

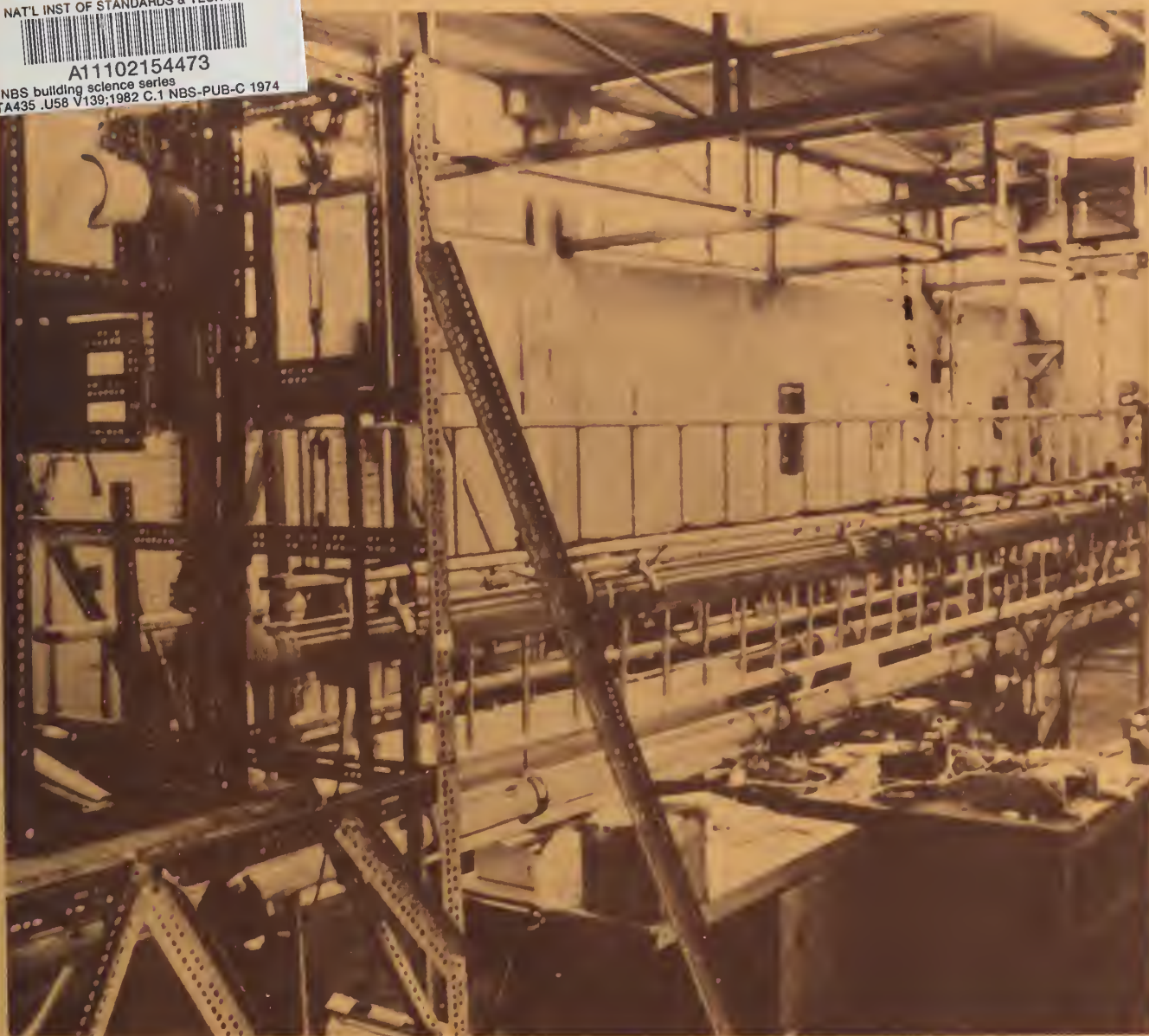
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Application of Method of Characteristics to Model the Transport of Discrete Solids in Partially-Filled Pipe Flow

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NBS BUILDING SCIENCE SERIES 139

Application of Method of Characteristics to Model the Transport of Discrete Solids in Partially-Filled Pipe Flow

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PREFACE

This report is one of a group documenting National Bureau of Standards (NBS) research and analysis efforts in developing water conservation test methods, analysis, economics, and strategies for implementation and acceptance. This work is sponsored by the Department of Housing and Urban Development/Office of Policy Development and Research, Division of Energy Building Technology and Standards, under HUD Interagency Agreement H-48-78.

The report was prepared by Dr. J. A. Swaffield, Senior Lecturer, Drainage Research Group, Department of Building Technology, Brunel University, Uxbridge, UK., during a study leave period as a guest research worker at NBS/Stevens Institute of Technology.

Experimental results included in this report are drawn from the published work of the Drainage Research Group at Brunel University.

ABSTRACT

The flow depth and velocity changes across a moving solid in partially-filled pipe flow are predicted by means of the application of the method of characteristics to solve the unsteady flow equations.

Simplified force models are presented which, when used in conjunction with empirical relationships linking leakage flow past the solid to upstream specific energy, are sufficient to provide the required moving solid boundary conditions that allow solid velocity prediction.

A wide range of simulated transport conditions are presented that confirm the applicability of this technique as a basis for the future evaluation of more complex body force models.

The predicted solid velocity during drain transport is shown to be compatible with laboratory observations of the influence of solid dimensions and position in inflow profile on transport characteristics.

Key words: computer based model; drainage; solid transport; unsteady flow

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Notation

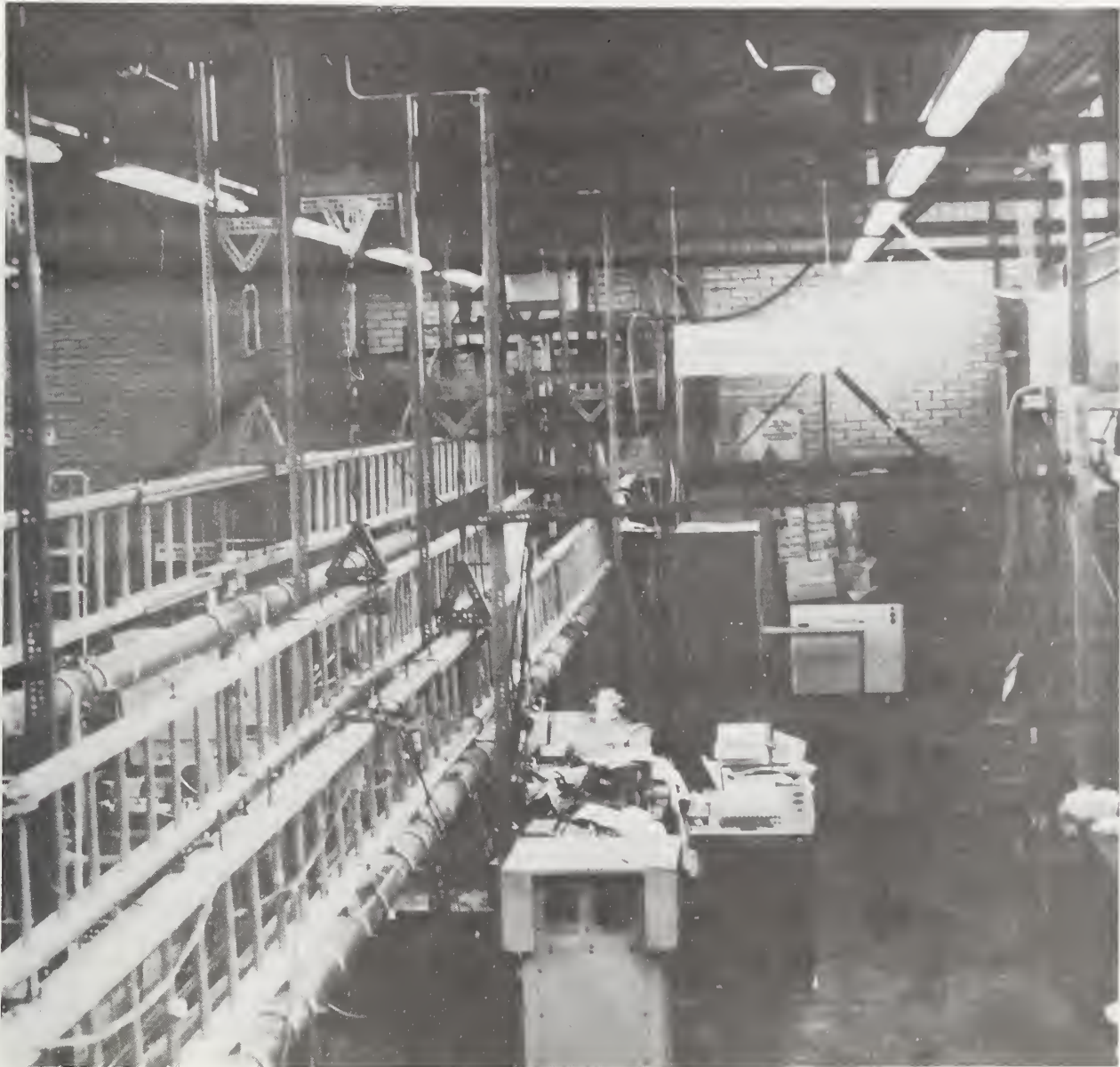
A	Pipe flow cross sectional area, m^2
B^+	Solid characteristic in xt plane
C^+, C^-	Notation referring to the positive and negative characteristics
c	Wave speed, m/sec
F_r	Froude $N^\circ = V/\sqrt{gh}$
F	Forces on solid, gm or kg
G	Pipe slope or Pipe Gradient
g	Acceleration due to gravity, m/sec^2
h	Flow depth, m
ℓ	Solid length, m
L	Distances in flow direction
m	Hydraulic mean depth, m
N, n	N° of pipe length sections employed
P	Wetted channel perimeter, m
Q	Flow rate, ℓ/s
SE	Specific energy = $h + V^2/2g$, m
SE_o	Minimum specific energy required to initiate flow past solid, m
S_o	Pipe slope
S	Slope of energy grade line, defined by Manning's Equation
T	Surface width of flow within partially filled channel, m
t	Time, sec (also t = thickness dimension solid in forces acting on body, m).
V	Local mean velocity, m/sec
V_B	Solid velocity, m/sec

NOTATIONS (Continued)

w	Solid width, m
X1-4	Functions of h, V, c and S calculated at each base point at each time step
x	Distance, positive in initial flow direction, m
α	$S_0 = \sin \alpha$ - Angle of solid relative to pipe
Δt	Time step, sec
Δx	Pipe section length, m
θ	$\Delta t / \Delta x$, sec/m
ρ	Fluid density gmsec ² /m ⁴
τ_0	Wall to fluid shear stress

Suffixes

A,B,C	Calculated points in an x-t grid at time t
abs	Absolute velocity
P	Calculated points in an x-t grid at time $t + \Delta t$
R,S	Interpolated points in an x-t grid at time t
re	Relative velocity
U,D	Upstream and downstream conditions relative to the solid boundary



1. INTRODUCTION

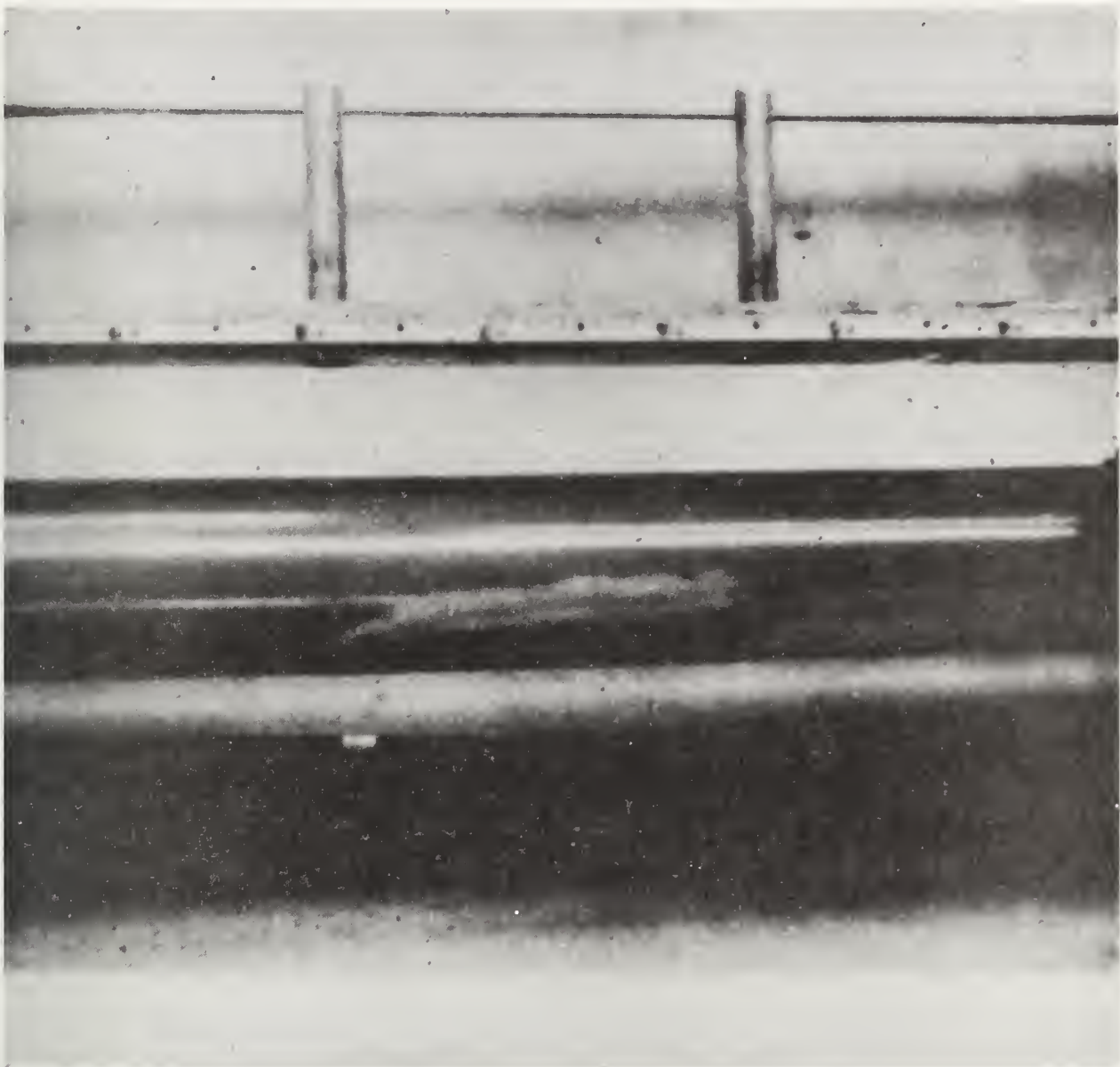
The prediction of solid transport in partially filled drainage pipe flow requires a knowledge of the forces acting on the solid and their relative importance. The treatment of the force and momentum equations for the body and surrounding flow is analytically complex; however, a numerical model capable of simulating the unsteady flow equations could be used to evaluate models of the body forces for comparison to laboratory observations.

Previous reports [1,2] have developed the application of the method of characteristics solution to the unsteady partially filled pipe flow equations. The introduction of a moving solid into the simulation requires the knowledge of leakage flow past the body as a function of upstream conditions, with a suitable model for the forces acting on the body. The passage of the simulated solid through the pipe may then be treated as a moving boundary condition by a similar technique to that applicable to the tracing of a shock wave or steep fronted wave motion.

The necessary computational techniques to allow inclusion of the solid boundary conditions are presented in this report with computer simulations involving three force models. The predicted solid motion characteristics are also compared to laboratory observed solid motion in drains which are set at a wide range of gradients.

The development of the method of characteristics solution is also summarized, and there is a statement of the necessary boundary conditions at the drain inlet and exit in both subcritical and supercritical flow regimes.

It is stressed that the objective of the study was the development of the necessary computational techniques to demonstrate the feasibility of the method coupling the hydraulic and solid motion. The development illustrates the applications of the basic modeling approach and the simultaneous solution of the governing equations of hydraulic interaction with that of the motion of the solid. A basis has been established for future comparison with development of other body force models representative of the test conditions for a wide range of body configurations for which observed laboratory solid transport results are obtained.



2. DEVELOPMENT OF THE NUMERICAL SOLUTION

2.1 SUMMARY OF THE METHOD OF CHARACTERISTICS SOLUTION OF THE EQUATIONS DEFINING UNSTEADY FLOW IN PARTIALLY FILLED PIPE FLOW

Referring to figure 1, it has been shown [1] that the equations of motion and continuity may be expressed as

$$g \frac{\partial h}{\partial x} + g(S - S_o) + v \frac{\partial V}{\partial x} + \frac{\partial V}{\partial t} = 0 \quad (1)$$

$$VT \frac{\partial h}{\partial x} + T \frac{\partial h}{\partial t} + A \frac{\partial V}{\partial x} = 0. \quad (2)$$

These equations may be combined to form a total derivative expression,

$$\frac{dV}{dt} + \frac{g}{c} \frac{dh}{dt} + g(S - S_o) = 0, \quad (3)$$

subject to

$$\frac{dx}{dt} = V + c, \quad (4)$$

the wave speed being defined by

$$c = \sqrt{\frac{gA}{T}} \quad (5)$$

where V = local average flow velocity

c = local wave speed

h = local flow depth

S_o = pipe slope

S = slope of the local energy grade line = $\frac{n^2 V^2}{m^{4/3}}$, n the Manning coefficient and m the hydraulic mean depth

T = water surface width

A = water depth cross sectional area.

Referring to figure 2, if the variables V and h are known at R and S then four equations may be written in terms of the unknowns at point P , by means of a first order approximation,

$$V_P - V_R + \frac{g}{c_R} (h_P - h_R) + g(S_R - S_o)\Delta t = 0 \quad (6)$$

$$x_P - x_R = (V_R + c_R)\Delta t \quad (7)$$

$$V_P - V_S - \frac{g}{c_S} (h_P - h_S) + g(S_R - S_o)\Delta t = 0 \quad (8)$$

$$x_P - x_S = (V_S - c_S)\Delta t. \quad (9)$$

It is stressed that these equations are paired and that equations 6 and 8 only apply as long as equation 7 and 9 are satisfied. This introduces the characteristics lines C^+ and C^- , shown in figure 3.

It is also necessary that the time step Δt is sufficiently small for R and S (points in the x - t plane) to fall within $\pm \Delta x$ of point P as shown in figure 2.

From figure 3 it will be seen, provided boundary equations governing the conditions at the extremities of the system are known, that an orderly solution may proceed yielding flow depth and velocity at each pipe section at each time increment.

The basis for the system boundary conditions is set out below.

2.2 PARTIALLY FILLED PIPE FLOW REGIMES

Two flow regimes may be identified for open channels or partially filled pipes:

(1) Subcritical flow, Froude $N^\circ = \frac{V}{\sqrt{gh}} < 1$

Here the local wave speed exceeds the flow average velocity, thus waves may be propagated both upstream and downstream in the flow, i.e., $c > V$.

(2) Supercritical flow, Froude $N^\circ > 1$

Here the local wave speed is less than the average flow velocity at that section and hence waves cannot be propagated upstream, i.e., $V > c$.

The flow regime applicable to any partially filled pipe flow may be determined by a comparison of the flow normal and critical depths.

Under steady uniform flow conditions the force balance equation for an element of flow is normally expressed by the Chezy equation

$$V = C \sqrt{m S_o} \quad (10)$$

m = hydraulic mean depth A/P , m (where A is the pipeflow cross section area)

S_o = $\sin \theta$ - duct slope

V = mean velocity m/s

C = Chezy constant.

P = pipe wetted perimeter.

The value of loss coefficient C was found by Manning to be dependent on hydraulic mean depth and duct surface roughness n . The Manning formula is the simplest of the open channel equations:

$$V = \frac{1}{n} m^{2/3} S_o^{1/2}$$

$$Q = \frac{1}{n} A m^{2/3} S_o^{1/2} \quad (11)$$

where Q is the flow rate m^3/s

A is the flow cross sectional area, m^2

The value of the Manning coefficient, n , varies with pipe or channel material; values in the range 0.009 to 0.020 apply to for materials commonly found in building drainage systems.

Equation 10 effectively determines the flow depth under steady, uniform conditions with only one value of h yielding the values of A and m necessary to satisfy the equation. As this depth is by definition constant downstream, $dh/dx = 0$, it must also be the terminal depth corresponding to the flow terminal velocity at that channel slope.

This depth, h_n , is commonly referred to as the normal depth.

The specific energy of the flow may be defined as

$$E = h + \frac{V^2}{2g} \quad (12)$$

where h = local flow depth, m

V = local average flow velocity, m/s

From equation 12 it may be seen that the flow specific energy has a minimum value below which the given flow conditions cannot exist. In a general, non-rectangular channel this value may be determined:

$$E = h + \frac{Q^2}{2gA^2}$$

$$\frac{dE}{dh} = 0 = 1 - \frac{Q^2}{gA^3} \frac{dA}{dh} \quad (13)$$

From figure 3

$$dA = T dh \quad (14)$$

where T is the surface width at any depth, h .

From equations (13) and (14) the minimum value of E will occur at a depth value, h_c , that satisfies the expression

$$1 - Q^2 T / g A^3 = 0 \quad (15)$$

where T and A are both $f(h)$

This value of h is referred to as the flow critical depth h_c .

If the normal flow depth h_n exceeds h_c then the terminal flow would be termed subcritical, or tranquil flow. If h_n is less than h_c then the flow is termed rapid or supercritical.

It should be stressed that h_c is independent of pipe slope and pipe surface roughness, while the normal depth is dependent on both. Thus the same volume flow rate in any particular pipe may be rapid or tranquil depending on pipe slope, and similarly, the same flow rate in a series of constant diameter pipes will be tranquil or rapid depending on roughness.

Pipes or channels in which rapid flow is normal are termed steep; pipes or channels in which tranquil flow is normal are termed of mild slope.

Figure 2 illustrates the importance of these two flow regimes on the solution of equations 6 to 9.

If $c > V$, then the conditions at P are determined by the intersection of the C^+ and C^- drawn from P into the AC and BC sections.

If $c < V$, then conditions in the downstream section BC cannot affect point P. The slope of the C^- characteristic, PS, becomes positive, and both R and S lie in the AC section as shown.

Both subcritical and supercritical flow are encountered in the drainage applications considered and the equations derived below cover both conditions.

Referring to figure 2 for subcritical flow:

$$\frac{V_C - V_R}{V_C - V_A} = \frac{x_C - x_R}{x_C - x_A} = (V_R + c_R) \frac{\Delta t}{\Delta x}$$

$$\frac{c_C - c_R}{c_C - c_A} = \frac{x_C - x_R}{x_C - x_A} = (V_R + c_R) \frac{\Delta t}{\Delta x}$$

$$\text{and } \frac{h_C - h_R}{h_C - h_A} = (V_R + c_R) \frac{\Delta t}{\Delta x}$$

$$\text{as } x_P = x_C \text{ and } x_P - x_R = (V_R + c_R)\Delta t.$$

The solution yields

$$V_R = \frac{V_C + \theta (-V_C c_A + c_C V_A)}{1 + \theta (V_C - V_A + c_C - c_A)} \quad (16)$$

$$c_R = \frac{c_C(1 - V_R \theta) + c_A V_R \theta}{1 + c_C \theta - c_A \theta} \quad (17)$$

$$h_R = h_C - (h_C - h_A)(\theta(V_R + c_R)) \quad (18)$$

where $\theta = \Delta t / \Delta x$.

Similarly,

$$V_S = \frac{V_C - \theta(V_C c_B - c_C V_B)}{1 - \theta(V_C - V_B - c_C + c_B)} \quad (19)$$

$$c_S = \frac{c_C + V_S \theta(c_C - c_B)}{1 + \theta(c_C - c_B)} \quad (20)$$

$$h_S = h_C + \theta(V_S - c_S)(h_C - h_B) \quad (21)$$

For the supercritical flow regime, the equations determining R in figure 2 remain unchanged. The interpolation equations for S' in figure 2 may be determined by an identical technique to that shown above,

$$V_C - V_{S'} = (V_C - V_A) \theta(V_{S'} - c_{S'})$$

$$c_C - c_{S'} = (c_C - c_A) \theta(V_{S'} - c_{S'})$$

$$\text{and } h_C - h_{S'} = (h_C - h_A) \theta(V_{S'} - c_{S'}).$$

The solution yields

$$V_{S'} = \frac{V_C(1 - c_A^\theta) - V_A c_C^\theta}{1 + \theta(V_C - V_A + c_A - c_C)} \quad (22)$$

$$c_{S'} = \frac{c_C + V_{S'} \theta(c_A - c_C)}{1 + c_A^\theta - c_C^\theta} \quad (23)$$

From equations 7 and 9 it will be seen that

$$\frac{dt}{dx} = \frac{1}{V \pm c} \quad (24)$$

hence, if $(V + c)$ becomes large, then Δt becomes small for a constant Δx . This implies that the progress of the numerical solution could become prohibitively slow for supercritical flow conditions. Fox [3] suggests a check within any program that will terminate the solution if Δt falls below a specified value; however, this comment by Fox applies to the existing applications of the method of characteristics, which have been limited to large civil engineering open channel or river flooding flow problems. It is likely that the reduction in Δt will not be a significant problem with the relative values of V and c encountered in drainage sized pipe applications due to their dependence on pipe geometry and flow rate.

The determination of conditions at P at time $t + \Delta t$ requires the following steps (i-iv), for either subcritical or supercritical flow conditions:

- (i) All conditions known at time t for nodal points A, B, C etc. (figure 2).

- (ii) Values of V , h and c at interpolation points R , S , or S' calculated from equations 16 - 23.
- (iii) Using these values of V , h , and c , the conditions at P , i.e. velocity V and depth h , at time $t + \Delta t$, are calculated by means of equations 6 and 8.
- (iv) The value of wave speed c at P at time $t + \Delta t$ is calculated from equation 5. The value of flow surface width and cross sectional area are calculated from flow depth, h , and the channel shape relationships.
- (v) The sequence is repeated at each time step.

2.3 APPLICATION OF THE METHOD OF CHARACTERISTICS SOLUTION TO DRAINAGE FLOW

For convenience, the application of the solution developed above to drainage pipe flow may be considered under two headings; namely, boundary conditions and characteristic equation solution at intermediate pipe sections. Both of these headings must be further subdivided depending on whether the flow is termed subcritical or supercritical.

The equations 6 to 9 may be restated as

$$V_P = X_2 - X_1 h_P \quad C^+ \quad (25)$$

$$x_P - x_R = (V_R + c_R)\Delta t$$

$$V_P = X_4 + X_3 h_P \quad C^- \quad (26)$$

$$x_P - x_S = (V_S - c_S)\Delta t$$

where $X_1 = g/c_R$

$$X_3 = g/c_S$$

$$X_2 = V_R + g \frac{h_R}{c_R} - g(S_R - S_0)\Delta t$$

$$X_4 = V_S - g \frac{h_S}{c_S} - g(S_S - S_0)\Delta t.$$

It will be noted that these equations apply in either subcritical or supercritical flow, the interpolated values of the conditions at S or S' being sufficient to define the flow regime, figure 2.

2.3.1 Initial Steady Conditions Along the Pipe Length

As will be seen from figure 3, the initial conditions along the whole pipe length at time $t = 0$ must be known in order for the solution to proceed. It is therefore necessary to calculate the steady state flow velocity and depth throughout the pipe length initially with the initial wave speed. This process may be carried out by the following steps:

- (i) Determine the steady flow normal and critical depths as set out previously. This determines whether the flow is subcritical or supercritical.
- (ii) For supercritical flow, the normal flow depth may be assumed to apply throughout the pipe length. As the velocity exceeds the wave speed, there is no effect propagated upstream from the pipe discharge point. This implies that the flow leaves the pipe at normal depth and, for a known flow rate and pipe dimension, allows the local velocity and wave speed to be calculated along the whole pipe length.
- (iii) For subcritical flow, the initial water surface profile is more complicated as the effect of the pipe discharge is propagated upstream. In subcritical flow, it has been found that the depth of flow is at its critical value at the discharge point, with the water depth then rising upstream until the normal steady flow depth is achieved. Calculation of this depth profile is presented in [2] and summarized below in terms of the gradually varied flow profile prediction technique.

