08 3.85 Sensible Heat Ratio: 0.807 SCFM per Ton: 486.99 0.0048 Indoor Airflow (CFM): 1206.87 15.11 Indoor Airflow (SCFM): 1209.38 15.22 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011296 Evap Exit Humidity Ratio (lbH2O/lbAir): 0.010301 Barometric Pressure (in HG): 29.85 Nozzle Temp (F): 63.32 0.46 Air Chamber Nozzle Pressure Drop (in Water): 1.003 0.025 Evaporator Coil Air Pressure Drop (in Water): 0.219 0.008 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 272.41 Upstream Temp (F): 104.49 0.731 0.828 Ref-side Cap (Btu/h) : 29478.53 993.29 Ref-side Cap (tons): 2.46 Refrigerant Mdot (lbm/h): 463.10 0.08 14.01 1.00 Coriolis Density (lbm/ft3): 81.72 Upstream R22 Tsat (F): 119.38 0.209 Average Subcooling (F): 14.89 0.849 0.303 1.352 Evap Exit Pressure (psia): 83.74 Evap Exit Avg Temp : 54.77 Exit Superheat (F): 14.43 1.352 0.208 Evap Exit Tsat (F): 40.33

Coil 8 R22, H5321, No Fan

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040521a.dat SUMMARY FILENAME: a040521a.sum Range ir-Side Conditions Range Total Air-Side Capacity: 34023.81 Indoor Dry-Bulb : 80.133 0.15 Sensible Cap (Btu/h): 29126.82 Air-Side Conditions 981.82 963.08 Indoor Inlet Dew (F): 60.562 0.02 Latent Cap (Btu/h): 4896.99 115.91 Indoor Exit Dry-Bulb: 63.116 0.15 EvapAir Delta T (F): Indoor Exit Dew (F): 58.688 0.03 Air/Ref Cap Pront Diff: EvapAir Delta T (F): 19.15 0.43 9.58 3.56 Sensible Heat Ratio: 0.856 0.0036 Indoor Airflow (CFM): 1375.64 17.99 Indoor Airflow (SCFM): 1380.73 17.33 SCFM per Ton: 486.97 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011300 Evap Exit Humidity Ratio (lbH2O/lbAir): 0.010557 Nozzle Temp (F): 62.11 0.60 Barometric Pressure (in HG): 29.84 Air Chamber Nozzle Pressure Drop (in Water):1.3040.033Evaporator Coil Air Pressure Drop (in Water):0.3120.015 _____ Refrigerant Side Conditions Expansion Valve Ref-side Cap (Btu/h) : 37280.82 519.41 Upstream Pressure (psia): 265.11 0.670 Ref-side Cap (tons): 3.11 0.04 Upstream Temp (F): 106.24 0.313 Refrigerant Mdot (lbm/h): 590.85 8.43 Coriolis Density (lbm/ft3): 72.75 0.43 Upstream R22 Tsat (F): 117.27 0.195 Average Subcooling (F): 11.03 0.384 Evap Exit Pressure (psia): 90.52 0.243 Evap Exit Avg Temp : 1.512 56.58 Exit Superheat (F): 11.74 1.521 0.157 Evap Exit Tsat (F): 44.84

DATA FILENAME: a04 Air-Side Conditions Indoor Dry-Bulb : 80.12 Indoor Inlet Dew (F): 60.48 Indoor Exit Dry-Bulb: 60.96 Indoor Exit Dew (F): 56.92 Indoor Airflow (CFM): 1373	0525a.dat Range 1 0.31 3 0.06 7 0.15 3 0.05 .54 11.2	SUMMAR Total Air Sensib Late EvapA Air/Ref Sensi	ir Delta T (F): 21.33 Cap Prcnt Diff: 2.90 ble Heat Ratio: 0.782 SCFM per Ton: 399.68	869.32 215.10 0.43 2.82	
Indoor Airflow (SCFM): 1385					
Evap Inlet Humidity Ratio (Evap Exit Humidity Ratio (
Barometric Pressure (in HG				16	
Air Chamber Nozzle Press	-				
Evaporator Coil Air Press	ure Drop	(in Water): 0.316 0.008		
Refrigerant Side Conditions Expansion Valve					
Upstream Pressure (psia):	269 25	0 853	Ref-side Cap (Btu/h)	· 42791 57	751 47
			Ref-side Cap (tons)		
1 1 · · ·			Refrigerant Mdot (lbm/h)	: 677.74	12.09
			Coriolis Density (lbm/ft3)	: 82.42	0.75
Upstream R22 Tsat (F):					
Average Subcooling (F):	12.36	0.273			
Evap Exit Pressure (psia):	84.72	0.243			
Evap Exit Avg Temp :					
Exit Superheat (F):					
Evap Exit Tsat (F):	41.00	0.165			

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040526a.dat SUMMARY FILENAME: a040526a.sum Range Air-Side Conditions Range Total Air-Side Capacity: 29513.51 480.65 Indoor Dry-Bulb : 79.841 0.15 Sensible Cap (Btu/h): 25443.70 460.28
 Indoor Inlet Dew (F): 60.427
 0.06
 Latent Cap (Btu/h): 4069.81

 Indoor Exit Dry-Bulb: 65.396
 0.18
 EvapAir Delta T (F): 16.71
 275.45 0.22 Indoor Exit Dew (F): 58.878 0.08 Air/Ref Cap Pront Diff: -3.10 2.06 Sensible Heat Ratio: 0.862 SCFM per Ton: 561.88 0.0083 Indoor Airflow (CFM): 1388.51 16.29 Indoor Airflow (SCFM): 1381.91 16.94 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011291 Evap Exit Humidity Ratio (lbH2O/lbAir): 0.010674 Barometric Pressure (in HG): 29.72 Nozzle Temp (F): 64.39 0.34 Air Chamber Nozzle Pressure Drop (in Water): 1.317 0.031 Evaporator Coil Air Pressure Drop (in Water): 0.312 0.016 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 269.95 Upstream Temp (F): 105.86 0.731 0.390 Ref-side Cap (Btu/h) : 28597.29 566.54 Ref-side Cap (tons): 2.38 Refrigerant Mdot (lbm/h): 452.35 0.05 8.52 Coriolis Density (lbm/ft3): 82.50 0.25 Upstream R22 Tsat (F): 118.67 0.210 Average Subcooling (F): 12.82 0.390 0.364 1.240 Evap Exit Pressure (psia): 97.57 Evap Exit Avg Temp : 64.00 Exit Superheat (F): 14.73 1.388 Evap Exit Tsat (F): 49.27 0.222

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040527a.dat SUMMARY FILENAME: a040527a.sum Range Range Total Air-Side Capacity: 41721.31 1434.02 Air-Side Conditions Indoor Dry-Bulb : 80.055 0.17 Sensible Cap (Btu/h): 33072.64 393.65
 Indoor Inlet Dew (F): 60.304
 0.60
 Latent Cap (Btu/h): 8648.66
 1514.12

 Indoor Exit Dry-Bulb: 60.780
 0.20
 EvapAir Delta T (F): 21.55
 0.22
 Indoor Exit Dew (F): 56.914 0.09 Air/Ref Cap Prcnt Diff: 3.26 5.66 Sensible Heat Ratio: 0.793 SCFM per Ton: 400.82 0.0305 Indoor Airflow (CFM): 1381.48 15.68 Indoor Airflow (SCFM): 1393.57 15.10 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011192 Evap Exit Humidity Ratio (lbH2O/lbAir): 0.009890 Barometric Pressure (in HG): 29.85 Nozzle Temp (F): 59.86 0.53 Air Chamber Nozzle Pressure Drop (in Water): 1.321 0.029 Evaporator Coil Air Pressure Drop (in Water): 0.318 0.014 _____ _____ _____ Refrigerant Side Conditions Expansion Valve 0.731 0.543 Upstream Pressure (psia): 267.87 Upstream Temp (F): 105.13 Ref-side Cap (Btu/h) : 43077.28 1092.28 Ref-side Cap (tons): 3.59 0.09 Refrigerant Mdot (lbm/h): 678.91 17.22 0.09 Coriolis Density (lbm/ft3): 82.18 0.34 Upstream R22 Tsat (F): 118.07 0.211 Average Subcooling (F): 12.94 0.684 0.485 1.507 Evap Exit Pressure (psia): 84.34 Evap Exit Avg Temp : 55.85 1.507 Exit Superheat (F): 15.11 0.330 Evap Exit Tsat (F): 40.74