Gradually varied flow is steady non-uniform flow of a special type. The flow parameters are assumed to change slowly, if at all, in the flow direction. The basic assumption in the treatment of this type of flow is that the local head loss at any section is given by the Manning expression (11), for the identical local flow depth and rate under assumed steady, uniform flow conditions.

Depth profile predictions by numerical integration are based on this assumption,

$$\frac{d}{dL} \left\{ \frac{V^2}{2g} + (Z_0 - S_0 L) + h \right\} = - \left\{ \frac{nQ}{A_m^{2/3}} \right\}^2 \quad (27)$$

where $(Z_0 - S_0 L)$ is the elevation at distance L along the channel, measured in the downstream direction; S_0 is $\sin \theta$, channel bed slope,

$$\text{hence} \quad - \frac{V}{g} \frac{dV}{dL} + S_0 - \frac{dh}{dL} = \left(\frac{nQ}{A_m^{2/3}} \right)^2 \quad (28)$$

and as, $Q = VA$

$$\frac{dV}{dL} A + V \frac{dA}{dL} = 0$$

and as $\frac{dA}{dh} = T$ from equation 5, it follows that

$$\frac{dV}{dL} = \frac{V}{A} \frac{dA}{dL} = - \frac{VT}{A} \frac{dh}{dL} = - \frac{QT}{A^2} \frac{dh}{dL},$$

and substituting in equation 28 yields

$$\frac{Q^2 T}{g A^3} \frac{dh}{dL} + S_o - \frac{dh}{dL} = \left\{ \frac{n Q}{A m^{2/3}} \right\}^2 \quad (29)$$

$$dL = \left\{ \frac{1 - Q^2 T / g A^3}{S_o - (n Q / A m^{2/3})^2} \right\} dh$$

$$L = \int_{h_o}^{h_1} \frac{1 - Q^2 T / g A^3}{S_o - (n Q / A m^{2/3})^2} dh \quad (30)$$

where L is the distance between two known depths h_o , h_1 .

The initial depth at each section Δx apart along the pipe may then be calculated from the profile produced by the integration of equation 30. Flow velocity is then calculated based on a constant flow rate through the pipe, and similarly, wave speed is determined based on flow depth and channel geometry.

Once the initial flow depth, velocity and wave speed have been determined the unsteady flow calculation procedure may begin.

2.3.2 Internal or Nodal Points

Simultaneous solution of equations 25 and 26 at all points Δx apart between $x = \Delta x$ and $x = (L - \Delta x)$ will yield the required values of flow depth and velocity at the end of each time step. Wave speed may then also be determined from equation 5. This process applies to either sub or supercritical flow conditions as the particular regime is represented in the interpolations required to fix points R , S or S' , figure 2.

2.3.3 Entry Boundary Conditions, Supercritical Flow

In this case the inflow profile alone determines the flow depth at pipe entry as downstream conditions, that would have been represented by the C^- characteristic in subcritical flow, cannot effect the flow conditions at the upstream boundary, as by definition the flow velocity exceeds the wave speed.

Hence the boundary condition is obtained from the flow profile $Q = f(t)$ solved with the normal depth expression

$$Q = \frac{1}{n} A m^{2/3} S_o^{1/2}$$

where A and m are both $f(h)$. This equation may be rewritten in the form

$$1 - \frac{(nQ)^2}{A^2 m^{4/3} S_o} = 0 \quad (31)$$

and this boundary expression may be solved at each time step with a known Q by the bisection technique, this technique is described later.

2.3.4 Entry Boundary Conditions, Subcritical Flow

For subcritical flow the downstream conditions do contribute to the entry flow depth and velocity. In this case the inflow profile $Q = f(t)$ is solved with the C^- characteristic

$$Q = f(t) = V_1 A_1$$

$$V_1 = X_4 + X_3 h_1$$

$$Q(t) = A_1 (X_4 + X_3 h_1) \quad (32)$$

where suffix 1 refers to the entry boundary location and $A = f(h)$ dependent on the pipe cross sectional geometry.

In the form

$$Q(t) - f(h_1)(X_4 + X_3 h_1) = 0 \quad (33)$$

this boundary equation may be solved by the bisection technique.

2.3.5 Exit Boundary Conditions, Supercritical Flow

As the flow velocity exceeds the local wave speed the exit boundary condition may be determined in the same manner as the upstream nodal points; namely, by the simultaneous solution of the C^+ and C^- characteristics. With reference to figure 2, both the R and S' points lie upstream of the pipe exit.

The exit condition may be included in the nodal point calculations for the supercritical flow case, no separate exit subroutine being necessary in the program, as equations 25 and 26 are sufficient.

2.3.6 Exit Boundary Conditions, Subcritical Flow

At pipe exit in the subcritical flow regime, the flow depth approaches the critical depth value, given by zero value of equation 15:

$$\frac{Q^2}{g A_{crit}^3} T_{crit} = 1,$$

where A and T are f(h).

This condition may be solved with the C^+ characteristic

$$V_{N+1} = X2 - X1 h_{N+1}$$

where N = N° of pipe length sections, Δx .

The boundary condition becomes

$$[(X2 - X1 h_{N+1}) A_{N+1}]^2 \frac{T_{N+1}}{g A_{N+1}^3} - 1 = 0. \quad (34)$$

The solution may again be achieved by use of the bisection method with the use of the area to depth relationship for the channel.

2.4 APPLICATION OF METHOD OF CHARACTERISTICS TO WASTE SOLID BOUNDARY, STATIONARY CONDITION

Considering a stationary solid deposited at some point along the waste pipe, the water depth and velocity upstream of the solid may be predicted if a suitable boundary equation may be written linking flow past the solid to upstream conditions.

Figure 4 illustrates the relationship between flow past a stationary solid and the specific energy upstream. These results were compiled during a Brunel University Drainage Research Group study of solid transport in drainage systems.

The flow past the solid (experimentally determined) may be expressed as

$$Q = K(h + \frac{V^2}{2g} - SE_o)^2 \quad (35)$$

where $SE = h + V^2/2g$, flow specific energy and SE_o is the flow specific energy required for flow initiation past the solid.

Equation 35 may then be solved with the C^+ characteristic, of figure 5,

$$V_I = X2 - X1 h_I$$

where $Q = V_I A_I$

so that

$$A_I(X_2 - X_1 h_I) = K \left| h_I + \frac{1}{2g} (X_2 - X_1 h_I)^2 - SE_o \right|^2.$$

This expression results in a quartic in terms of depth upstream of the solid, h_I (see appendix 2). This quartic must be solved by an iterative technique as the flow area, A_{N+1} , is a function of h_I . The Newton Raphson method may be employed to carry out the necessary iterative solution. Once the value of h_I has been determined, the value of V_I and c_I may be determined.

As mentioned, the SE_o term is the flow specific energy required to initiate flow past the stationary solid. If the value of flow specific energy at time t is less than that of SE_o , then the value of flow velocity at the solid at time $t + \Delta t$ is set equal to zero. The flow depth then comes directly from equation 25 as:

$$h_I = X_2/X_1. \quad (36)$$

This implies that the flow depth upstream of the solid must rise to SE_o prior to the initiation of flow past the solid. This solution is set out in detail in appendix 2, and it has been shown to be capable of simulating depth increase upstream of a stationary solid [1].

It should be noted that the analysis above applies to both subcritical and supercritical flow regimes, as only the C^+ characteristic is involved.

2.5 APPLICATION OF METHOD OF CHARACTERISTICS TO WASTE SOLID BOUNDARY, MOVING CONDITION

Prior to application of the moving boundary conditions representing the solid motion, it is necessary to determine the solid motion initiation time. This may be accomplished by monitoring the net force acting on the solid.

2.5.1 Model of Forces Acting on the Solid

Figure 6 illustrates the forces assumed to act on the rectangular section solid, namely, hydrostatic pressure forces, F_{p1} , F_{p2} , acting on the trailing and leading edge projected areas, body weight force, frictional force due to wall to body contact, F_S , and a bouyancy force, F_B , dependent on the solid position in the flow.

The net force acting on the solid may be expressed as, figure 6,

$$F_{p1} - F_{p2} + mg \sin\theta - F_S = F_{BODY} \quad (37)$$

where $F_S = f(mg \cos\theta - F_B)$

and f is the wall to solid friction factor, its value being reduced from the static friction coefficient to the sliding friction value if F_{BODY} becomes positive.

If $F_{\text{BODY}} > 0$, then solid motion is initiated and the solid velocity at the end of a computational time step Δt is given by:

$$F_{\text{BODY}} = m \frac{dV}{dt} = m \frac{\Delta V}{\Delta t} \quad (38)$$

$$\text{where } \Delta V = V_{t+\Delta t} - V_t \text{ and } m = \text{mass of body.} \quad (39)$$

(note values of $V_t = 0$ for the first time step)

$$\text{Hence, } \Delta V = V_{t+\Delta t} = V_t + \frac{\Delta t}{m} F_{\text{BODY}}. \quad (40)$$

The distance traveled by the solid in the time step may be approximated by

$$X_B = X_o + \frac{1}{2}(V_{t+\Delta t} + V_t)\Delta t \quad (41)$$

where X_o is the solid position at time t and X_B the final position at the end of the time step.

Equations 37 to 41 apply to subsequent time steps with the mentioned modifications to the value of wall to solid friction coefficient in equation 37. The net force on the body may become negative in subsequent time steps; however, this represents solid deceleration and no modification to the equations is necessary until the predicted value of $V_{t+\Delta t}$ (equation 40) becomes either zero or negative (the condition for the body coming to rest).

Figure 7 illustrates the forces assumed to act on the solid. The calculation of the buoyancy force, F_B , (equation 37) requires the solution of the body force system. Values of F_1 , F_2 and F_D may be approximated by the hydrostatic equation; however, the force F_u is not readily estimated due to the curvature of the solid to pipe boundaries.

Laboratory observations have shown, that the model solids, maternity pads [4], due to their flexibility, tend to take up the shape shown in figure 7. Taking moments about the leading edge point A, as shown in figure 7, allows F_u to be estimated.

The buoyancy force F_B may then be determined as

$$F_B = (F_u - F_D) \cos \alpha \quad (42)$$

where α is the slope of the solid surface relative to the pipe wall.

Figure 8 illustrates three force models investigated in this study:

Model 1 - buoyancy forces neglected, the value of $F_B = 0$

Model 2 - downthrust force $F_D = 0$. The justification for this model comes from test observations. In the boundary equations for the solid leading edge, i.e. downstream, the leakage flow is assumed to take up its normal depth at once. Laboratory observations indicate a downstream transition length so that the flow depth immediately ahead of the solid is less than that predicted.

Model 3 - all forces shown in figure 7 included.

2.5.2 Equations Governing Flow Past the Moving Solid

It may be assumed that the relationship between specific energy and flow past the solid may be employed in the moving solid case, provided that the absolute fluid velocity employed in equation 35 is replaced by a relative water to solid velocity. The value of SE_0 , the specific energy term to initiate flow past the body, remains unchanged.

Equation 35 is therefore rewritten as

$$Q = K(h + \frac{(V - V_B)^2}{2g} - SE_0)^2 \quad (43)$$

where Q is the leakage past the moving solid, because

$$Q = V_{re}A = (V_{abs} - V_B)A = (X2 - X1h - V_B)A \quad (44)$$

where A is the flow area upstream of the solid and V_{abs} is the fluid velocity expressed by the C^+ characteristic, figure 5.

Appendix 2 presents the full solution to this boundary condition in a general form, applicable to both the initially stationary and moving solid.

The prediction of solid velocity allows the solid path to be drawn in the $x-t$ plane as shown in figure 9. The B^+ lines drawn in the plane are the equivalent to the fluid characteristics; the gradient of B^+ is hence given by

$$dx/dt = V_B. \quad (45)$$

Figures 10 and 11 illustrate the necessary techniques to allow the solution to proceed with a moving solid. A slightly different solution is required, depending on whether the flow is subcritical or supercritical.

Figure 10 presents the subcritical case. Assume that the solid was at point C at time t and is predicted to move to P' by time $t + \Delta t$. In order to calculate

the conditions at $t + \Delta t$, it is necessary to set up the interpolated base values at R and S; therefore, for conditions immediately upstream and downstream of the solid, a new Δx grid A'P' to P'C' must be set up.

Using the position P' predicted from solid velocity, the points A' and C' are determined. The conditions at R and S are then calculated by interpolation (equations 16-21).

Point R may be used to yield the C^+ characteristic RP' that may be solved with the solid leakage equation 43 to yield depth and flow velocity upstream of the solid.

The conditions on the downstream face of the solid are calculated by a similar technique applied to C'B'. The C^- characteristic is solved with the flow rate at the solid by the technique utilized at pipe entry in subcritical flow (equations 32-33).

Points W, X and Z, figure 10, may be dealt with by the nodal point equations, 25 and 26, as the necessary interpolations are not affected by the presence of the solid at P'.

Conditions at P and Y, however, cannot be readily calculated due to the B^+ characteristic. Conditions at these points, however are required as base conditions for the next time step. As the Δx and Δt values are small, it is reasonable to determine conditions at P and Y by interpolation between X and P' and P' and Z respectively.

Figure 11 illustrates the solution for the supercritical case. It remains necessary to approximate conditions at P and Y and the conditions downstream of the solid are determined by the use of equation 31 (the normal depth calculation).

2.6 SIMULATION CASES COVERED BY THE PROPOSED MODEL

Two types of solid motion must be covered by a model of the type presented. The motion of the solid subsequent to injection into the flow with a downstream velocity must be dealt with, as this represents the introduction of solids with finite velocities in the drain from water closet discharge. Similarly, the motion of a deposited solid in response to a flow must be considered, as this covers the partial system clearance that results in any long drainage pipe exhibiting a series of depositions along its length, each of which is moved on slightly by each incoming flow.

Both cases may be dealt with by the proposed model. The injection case is covered by assuming that, at some instant of time and position, the solid appears in the flow, moving at the local flow velocity that was calculated at that section by the characteristics solution run up to this time with no solid present.

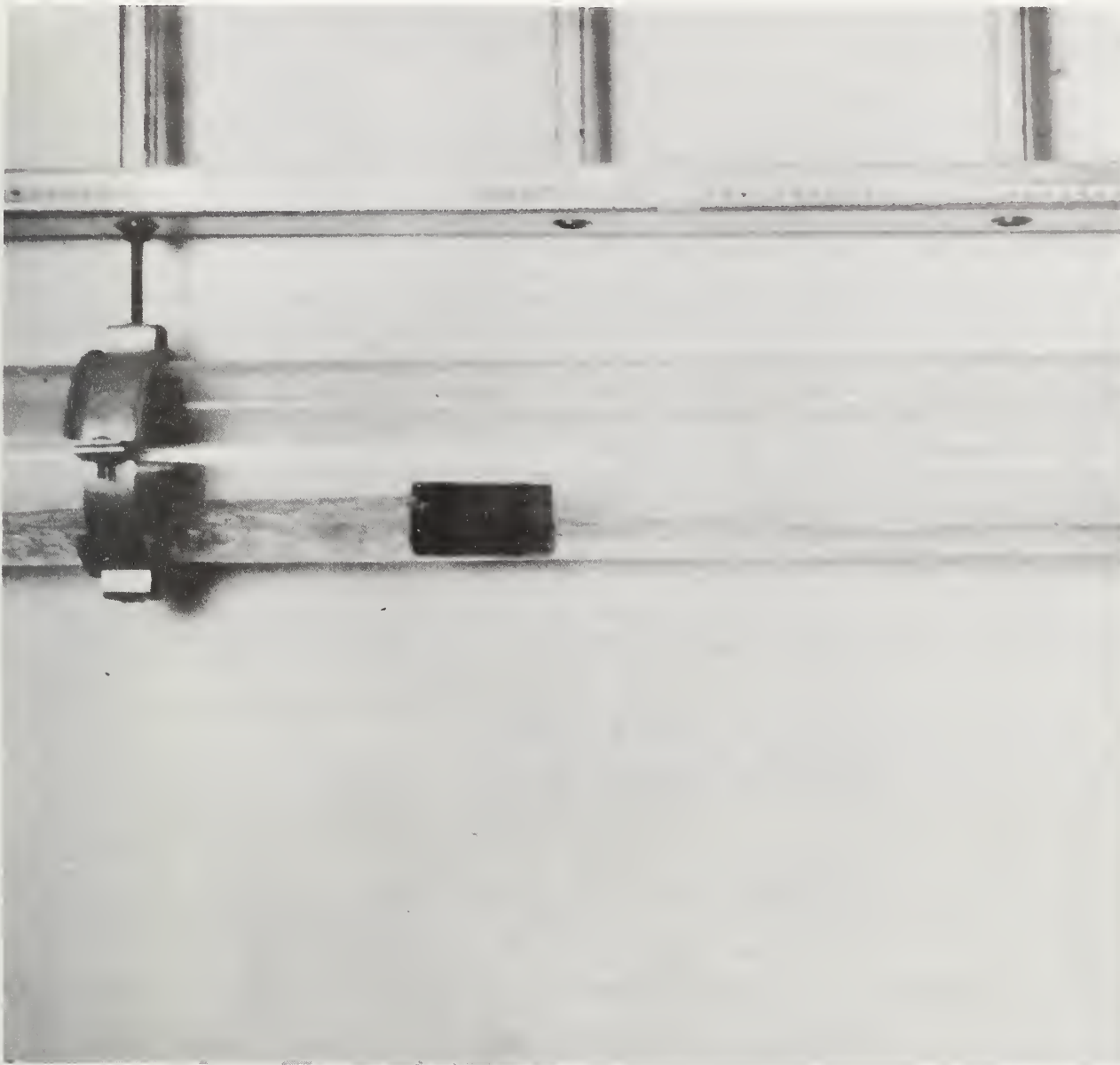
The deposited solid case, at any downstream location, is simply dealt with by the technique described above and more fully in [1]. In this case, the solid is assumed to be present from the first computing time step.

Similarly, the model must be capable of dealing with both subcritical and supercritical flow regimes. The techniques for these cases have been set out; however, care must be taken in the supercritical case.

Figure 12 illustrates the problem encountered in supercritical flow. In the case of a stationary, or even moving solid, the depth increase upstream of the solid may be sufficient to produce a subcritical zone in an otherwise supercritical flow condition. In order for the upstream supercritical flow to become subcritical behind the solid, a depth change wave, or series of depth change waves must be propagated upstream. If the depth change upstream of the solid is rapid, as would happen with a rapidly increasing inflow profile, the depth change waves propagating upstream at the wave speed $\sqrt{g A/T}$ combine to form a steep fronted wave that moves at a velocity greater than $\sqrt{g A/T}$, and hence the solution breaks down.

If the inflow profile is not sufficiently rapid, then the transition from supercritical to subcritical flow may be accommodated by introducing a flow condition check into the calculations at the stage represented by figure 2. If the velocity at a section at time t is less than the calculated wave speed at that section in an initially supercritical flow condition, then the flow locally is assumed to have become subcritical and the interpolated values, (figure 2) switch from R, S' to R and S .

The speed of propagation of a steep-fronted wave may be calculated and included in the model in a manner similar to that described for the solid motion. Further studies will include this facility. The test cases presented in this report were not affected by this effect, due to the inflow profile shape and the initial position of the solid in the pipe.



3. CALCULATION TECHNIQUES AND PRESENTATION OF RESULTS

3.1 DETERMINATION OF NORMAL AND CRITICAL DEPTHS

The bisection method was used to solve the equation defining both critical flow depth

$$X = 1 - Q^2 T / g A^3$$

and normal flow depth

$$Y = S_o - (n Q / A m^{2/3})^2$$

that feature as boundary conditions.

It may be assumed that both X and Y have zero values for some value of depth h in the range $0 < h < D$ for the pipe case.

This initial interval, $0 < h < D$ is bisected and $h = D/2$ used to evaluate X, Y. If the resulting values are positive, the root is less than the midpoint; then, the upper limit is reset equal to the h value just used and the remaining interval 0 to D/2 bisected. The process is repeated, with the upper limit replaced until the value of X and Y become zero, i.e., the solution desired for the critical and normal flow depths. If the X or Y value had been negative, then the root would be greater than the trial h value; in this case the lower limit would be initially reset to the trial h value, $D/4$ ($D/4 < h < D$), and the interval bisected to a new value of $3/4D$. The process is repeated until a root is obtained.

Due to the need to include the area depth relationship, this solution must be undertaken by an iterative process. The time taken depends on the complexity of the area-depth function.

3.2 NUMERICAL INTEGRATION FOR SURFACE PROFILES

The integration of the position vs depth profile

$$L = \int_{h_1}^{h_2} \frac{1 - QT^2/gA^3}{S_o - (nQAm^{2/3})^2} dh$$

is achieved by means of Simpson's Rule. Let the integral $X = \int_{h_0}^{h_1} F(h) dh$;

then, if the interval $h_1 - h_0$ is divided into 2 equal increments, the value of X is given by

$$X = \frac{1}{3} dh [F(h_0) + 4F(h_0 + dh) + F(h_0 + 2 dh)].$$

As the integration moves on, the length traversed may be accumulated as the added interval X with the prior L, $L = L + X$, at the completion of each integration.

3.3 CHOICE OF TIME STEP

Referring to figure 4, it will be seen that the time step chosen must be such that the points R and S fall within $\pm \Delta x$ of point P. In order for this to occur for all sections along the pipe, it follows that

$$\Delta t = \frac{\Delta x}{(V + c)_{\max}}. \quad (35)$$

This expression yields the smallest possible time step, as the maximum values of flow velocity and wave speed at any pipe section have been used.

In order to ensure that the computation proceeds as quickly as possible, the computer program presented calculates a new time step magnitude at each time increment so that the time step increases when V and c decrease, but decreases to maintain a stable solution when V and c are increasing in response to an inflow surge.

3.4 PRESENTATION OF RESULTS

The objectives of the numerical method for computation of the transport mechanisms of solids impartially filled pipe flow were to: (a) identify the potential application of coupling the method of characteristics solution for the hydraulic phenomena with the solution of the equation of motion for the solid based upon modeling the liquid/solid interface forces; and (b) highlight any limitations inherent to the technique. The simulated pipe flow/solids motion numerical data were developed from use of the Fortran computer program TRANSCC, run on the NBS CBT Perkin Elmer 732 computer.

The following test cases were investigated and are reported here

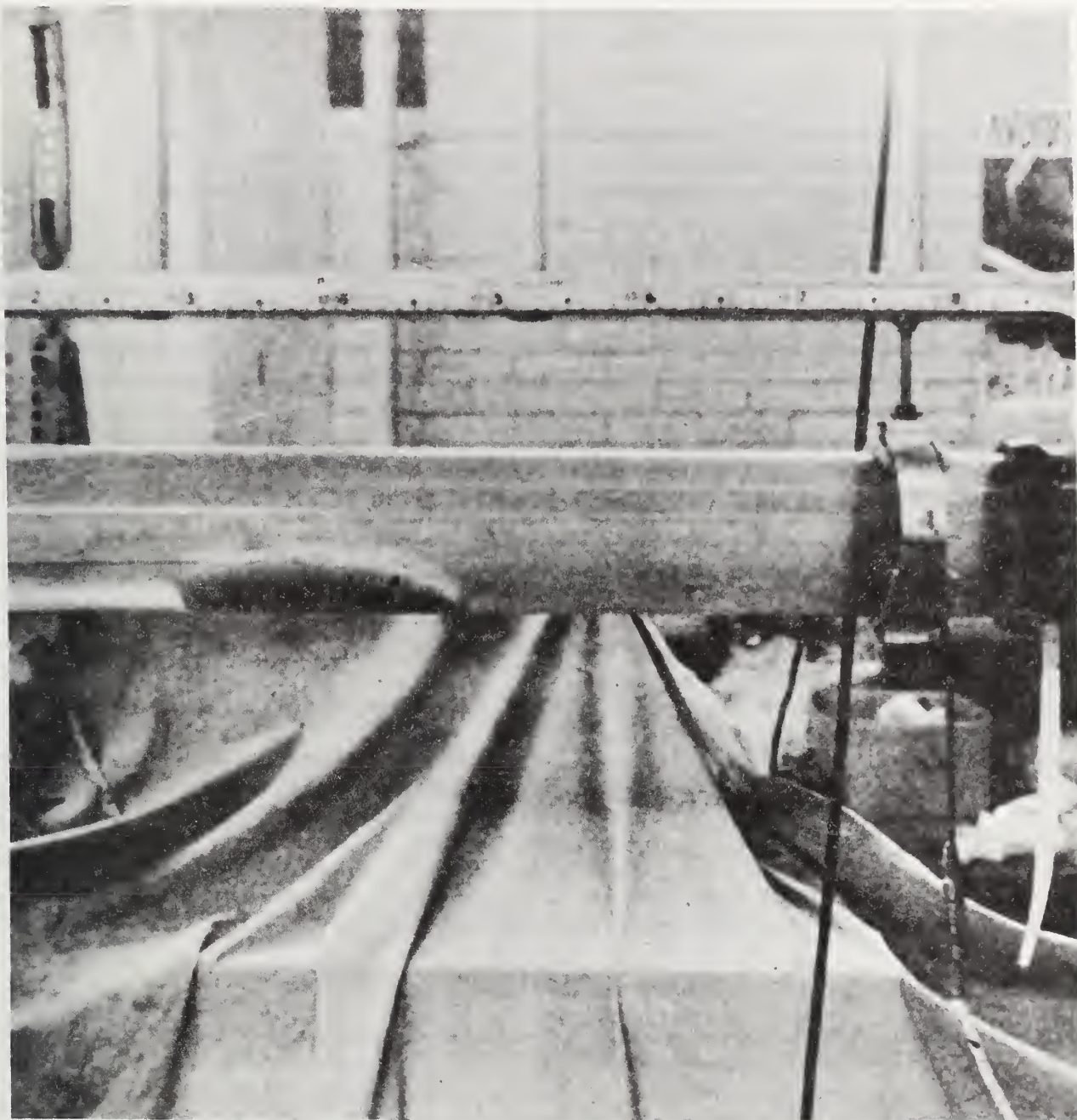
- (1) Solid types -- two cases represented by figure 4, 270 mm x 20 mm x 70 mm and 270 mm x 20 mm x 35 mm with saturated weights of 250 g and 125 g
- (2) Pipe gradients -- 1/40 to 1/300
- (3) Inflow profile -- constant profile employed with peak flow of 4.2 l/s, overall duration 9 seconds
- (4) Pipe roughness coefficient -- constant at 0.015
- (5) Solid friction factors -- 0.10 sliding and 0.15 static
- (6) Solid position in flush, 3 s and 4 s from flow initiation in the moving solid insert case, at 2.7 m from entry
- (7) Solid position -- 4.2 m from entry for deposited solid
- (8) Force models -- three models as illustrated in Figure 8.

3.5 CHOICE OF CALCULATION CONSTANTS

In order to undertake the calculation procedure described, it is necessary to have values of leakage constants and initial specific energy for the solid. In the simulations presented, the values of these constants are drawn from the

results illustrated in figure 4, referring to transport tests at Brunel using large deformable solids.

The surface to pipe wall friction factors are also required. No values are at present available for the deformable solids tested; however, similar tests conducted in the Plumbing Research Laboratory at the National Bureau of Standards utilizing impermeable cylindrical solids suggest values for friction factors in the range 0.6-0.8 for the sliding and static cases. It is likely that the deformable solids will have lower values, due to the presence of the material saturating water that will tend to provide a degree of lubrication. All the simulations presented were carried out with values of 0.1 sliding friction factor and 0.15 static friction coefficient.