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: b040527b.dat SUMMARY FILENAME: b040527b.sum Range Air-Side Conditions Range Total Air-Side Capacity: 41707.19 1020.24 Indoor Dry-Bulb : 79.862 0.19 Sensible Cap (Btu/h): 32752.75 819.05 Indoor Inlet Dew (F): 60.391 0.07 Latent Cap (Btu/h): 8954.44 Indoor Exit Dry-Bulb: 60.734 0.09 EvapAir Delta T (F): 21.32 263.78 0.32 Indoor Exit Dew (F): 56.888 0.03 Air/Ref Cap Pront Diff: 3.12 3.21 Sensible Heat Ratio: 0.785 SCFM per Ton: 401.39 0.0048 Indoor Airflow (CFM): 1382.69 15.13 (0.075 lb/ft3 standard air) Indoor Airflow (SCFM): 1395.06 15.46 Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011227 Evap Exit Humidity Ratio (lbH2O/lbAir): 0.009881 Barometric Pressure (in HG): 29.85 Nozzle Temp (F): 59.77 0.14 Air Chamber Nozzle Pressure Drop (in Water): 1.324 0.029 Evaporator Coil Air Pressure Drop (in Water): 0.317 0.012 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 268.09 Upstream Temp (F): 105.41 0.731 0.294 Ref-side Cap (Btu/h) : 43005.16 831.09 Ref-side Cap (tons): 3.58 Refrigerant Mdot (lbm/h): 678.73 0.07 12.46 Coriolis Density (lbm/ft3): 82.29 0.47 Upstream R22 Tsat (F): 118.14 0.211 Average Subcooling (F): 12.72 0.343 0.243 1.860 Evap Exit Pressure (psia): 84.17 Evap Exit Avg Temp : 54.43 Exit Superheat (F): 13.81 1.943 Evap Exit Tsat (F): 40.63 0.165

DATA FILENAME: a04 Air-Side Conditions Indoor Dry-Bulb : 80.15 Indoor Inlet Dew (F): 60.54 Indoor Exit Dry-Bulb: 63.31 Indoor Exit Dew (F): 58.33 Indoor Airflow (CFM): 1390 Indoor Airflow (SCFM): 1395	0603a.dat Range 0 0.25 1 0.06 0 0.17 1 0.24 .38 10.1 .23 10.2	E SUMMAR Total Air Sensib Late EvapA Air/Ref Sensi 2 23 (0	ir Delta T (F): 18.99 Cap Prcnt Diff: 2.84 ble Heat Ratio: 0.834 SCFM per Ton: 478.63 .075 lb/ft3 standard air)	519.27 0.32 2.75	
Evap Inlet Humidity Ratio (
Evap Exit Humidity Ratio (Barometric Pressure (in HG				46	
Air Chamber Nozzle Press	,		1, ,	10	
Evaporator Coil Air Press	ure Drop	(in Water): 0.312 0.009		
Refrigerant Side Conditions Expansion Valve					
Upstream Pressure (psia):	273.51	0.792	Ref-side Cap (Btu/h)	: 35974.64	595.49
Upstream Temp (F):	105.60	0.455	Ref-side Cap (tons)		
			Refrigerant Mdot (lbm/h)		
Upstream R22 Tsat (F):	119 69		Coriolis Density (lbm/ft3)	: 82.41	0.16
Average Subcooling (F):					
	,				
Evap Exit Pressure (psia):	91.83	0.425			
Evap Exit Avg Temp :					
Exit Superheat (F):					
Evap Exit Tsat (F):	45.69	0.271			