4. DISCUSSION OF UNSTEADY FLOW SIMULATION RESULTS

As outlined in the introduction, the objective of the study was the development of a technique, based on the method of characteristics, that would allow the transport of discrete solids in partially filled pipe flow to be modeled mathematically.

It was recognized that insufficient data on the frictional characteristics of model solids used in laboratory test programs at Brunel and NBS were available to attempt to predict actual solid transport velocity profiles. However, the

models of the forces acting on the solid were based on current research at Brunel and NBS, and the values of friction factors assumed were, as already discussed, based on the best available information.

It is more important in this effort to demonstrate the ability of the analysis techniques to yield the solid velocity and the associated flow depth and velocities during the transport along the pipe. Subsequently, modifications based upon improved force models, friction factors derived from tests and other empirical adjustments, can be introduced to fit predicted data to experimental results.

From the examples computed for the conditions of 3.4, it is worth noting the form of the relationships of solid velocity to pipe length and gradients. Figure 13 represents typical empirical results for the single maternity pad solid tested at Brunel. This solid has dimensions 270 mm x 20 mm x 70 mm, a saturated weight of 250 g, and a specific energy to leakage flow relationship in a 100 mm pipe as shown in figure 4. This solid, with a half width version, was used as a basis for the computer simulations presented.

It will be seen from figure 13 that the velocity of the solid over the major length of the drain is governed by the $\sqrt{L/G}$ term; i.e., the square root of distance travelled divided by pipe gradient. This effect will be studied by plotting the computed velocity results against this term. Wherever possible, simulations are presented at pipe slopes of 1/40 and 1/100 in order to represent both supercritical and subcritical flow regimes. In addition, these gradients represent the common spread of slopes employed in drainage system design.

It should also be noted that the water depth and velocity results presented are immediately upstream and downstream of the solid, and thus refer to a location that moves down the pipe at the solid velocity.

4.1 INFLUENCE OF BODY FORCE MODEL ON PREDICTED SOLID VELOCITY

Figure 14 illustrates the predicted solid velocity for the three force models presented in figure 8. It was found from the values of force predicted by these models that, for the range of model sizes simulated, the downthrust on the leading surface of the solid materially increased the surface frictional force. This is represented in figure 14 by the observation that at both 1/40 and 1/100 gradients, the model 3 results yielded the lowest solid velocity. As expected, therefore, the exclusion of the downthrust force, F_D , (figure 8) yielded the highest solid velocity. The omission of F_D is reasonable on the basis of laboratory observations. The water depth tends to require a transition length downstream of the solid to achieve the normal depth appropriate to the flow past the solid. Hence, the water depth predicted by the analysis, the effective normal depth, will be an overestimate of the depth of this location.

Figure 14 is also based on the assumption that the solid appears in the flow at a particular x, t coordinate traveling at local water speed. This is a

reasonable assumption that leads inevitably to a rapid deceleration of the solid accompanied by a buildup of water depth immediately upstream of the solid. The adjustment to a new water-driven velocity is rapid, and any non-realistic effects due to the insertion model are likely to decay rapidly.

All force models were used in the collection of the data presented; each figure carries a note as to the applicable model.

4.2 INFLUENCE OF SOLID DIMENSIONS AND POSITION IN THE INFLOW PROFILE ON PREDICTED SOLID VELOCITIES

Laboratory experiments and data analysis presented in [4] have shown that the volume available behind a solid in the flush significantly determines its transport properties.

Referring to figure 15, it will be seen that introducing the solid at 2.7 m from entry at 4 seconds into the flush, as opposed to 3 seconds, does support these observations. Although the predicted differences are small, they are consistent.

Similarly, laboratory tests have shown that base area, defined in the case of a rectangular model solid (figure 6), as thickness, t , times width, w , is a major factor in determining transport performance. Small base area solids (e.g., tampons or sheets of toilet tissue) travel badly when compared to larger solids. This is due to the increased flow past the solid that reduces the depth buildup behind the solid, and from equation 37, leads to smaller body forces. Figure 16 clearly demonstrates this effect for both the subcritical flow at $1/100$ and the supercritical flow at $1/40$.

4.3 COMPARISON OF SOLID MOTION FROM BOTH INITIAL DEPOSITION AND INSERTION AT WATER VELOCITY MODELS

Figures 17 and 18, and 19 and 20 compare (for slopes of $1/40$ and $1/100$) the flow, solid velocity, and depth changes for a solid accelerated from rest to that for a solid assumed to enter the flow at local water speed.

A number of general observations may be made from these results that find confirmation in previous observations of laboratory tests:

- (1) At both pipe gradients, the maximum depth upstream of the solid occurs in the acceleration from rest case.
- (2) Perhaps more surprisingly, the maximum depth occurs in both test cases in the steeper pipe. This is a direct result of the application of equation 36.

In the supercritical flow at slope $1/40$, the velocity term is greater than at $1/100$, and consequently, the flow depth is less. Thus the "destruction" of the flow momentum by the partial blockage formed by the solid results

in a greater depth change in the steeper pipe. Similarly, this enhanced depth change leads to a higher force acting on the solid and results in the earlier motion of the solid in the 1/40 pipe case. Figure 17 indicates solid motion at 1.4 s for 1/40 and 4.2 s at 1/100 pipe gradients.

- (3) Both the depth upstream of the solid as it moves along the pipe and the associated solid and water velocities display oscillations. This is entirely attributable to the choice of time step, and the fact that the simulation equations 40, 41 are only first approximations; no return iterative technique has been introduced. Subsequent time steps may then underestimate the solid velocity. These oscillations are reflected in the water depth upstream of the solid. This link between upstream depth and solid velocity is clearly demonstrated in figure 18 by the sharp dip motion at $t = 1.4$ seconds. All simulations involved a grid length of 15/50 m, time step dependent on wavespeed.

4.4 COMPARISON OF PREDICTED SOLID VELOCITIES TO EMPIRICAL RELATIONSHIPS

Figure 13 indicated that solid velocity is dependent on the experimentally derived group $\sqrt{L/G}$,

$$V_B = C_1 - C_2 \sqrt{L/G} ,$$

where C_1 and C_2 are experimentally measured.

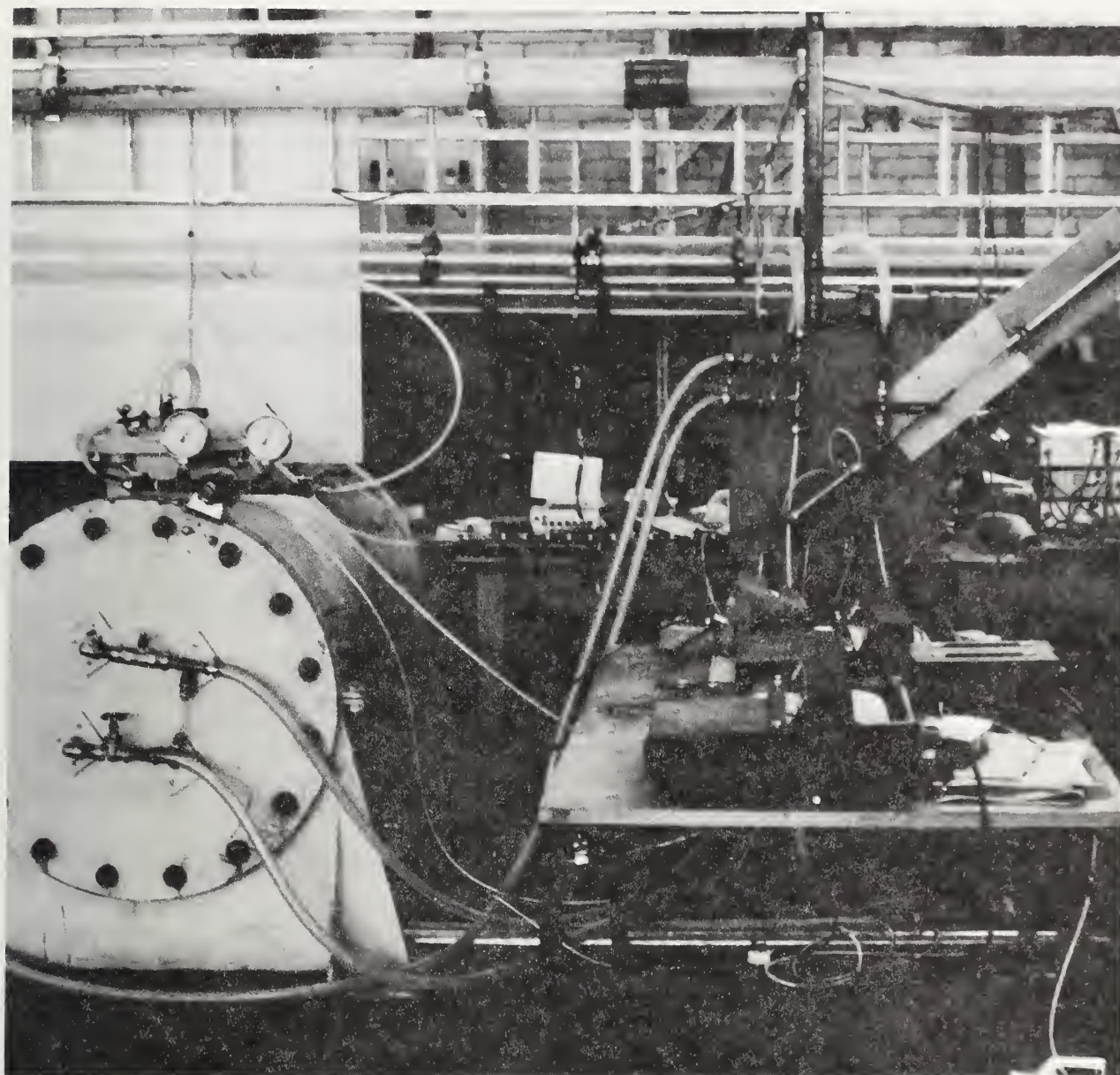
Figures 21 and 22 present simulated solid velocity results plotted against the $\sqrt{L/G}$ term for two force models and pipe slopes from 1/40 to 1/300.

The results indicate that the solid velocity in each case is linearly dependent on \sqrt{L} over the major portion of the pipe length. The dependence on $G^{-1/2}$ is not clearly defined by the results; however, it is clear that a pipe gradient term is present and would have an index greater than 0.5. Alternatively, and more probably, the deviation is due to factors not yet included in the force models, for example, the surface to water shear force arising from the water flow over the solid has not been included, as the surface shear stress is unknown. However, the results are encouraging in that the general form of the predicted solid velocity curves approximates the observed laboratory results. This also indicates that the force models employed were reasonable, as well as the values of surface to wall friction coefficients assumed.

The forces acting on the solid have not been presented in graphical form, as they were generally found to remain roughly constant during any simulation, although exhibiting the oscillations mentioned previously. Typical values for the zero downthrust model, figure 14, at 1/40 were -0.2 N during the initial deceleration, falling to -0.01 N during the subsequent motion. At 1/100 the comparable values were in the range -0.2 N initially, falling to around -0.02 N.

4.5 LIMITATIONS TO THE SIMULATION

As fully discussed in [2], the method of characteristics solution requires an initial flow in the pipe that continues beyond the termination of any inflow profile. This effectively means that a simulated solid will achieve a terminal velocity in the pipe, or alternatively, will be deposited and moved on continuously as the residual flow acts to increase upstream depth. This effect is not readily apparent from the results presented due to both the relatively short pipe length, 15 m, and curtailed run duration of 30 seconds. For the purpose of investigating the force model to be used, this limitation is not major and, indeed, could be duplicated in any parallel experimental work.



5. CONCLUSIONS AND FURTHER WORK

The objective of this study was the evaluation of the coupling of the method of characteristics with the equation of motion of a solid based upon an assumed force model to provide a numerical analysis base for modelling the transport of discrete solids in partially filled pipe flow.

The results presented show that the method is applicable, and that the motion of the solid may be satisfactorily tracked through an x - t grid representing the

pipe by introducing a solid characteristic whose slope in the plane is governed by the forces acting on the solid.

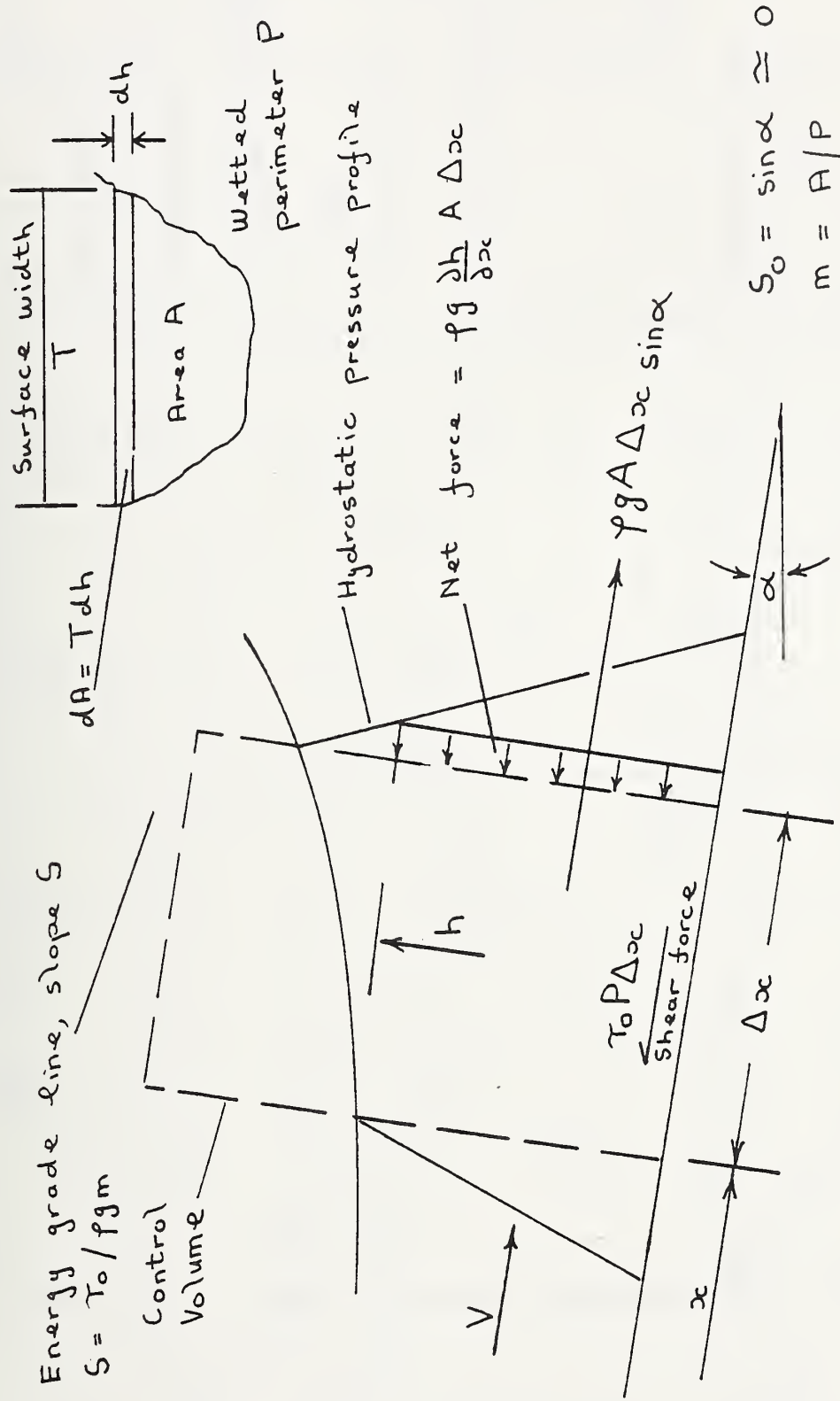
A wide range of simulations in both subcritical and supercritical flow regimes yielded solid velocity results that were compatible with laboratory observations.

Further work is required to establish the true values of the solid sliding friction coefficient, with further study of the force models to be used as the moving solid boundary condition. Similarly, the specific energy vs. relative flow rate over the solid requires further investigation to extend the range of solid geometry available at present.

6. REFERENCES

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- [2] Swaffield, J. A. "Application of the Method of Characteristis to Predict Attenuation in Unsteady Partially Filled Pipe Flow." NBS Report October 1980.
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- [4] Swaffield, J. A. "Dependence of Model Waste Solid Transport Characteristics in Drainage Systems on Solid Geometry, Mass and Pipe System Parameters." NBS Report August 1980.





Note 2nd order terms neglected

Figure 1. Application of momentum equation to unsteady flow in a general open channel

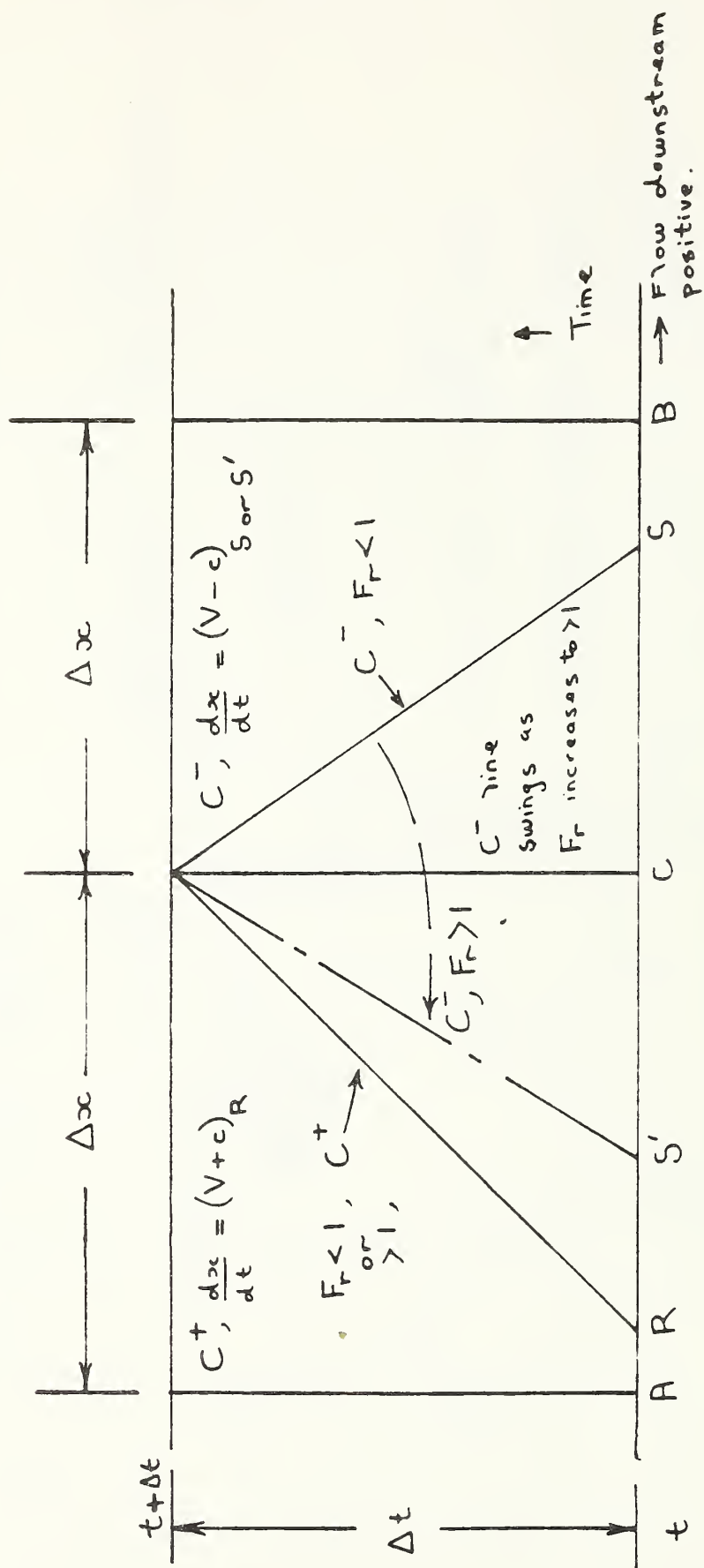


Figure 2. Modification to specified time interval grid for subcritical and supercritical flow regimes

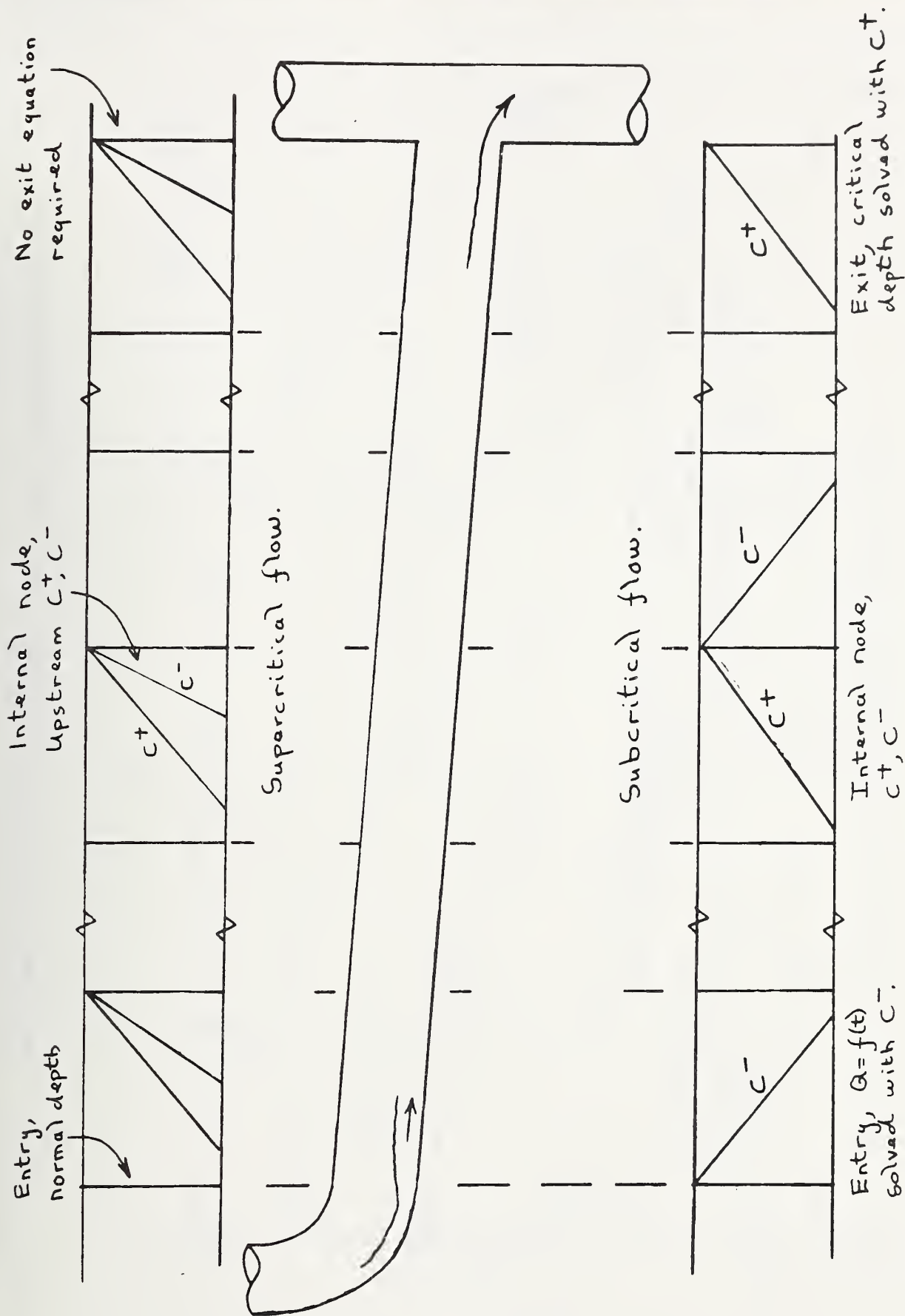


Figure 3. Solution at pipe entry, exit and internal nodes for subcritical and supercritical flow regimes

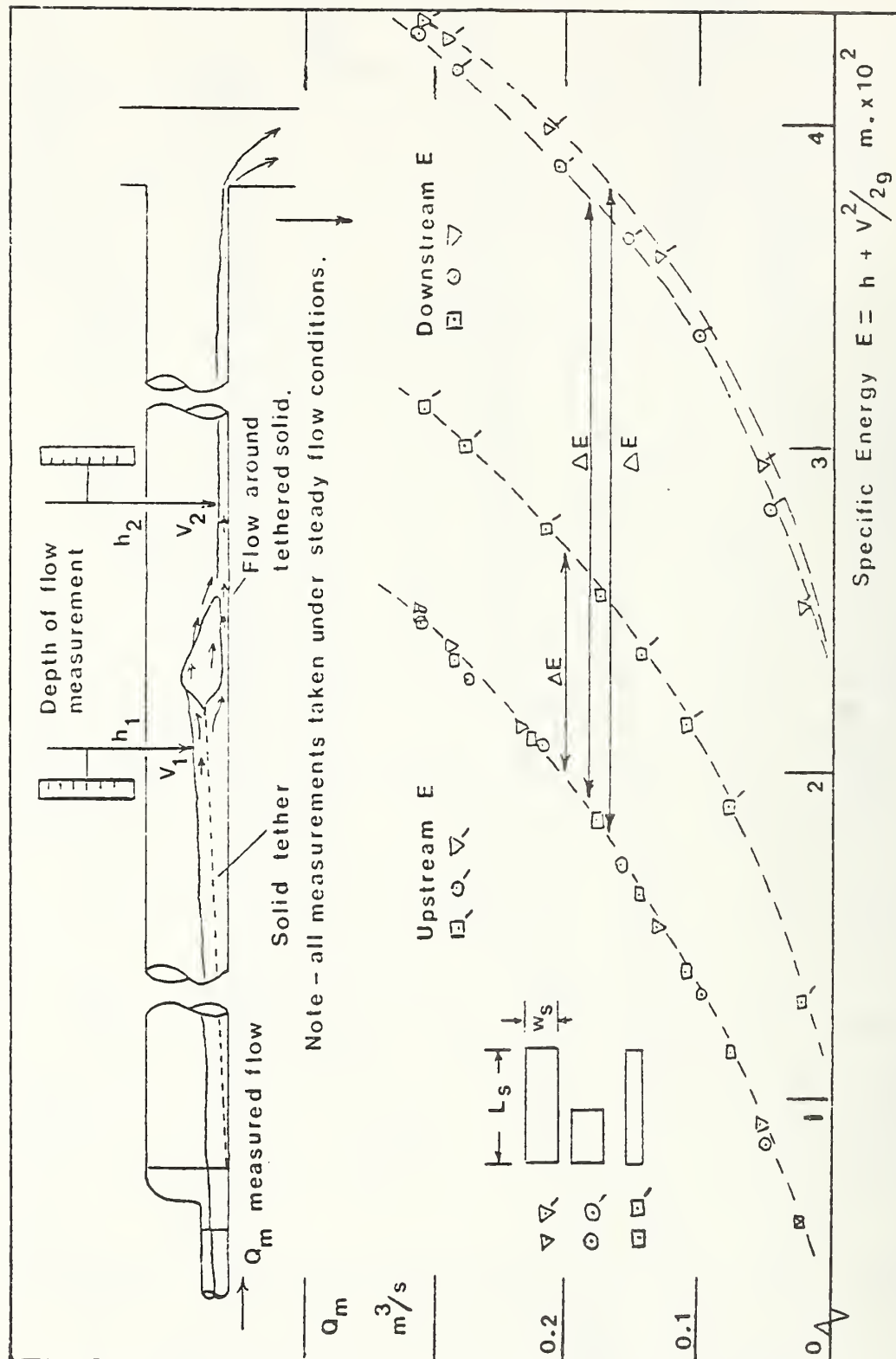


Figure 4. Measurement of the flow specific energy change across a solid tethered in the waste pipe under steady flow conditions