			R TEST SUMMARY SHEET FILENAME: a040607a.sum	
			Range	
Air-Side Conditions	Range	Total Air-	Side Capacity: 27090.45 778.33	
Indoor Dry-Bulb : 80.20	5 0.17	Sensibl	e Cap (Btu/h): 24679.42 794.58	
			t Cap (Btu/h): 2411.02 212.56	
			r Delta T (F): 16.11 0.43	
Indoor Exit Dew (F): 59.61	7 0.05	Air/Ref C	ap Prcnt Diff: -1.12 3.30	
			le Heat Ratio: 0.911 0.0085	
Indoor Airflow (CFM): 1395 Indoor Airflow (SCFM): 1390	.31 13.7	1	SCFM per Ton: 615.80	
Evap Inlet Humidity Ratio (
Evap Exit Humidity Ratio (
	,		zle Temp (F): 65.33 0.57	
Air Chamber Nozzle Press	-			
Evaporator Coil Air Press	ure Drop	(in Water)	: 0.307 0.013	
Refrigerant Side Conditions				
Expansion Valve				
-	273 06	0 197	Ref-side Cap (Btu/h) : 26784.	01 150 70
			Ref-side Cap (btu/ii) : 20704. Ref-side Cap (tons): 2.	
opscream remp (r).	103.00	0.515	Refrigerant Mdot (lbm/h): 423.	
		C	oriolis Density (lbm/ft3): 82.	
Upstream R22 Tsat (F):	119 56		0110113 Density (10m/103). 02.	10 0.11
Average Subcooling (F):		0.100		
include subcooting (1).	13 89	0 315		
	13.89	0.315		
Evap Exit Pressure (psia):				
Evap Exit Pressure (psia): Evap Exit Avg Temp :	99.96	0.243		
Evap Exit Avg Temp :	99.96 64.36	0.243 1.181		
	99.96 64.36 13.65	0.243 1.181 1.181		

Coil 9 <u>R410A, A01154, Fan</u>

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040716a.dat SUMMARY FILENAME: a040716a.sum Range ir-Side Conditions Range Total Air-Side Capacity: 19952.67 Indoor Dry-Bulb : 79.986 0.14 Sensible Cap (Btu/h): 12845.02 Air-Side Conditions 354.03 284.44 Indoor Inlet Dew (F): 60.436 0.06 Latent Cap (Btu/h): 7107.65 136.91 Indoor Exit Dry-Bulb: 58.954 0.16 EvapAir Delta T (F): Indoor Exit Dew (F): 52.186 0.10 Air/Ref Cap Pront Diff: EvapAir Delta T (F): 23.24 0.32 Air/Ref Cap Prcnt Diff: 0.48 Sensible Heat Ratio: 0.644 2.14 0.0049 Indoor Airflow (CFM): 501.58 5.80 Indoor Airflow (SCFM): 502.60 6.20 SCFM per Ton: 302.28 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011330 Evap Exit Humidity Ratio (lbH2O/lbAir): 0.008365 Barometric Pressure (in HG): 29.63 Nozzle Temp (F): 60.37 0.82 Air Chamber Nozzle Pressure Drop (in Water): 0.905 0.021 Evaporator Coil Air Pressure Drop (in Water): 1.940 0.000 _____ Refrigerant Side Conditions Expansion Valve Ref-side Cap (Btu/h) : 20047.22 Upstream Pressure (psia): 425.06 2.071 377.05 Upstream Temp (F): 104.08 0.289 Ref-side Cap (tons): 1.67 frigerant Mdot (lbm/h): 313.67 0.03 Refrigerant Mdot (lbm/h): 313.67 5.95 Coriolis Density (lbm/ft3): 72.80 0.16 Upstream R22 Tsat (F): 118.59 0.377 Average Subcooling (F): 14.52 0.458 Evap Exit Pressure (psia): 148.69 0.728 Evap Exit Avg Temp : 61.26 0.676 Exit Superheat (F): 14.55 0.697 Evap Exit Tsat (F): 46.71 0.295

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040728a.dat SUMMARY FILENAME: a040728a.sum Range Range Total Air-Side Capacity: 13018.25 Air-Side Conditions 438.26