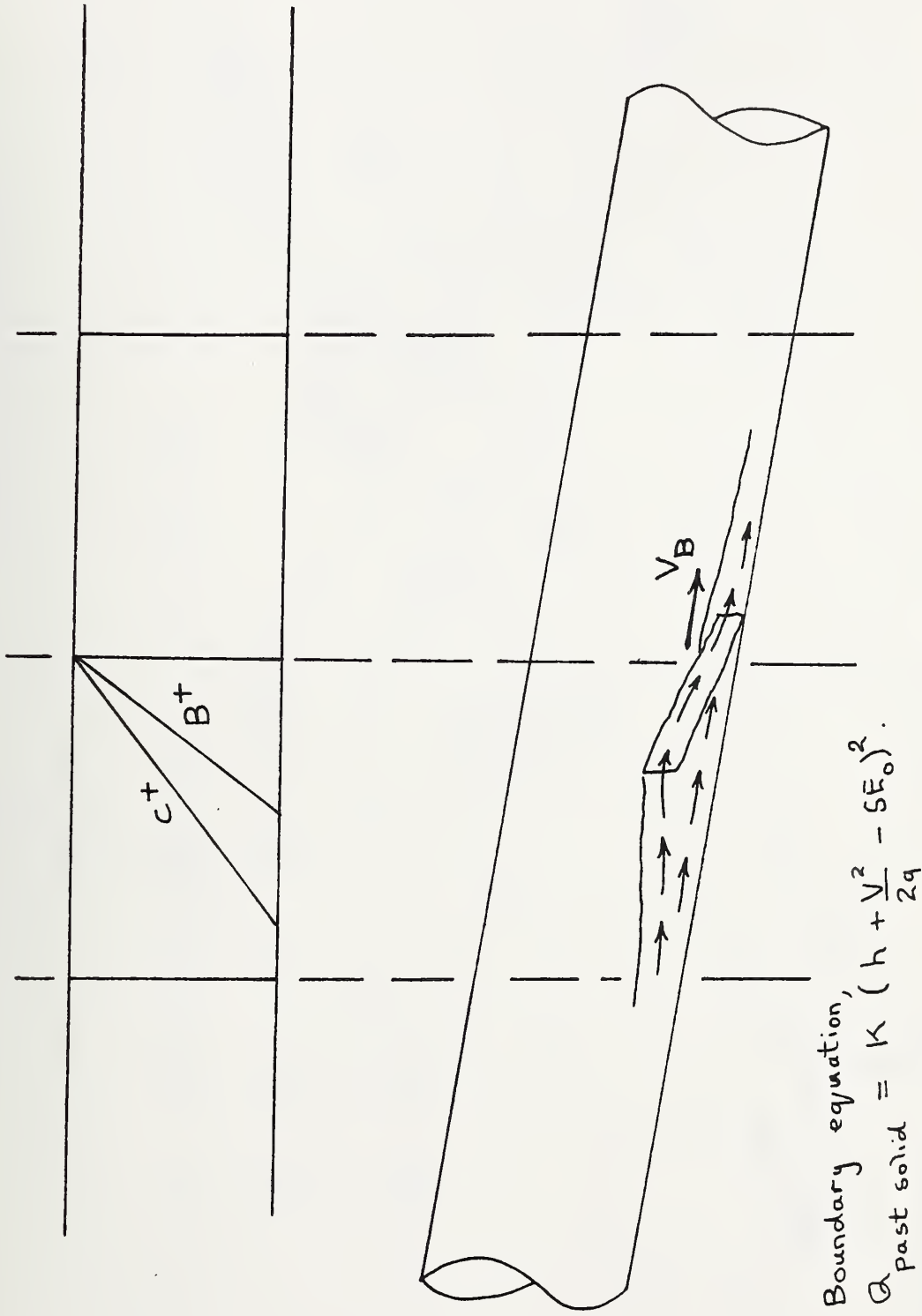


Figure 5. Solution of C^+ characteristic with body equivalent B^+ characteristic

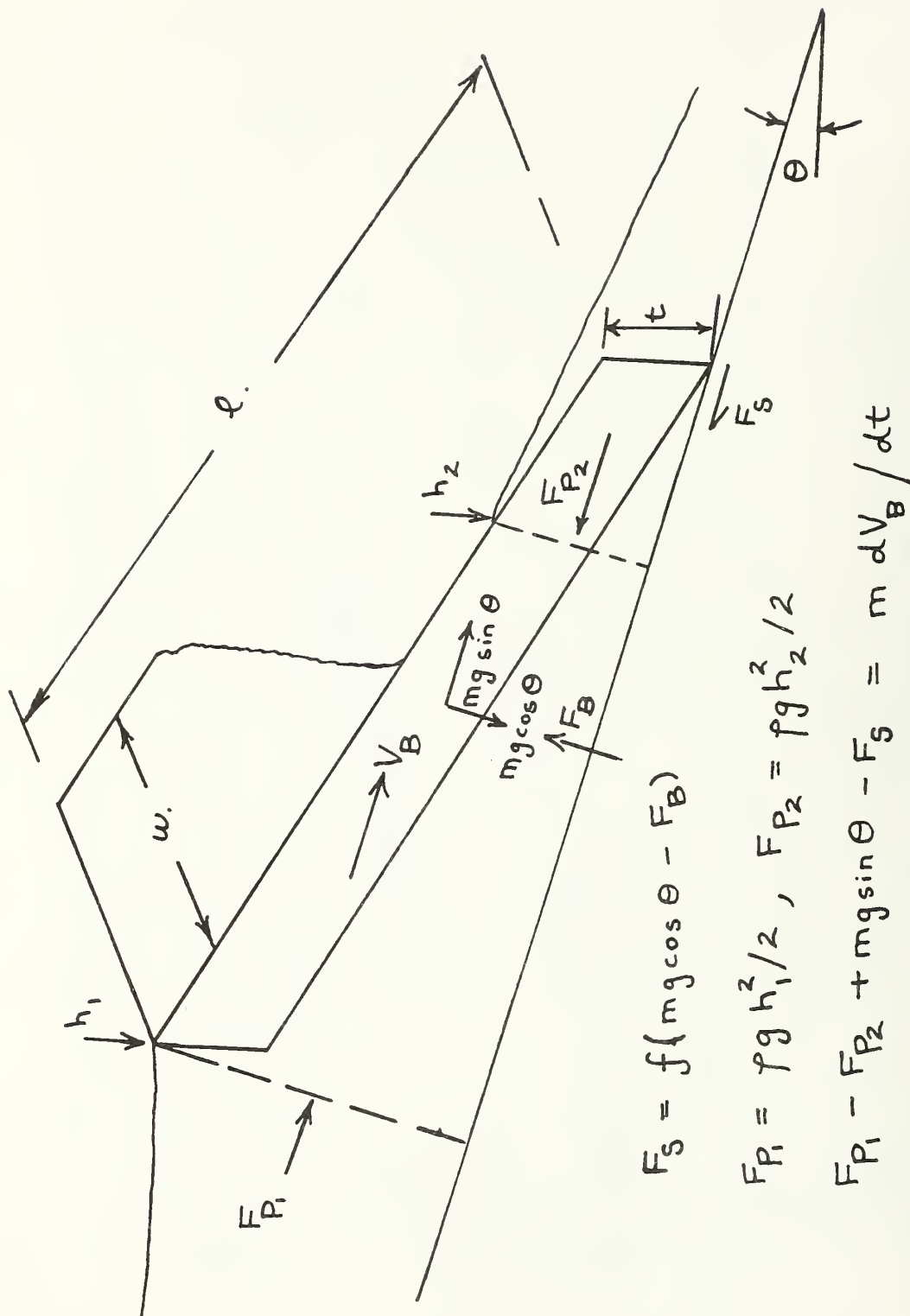
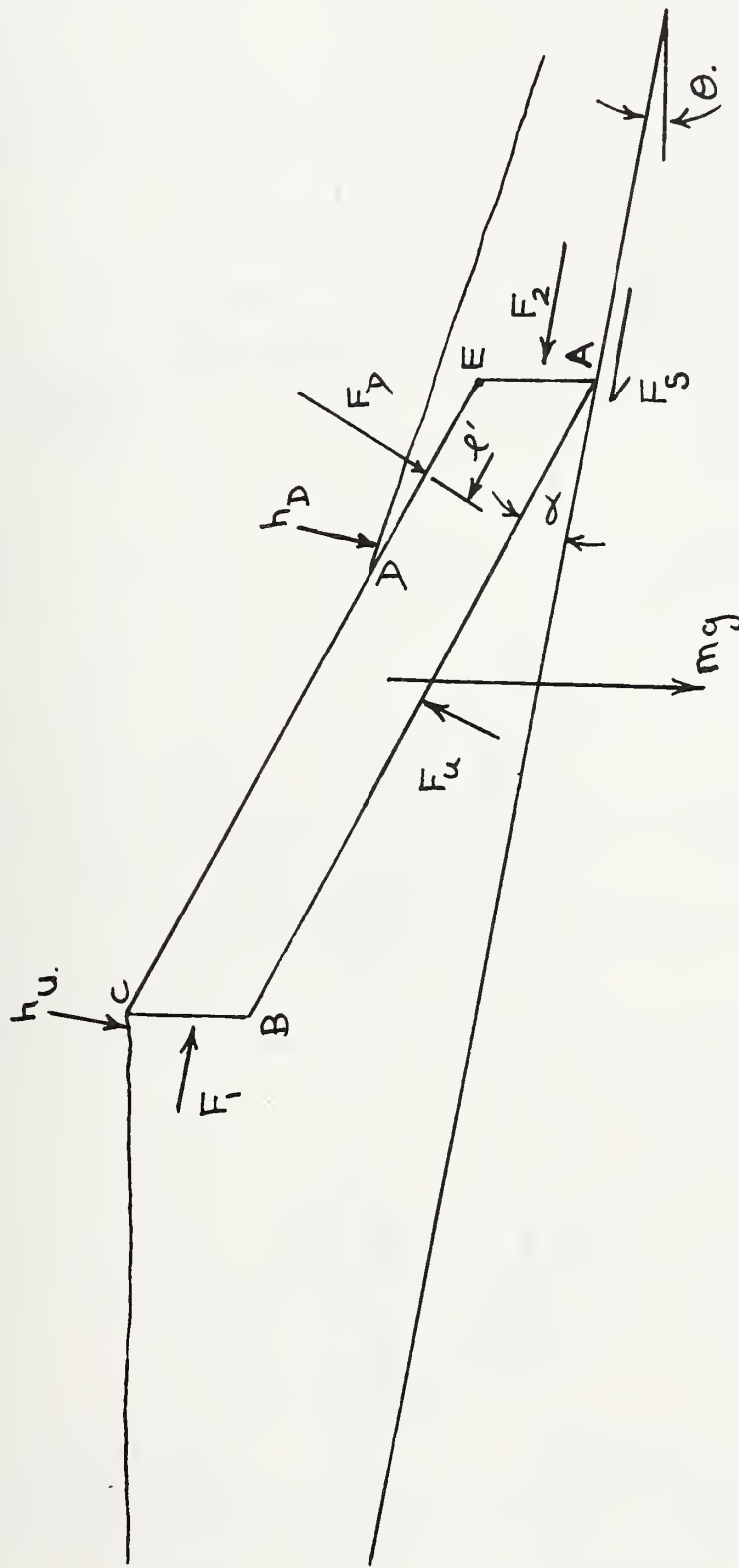


Figure 6. Equation of motion applied to a rectangular section solid



$$F_1(h_u - t/2) + F_u \cdot \ell/2 - mg(\cos \theta) \ell/2 - F_D \cdot \ell' - F_2 t/2 = 0$$

(Equation for small α)

Figure 7. Calculation of buoyancy forces

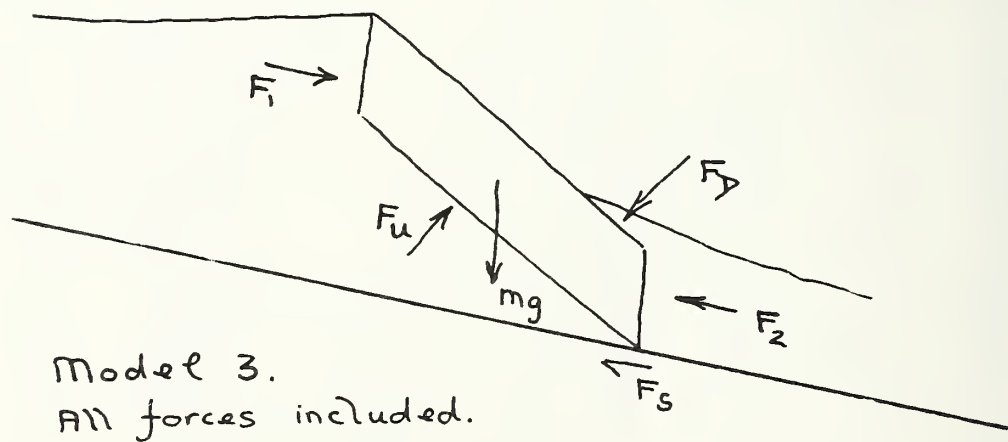
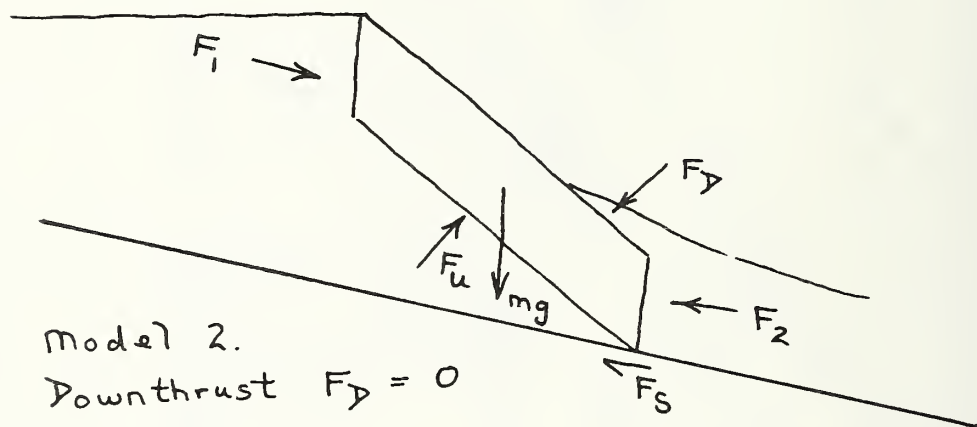
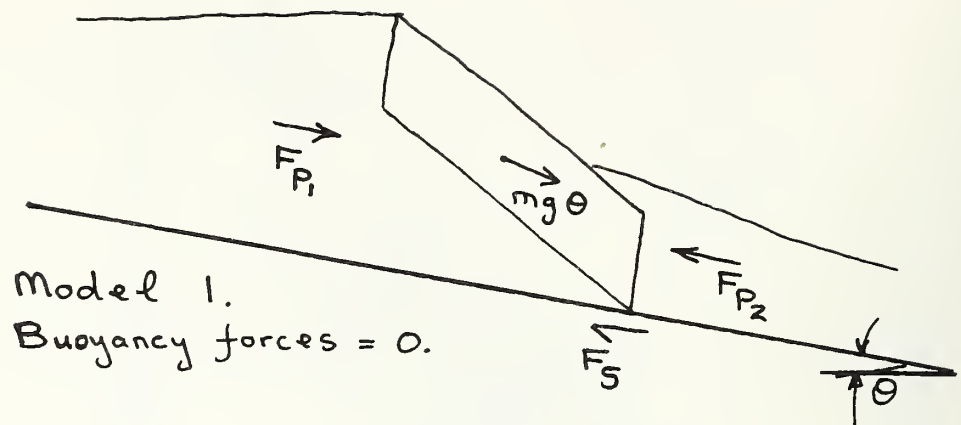


Figure 8. Summary of alternative force models

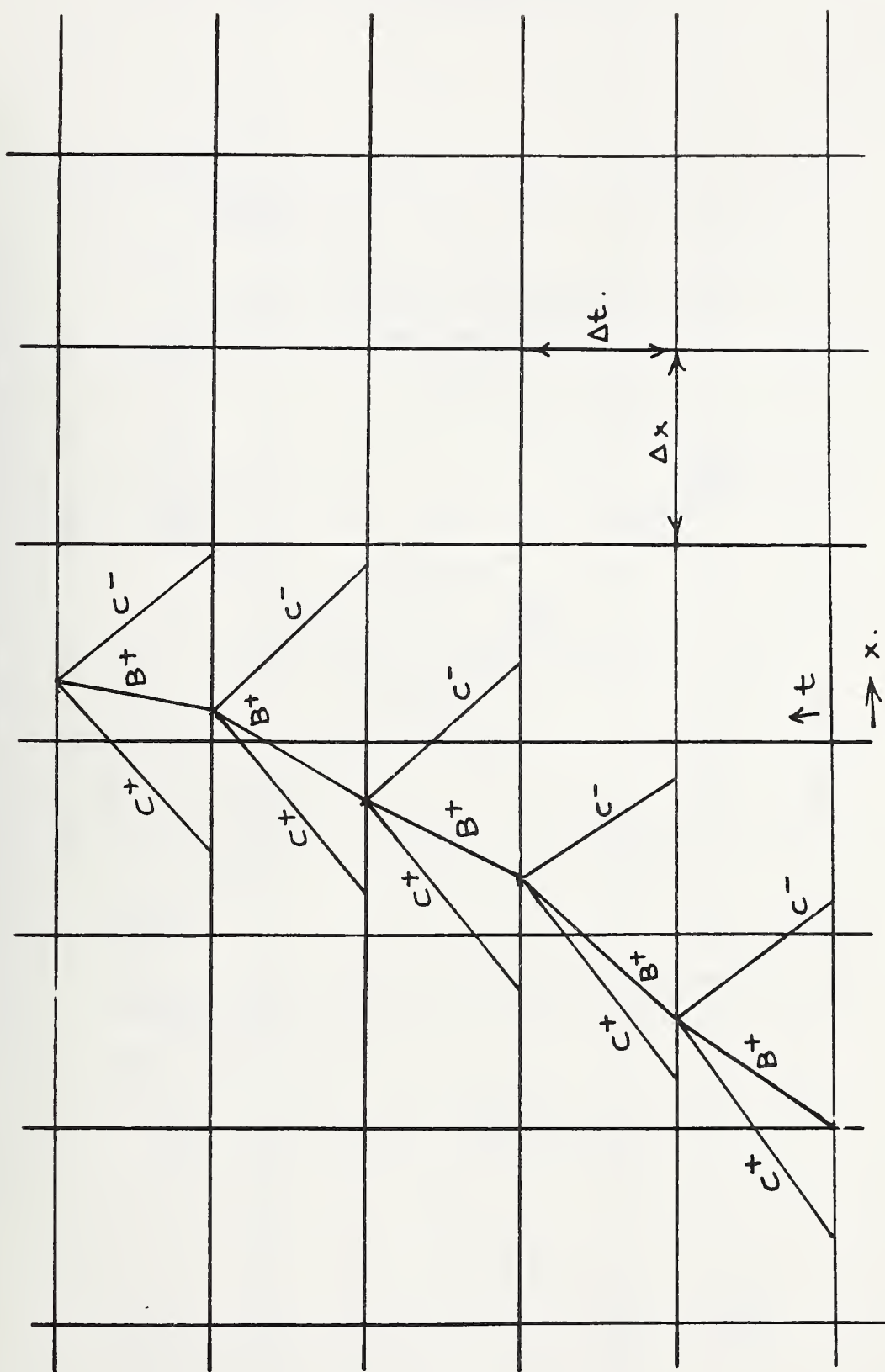
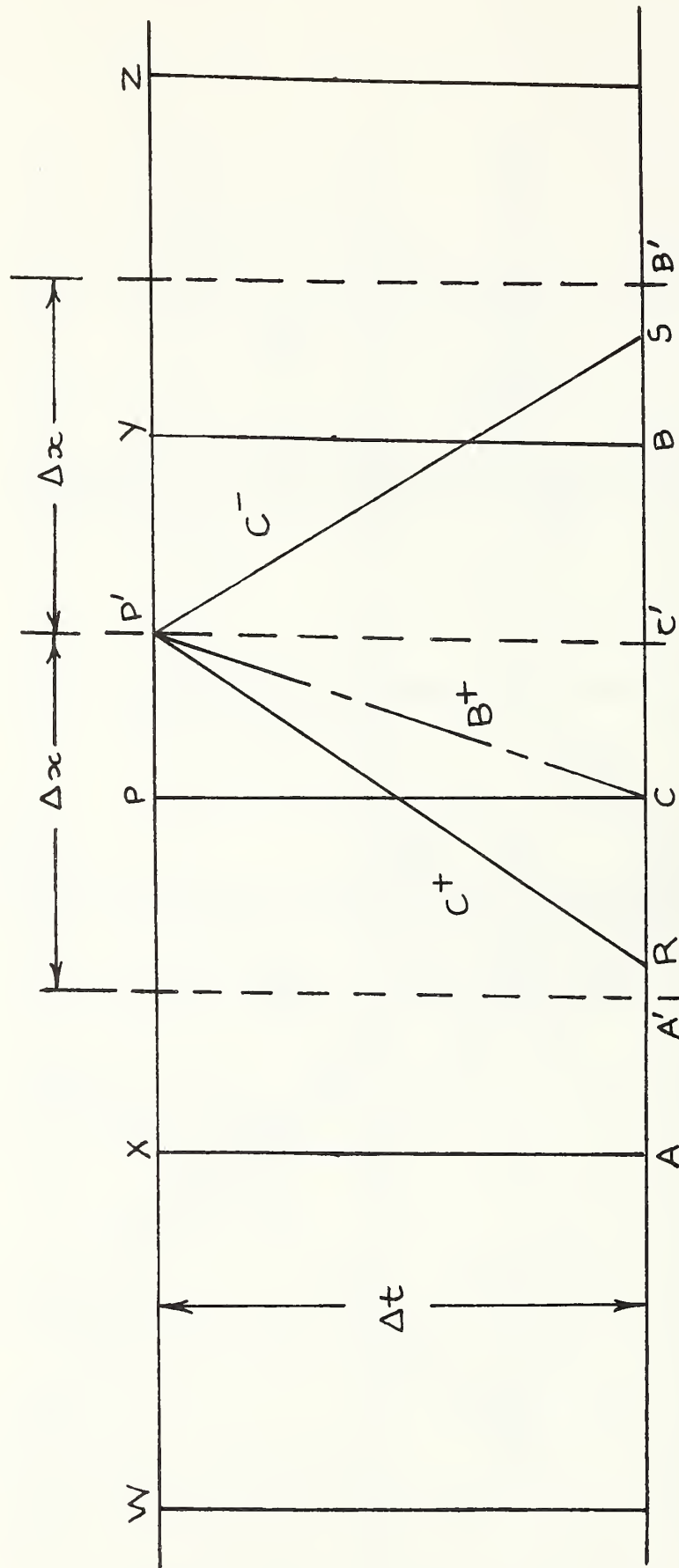


Figure 9. Schematic representation of solid motion in the xt plane



$$C^+ \frac{\Delta x}{\Delta t} = (V+c)_R, \quad C^- \frac{\Delta x}{\Delta t} = (V-c)_S$$

$$B^+ \frac{\Delta x}{\Delta t} = V_{\text{BODY}}.$$

Figure 10. Modifications to xt grid adjacent to the solid position for subcritical flow

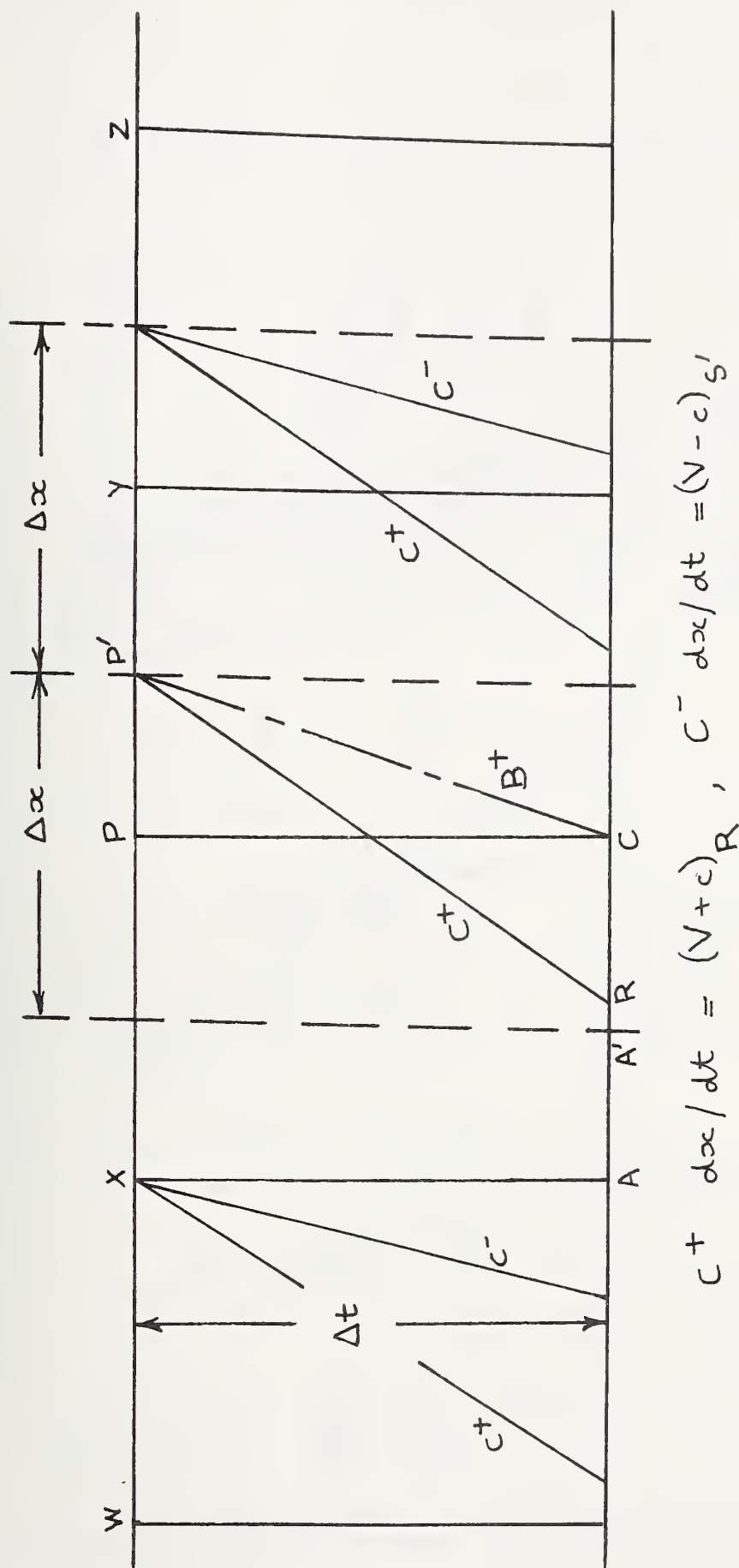


Figure 11. Modifications to xt grid adjacent to the solid position for supercritical flow