 Indoor Dry-Bulb:
 80.075
 0.20
 Sensible Cap (Btu/h):
 9855.61

 Noor Inlet Dew (F):
 60.371
 0.05
 Latent Cap (Btu/h):
 3162.64

 Noor Exit Dry-Bulb:
 64.382
 0.22
 EvapAir Delta T (F):
 17.85

 293.12 Indoor Inlet Dew (F): 60.371 0.05 Indoor Exit Dry-Bulb: 64.382 0.22 233.87 0.43 Indoor Exit Dew (F): 56.937 0.26 Air/Ref Cap Prcnt Diff: 3.39 6.66 Sensible Heat Ratio: 0.757 SCFM per Ton: 462.20 0.0126 Indoor Airflow (CFM): 502.39 5.71 Indoor Airflow (SCFM): 501.42 5.74 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011241 Evap Exit Humidity Ratio (lbH20/lbAir):0.009919Barometric Pressure (in HG):29.79Nozzle Temp (F):64.770.64 Air Chamber Nozzle Pressure Drop (in Water): 0.904 0.020 0.000 Evaporator Coil Air Pressure Drop (in Water): 2.000 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 425.00 1.279 Upstream Temp (F): 104.53 0.350 Ref-side Cap (Btu/h) : 13458.06 676.75 Ref-side Cap (tons): 1.12 Refrigerant Mdot (lbm/h): 211.23 0.06 10.62 Coriolis Density (lbm/ft3): 72.85 0.36 Upstream R22 Tsat (F): 118.58 Average Subcooling (F): 14.05 0.233 0.483 0.485 1.716 Evap Exit Pressure (psia): 160.83 Evap Exit Avg Temp : 64.99 Exit Superheat (F): 13.50 1.902 Evap Exit Tsat (F): 51.49 0.186

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040729a.dat SUMMARY FILENAME: a040729a.sum Range Air-Side Conditions Range Total Air-Side Capacity: 20056.82 491.41 Indoor Dry-Bulb : 79.633 0.40 Sensible Cap (Btu/h): 12753.21 283.59 Indoor Inlet Dew (F): 60.733 0.10 Indoor Exit Dry-Bulb: 58.829 0.13 Latent Cap (Btu/h): 7303.61 EvapAir Delta T (F): 22.94 246.33 0.32 Indoor Exit Dew (F): 52.283 0.34 Air/Ref Cap Pront Diff: 2.06 7.48 Sensible Heat Ratio: 0.636 SCFM per Ton: 302.43 0.0039 Indoor Airflow (CFM): 499.63 5.05 Indoor Airflow (SCFM): 505.48 4.62 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011351 Evap Exit Humidity Ratio (lbH2O/lbAir): 0.008322 Barometric Pressure (in HG): 29.89 Nozzle Temp (F): 59.92 0.55 Air Chamber Nozzle Pressure Drop (in Water): 0.906 0.017 Evaporator Coil Air Pressure Drop (in Water): 2.000 0.000 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 420.74 5.177 Upstream Temp (F): 105.86 2.763 Ref-side Cap (Btu/h) : 20469.27 1264.18 Ref-side Cap (tons): 1.71 Refrigerant Mdot (lbm/h): 324.24 0.11 14.01 Coriolis Density (lbm/ft3): 73.10 0.81 Upstream R22 Tsat (F): 117.80 Average Subcooling (F): 11.95 0.947 3.591 Exit Pressure (psia): 145.54 2.669 Evap Exit Avg Temp : 59.76 10.064 Exit Superheat (F): 14.34 11.159 Evap Exit Pressure (psia): 145.54 Evap Exit Tsat (F): 45.42 1.095

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: b040729b.dat SUMMARY FILENAME: b040729b.sum Range Range Total Air-Side Capacity: 20078.83 Air-Side Conditions 368.42 Indoor Dry-Bulb : 80.044 0.28 Sensible Cap (Btu/h): 12900.77 277.15 Indoor Inlet Dew (F): 60.663 0.10 Indoor Exit Dry-Bulb: 59.059 0.12 Latent Cap (Btu/h): 7178.06 EvapAir Delta T (F): 23.24 142.28 0.32 Indoor Exit Dew (F): 52.348 0.08 Air/Ref Cap Pront Diff: 2.43 3.30 Sensible Heat Ratio: 0.643 SCFM per Ton: 301.73 0.0043 Indoor Airflow (CFM): 499.25 5.00 Indoor Airflow (SCFM): 504.86 4.90 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011322 Evap Exit Humidity Ratio (lbH2O/lbAir): 0.008341 Barometric Pressure (in HG): 29.89 Nozzle Temp (F): 60.17 0.83 Air Chamber Nozzle Pressure Drop (in Water): 0.904 0.018 0.000 Evaporator Coil Air Pressure Drop (in Water): 2.000 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 422.34 Upstream Temp (F): 105.76 0.853 0.454 Ref-side Cap (Btu/h) : 20565.08 359.86 Ref-side Cap (tons): 1.71 Refrigerant Mdot (lbm/h): 325.54 0.03 6.05 Coriolis Density (lbm/ft3): 73.13 0.23 Upstream R22 Tsat (F): 118.10 Average Subcooling (F): 12.34 0.156 0.365 0.303 1.633 Evap Exit Pressure (psia): 146.06 Evap Exit Avg Temp : 58.79 Exit Superheat (F): 13.15 1.633 Evap Exit Tsat (F): 45.64 0.125