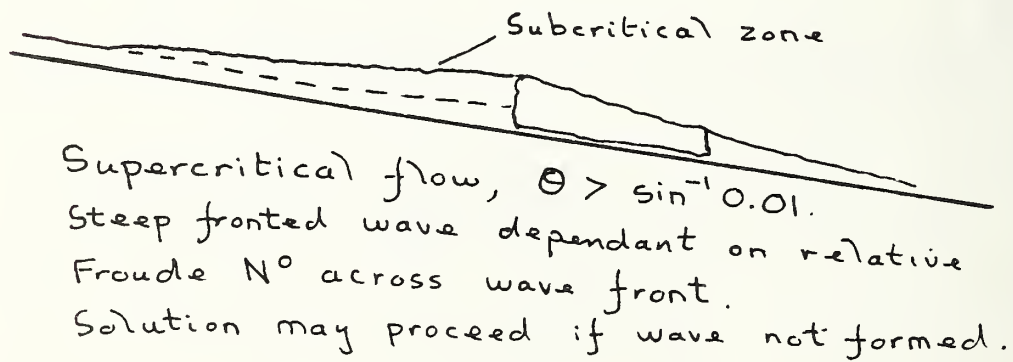
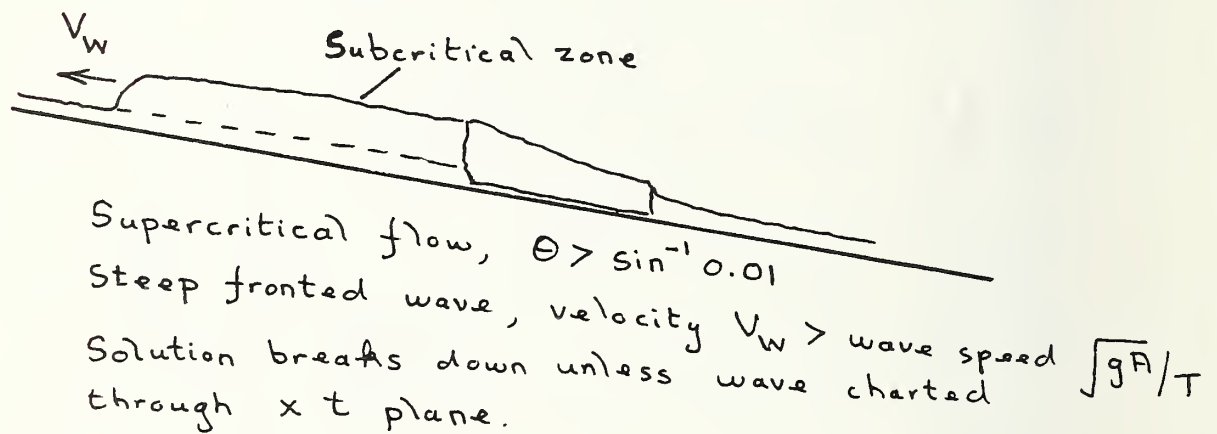
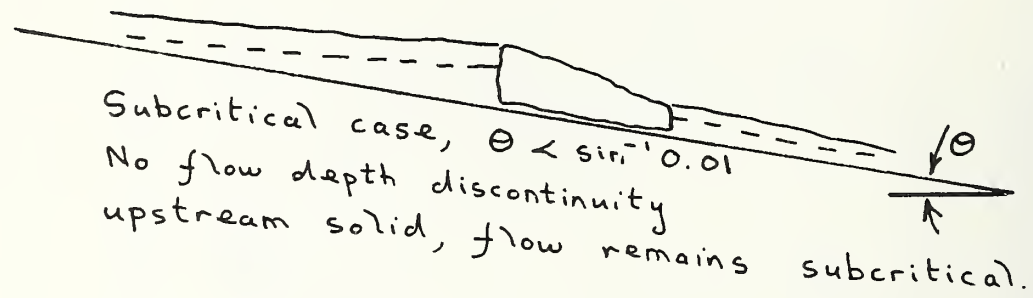


Figure 12. Propagation of steep fronted wave upstream from the solid position

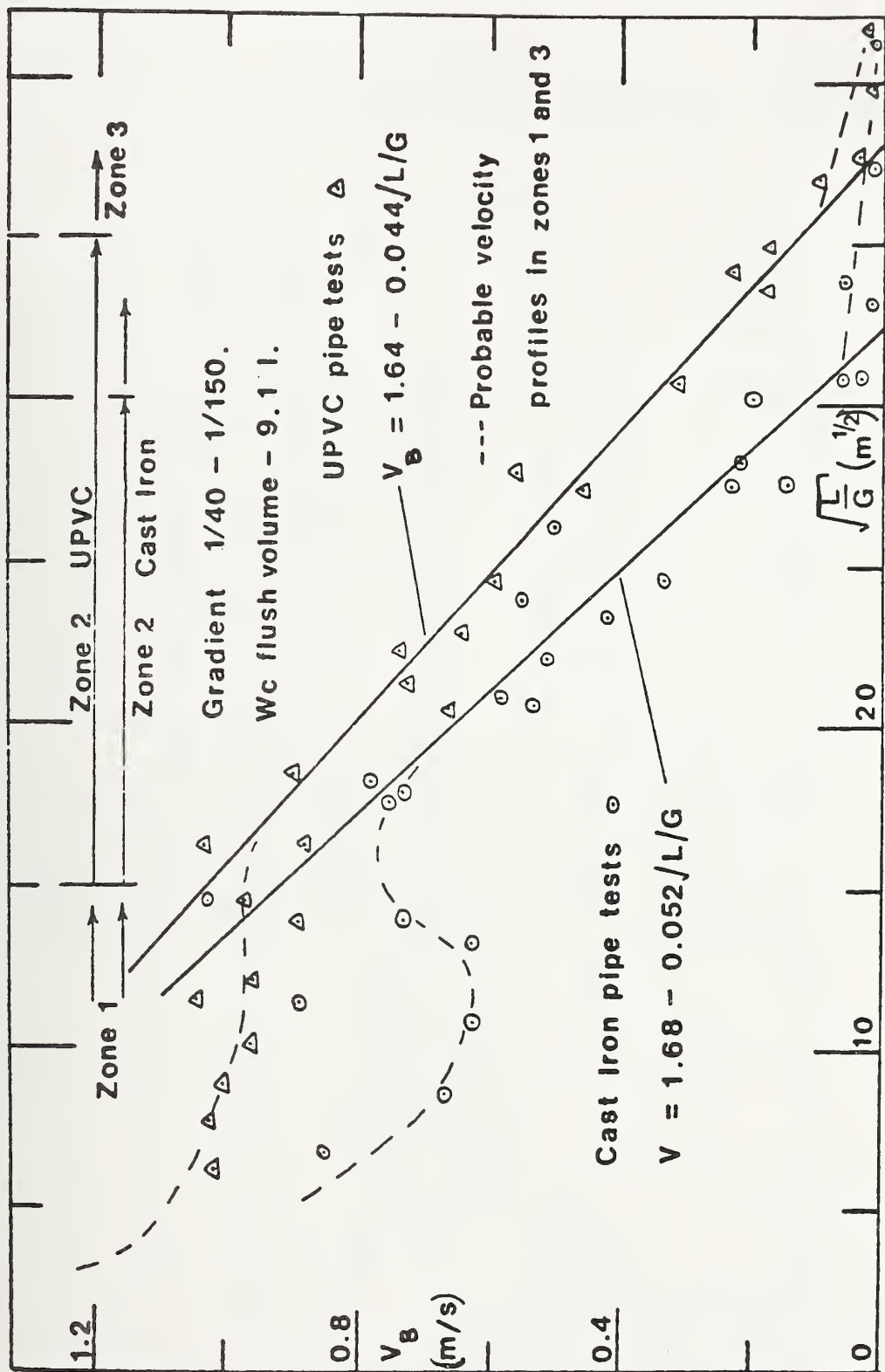


Figure 13. Comparison of maternity pad transport in UPVC or cast iron 100 mm diameter pipe

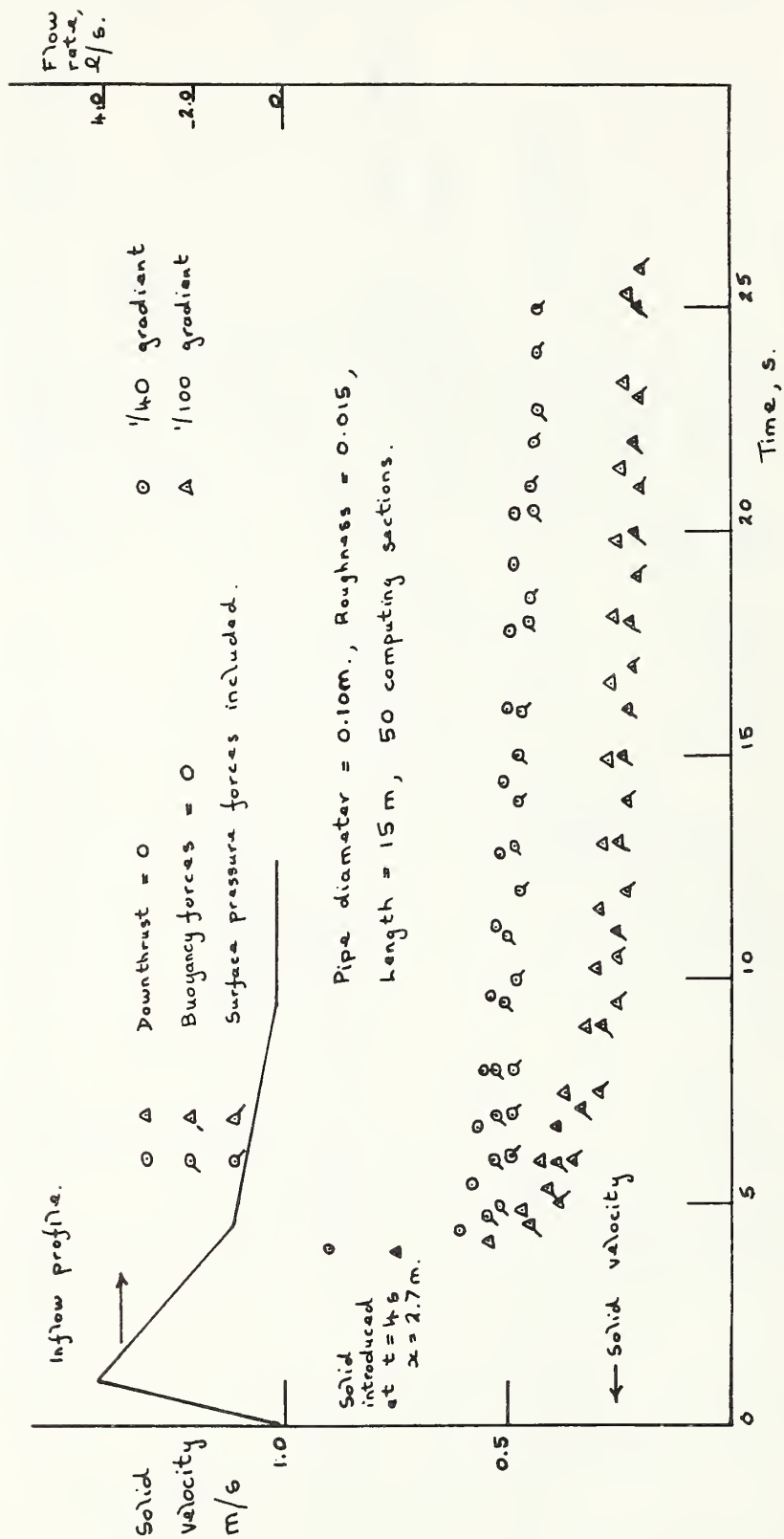


Figure 14. Influence of force model on the predicted solid velocity

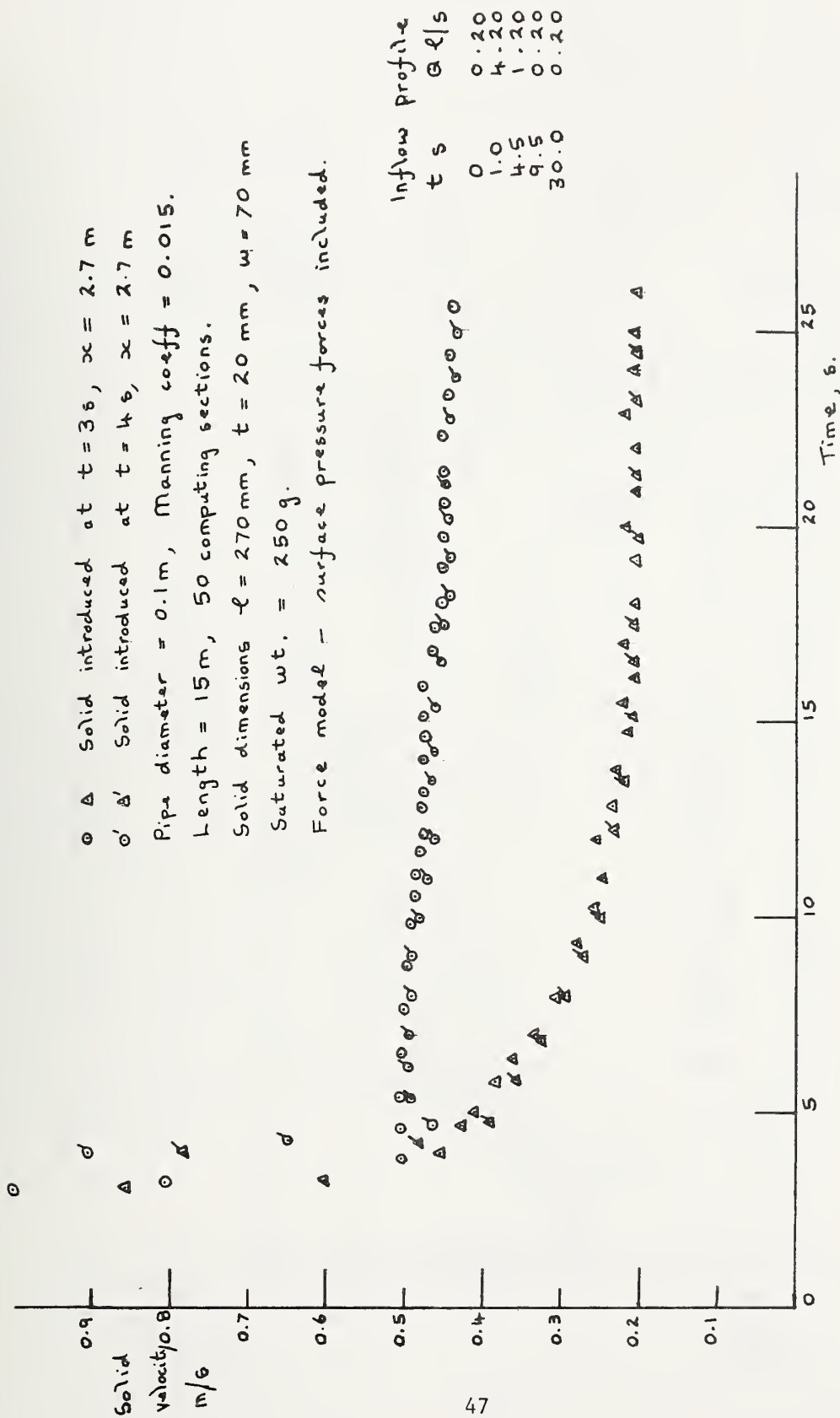


Figure 15. Influence of solid position in the inflow profile on predicted solid velocity

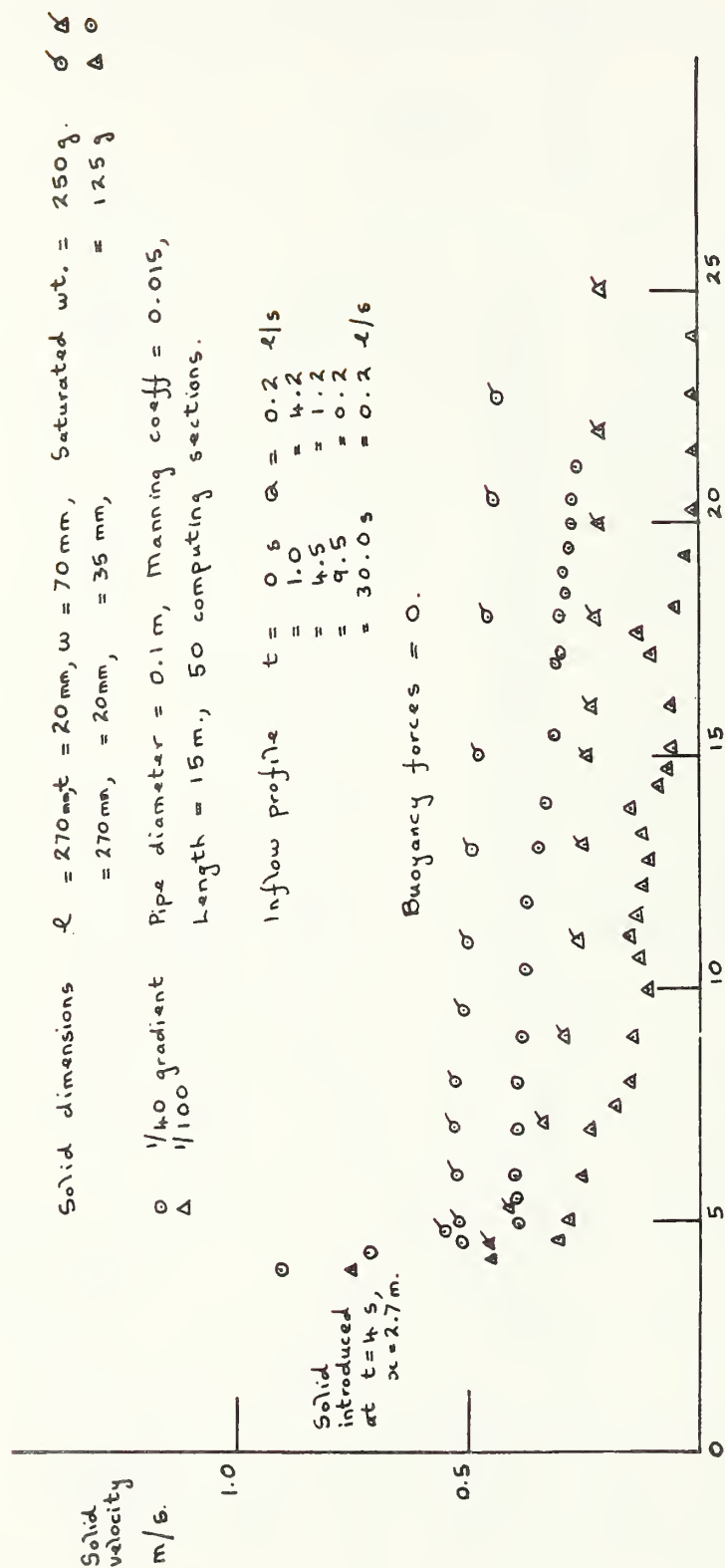


Figure 16. Influence of solid size on predicted velocity

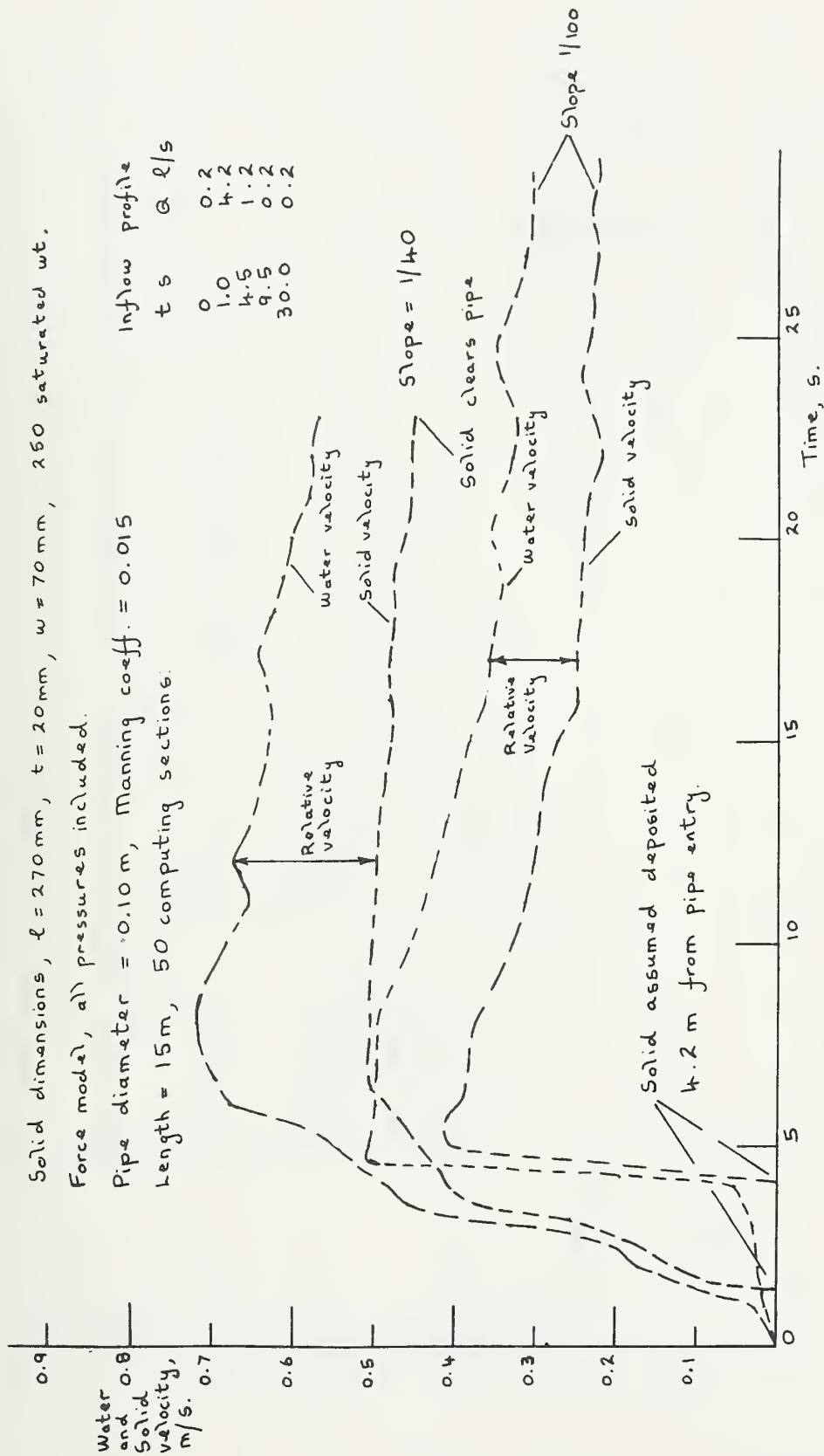


Figure 17. Initially stationary solid, predicted water and solid velocities illustrating relative flow over the body

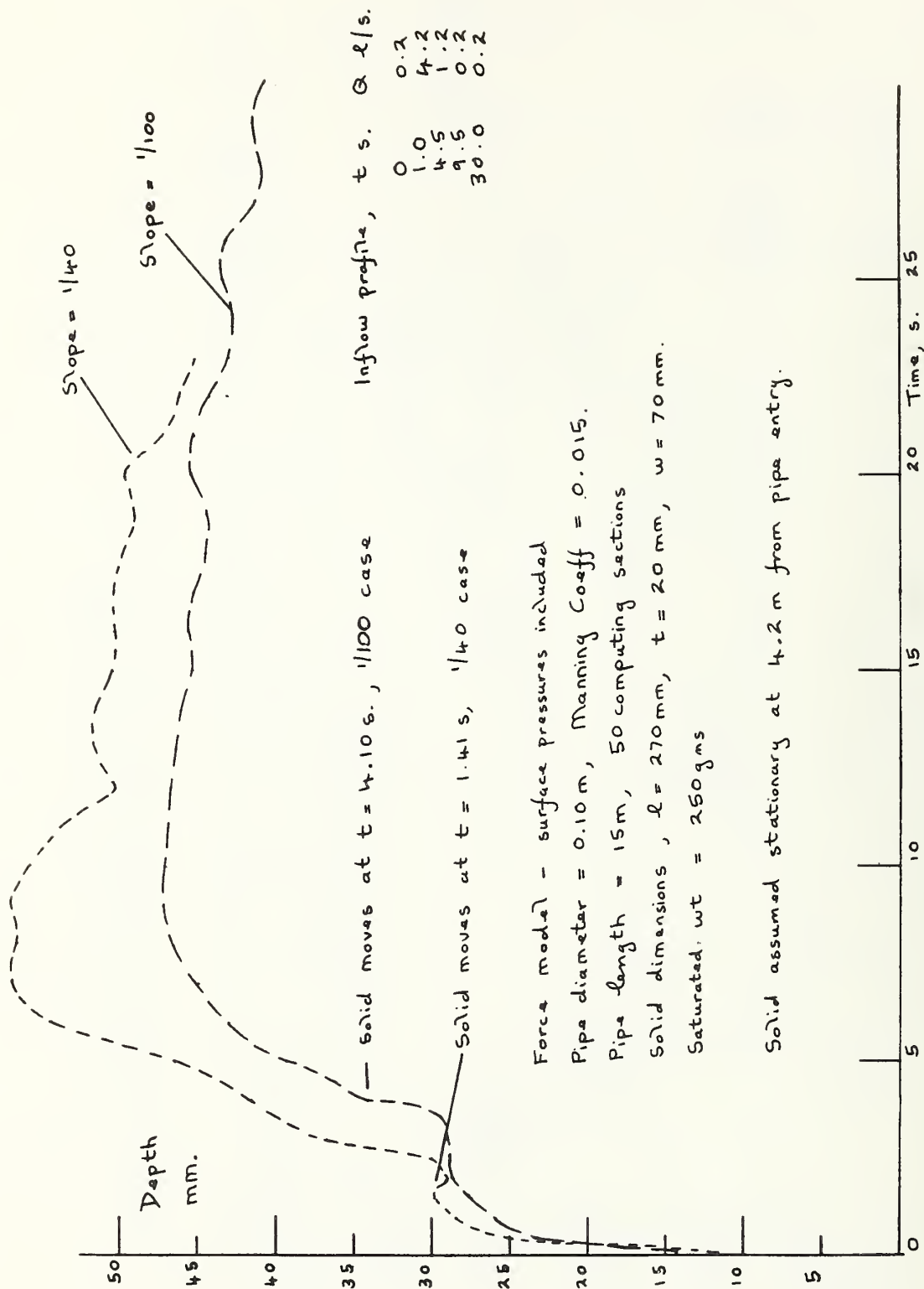


Figure 18. Initially stationary solid, depth upstream of the solid during motion

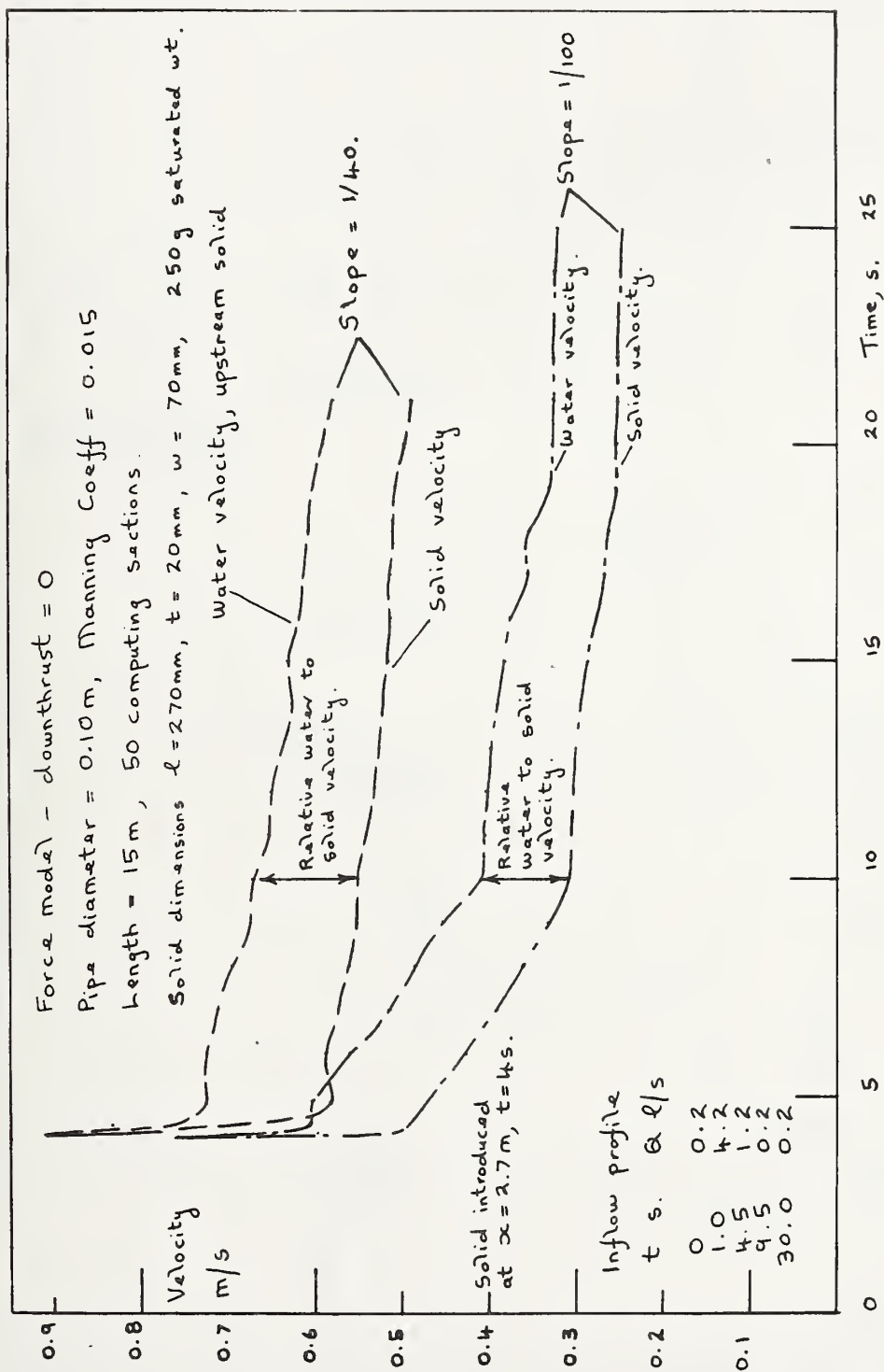


Figure 19. Solid injected into flow, predicted water and solid velocities illustrating relative flow over the body

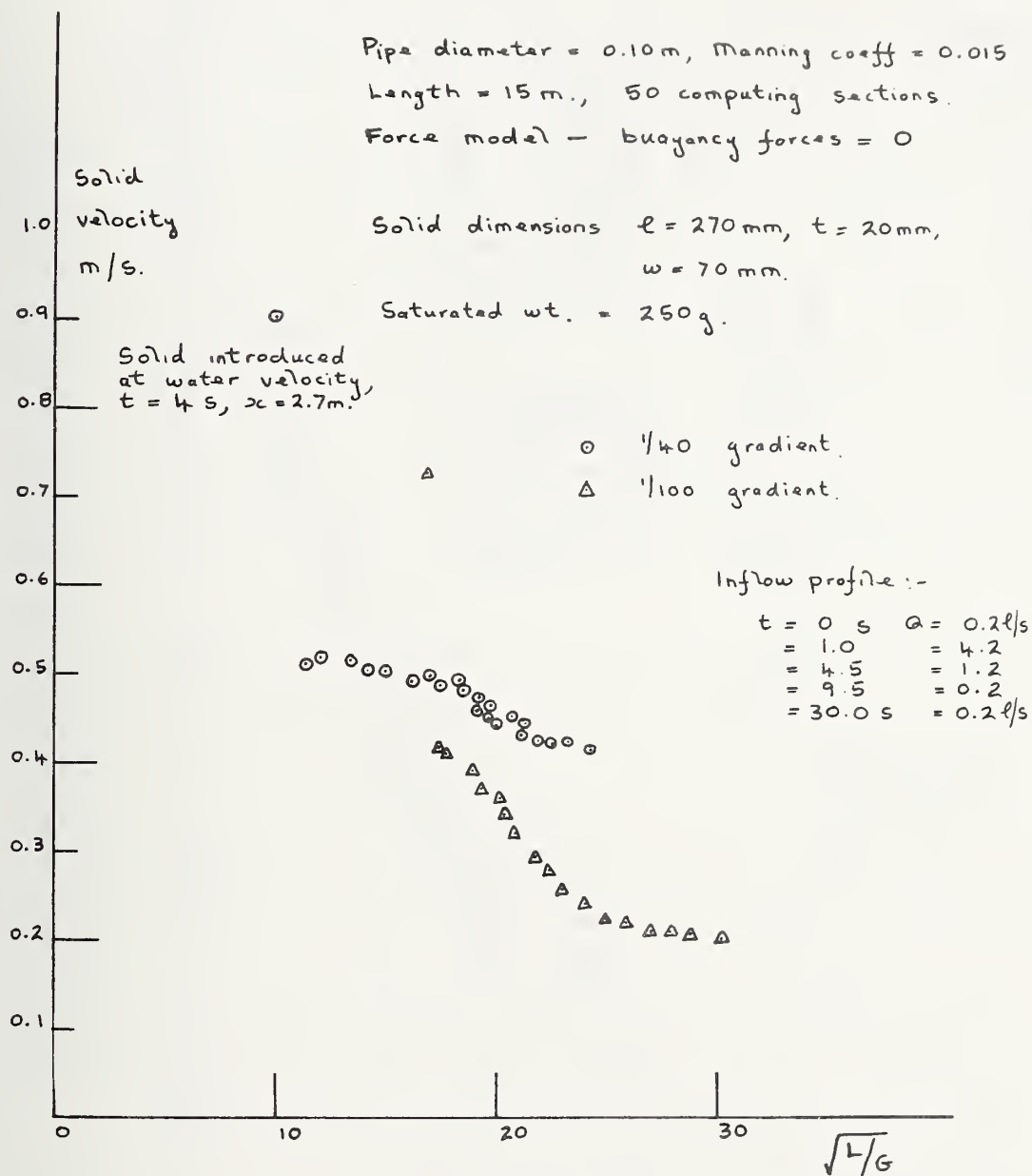


Figure 21. Predicted solid velocity plotted vs $\sqrt{L/G}$, pipe slopes 1/40 and 1/100

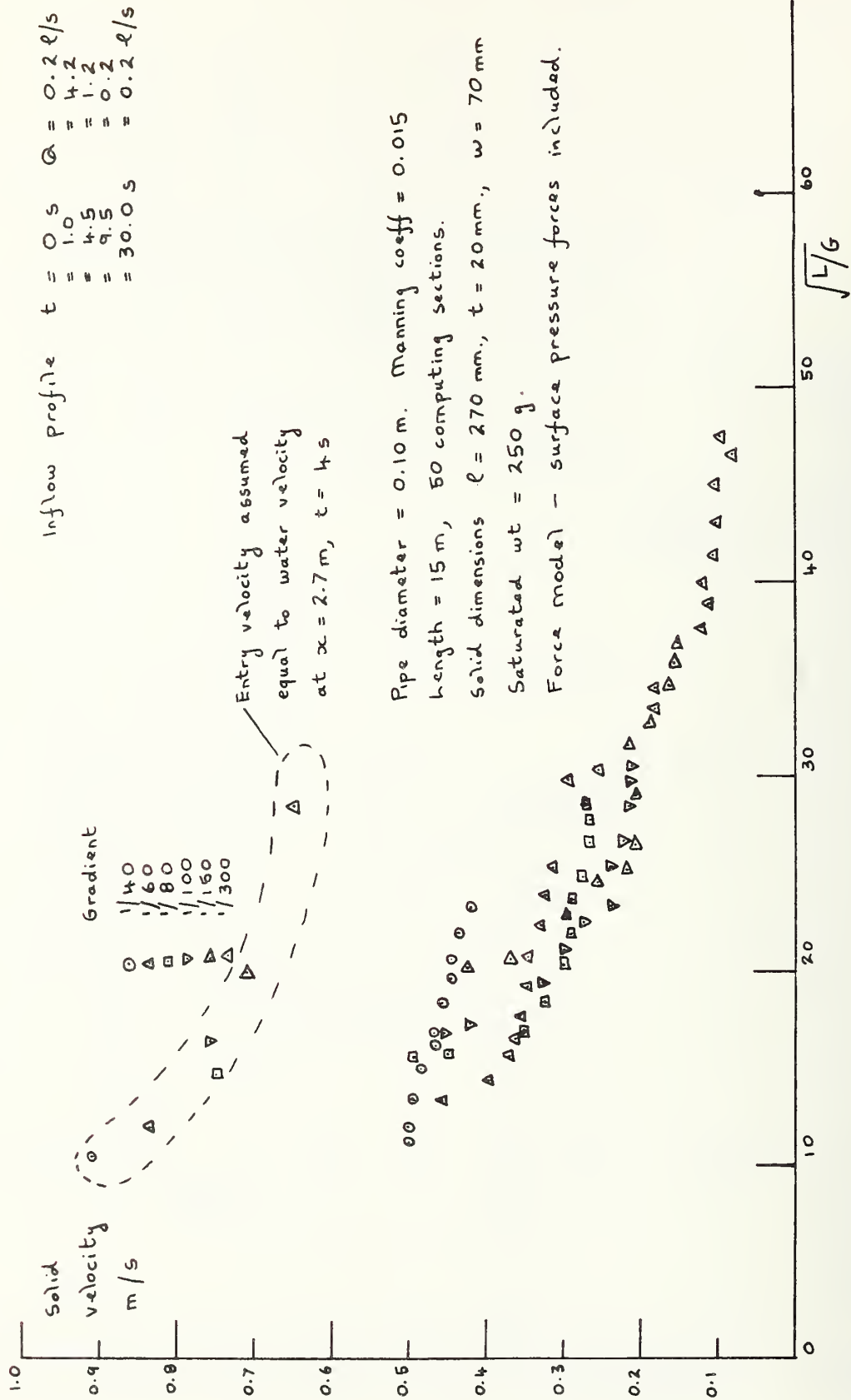


Figure 22. Predicted solid velocity plotted vs $\sqrt{L/G}$, pipe slopes 1/40 to 1/300

APPENDIX I
Program TRANSCD

Program TRANSCD

This appendix presents a complete print out of this program, written in Fortran, a flow chart, and sample input data. The program was run on the NBS Center for Building Technology Perkin Elmer 732 computer.

The program accepts data in SI units with the exception of the inflow profile, which is read in as litres/second and corrected to m^3/s within the program.

The program is written in terms of a series of subroutines that deal with specific aspects of the numerical solution presented in the report. In order to aid the understanding of the program, each subroutine is discussed individually, with the calculation methods outlined in each case. The titles used refer to the program printout included in this appendix.

Note that the notation employed in this appendix in describing the various subroutines is compatible with that used in the main report and not the program notation, although in most cases the variation is small.

The program as written applies only to simple straight pipes with choice of constant gradient, diameter and roughness; however, these subroutines can obviously be utilized in the modelling of more complex pipe networks in future programs.

Subroutine TIMINC

This subroutine determines the maximum values of wave speed and velocity at any section along the pipe at each time step. This ensures that the next time increment

$$\Delta t = \frac{\Delta x}{(V + c)}$$

is always sufficiently small to ensure a stable solution. This effectively removes the need for a time step factor, but this is retained in the program and normally set to unity.

Subroutine LOSS

This subroutine calculates the equivalent steady flow friction loss over each pipe section by means of the Manning equation, defined as

$$S = V |V| n^2 / m^{4/3}.$$

Note the use of V times absolute value of V to ensure that frictional forces always oppose the local flow direction.

Subroutine DEPTH

This subroutine is only called at the initial time zero to calculate the normal and critical depths based on the initial assumed flow. The values of h_c and h_n are then used to guide the solution whenever a subcritical or supercritical flow calculation choice arises.

Subroutine INFLOW

This subroutine calculates the inflow to the pipe at any time during the simulation, based on linear interpolation between successive pairs of Q, T coordinates.

Subroutine SHAPE

This subroutine calculates flow surface width, T, area A, and wetted perimeter depth.

It is also used, at the initial time zero, to calculate the terms necessary to provide the subcritical water surface profile.

It should be noted that this subroutine could be rewritten for any other pipe cross sectional shape and that the program in general is not restricted to circular cross section pipes. SHAPE is called from many of the other subroutines.

Subroutine WAVSPD

In this subroutine, the local wavespeed is simply based on

$$c = \sqrt{\frac{gA}{T}}$$

and utilizes SHAPE.

Subroutine PROFIL

This subroutine is only fully employed if the initial flow is shown to be subcritical as a result of the normal and critical depths calculated via DEPTH.

The water surface profile is calculated from an assumed critical depth at pipe exit by means of the techniques described in the report. The calculation utilizes SHAPE. If the flow is supercritical, then PROFIL sets all depths equal to the normal flow depth.

Subroutine INTER

This subroutine carries out the necessary interpolations to fix conditions at points R and S in subcritical flow and R and S' in supercritical flow (figure 4).

Subroutine ENTRY

This subroutine deals with the flow depth, velocity and wave speed at the upstream boundary. The inflow at any time is calculated from INFLOW and this flow rate is then employed, in the subcritical case, in conjunction with the appropriate C^- characteristic to yield the required parameter values referred to in figure 5.

In the supercritical flow case, identified in terms of the initial flow normal to critical flow depth comparison, the inflow curve is solved in conjunction with the normal depth relationship as the downstream conditions, represented by the C^- characteristic previously employed, can no longer effect conditions at pipe entry.

Subroutine NODAL

This subroutine solves the C^+ and C^- characteristics at all internal pipe sections between $x = \Delta x$ and $x = L - \Delta x$ (figure 4) for both subcritical and supercritical flow.

In addition for supercritical flow, it also calculates the flow exit condition, which is based solely on upstream conditions.

Subroutine EXIT

This subroutine is only utilized for the subcritical flow case. The exit boundary conditions are determined by solution of the appropriate C^+ characteristic (figure 4) with the critical depth expression

$$\frac{Q^2}{g A^3} T - 1 = 0$$

$$\text{and } Q = VA = A(X2 - X1h).$$

As this is effectively a loss coefficient concentrated at pipe exit, the boundary equation must be solved in the form

$$\frac{Q |Q|}{g A^3} T - 1 = 0$$

$$\text{or } (X2 - X1h) |(X2 - X1h)| \frac{T}{g A^3} = 1$$

where $| |$ indicate the absolute value of the term enclosed.

The solution is performed by means of the bisection technique described in the main text.

Subroutine ASSIGN

This subroutine reassigns the values calculated at the end of a time step, points P in figure 4 to allow the calculation procedures to move on one time increment. This is necessary to avoid program storage space problems.

Subroutine INSERT

This subroutine ensures that the solid upstream water velocity, depth, and wave speed are equated to those calculated at the insertion time and pipe section preset in the input data. The solid velocity is set equal to the fluid velocity at this stage. INSERT is only called once; at subsequent time steps, subroutine SOLID calculates the conditions at the solid.

Subroutine SOLID

This subroutine calculates the water velocity and depth upstream of the solid by means of the specific energy vs. relative flow rate boundary equation. The flow conditions downstream of the solid are determined in the same manner as ENTRY, dependent on flow regime.

Subroutine FORCE

This subroutine calculates the force acting on the solid. Initially it determines the inception of motion by monitoring the force acting on the solid. Various force models may be investigated by modifying this routine.

FLOW CHART PROGRAM TRANSCD

Set up initial conditions.

Time = 0

Read pipe data - Line 1 data table

Read calculation data - Line 2 data table

Read inflow profile - Lines 3-8 in example data

Read solid position - Line 9 in example data

Read solid dimensions - Line 10 in example data

Read specific energy to flow over solid coefficients - Line 11 in example data

Read force model indicators and friction coefficients - Line 12 in example data

Adjust inflow rate from ℓ/s to m^3/s solid dimensions from mm to m solid saturated weight from g to kg.

Calculation of initial steady conditions at time zero.

CALL DEPTH - Calculation of normal and critical depths at initial flow.

$$h_c < h_n$$

Subcritical flow
CALL PROFIL - calculate
water surface profile and
interpolate for section
depths.

$$h_n < h_c$$

Supercritical flow
CALL PROFIL - set all depths
to normal value.

CALL ASSIGN - set up base arrays H, V, C

CALL TIMINC - identify maximum V, C to yield stable time step.

$$\Delta\infty = PL/N$$

$$\Delta t = \Delta\infty / (V + c)_{\max}$$

Output - Initial conditions and pipe description

- Solid dimensions and model indicators
- Depth, velocity, wavespeed at each increment if $N < 10$,
at 1/10 pipe length points if $N > 10$ and a multiple of 10

A - Update time and commence unsteady flow simulation.

CALL TIMINC - Identify new time step based on $(V, C)_{\max}$

Check Time vs. TMAX

$$\text{Time} < TMAX$$

Go to B

$$\text{Time} \geq TMAX$$

Go to G

B - Unsteady flow calculations.

CALL INFLOW - Calculate pipe inflow rate from data profile.

CALL INTER - Interpolate to obtain base conditions HR, HS or HS' etc.
Contains choices based on flow regime and presence of the
solid between any two computing points.

CALL LOSS - Calculation of equivalent steady flow loss terms, SR, SS.

CALL ENTRY - Solves upstream boundary condition for either sub or super-
critical flow.

CALL NODAL - Solves C^+C^- characteristics based on output of INTER and LOSS.
Omits the two nodes bracketting a moving solid and the initial
location node of a stationary solid. In supercritical flow,
NODAL also provides exit conditions.

For subcritical flow only, CALL EXIT - exit depth based on critical depth at pipe discharges.

Check solid model being simulated:

Injected solid, time < injection time, Go to C

Injected solid, time \geq injection time, on the first occasion, Go to D

Initially stationary solid, Go to E

Injected solid, time > injection time, following first occasion, Go to E

D - CALL INSERT - assigns water velocity at solid entry station and time to be solid velocity.

Go to C

E - CALL SOLID - calculate conditions on upstream and downstream solid faces. Downstream velocity given by same technique as ENTRY dependnet on flow regime.

Go to C

C - CALL ASSIGN - sets up base arrays for next time step.
Output of simulation results.

Velocity, depth, flow and wavespread at solid and at 2 points each 1/10 pipe length upstream and downstream of the moving solid.
Solid velocity and body forces.
Solid position.

Check presence of solid, no solid Go to B, solid present Go to F.

F - CALL FORCE - calculation of forces acting on solid over next time step.
Calculation of solid position and velocity at end of next time step.

Check solid still in pipe at end of next time step:

Solid position > pipe length, set solid indicators to no solid and continue calculation to TMAX, Go to B.

G - Program terminates.

SAMPLE INPUT DATA, PROGRAM TRANSCD.

Line 1.

Pipe diameter, Manning coeff., slope, length.

Format 4F10.4.

VVVV -.1000 VVVV 0.0150 VVVV 0.0100 VVVV 15.0000

Line 2.

N° calculation steps, Run time, Time step factor. (Note, N° calculation sections < 10 or multiple of 10 to match output format, time step factor, normally set = 1.)

Format I3, 2F10.4

V 50 VVV 30.0000 VVVV 1.000

Line 3.

N° pairs of coordinates on inflow-time curve.

Format I3

VV 5

Line 4 to 8 (note actual number depends on Line 3).

Inflwo QIN or time TIN

Format 2F10.4

VVVV 0.2000 VVVV 0.0000

VVVV 4.2000 VVVV 1.0000

VVVV 1.2000 VVVV 4.5000

VVVV 0.2000 VVVV 9.5000

VVVV 0.2000 VVV 50.0000

Line 9.

Solid initial position in pipe, must be at a section not an intermediate location. Applies to both initially stationary and injected models.

Format I3

V 10

Line 10.

Solid dimensions, length, width, thickness, saturated weight.

Format 4F10.4

VV 270.0000 VVV 70.0000 VVVV 20.0000 VV 250.0000.

Line 11.

Solid minimum specific energy to allow bypass flow, Specific energy vs. Q coefficient.

Format 2F10.4

VVVV 0.0200 VVVV 0.6000

Line 12.

Buoyancy force indicator, 0. force omitted, 1. force included. Downthrust force indicator, 0. force omitted, 1. force included. Solid surface shear stress, set 0. Sliding friction factor, static friction coefficient.

Format 5F10.4

VVVV 1.0000 VVVV 0.0000 VVVV 0.0000 VVVV 0.1000 VVVV 0.1500

Line 13.

Solid insertion time, zero for stationary solid. Solid insertion model indicator, zero for stationary solid, > 0 for moving solid.

Format F10.4 I3

VVVV 4.0000 VV 4

Units - SI units used in data field except for inflow QIN in ℓs , converted to m^3/s in program. Output in S.I., except flow rate in ℓs . Solid dimensions and saturated weight read in mm and g, converted to m and kg in program.

TTTTTTT	RRRRRR	AAAAA	NNN	NN	SSSSS	CCCLCC	UUUUUUU
TTTTTTT	RRRRRR	AAAAAAA	NNN	NN	SSSSSSS	CCCLCCCL	UUUUUUUU
TT	RR	AA	NNN	NN	SS	CC	UU
TT	RR	AA	NNN	NN	SS	CC	UU
TT	RRRRRR	AAAAAAA	NNN	NN	SSSSSSS	CC	UU
TT	RRRRRR	AAAAAAA	NNN	NN	SSSSSSS	CC	UU
TT	RR	AA	NNN	NN	SS	CC	UU
TT	RR	AA	NNN	NN	SS	CC	UU
TT	RR	AA	NNN	NN	SSSSSSS	CCCLCCCL	UUUUUUUU
TT	RR	AA	NNN	NN	SSSSSSS	CCCLCCCL	UUUUUUUU

AAAAA	CCCCC	UUUUUUUU	UUUUUUUU	UUUUUUUU	UUUUUUUU	UUUUUUUU	UUUUUUUU
AAAAAAA	CCCCCCC	UUUUUUUU	UUUUUUUU	UUUUUUUU	UUUUUUUU	UUUUUUUU	UUUUUUUU
AA	CC	UU	UU	UU	UU	UU	UU
AA	CC	UU	UU	UU	UU	UU	UU
AAAAAAA	CCCCC	UUUUUUUU	UUUUUUUU	UUUUUUUU	UUUUUUUU	UUUUUUUU	UUUUUUUU
AAAAAAA	CCCCC	UUUUUUUU	UUUUUUUU	UUUUUUUU	UUUUUUUU	UUUUUUUU	UUUUUUUU
AA	CC	UU	UU	UU	UU	UU	UU
AA	CC	UU	UU	UU	UU	UU	UU
AA	CC	UUUUUUUU	UUUUUUUU	UUUUUUUU	UUUUUUUU	UUUUUUUU	UUUUUUUU
AA	CC	UUUUUUUU	UUUUUUUU	UUUUUUUU	UUUUUUUU	UUUUUUUU	UUUUUUUU

111	111	111	111	111	111	111	111
111	111	111	111	111	111	111	111
11	11	11	11	11	11	11	11
11	11	11	11	11	11	11	11
11	11	11	11	11	11	11	11
11	11	11	11	11	11	11	11
11	11	11	11	11	11	11	11
1111111	1111111	1111111	1111111	1111111	1111111	1111111	1111111
1111111	1111111	1111111	1111111	1111111	1111111	1111111	1111111

0000000000	0000000000	0000000000	0000000000	0000000000	0000000000	0000000000	0000000000
0000000000	0000000000	0000000000	0000000000	0000000000	0000000000	0000000000	0000000000
00	00	00	00	00	00	00	00
00	00	00	00	00	00	00	00
00	00	00	00	00	00	00	00
00	00	00	00	00	00	00	00
00	00	00	00	00	00	00	00
00	00	00	00	00	00	00	00
0000000000	0000000000	0000000000	0000000000	0000000000	0000000000	0000000000	0000000000
0000000000	0000000000	0000000000	0000000000	0000000000	0000000000	0000000000	0000000000

C TRANSC ARE A SERIES OF PROGRAMS DESIGNED TO APPLY THE METHOD OF
C CHARACTERISTICS SOLUTION TO THE EQUATIONS DEFINING
C UNSTEADY FLOW IN PARTIALLY FILLED CHANNELS.