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040730a.dat SUMMARY FILENAME: a040730a.sum Range Range Total Air-Side Capacity: 23873.45 Air-Side Conditions 528.34 Indoor Dry-Bulb : 79.875 0.22 Sensible Cap (Btu/h): 14650.46 408.94
 Indoor Inlet Dew (F): 60.410
 0.10
 Latent Cap (Btu/h): 9222.99

 Indoor Exit Dry-Bulb: 55.759
 0.09
 EvapAir Delta T (F): 26.22
 136.03 0.43 Indoor Exit Dew (F): 49.191 0.05 Air/Ref Cap Prcnt Diff: 2.59 2.58 Sensible Heat Ratio: 0.614 SCFM per Ton: 255.62 0.0054 Indoor Airflow (CFM): 498.81 5.64 Indoor Airflow (SCFM): 508.54 5.84 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011196 Evap Exit Humidity Ratio (lbH2O/lbAir): 0.007394 Barometric Pressure (in HG): 29.95 Nozzle Temp (F): 57.28 0.79 Air Chamber Nozzle Pressure Drop (in Water): 0.910 0.021 0.000 Evaporator Coil Air Pressure Drop (in Water): 2.000 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 420.09 0.975 Upstream Temp (F): 104.60 0.341 Ref-side Cap (Btu/h) : 24489.87 230.39 0.02 Ref-side Cap (tons): 2.04 Refrigerant Mdot (lbm/h): 384.57 3.21 Coriolis Density (lbm/ft3): 72.80 0.27 Upstream R22 Tsat (F): 117.68 Average Subcooling (F): 13.08 0.179 0.374 0.425 0.591 Evap Exit Pressure (psia): 138.64 Evap Exit Avg Temp : 56.11 Exit Superheat (F): 13.59 0.581 0.181 Evap Exit Tsat (F): 42.53

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040803a.dat SUMMARY FILENAME: a040803a.sum Range Range Total Air-Side Capacity: 15230.41 Air-Side Conditions 604.05 Indoor Dry-Bulb : 80.216 0.47 Sensible Cap (Btu/h): 11003.77 360.44 Indoor Inlet Dew (F): 60.383 0.44 Indoor Exit Dry-Bulb: 62.392 0.27 Latent Cap (Btu/h): 4226.64 EvapAir Delta T (F): 19.91 435.63 0.43 Indoor Exit Dew (F): 55.700 0.25 Air/Ref Cap Pront Diff: 3.44 7.17 Sensible Heat Ratio: 0.722 SCFM per Ton: 395.56 0.0211 Indoor Airflow (CFM): 500.37 5.94 Indoor Airflow (SCFM): 502.05 5.68 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011227 Wap fillet Humidity Ratio (lbH20/lbAir):0.009462Barometric Pressure (in HG):29.84Nozzle Temp (F):63.020.70 Air Chamber Nozzle Pressure Drop (in Water): 0.901 0.021 0.000 Evaporator Coil Air Pressure Drop (in Water): 2.000 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 426.42 4.507 Upstream Temp (F): 105.37 1.638 Ref-side Cap (Btu/h) : 15753.76 782.81 Ref-side Cap (tons): 1.31 Refrigerant Mdot (lbm/h): 248.70 0.07 14.29 Coriolis Density (lbm/ft3): 73.10 0.60 Upstream R22 Tsat (F): 118.84 Average Subcooling (F): 13.48 0.819 1.173 1.213 3.001 Evap Exit Pressure (psia): 159.78 Evap Exit Avg Temp : 65.49 Exit Superheat (F): 14.40 3.292 Evap Exit Tsat (F): 51.09 0.466