C
C
C
C
C
C
C

102

104

50

```

C      SOLTIM-TIME POSITION OF SOLID IN INFLOW PROFILE,NOTE
C      ZERO VALUE INDICATES STATIONARY IN PIPE AT DESIGNATED
C      SECTION NSOL,INSOL-INDICATOR OF SOLID VELOCITY,GT.0
C      INDICATES THAT FLOW VELOCITY AT SECTION NSOL IS ASSUMED
C      AS CALCULATION START POINT.
      READ(4,102) NSOL
      IF (NSOL.EQ.0)GOTO 729
      READ(4,100) TL,TM,TT,SM
      READ(4,104) SEQ,XK
      READ(4,109)XFAC,XFAC2,TAU,FMOV,FSTAT
109      FORMAT(5F10.4)
      READ(4,105)SOLTIM,INSOL
105      FORMAT(F10.4,I3)
729      CONTINUE
      NSOL1=NSOL
      IF(INSOL.GT.0) NSOL=J

C
C
C
C
C      CALCULATION OF INITIAL CONDITIONS ALONG THE PIPE
C      BASED ON GRADUALLY VARIED FLOW EQUATIONS. THE
C      TERMINAL CONDITIONS IN THE PIPE ARE BASED ON
C      CRITICAL DEPTH AT PIPE EXIT.
      CALL DEPTH(TIME)
      CALL PROFIL(GIN(1),HN,HC,XN)
      CALL ASSIGN(N)
      IF(TIME.LE.SOLTIM.AND).INSOL.GT.0) VSOL=V(NSOL)
C      CALCULATION OF TIME STEP AND LENGTH SECTION.
      CALL TIMINC(N,VP,CP,VN,CN)
      DX=PL/FLOAT(N)
      DT=DX/(TFAC*(CN+VN))
      DTD=DT

C
C      CALCULATION OF SOLID INITIAL POSITION
      IF(NSOL1.GT.0) XSOL=DX*FLOAT(NSOL1-1)
      IF(INSOL1.GT.0) XPDS=DX*FLOAT(NSOL1-1)

C
C
C
C      OUTPUT TEST DESCRIPTION PLUS INITIAL CONDITIONS.
      WRITE(3,202)D,RM,SO,PL
202      FORMAT(1H1,/10X,'TEST PIPE CONFIGURATION:-',
1 /10X,'DIAMETER = ',F10.4,' M.',
1 10X,'MANNING COEFFICIENT:-',F10.4,
1 /10X,'PIPE SLOPE = ',F10.4,' PIPE LENGTH = ',
1 F10.4,' M.',//)
      IF(HC.GT.HN) WRITE(3,200)HN,HC
      IF(HC.LE.HN) WRITE(3,201)HN,HC
200      FORMAT(10X,'FLOW SUPERCRITICAL, ',NORMAL DEPTH = ',F10.4,
1 ' M.', AND CRITICAL DEPTH = ',F10.4,' M.',//)
201      FORMAT(10X,'FLOW SUBCRITICAL, ',NORMAL DEPTH = ',
1 F10.4,' M. AND CRITICAL DEPTH = ',F10.4,' M.',//)
      QIN(1)=QIN(1)*1000.0
      WRITE(3,203)QIN(1),HN,CN
      QIN(1)=QIN(1)/1000.0
203      FORMAT(10X,'INITIAL FLOW RATE = ',F10.4,' L/S.',
1 ' INITIAL DEPTH = ',F10.4,' M.',
2 ' INITIAL WAVE SPEED = ',F10.4,' M/S.',/I
      N1=N+1

```

```

WRITE(3,204)UT,DX,N1,TFAC
204  FORMAT(10X,'CALCULATION TIME STEP = ',F10.4,' S.').
1  'LENGTH INCREMENT = ',F10.4,' M.'. 'NUMBER OF MODES = ',I3.
2  ' TFAC = ',F5.2,/)
IF(NSOL1.EQ.0) GOTO 730
WRITE(3,220)
220  FORMAT(10X,'SOLID DESCRIPTION DATA.')./
WRITE(3,221)TL,TW,TT,SW,NSCL1,XSOL
221  FORMAT(10X,'LENGTH = ',F7.2,' MM.'. 'WIDTH = ',F7.2,
1  ' MM.'. 'THICKNESS = ',F7.2,' MM.'. 'SATURATED WT. = ',
2  F7.2,' GN.',//,
3  10X,'SOLID POSITION, SECTION NUMBER = ',I3,
4  ' DISTANCE FROM ENTRY = ',F7.3,' M.//)
WRITE(3,222)FSTAT,FMOV,TAU
222  FORMAT(10X,'STATIC FRICTION FACTOR = ',F6.3,
1  ' SLIDING FRICTION FACTOR = ',F6.3,
2  '/,10X,'SOLID SURFACE SHEAR COEFF. = ',F7.4,/)
WRITE(3,271)XFAC,XFAC2
271  FORMAT(10X,'BOLYANCY FACTOR XFAC = ',F5.2,/
1  ',10X,'DOWNTHRUST FACTOR XFAC2 = ',F5.2,/)
IF(SOLTIM.GT.0.0) WRITE(3,223)SCLTIM
223  FORMAT(10X,'SOLID POSITION IN INFLOW PROFILE = ',
1  F6.2,' SECONDS FROM FLOW INCEPTION.//)
TL=TL/1000.0
TW=TW/1000.0
TT=TT/1000.0
SW=SW/1000.0
730  CONTINUE
C  OUTPUT TEST SIMULATION RESULTS.
IF(NSOL.GT.0) GOTO 733
WRITE(3,205)(XM(I),I=1,N1,N2)
205  FORMAT(/18X,' POSITION FROM ',/,18X,' ENTRY M.',6X,11F7.3,/)
WRITE(3,206)TIME,(HP(I),I=1,N1,N2)
206  FORMAT(2X,'TIME = ',F6.2,' S.'. 'DEPTH',7X,'M=',11F7.4)
WRITE(3,207)(VP(I),I=1,N1,N2)
WRITE(3,307)(CP(I),I=1,N1,N2)
307  FORMAT(18X,' FLOW RATE L/S=',11F7.4)
WRITE(3,208)(CF(I),I=1,N1,N2)
207  FORMAT(18X,' VELOCITY M/S=',11F7.4)
208  FORMAT(18X,' WAVE SPD. M/S=',11F7.4,/)
C
GOTO 734
733  CONTINUE
N3=NSOL-2*N2
N4=NSOL-1.2
N5=NSOL+N2
N6=NSOL+2*N2
IF(N3.LE.0) N3=NSOL-2
IF(N4.LE.0) N4=NSOL-1
WRITE(3,305)VSOL
305  FORMAT(/54X,'SOLID POSITION',/54X,'SOLID VELOCITY',/,
1  54X,' = ',F6.3,' M/S.').
WRITE(3,205)XM(1),XM(N3),XM(N4),XSOL,XSOL,XM(N5),XM(N6),XM(N1)
WRITE(3,206)TIME,HP(1),HP(N3),HP(N4),HPUS,HPDS,HP(N5),HP(N6),
1  HP(N1)
WRITE(3,207)VP(1),VP(N3),VP(N4),VPUS,VPDS,VP(N5),VP(N6),VP(N1)
WRITE(3,307)CF(1),CP(N3),CP(N4),CPSOL,QPSOL,CP(N5),CP(N6),CP(N1)
WRITE(3,208)CP(1),CP(N3),CP(N4),CPUS,CPDS,CP(N5),CP(N6),CP(N1)
734  CONTINUE
C
C
C  UPDATE TIME AND CHECK CALCULATION LENGTH.
600  CONTINUE

```

```

501  CONTINUE
      CALL TIMINC(N,VP,CP,VN,CN)
      DT=DX/(TFAC*(CN+VN))
      DTO=DT
      TIME=TIME+DT

      IF(TIME.GT.TMAX) GOTO 500

C
C
C
C
C
C
-SET UP CALCULATIONS FOR THIS TIME STEP.
DTRAT=DT/DTO
VSOL=VPSOL
IF(DTRAT.LT.0.06) GOTO 500
CALL INFLOW(TIME,Q)
J1=1
CALL INTER(N)
J1=2
CALL LOSS(VR,VS,HR,HS,M,SR,SS,RP)
J1=3
CALL ENTRY(TIME)
J1=4
CALL MODAL(N)
IF(TIME.GE.SOLTIM.AND.NSOL.GT.0) CALL SOLID(TIME)
IF(TIME.GT.SOLTIM.AND.INSOL.GT.0) CALL INSERT(XN,TIME)
IF(TIME.GE.SOLTIM.AND.NSOL.GT.0) XPOS=XSOL
J1=5
IF(HN.GT.HC)CALL EXIT(TIME)
IF(DT.LT.DTO) GOTO 500
DT=DTO
J1=6
CALL ASSIGN(N)
IF(TIME.GE.SOLTIM.AND.NSOL.GT.0) CALL FORCE(TIME,XN,FSOL)
IF(NSOL.GT.0) GOTO 731
J1=7
787  CONTINUE
      WRITE(3,206)TIME,(HP(I),I=1,N1,N2)
      WRITE(3,207)(VP(I),I=1,N1,N2)
      WRITE(3,307)(CP(I),I=1,N1,N2)
      WRITE(3,208)(CF(I),I=1,N1,N2)
      GOTO 501
731  CONTINUE
      N3=NSOL-2*N2
      N4=NSOL-N2
      N5=NSOL+N2
      N6=NSOL+2*N2
      IF(N6.GE.N1) N5=NSOL+1
      IF(N6.GE.N1) N6=NSOL+2
      IF(NSOL.GE.N-1) NSOL=0
      IF(N3.LE.0) N4=NSOL-1
      IF(N3.LE.0) N3=NSOL-2
      IF(NSOL.EQ.0) WRITE(3,224)
224  FORMAT(///30X,'SOLID WITHIN 2 SECTIONS OF PIPE DISCHARGE.',/,
1 30X,'SOLID ASSUMED TO CLEAR PIPE,CALCULATION TERMINATED,SOLUTION'
2 ,/30X,'CONTINUES WITH SOLID FREE PIPE FLOW.',/)
      IF(NSOL.EQ.0)WRITE(3,205)XN(1),XN(N3),XN(N4),XPOS,XPOS,XN(N5),
1 XN(N5),XN(N1)
      IF(NSOL.EQ.0) GOTO 787
      WRITE(3,308) SOLVEL
308  FORMAT(/54X,'SOLID VELOCITY',/54X,' = ',F6.3,' M/S. ')
      IF(VSOL.GT.0.0) GOTO 577

```

```

577      GOTO 578
      CONTINUE
      WRITE(3,205)XN(1),XN(3),XN(4),XPOS,XPOS,XN(5),XN(6),XN(1)
578      CONTINUE
      WRITE(3,206)TIME,HP(1),HP(3),HP(4),HPUS,HPDS,HP(5),HP(6),
1      HP(1)
      WRITE(3,207)VP(1),VP(3),VP(4),VPUS,VPDS,VP(5),VP(6),VP(1)
      WRITE(3,307)QP(1),QP(3),QP(4),QPSOL,QPSOL,QP(5),QP(6),QP(1)
      WRITE(3,208)CP(1),CP(3),CP(4),CPUS,CPDS,CP(5),CP(6),CP(1)
      GOTO 501
500      CONTINUE
      END

C
C
C
C
C
C
      SUBROUTINE TIMINC(N,VP,CP,VN,CN)
      COMMON/CM8/INSOL,NSOL1,NSOL
      COMMON/CM9/SOLVEL,HDS,VDS,CDS,HPDS,VPDS,CPDS
      COMMON/CM10/XPOS,XSOL,VPSOL,VSOL,QPSOL,HUS,VUS,CUS,HPUS,VPUS,CPUS
C      THIS SUBROUTINE IDENTIFIES THE HIGHEST WAVE SPEED
C      AND THE HIGHEST AVERAGE FLOW VELOCITY IN
C      THE SIMULATED FLOW IN ORDER TO ENSURE THAT THE TIME STEP
C      CHOSEN IS THE SMALLEST, HENCE ENSURING STABILITY.
      DIMENSION VF(61), CP(61)
      CN=0.0
      DO 1 I=1,N+1
      IF(I.EQ.NSOL)GOTO 1
      IF(CP(I).GE.CN) CN=CP(I)
1      CONTINUE
      VN=0.0
      DO 2 I=1,N+1
      IF(I.EQ.NSOL) GOTO 2
      IF(VP(I).GE.VN) VN=VP(I)
2      CONTINUE
      IF(CPUS.GT.CN) CN=CPUS
      IF(CPDS.GT.CN) CN=CPDS
      IF(VPUS.GT.VN) VN=VPUS
      IF(VPDS.GT.VN) VN=VPDS
      RETURN
      END

C
C
C
C
C
C
C
      SUBROUTINE LOSS(VR,VS,HR,HS,N,SR,SS,CM)
      DIMENSION VF(61),VS(61),HR(61),PS(61),SR(61),SS(61)
      COMMON/CM5/HC,HM
C      THIS SUBROUTINE CALCULATES THE EQUIVALENT STEADY STATE
C      LOSS BASED ON THE MANNING COEFFICIENT.
C
      DO 1 I=2,N+1
      CALL SHAPE(TIME,HR(I),A,T,PER)
      SR(I)=((VF(I)*ABS(VR(I))*R**2))/(A/PER)**1.333
1      CONTINUE
      NZ=N
      NY=1

```



```

      IF(HN.LE.HC) NY=2
      IF(HN.LE.HC) NZ=N+1
      DO 2 I=NY,NZ
      CALL SHAPE(TIME,HS(I),A,T,PER)
      SS(I)=((VS(I)*ABS(VS(I))*RM**2))/(A/PER)**1.333
2     CONTINUE
      RETURN
      END

C
C
C
C
C
C
      SUBROUTINE DEPTH(TIME)
C     THIS SUBROUTINE USES A SECTION OF ENTRY TO CALCULATE NORMAL
C     AND CRITICAL FLOW DEPTHS.
      DIMENSION QIN(30),TIN(30)
      COMMON/CM3/NPTS,QIN,TIN
      COMMON/CM5/PC,MN
      CALL ENTRY(TIME)
      RETURN
      END

C
C
C
C
C
C
      SUBROUTINE INFLOW(TIME,QAV)
C     THIS SUBROUTINE CALCULATES INFLOW RATES AT PIPE ENTRY BASED
C     ON THE ENTRY FLOW PROFILE DATA. NOTE THAT THE Q CALCULATED
C     IS AN AVERAGE VALUE FOR THIS TIME STEP.
      DIMENSION Q(30),T(30),QX(30)
      COMMON/CM1/ETO,DT,DX,D,SO,PL,SEC,XK,KM
      COMMON/CM3/NPTS,Q,T
      T1=TIME
      TO=TIME-DT
      J=1
      TX=T1
      DO 3 I=1,NPTS-1
      IF(TX.GE.T(I).AND.TX.LE.T(I+1)) GO TO 4
      CONTINUE
3     QX(J)=Q(I)+(Q(I+1)-Q(I))*(TX-T(I))/(T(I+1)-T(I))
4     QAV=QX(J)
      RETURN
      END

C
C
C
C
C
C
      SUBROUTINE SHAPE(TIME,H,A,T,PER)
C
C
      DIMENSION QIN(30),TIN(30)
      COMMON/CM1/ETO,DT,DX,D,SO,PL,SEC,XK,KM
      COMMON/CM3/NPTS,QIN,TIN
      COMMON/CM7/DL
C     THIS SUBROUTINE CALCULATES FLOW AREA,SURFACE WIDTH AND
C     WETTED PERIMETER BASED ON FLOW DEPTH

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C      THIS SUBROUTINE ALSO CALCULATES WATER SURFACE PROFILE
C      AND SETS UP BASE CONDITIONS ALONG THE PIPE AT TIME ZERO.
      R=D/2.0
      PI=3.142
      IF(H.LT.R)THETA=2.0*ATAN(SQRT(H*(D-H))/(R-H))
      IF(H.EQ.R)THETA=PI
      IF(H.GT.R)THETA=PI+2.0*ATAN((H-R)/(SQRT(H*(D-H))))
      A=((D**2)/8.0)*(THETA-SIN(THETA))
      PER=D*THETA/2.0
      T=2.0*((H*(D-H))**.5)
      IF(TIME.GT.0.0) GOTO 1
      Q=QIN(1)
      G=9.81
      COM=RM**2/SO
      HCRIT=1.0-(0**2)*T/(G*A**3)
      HMORM=1.0-(0**2)*COM/((A**3.333)/(PER**1.333))
      DL=HCRIT/(HMORM**SO)
1      CONTINUE
      RETURN
      END

C
C
C
C
C
C      SUBROUTINE WAVSPD(H,C)
C
C      THIS SUBROUTINE CALCULATES WAVE SPEED BASED ON DEPTH AND CROSS
C      SECTION SHAPE.
      CALL SHAPE(TIME,H,AREA,T,PER)
      C=SQRT(9.81*AREA/T)
      RETURN
      END

C
C
C
C
C      SUBROUTINE PROFIL(Q,HN,HC,XM)
C      THIS SUBROUTINE CALCULATES THE INITIAL WATER SURFACE
C      PROFILE BASED ON CRITICAL DEPTH AT PIPE EXIT.
      DIMENSION HP(61),VP(61),QP(61),CP(61)
      DIMENSION X(30),DEP(30),XM(61)
      DIMENSION X1(30),DEP1(30)
      COMMON/CH1/DTG,DT,DX,D,SO,PL,SEC,XK,RH
      COMMON/CH2/N,TMAX
      COMMON/CH3/OP,VP,HP,CP
      COMMON/CH7/EL
      COMMON/CH6/INSOL,NSOL1,NSOL
      COMMON/CH9/SOLVEL,HOS,VDS,CDS,MPDS,VPDS,LPDS
      COMMON/CH10/XPDS,XSOL,VPSL,VVOL,QPSJL,HUS,VUS,CUS,HPUS,VPUS,CPUS

C      IF(HN.LE.HC) GOTO 900
      DH=(HN-HC)/30.0
      IS=1
      H1=HC
      CALL SHAPE(TIME,H1,A,T,PER)
      X(1)=PL
      DEP(1)=HC
      SL=0.0
C      WATER SURFACE PROFILE CALCULATIONS.
      DO 80 I=1,200,2
      IS=IS+1

```

```

M2=HC+DH*FLOAT(I+1)
M3=HC+DH*FLOAT(I)
CALL SHAPE(TIME,M1,A,T,PER)
DL1=DL
CALL SHAPE(TIME,M2,A,T,PER)
DL2=DL
CALL SHAPE(TIME,M3,A,T,PER)
DL3=DL
DXP=DH*(DL1+DL2+4.0*DL3)/3.0
SL=SL-DXP
M1=M2
IF(SL.GE.PL) GOTO 81
X(IS)=PL-SL
IF(M1.GE.MN) GOTO 83
DEP(IS)=M1
80 CONTINUE
81 X(IS)=0.0
NIS=IS
IF(M1.GE.MN) GOTO 83
DEP(IS)=M1
GOTO 84
83 DEP(IS)=MN
GOTO 84
84 IF(X(IS).GT.C.C) GOTO 85
GOTO 86
85 X(IS)=0.0
DEP(IS)=MN
NIS=IS
86 CONTINUE
C
C
C INTERPOLATION REQUIRED TO DETERMINE DEPTH AT EACH NODE.
900 CONTINUE
DX=PL/FLOAT(N)
XN(1)=0.0
DO 87 I=2,N+1
XN(I)=XN(I-1)+DX
87 CONTINUE
IF(MN.LE.HC) GOTO 901
N2=NIS+1
DO 94 J=1,NIS
N2=N2-1
X1(J)=X(N2)
DEP1(J)=DEP(N2)
WRITE(3,93)X1(J),DEP1(J)
93 FORMAT(10X,2F10.5)
94 CONTINUE
DO 95 J=1,NIS
X(J)=X1(J)
DEP(J)=DEP1(J)
95 CONTINUE
HP(1)=DEP(1)
HP(N+1)=HC
DO 88 I=2,N
DO 89 K=1,NIS-1
IF(XN(I).GT.X(K).AND.XN(I).LE.X(K+1)) GOTO 90
89 CONTINUE
90 HP(I)=DEP(K)+(DEP(K+1)-DEP(K))*(XN(I)-X(K))/(X(K+1)-X(K))
88 CONTINUE
C SET UP BASE CONDITIONS AT TIME ZERO.
901 CONTINUE

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8      V(I)=VCU
      H(I)=HCU
      C(I)=CCU
      V(I-1)=VA
      H(I-1)=HA
      C(I-1)=CA
9      CONTINUE
      IF(VSOL.LE.0.0.AND.I.EQ.NSOL) V(I)=VUS
      IF(VSOL.LE.0.0.AND.I.EQ.NSOL) C(I)=CUS
      IF(VSOL.LE.0.0.AND.I.EQ.NSOL) H(I)=HJS
      IF(VSOL.LE.0.0.AND.I.EQ.NSOL+1) V(I-1)=VDS
      IF(VSOL.LE.0.0.AND.I.EQ.NSOL+1) C(I-1)=CDS
      IF(VSOL.LE.0.0.AND.I.EQ.NSOL+1) H(I-1)=HDS
      VR(I)=(V(I)+THETA*(C(I)*V(I-1)-V(I)*C(I-1)))
1      /(1.0+THETA*(V(I)-V(I-1)+C(I)-C(I-1)))
      CR(I)=(C(I)*(1.0-VR(I)*THETA)+C(I-1)*VR(I)*THETA)
1      /(1.0+C(I)*THETA-C(I-1)*THETA)
      HR(I)=H(I)-(H(I)-H(I-1))*THETA*(VR(I)+CR(I))
1      CONTINUE
      IF(HN.LE.HC) GOTO 4
      DO 2 I=1,N
      IF(I.EQ.NSOL.AND.VSOL.GT.0.0) GOTO 10
      GOTO 11
10     V(I)=VCD
      H(I)=HCD
      C(I)=CCD
      V(I+1)=VB
      H(I+1)=HB
      C(I+1)=CB
11     CONTINUE
      IF(VSOL.LE.0.0.AND.I.EQ.NSOL) V(I)=VDS
      IF(VSOL.LE.0.0.AND.I.EQ.NSOL) C(I)=CJS
      IF(VSOL.LE.0.0.AND.I.EQ.NSOL) H(I)=HJS
      IF(VSOL.LE.0.0.AND.I.EQ.NSOL-1) V(I+1)=VUS
      IF(VSOL.LE.0.0.AND.I.EQ.NSOL-1) C(I+1)=CUS
      IF(VSOL.LE.0.0.AND.I.EQ.NSOL-1) H(I+1)=HUS
      VS(I)=(V(I)-THETA*(V(I)*C(I+1)-C(I)*V(I+1)))
1      /(1.0-THETA*(V(I)-V(I+1)-C(I)+C(I+1)))
      CS(I)=(C(I)+VS(I)*THETA*(C(I)-C(I+1)))
1      /(1.0+THETA*(C(I)-C(I+1)))
      HS(I)=H(I)+THETA*(VS(I)-CS(I))*(H(I)-H(I+1))
2      CONTINUE
      GOTO 3
4      DO 5 I=2,N+1
      IF(VSOL.GT.0.0.AND.I.EQ.NSOL+1) GOTO 5
      IF(NSOL.GT.0.0.AND.I.EQ.NSOL+1) GOTO 20
      GOTO 80
20     V(I-1)=VDS
      H(I-1)=HDS
      C(I-1)=CDS
80     CONTINUE
      VS(I)=(V(I)*(1.0+THETA*C(I-1))-V(I-1)*THETA*C(I))/
1      (1.0+THETA*(V(I)-V(I-1)+C(I-1)-C(I)))
      CS(I)=(C(I)+VS(I)*(C(I)-C(I-1)))/(1.0+THETA*(C(I-1)-C(I)))
      HS(I)=H(I)-(H(I)-H(I-1))*THETA*(VS(I)-CS(I))
5      CONTINUE
3      CONTINUE
      IF(NSOL.EQ.0) GOTO 13
      IF(HN.GE.HC) GOTO 18
      DO 17 I=1,NSOL-1
      IF(V(I).GT.C(I)) GOTO 17
      VS(I)=(V(I)-THETA*(V(I)*C(I+1)-C(I)*V(I+1)))
1      /(1.0-THETA*(V(I)-V(I+1)-C(I)+C(I+1)))

```



```

      HM=HNM
      GOTO 9
14    HM=HNM
11    CONTINUE
      IF (TIME.EQ.0.0) GOTO 500
C
C
C
600   CALCULATION OF BOUNDARY DEPTH.
      CONTINUE
      IF (HM.LE.HC) GOTO 700
      UP=D
      DN=0.0
      HB=(UP+DN)/2.0
15    CONTINUE
      CALL SHAPE (TIME,HB,AREA,T,PER)
      X3=G/CS(1)
      X4=VS(1)-G*(SS(1)-S0)*DT-X3*HS(1)
      HFLOW=Q-(X4+X3*HB)*AREA
      IF (HFLOW)16,17,18
16    UP=HB
      GOTO 19
18    DN=HB
19    HBB=(UP+DN)/2.0
      IF (ABS((HBB-HB)/HB).LE.0.001) GOTO 20
      HB=HBB
      GOTO 15
20    HB=HBB
17    CONTINUE
      HP(1)=HB
      VP(1)=X4+X3*HP(1)
      CALL SHAPE (TIME,HB,AREA,T,PER)
      QP(1)=AREA*VP(1)*1000.0
      CP(1)=SORT(C*AREA/T)
500   CONTINUE
      GOTO 800
700   CONTINUE
C     CALCULATION OF NORMAL DEPTH.
      UP=D
      DN=0.0
      HB=(UP+DN)/2.0
79    CONTINUE
      CALL SHAPE (TIME,HB,AREA,T,PER)
      HNORM=1.0-(C**2)*CJN/((AREA**3.333)/(PER**1.333))
      IF (HNORM)80, 1,82
80    DN=HB
      GOTO 83
82    UP=HB
83    HBB=(UP+DN)/2.0
      IF (ABS((HBB-HB)/HB).LE.0.001) GOTO 84
      HB=HBB
      GOTO 79
84    HB=HBB
81    CONTINUE
      HP(1)=HB
      CALL SHAPE (TIME,HB,AREA,T,PER)
      VP(1)=Q/AREA
      GF(1)=Q*1000.0
      CP(1)=SORT(C*AREA/T)
800   CONTINUE
      RETURN
      END
C

```

וְהָיָה כִּי יִשְׁמַע ה' בְּקוֹל מִלְּךָ וְיִשְׁמַע ה' בְּקוֹל מִלְּךָ

CCCC

הנהגות

CCCCC

C

```

X1=G/CR(N+1)
X2=X1*HR(N+1)+VR(N+1)-G*(SR(N+1)-SO)*DT
UP=D
DN=0.0
HB=(UP+DN)/2.0
CALL SHAPE(TIME,HB,A,T,PER)
HEXIT=1.0-(ABS(X2-X1*HB)*(X2-X1*HB))*T/(G*A)
IF(HEXIT)1,2,3
DN=HB
GOTO 4
UP=HB
GOTO 4
HBB=(UP+DN)/2.0
IF(ABS((HBB-HB)/HB).LT.0.00001) GOTO 2
HB=HBB
GOTO 5
CONTINUE
VP(N+1)=X2-X1*HB
HP(N+1)=HB
CALL SHAPE(TIME,HB,A,T,PER)
CALL WAYSPEED(HB,CP(N+1))
QP(N+1)=1000.0*A*VP(N+1)
RETURN
END

```

SUBROUTINE SOLID(TIME)

```

DIMENSION CP(61),JIN(30),TIM(30),VP(61),HP(61),CP(61)
DIMENSION V(61),H(61)
DIMENSION VF(61),HP(61),CP(61),VS(61),HS(61),CS(61),SS(61)
DIMENSION FS(2),SR(61),XR(61),XS(61),XN(61),C(61)
COMMON/CM1/DT,DT,DY,D,SO,FL,SEC,XR,XH
COMMON/CM2/N,TMAX
COMMON/CM3/NPTS,QIN,TIN
COMMON/CM4/V,H,C,VR,HR,CR,XK,SH,VS,HS,CS,XS,SS,XN
COMMON/CM5/HC,HN
COMMON/CM6/CF,VP,HP,CP
COMMON/CM7/INSOL,NSOL1,NSOL
COMMON/CM9/SCLVEL,HDS,VDS,CDS,HPLS,VPDS,CPDS
COMMON/CM10/XPOS,XSOL,VPOL,VSL,DPSOL,HUS,VUS,CUS,HPUS,VPUS,CPUS
COMMON/CM11/TL,TH,TF,SH
THIS SUBROUTINE CALCULATES THE FLOW DEPTH, LEAKAGE RATE AND
WAVE SPEED AT THE DOWNSTREAM BOUNDARY FORMED BY AN INITIALLY
STATIONARY SOLID.
G=9.81
CON=RM**2/SG
QPSOL=QPSOL/1000.0
IZ=0
SEV=SE0
J=1
HO=HUS
60 CONTINUE
J=1
8000 CALL SHAPE(TIME,HO,A1,T,PER)
X1=G/CR(NSOL)
X2=X1*HR(NSOL)+VP(NSOL)-G*(SR(NSOL)-SO)*DT
SE=HUS*(VUS**2)/(2.0*G)
IF(SE.LT.SE0) GOTO 6

```

```

05  CONTINUE
    U=(X2-VPSOL)*A1/XK
    B=X1*A1/XK
    W=(X1**2)/(2.0*G)
    Y=(X2**2)/(2.0*G)-SEO-VPSOL*X2/G+(VPSOL**2)/(2.0*G)
    Z=X1*VPSOL/G+1.0-X2*X1/G
    Z4=W**2
    Z3=2.0*W*Z
    Z2=Z**2+2.0*W*Y
    Z1=2.0*Y*Z+B
    ZC=Y*ABS(Y)-U
    F=Z4*H0**4+Z3*H0**3+Z2*H0**2+Z1*H0+Z0
    FS(J)=F
    IF(J.EQ.2) GOTO 7000
    J=2
    H0=H0+0.0001*H0
    GOTO 8000
7000 DF=(FS(2)-FS(1))/(40/10000.0)
    DH=FS(1)/DF
    H1=H0-DH
    IF(ABS((H1-H0)/H0).LE.0.005) GOTO 70
    IF(H1.GT.0) H1=1.1*H0
    H0=H1
    IZ=IZ+1
    GOTO 60
70  CALL SHAPE(TIME,H1,A2,T,PEF)
    IF(ABS((A2-A1)/A1).LE.0.005) GOTO 80
    A1=(A1+A2)/2.0
    H0=H1
    GOTO 65
80  CONTINUE
    HPUS=H1
    VPUS=X2-X1*H1
    QPSOL=VPUS**2
    IF(VPUS.LT.VPSOL) GOTO 37
    GOTO 5
37  CONTINUE
    VPUS=VPSOL
    HPUS=(X2-VPUS)/X1
    CALL SHAPE(TIME,HPUS,A2,T,PER)
    QPSOL=VPUS**2
    GOTO 5
6   VPUS=VPSOL
    HPUS=(X2-VPUS)/X1
    CALL SHAPE(TIME,HPUS,A2,T,PER)
    QPSOL=VPUS**2
    GOTO 5
5   CALL WAVSPD(HPUS,CPUS)
    SEO=SEV
    DT=DT0
    GOTO 806
806 CONTINUE
    IF(HN.LE.HC) GOTO 8061
    GOTO 8062
8061 CONTINUE
    Q=QPSOL
    IF(0.LE.0.0) Q=0.05/(10.0*10.0**4)
    C  CALCULATION OF NORMAL DEPTH.
    UP=0
    DN=0.0
    HB=(UP+DN)/2.0
79  CONTINUE
    CALL SHAPE(TIME,HB,AREA,T,PEK)

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      MNORM=1.0-(C**2)*CON/((AREA**3.333)/(PER**1.333))
      IF(MNORM)90,91,92
90      ORF8893
92      UP=HB
93      HBB=(UP+DN)/2.0
      IF(ABS((HBB-HB)/HB).LE.0.001) GOTO 94
      HB=HBB
      GOTO 79
94      HB=HBB
91      CONTINUE
      MPDS=HB
      CALL SHAPE(TIME,HB,AREA,T,PER)
      VPDS=Q/AREA
      QPDS=Q*1000.0
      QPSOL=QPDS
      CPDS=SQRT(G*AREA/T)
      GOTO 934
8062      X3=G/CS(NSOL)
      X4=VS(NSOL)-G*(SS(NSOL)-SO)*DT-X3*HS(NSOL)
      IF(QPSOL.EC.C.C) GOTO 932
      UP=0
      DN=0.0
      HB=(UP+DN)/2.0
15      CONTINUE
      CALL SHAPE(TIME,HB,AREA,T,PER)
      HFLOW=QPSOL-(X4+X3*HB)*AREA
      IF(HFLOW)16,17,18
16      UP=HB
      GOTO 19
18      DN=HB
19      HBB=(UP+DN)/2.0
      IF(ABS((HBB-HB)/HB).LE.0.001) GOTO 20
      HB=HBB
      GOTO 15
20      HB=HBB
17      CONTINUE
      MPDS=HB
      VPDS=X4+X3*HPLS
      CALL SHAPE(TIME,HB,AREA,T,PER)
      QPSOL=AREA*VPDS*1000.0
      CPDS=SQRT(G*AREA/T)
      GOTO 933
932      CONTINUE
      MPDS=-X4/X3
      VPDS=0.0
      CALL WAVSPD(MPDS,CPDS)
933      CONTINUE
      IF(VPSOL.GT.C.C) GOTO 934
      GOTO 935
934      CONTINUE
      DXX=DX/(XSOL-XN(NSOL-1))
      VP(NSOL)=VP(NSOL-1)+DXX*(VPUS-VP(NSOL-1))
      HP(NSOL)=HP(NSOL-1)+DXX*(HPUS-HP(NSOL-1))
      CP(NSOL)=CP(NSOL-1)+DXX*(CPUS-CP(NSOL-1))
      DXX=(XN(NSOL+1)-XSOL)/(XN(NSOL+2)-XSOL)
      VP(NSOL+1)=VPDS+DXX*(VP(NSOL+2)-VPDS)
      HP(NSOL+1)=MPDS+DXX*(HP(NSOL+2)-MPDS)
      CP(NSOL+1)=CPDS+DXX*(CP(NSOL+2)-CPDS)
935      CONTINUE
      RETURN
      END
C
C