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: b040803b.dat SUMMARY FILENAME: b040803b.sum Range Range Total Air-Side Capacity: 15328.62 Air-Side Conditions 177.88 Indoor Dry-Bulb : 80.106 0.21 Sensible Cap (Btu/h): 10983.96 159.46 Indoor Inlet Dew (F): 60.463 0.05 Indoor Exit Dry-Bulb: 62.313 0.11 Latent Cap (Btu/h): 4344.66 EvapAir Delta T (F): 19.86 70.27 0.22 Indoor Exit Dew (F): 55.656 0.03 Air/Ref Cap Pront Diff: 2.61 3.99 Sensible Heat Ratio: 0.717 SCFM per Ton: 393.29 0.0044 Indoor Airflow (CFM): 500.68 5.04 Indoor Airflow (SCFM): 502.38 4.71 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011259 Wap Infect Humidity Ratio (15H20/15Air):0.009447Evap Exit Humidity Ratio (15H20/15Air):0.009447Barometric Pressure (in HG):29.84Nozzle Temp (F):63.000.62 Air Chamber Nozzle Pressure Drop (in Water): 0.903 0.017 0.000 Evaporator Coil Air Pressure Drop (in Water): 2.000 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 427.81 1.766 Upstream Temp (F): 105.94 0.429 Ref-side Cap (Btu/h) : 15728.51 604.89 0.05 Ref-side Cap (tons): 1.31 Refrigerant Mdot (lbm/h): 249.30 9.07 Coriolis Density (lbm/ft3): 73.21 0.21 Upstream R22 Tsat (F): 119.09 Average Subcooling (F): 13.15 0.320 0.518 0.243 Evap Exit Pressure (psia): 159.82 Evap Exit Avg Temp : 65.51 Exit Superheat (F): 14.41 1.029 1.122 Evap Exit Tsat (F): 51.10 0.093

DOE/ARI MIX-MATCH EVAPORATOR TEST SUMMARY SHEET DATA FILENAME: a040817a.dat SUMMARY FILENAME: a040817a.sum Range Range Total Air-Side Capacity: 11007.81 Air-Side Conditions 265.30 Indoor Dry-Bulb : 79.944 0.34 Sensible Cap (Btu/h): 9076.99 Noor Inlet Dew (F): 60.380 0.15 Latent Cap (Btu/h): 1930.83 Noor Exit Dry-Bulb: 65.709 0.17 EvapAir Delta T (F): 16.35 221.25 Indoor Inlet Dew (F): 60.380 0.15 Indoor Exit Dry-Bulb: 65.709 0.17 110.83 0.22 Indoor Exit Dew (F): 58.334 0.18 Air/Ref Cap Pront Diff: 5.15 3.35 Sensible Heat Ratio: 0.825 SCFM per Ton: 549.33 0.0077 Indoor Airflow (CFM): 504.95 6.74 Indoor Airflow (SCFM): 503.91 7.26 (0.075 lb/ft3 standard air) Evap Inlet Humidity Ratio (lbH2O/lbAir): 0.011211 Evap Exit Humidity Ratio (lbH20/lbAir):0.010407Barometric Pressure (in HG):29.88Nozzle Temp (F):66.270.55 Air Chamber Nozzle Pressure Drop (in Water): 0.913 0.025 Evaporator Coil Air Pressure Drop (in Water): 2.000 0.000 _____ _____ _____ Refrigerant Side Conditions Expansion Valve Upstream Pressure (psia): 432.75 Upstream Temp (F): 104.11 1.157 0.487 Ref-side Cap (Btu/h) : 11574.22 244.37 0.02 Ref-side Cap (tons): 0.96 Refrigerant Mdot (lbm/h): 181.14 3.66 Coriolis Density (lbm/ft3): 72.91 0.21 Upstream R22 Tsat (F): 119.98 0.208 Average Subcooling (F): 15.87 0.596 0.728 0.893 Evap Exit Pressure (psia): 167.22 Evap Exit Avg Temp : 67.73 Exit Superheat (F): 13.83 0.983 Evap Exit Tsat (F): 53.90 0.270