```

```

SUBROUTINE INSERT(XN,TIME)
DIMENSION XN(61),QP(61),VP(61),HP(61),CP(61)
COMMON/CM6/QP,VP,HP,CP
COMMON/CM6/INSOL,NSOL1,NSOL
COMMON/CM9/SOLVEL,HDS,VDS,CDS,HPDS,VPDS,CPDS
COMMON/CM10/XPOS,XSOL,VP SOL,VSOL,QPSOL,HUS,VUS,CUS,HPUS,VPUS,CPUS

```

C

```

INSOL=0
NSOL=NSOL1
VPUS=VP(NSOL)
HPUS=HP(NSOL)
CPUS=CP(NSOL)
VPDS=VP(NSOL)
HPDS=HP(NSOL)
CPDS=CP(NSOL)
QPSOL=QP(NSOL)
VSOL=VPUS
VP SOL=VSOL
DX=XN(NSOL)-XN(NSOL-1)
DXX=DX/(XSOL-XN(NSOL-1))
VP(NSOL)=VP(NSOL-1)+DXX*(VPUS-VP(NSOL-1))
HP(NSOL)=HP(NSOL-1)+DXX*(HPUS-HP(NSOL-1))
CP(NSOL)=CP(NSOL-1)+DXX*(CPUS-CP(NSOL-1))
DXX=(XN(NSOL+1)-XSOL)/(XN(NSOL+2)-XSOL)
VP(NSOL+1)=VPDS+DXX*(VP(NSOL+2)-VPDS)
HP(NSOL+1)=HPDS+DXX*(HP(NSOL+2)-HPDS)
CP(NSOL+1)=CPDS+DXX*(CP(NSOL+2)-CPDS)
RETURN
END

```

C

C

```

SUBROUTINE FORCE(TIME,XN,FSOL)

```

C

C

C

C

C

THIS SUBROUTINE CALCULATES THE FORCE ACTING ON THE SOLID
AND DETERMINES ITS VELOCITY AND POSITION AT THE END OF THE
NEXT TIME STEP.

```

DIMENSION XN(61)
COMMON/CM1/DTG,DT,DX,D,SO,PL,SEC,XK,RM
COMMON/CM2/N,THAX
COMMON/CM8/INSOL,NSOL1,NSOL
COMMON/CM9/SOLVEL,HDS,VDS,CDS,HPDS,VPDS,CPDS
COMMON/CM10/XPOS,XSOL,VP SOL,VSOL,QPSOL,HUS,VUS,CUS,HPUS,VPUS,CPUS
COMMON/CM11/TL,TW,TT,SH
COMMON/CM12/XFAC2,XFAC,TAU,FMOV,FSTAT

```

C

```

G=9.81
RHO=1000.0
FRICT=FSTAT
FM1=RHO*G*(HUS-TT/2.0)*TW*TT*TT/2.0
FM2=RHO*G*(TT/2.0)*T*TT*0.5*(HDS-TT+HDS)
FM3=SH*G*TL*0.5*COS(ASIN((HUS-TT)/TL))
TX=(HDS-TT)/SIN(ASIN((HUS-TT)/TL))
FM4=XFAC2*FHC*G*0.5*(HDS-TT)*TW*0.5*TX**2
IF(HDS.LE.TT) FM4=0.0
FP=(0.5/TL)*(FM2+FM3+FM4-FM1)
FP2=(FP+FM4/10.5*TX)/COS(ASIN((HUS-TT)/TL))
IF(VSOL.GT.0.0) FRICT=FMOV
HSH=TT+0.5*(HPUS-TT)
CALL SHAPE(TIME,HSH,ASH,TSH,PER)
FLOAR=ASH-TT*TH

```

```

CALL SHAPE(TIME,HPUS,ARUS,TUS,PER)
QSH=ARUS*(VPUS-VSOL)
SHERV=QSH/ASH
SHERF=TAU*0.5*RHO*2.0*TL*TT*SHERV**2
IF(HPUS.LT.TT) FP2=0.0
FP2=XFAC*FP2
FSUR=FRIC*(SH*G*COS(ASIN(SQ))-FP2)
IF(FSUR.LT.0.0) FSUR=0.0
FSOL=RHO*G*TW*0.5*(HPUS**2-HPDS**2)+SH*G*SQ-FSUR
VPSOL=VSOL+DT*FSOL/SH
WRITE(3,53)FSOL,FP2,FSUR
53  FORMAT(10X,'FSOL=',F10.4,' FP2=',F10.4,' FSUR=',F10.4,/)
IF(VPSOL.LE.0.0) VPSOL=0.0
XSOL=0.5*DT*(VPSOL+VSOL)*XSOL
IF(VPSOL.GT.0.0.AND.VSOL.LE.0.0) GOTO 5
DO 4 I=1,N
IF(XN(I).LE.XSOL.AND.XN(I+1).GT.XSOL) NSOL=I
4  CONTINUE
5  CONTINUE
RETURN
END

C
C
C
C
C
C
SUBROUTINE ASSIGN(N)
C  THIS SUBROUTINE SETS UP THE NEW BASE CONDITIONS ALONG THE
C  PIPE IN PREPARATION FOR THE NEXT TIME STEP.
DIMENSION OP(61),OIN(30),TIN(30),VP(61),HP(61),CP(61)
DIMENSION V(61),H(61)
DIMENSION VR(61),HR(61),CR(61),VS(61),HS(61),CS(61),SS(61)
DIMENSION SR(61),XR(61),XS(61),XM(61),C(61)
COMMON/CM3/NPTS,GIN,TIN
COMMON/CM4/V,H,C,VR,HR,CR,XR,SR,VS,HS,CS,XS,SS,XH
COMMON/CM6/CP,VP,HP,CP
COMMON/CM8/INSOL,NSOL1,NSOL
COMMON/CM9/SELVEL,HDS,VDS,CDS,HPUS,VPUS,CPUS
COMMON/CM10/XPCS,XSOL,VPSOL,VSOL,OPSOL,HUS,VUS,CUS,HPUS,VPUS,CPUS
DO 1 I=1,N+1
IF(VSOL.EQ.0.0.AND.I.EQ.NSOL) GOTO 2
V(I)=VP(I)
H(I)=HP(I)
C(I)=CP(I)
IF(INSOL.GT.0.AND.I.EQ.NSOL1) GOTO 6
7  CONTINUE
IF(VSOL.EQ.0.0.AND.NSOL1.GT.0) GOTO 2
GOTO 1
2  HUS=HPUS
VUS=VPUS
CUS=CPUS
HDS=HPDS
VDS=VPDS
CDS=CPDS
HP(NSOL)=HPUS
VP(NSOL)=VPUS
CP(NSOL)=CPUS
H(NSOL)=HPUS
V(NSOL)=VPUS
C(NSOL)=CPUS
GOTO 1
6  HPUS=HP(I)

```

```

      VPUS=VP(1)
      VPDS=VP(1)
      CPUS=CP(1)
      CPDS=CP(1)
      GOTO 7
1     CONTINUE
      SOLVEL=VSOL
      VSOL=VPSOL
      IF (VPSOL.GE.0.0) GOTO 3
      GOTO 4
3     VSOL=VPSOL
      HUS=HPUS
      VUS=VPUS
      CUS=CPUS
      HDS=HPDS
      VDS=VPDS
      CDS=CPDS
4     CONTINUE
      RETURN
      END
$BEND

```



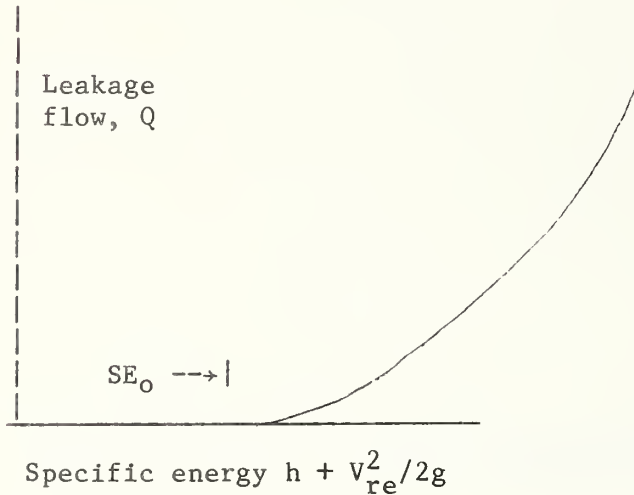
Appendix 2

**Derivation of solid boundary equations
used in Subroutine SOLID**

Derivation of solid boundary equations employed in Subroutine SOLID.

Available equations at moving solid boundary.

1) Leakage flow past solid.



$$Q = XK \{SE - SE_0\}^2$$

where SE is the specific energy relative to moving solid.

XK , SE_0 determined by measurement.

2) Flow over solid in terms of flow area



v_B = solid velocity

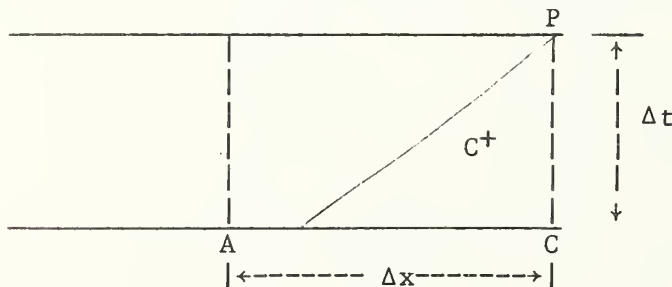
Relative velocity $v_{re} = v_a - v_B$

Flow area $A = f(h)$

Total flow $= v_a A = v_a f(h)$

Flow past solid $= v_{re} A = v_{re} f(h)$.

3) Characteristic equation, C^+ in both sub and supercritical flow conditions.



C^+ links R at t to P at t + Δt

C^+ equation $V_p = X2 - X1h_p$

$$X1 = g/cR$$

$$X2 = V_R + gh_R/c_R - g(S_R - S_O)\Delta t$$

Note characteristics equations in terms of absolute velocity.

The flow Q over the solid is given by the empirical relation,

$$Q = XK \left(h + \frac{V_{re}^2}{2g} - SE_O \right)^2$$

where V_{re} is the flow velocity relative to the moving solid.

$$Q = V_{re}A = (V_{abs} - V_B)A = (X2 - X1h - V_B)A$$

$$\begin{aligned} \text{Also, } Q &= XK \{ SE - SE_O \}^2 \\ &= XK \left\{ h + \frac{V_{abs}^2}{2g} - V_B^2 - SE_O \right\}^2 \end{aligned}$$

Hence

$$(X2 - X1h - V_B)A = XK \left\{ h + \frac{(X2 - X1h - V_B)^2}{2g} - SE_O \right\}^2$$

Collecting terms

$$U = (X2 - V_B)A/XK; \quad B = XI \ A/XK;$$

$$W = (X1^2)/2g; \quad Y = X2^2/2g - SE_O - V_B X2/g + V_B^2/2g;$$

$$Z = XI \cdot V_B/g + 1.0 \ 0 \ X2X1/g$$

$$\begin{aligned} U - Bh &= \{ Zh + Y + Wh^2 \}^2 \\ &= Z^2 h^2 + Y^2 + W^2 h^4 + 2YWh^2 + 2ZYh + 2ZWh^3 \end{aligned}$$

$$W^2 h^4 + 2ZWh^3 + (Z^2 + 2YW)h^2 + (2ZY + B)h + (Y \cdot 1Y1 - U) = 0$$

Note: $Y \cdot ABS \ |Y|$ retains sign Y.

This quartic is solved by the Newton Raphson method as B and U involve f(h) through the flow area term.

APPENDIX 3

Typical Output Program TRANSCD

TEST PIPE CONFIGURATION:-
 DIAMETER = 0.1000 M.
 PIPE SLOPE = 0.0100
 HAMMING COEFFICIENT = 0.0150
 PIPE LENGTH = 15.0000 M.

FLOW SUPERCRITICAL, NORMAL DEPTH = 0.0144 M. AND CRITICAL DEPTH = 0.3138 M.

INITIAL FLOW RATE = 0.2000 L/S. INITIAL DEPTH = 0.0144 M. INITIAL WAVE SPEED = 0.3110 M/S.

CALCULATION TIME STEP = 0.0001 S. LENGTH INCREMENT = 0.3000 M. NUMBER OF NUDES = 51 IFAC = 1.00

SOLID DESCRIPTION DATA-

LENGTH = 270.00 MM. WIDTH = 20.00 MM. THICKNESS = 20.00 MM. SATURATED WT. = 250.00 GM.

SOLID POSITION, SECTION NUMBER = 10 DISTANCE FROM ENTRY = 2.700 M.

STATIC FRICTION FACTOR = 0.150 SLIDING FRICTION FACTOR = 0.100

SOLID SURFACE SHEAR COEFF. = 0.

BOUANCY FACTOR XFAC = 1.00

DOWNTHRUST FACTOR XFAC2 = 0.

SOLID POSITION IN INFLOW PROFILE = 4.00 SECONDS FROM FLOW INCEPTION.

POSITION FROM ENTRY M.		0.	1.500	3.000	4.500	6.000	7.500	9.000	10.500	12.000	13.500	15.000
TIME = 0.	S. DEPTH	M = 0.0144	0.0144	0.0144	0.0144	0.0144	0.0144	0.0144	0.0144	0.0144	0.0144	0.0130
	VELOCITY M/S	M = 0.2875	0.2875	0.2875	0.2875	0.2875	0.2875	0.2875	0.2875	0.2875	0.2875	0.2875
	FLOW RATE L/S	M = 0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000
	WAVE SPD. M/S	M = 0.3110	0.3110	0.3110	0.3110	0.3110	0.3110	0.3110	0.3110	0.3110	0.3110	0.3052
TIME = 0.49 S.	S. DEPTH	M = 0.0341	0.0144	0.0144	0.0144	0.0144	0.0144	0.0144	0.0144	0.0144	0.0144	0.0130
	VELOCITY M/S	M = 0.9072	0.2875	0.2875	0.2875	0.2875	0.2875	0.2875	0.2875	0.2875	0.2875	0.2875
	FLOW RATE L/S	M = 2.1446	0.1999	0.1999	0.1999	0.1999	0.1999	0.1999	0.1999	0.1999	0.1999	0.1999
	WAVE SPD. M/S	M = 0.4947	0.3110	0.3110	0.3110	0.3110	0.3110	0.3110	0.3110	0.3110	0.3110	0.3051
TIME = 0.70 S.	S. DEPTH	M = 0.0395	0.0144	0.0144	0.0144	0.0144	0.0144	0.0144	0.0144	0.0144	0.0144	0.0130
	VELOCITY M/S	M = 1.0395	0.2875	0.2875	0.2875	0.2875	0.2875	0.2875	0.2875	0.2875	0.2875	0.2875
	FLOW RATE L/S	M = 3.0021	0.1999	0.1999	0.1999	0.1999	0.1999	0.1999	0.1999	0.1999	0.1999	0.1999
	WAVE SPD. M/S	M = 0.5384	0.3110	0.3110	0.3110	0.3110	0.3110	0.3110	0.3110	0.3110	0.3110	0.3046
TIME = 0.89 S.	S. DEPTH	M = 0.0451	0.0144	0.0144	0.0144	0.0144	0.0144	0.0144	0.0144	0.0144	0.0144	0.0137
	VELOCITY M/S	M = 1.1970	0.2875	0.2875	0.2875	0.2875	0.2875	0.2875	0.2875	0.2875	0.2875	0.2875
	FLOW RATE L/S	M = 3.7446	0.1999	0.1999	0.1999	0.1999	0.1999	0.1999	0.1999	0.1999	0.1999	0.1999
	WAVE SPD. M/S	M = 0.5421	0.3110	0.3110	0.3110	0.3110	0.3110	0.3110	0.3110	0.3110	0.3110	0.3042
TIME = 1.07 S.	S. DEPTH	M = 0.0499	0.0144	0.0144	0.0144	0.0144	0.0144	0.0144	0.0144	0.0144	0.0144	0.0137
	VELOCITY M/S	M = 1.3044	0.2875	0.2875	0.2875	0.2875	0.2875	0.2875	0.2875	0.2875	0.2875	0.2875
	FLOW RATE L/S	M = 4.1439	0.1999	0.1999	0.1999	0.1999	0.1999	0.1999	0.1999	0.1999	0.1999	0.1999
	WAVE SPD. M/S	M = 0.6047	0.3110	0.3110	0.3110	0.3110	0.3110	0.3110	0.3110	0.3110	0.3110	0.3040
TIME = 1.25 S.	S. DEPTH	M = 0.0491	0.0144	0.0144	0.0144	0.0144	0.0144	0.0144	0.0144	0.0144	0.0144	0.0137
	VELOCITY M/S	M = 1.0420	0.2875	0.2875	0.2875	0.2875	0.2875	0.2875	0.2875	0.2875	0.2875	0.2875
	FLOW RATE L/S	M = 3.9953	0.1999	0.1999	0.1999	0.1999	0.1999	0.1999	0.1999	0.1999	0.1999	0.1999
	WAVE SPD. M/S	M = 0.6134	0.3110	0.3110	0.3110	0.3110	0.3110	0.3110	0.3110	0.3110	0.3110	0.3038

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[illegible]

[illegible][illegible]

TIME	5-57 S.	POSITION FROM	ENTRY M.	DETH.	M	0.	0.3334	0.3112	0.3196	0.0417	3.4679	3.4699	4.800	6.300	15.000
		VELOCITY	M/S	-0.4291	-0.5035	-0.5417	-0.5741	-0.5741	-0.5741	-0.5741	-0.5741	-0.5741	-0.5741	-0.5741	-0.5741
		FLOW RATE	L/S	-0.9471	-1.0537	-1.5705	-1.5705	-1.5705	-1.5705	-1.5705	-1.5705	-1.5705	-1.5705	-1.5705	-1.5705
		WAVE SPO	M/S	-0.8491	-0.8707	-0.5147	-0.5147	-0.5147	-0.5147	-0.5147	-0.5147	-0.5147	-0.5147	-0.5147	-0.5147
		F50L		-0.0049	FP2		FSUR								

[illegible]

TIME	6.03	5.	4.	POSITION	μm	ERR
INITIAL					0.	0.
ADJ1					0.0000	2.100
ADJ2					0.0000	1.600
ADJ3					0.0000	1.000
ADJ4					0.0000	0.500
ADJ5					0.0000	0.250
ADJ6					0.0000	0.125
ADJ7					0.0000	0.062
ADJ8					0.0000	0.031
ADJ9					0.0000	0.016
ADJ10					0.0000	0.008
ADJ11					0.0000	0.004
ADJ12					0.0000	0.002
ADJ13					0.0000	0.001
ADJ14					0.0000	0.000
ADJ15					0.0000	0.000
ADJ16					0.0000	0.000
ADJ17					0.0000	0.000
ADJ18					0.0000	0.000
ADJ19					0.0000	0.000
ADJ20					0.0000	0.000
ADJ21					0.0000	0.000
ADJ22					0.0000	0.000
ADJ23					0.0000	0.000
ADJ24					0.0000	0.000
ADJ25					0.0000	0.000
ADJ26					0.0000	0.000
ADJ27					0.0000	0.000
ADJ28					0.0000	0.000
ADJ29					0.0000	0.000
ADJ30					0.0000	0.000
ADJ31					0.0000	0.000
ADJ32					0.0000	0.000
ADJ33					0.0000	0.000
ADJ34					0.0000	0.000
ADJ35					0.0000	0.000
ADJ36					0.0000	0.000
ADJ37					0.0000	0.000
ADJ38					0.0000	0.000
ADJ39					0.0000	0.000
ADJ40					0.0000	0.000
ADJ41					0.0000	0.000
ADJ42					0.0000	0.000
ADJ43					0.0000	0.000
ADJ44					0.0000	0.000
ADJ45					0.0000	0.000
ADJ46					0.0000	0.000
ADJ47					0.0000	0.000
ADJ48					0.0000	0.000
ADJ49					0.0000	0.000
ADJ50					0.0000	0.000
ADJ51					0.0000	0.000
ADJ52					0.0000	0.000
ADJ53					0.0000	0.000
ADJ54					0.0000	0.000
ADJ55					0.0000	0.000
ADJ56					0.0000	0.000
ADJ57					0.0000	0.000
ADJ58					0.0000	0.000
ADJ59					0.0000	0.000
ADJ60					0.0000	0.000
ADJ61					0.0000	0.000
ADJ62					0.0000	0.000
ADJ63					0.0000	0.000
ADJ64					0.0000	0.000
ADJ65					0.0000	0.000
ADJ66					0.0000	0.000
ADJ67		</				

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• 0.414 M/S.

TIME = 6.26 S. POSITION FROM
ENTRY M. U. 0.400 2.100 1.707 3.707 5.100 6.600 15.000
DEPTH M. 0.0711 0.0174 0.0174 0.0174 0.0174 0.0174 0.0174
VELOCITY M/S. 0.4073 0.4104 0.4097 0.4091 0.4092 0.4091 0.4091
FLOW RATE L/S. 0.4045 0.4116 0.4103 0.4099 0.4099 0.4099 0.4099
WAVE SPD. M/S. 0.4700 0.4851 0.4841 0.4834 0.4831 0.4831 0.4831
FSOL = -0.0018 FP2 = 0.1847

SOLID VELOCITY
• 0.411 M/S.

TIME = 6.50 S. POSITION FROM
ENTRY M. U. 0.900 2.400 3.004 3.904 5.400 6.900 15.000
DEPTH M. 0.0303 0.0337 0.0359 0.0477 0.0418 0.0355 0.0137
VELOCITY M/S. 0.3980 0.4274 0.5460 0.5440 0.6474 0.6717 0.2909
FLOW RATE L/S. 0.7997 0.9452 1.135 2.0120 2.0120 1.6754 0.2127
WAVE SPD. M/S. 0.4631 0.4913 0.5040 0.4024 0.5560 0.5057 0.3131
FSOL = -0.0205 FP2 = 0.1847

SOLID VELOCITY
• 0.410 M/S.

TIME = 6.73 S. POSITION FROM
ENTRY M. U. 0.900 2.400 3.900 3.900 5.400 6.900 15.000
DEPTH M. 0.0295 0.0331 0.0351 0.0467 0.0412 0.0364 0.0137
VELOCITY M/S. 0.3895 0.4204 0.5102 0.5125 0.6292 0.6639 0.3347
FLOW RATE L/S. 0.7947 0.9554 1.3051 1.4223 1.4223 1.7168 0.2749
WAVE SPD. M/S. 0.4415 0.4867 0.5029 0.5945 0.5517 0.5134 0.3304
FSOL = -0.0030 FP2 = 0.1847

SOLID VELOCITY
• 0.390 M/S.

TIME = 6.97 S. POSITION FROM
ENTRY M. U. 0.900 2.400 4.074 4.074 5.400 6.900 15.000
DEPTH M. 0.0287 0.0325 0.0345 0.0469 0.0408 0.0372 0.0201
VELOCITY M/S. 0.3747 0.4127 0.5168 0.5173 0.6186 0.6554 0.4945
FLOW RATE L/S. 0.7071 0.9153 1.2418 1.4660 1.4660 1.7452 0.5137
WAVE SPD. M/S. 0.4444 0.4324 0.4979 0.5959 0.5447 0.5198 0.3416
FSOL = -0.0013 FP2 = 0.1847

SOLID VELOCITY
• 0.387 M/S.

TIME = 7.21 S. POSITION FROM
ENTRY M. U. 1.100 2.700 4.106 4.106 5.700 7.200 15.000
DEPTH M. 0.0276 0.0329 0.0344 0.0471 0.0411 0.0364 0.0137
VELOCITY M/S. 0.3647 0.4106 0.4951 0.5156 0.6131 0.6512 0.4945
FLOW RATE L/S. 0.6774 0.9437 1.2756 1.4774 1.4774 1.6016 0.4725
WAVE SPD. M/S. 0.4416 0.4350 0.5026 0.5917 0.5530 0.5114 0.3416
FSOL = -0.0211 FP2 = 0.1847

SOLID VELOCITY
• 0.385 M/S.

POSITION FROM

TIME = 7.45 S. POSITION FROM
 ENTRY M. U. 1.500 2.700 4.250 4.250 5.700 7.200 15.000 15.000
 DEPTH M. 0.021 0.011 0.011 0.011 0.011 0.011 0.011 0.011
 VELOCITY M/S 0.317 0.317 0.317 0.317 0.317 0.317 0.317 0.317
 FLOW RATE L/S 0.317 0.317 0.317 0.317 0.317 0.317 0.317 0.317
 WAVE SPD. M/S 0.317 0.317 0.317 0.317 0.317 0.317 0.317 0.317
 FSOL = -0.0050 FP2 = 0.1847

SOLID VELOCITY
 = 0.360 M/S.

TIME = 7.69 S. POSITION FROM
 ENTRY M. U. 1.500 2.700 4.250 4.250 5.700 7.200 15.000 15.000
 DEPTH M. 0.021 0.011 0.011 0.011 0.011 0.011 0.011 0.011
 VELOCITY M/S 0.317 0.317 0.317 0.317 0.317 0.317 0.317 0.317
 FLOW RATE L/S 0.317 0.317 0.317 0.317 0.317 0.317 0.317 0.317
 WAVE SPD. M/S 0.317 0.317 0.317 0.317 0.317 0.317 0.317 0.317
 FSOL = -0.0003 FP2 = 0.1847

SOLID VELOCITY
 = 0.360 M/S.

TIME = 7.94 S. POSITION FROM
 ENTRY M. U. 1.500 3.000 4.437 4.437 6.000 7.500 15.000 15.000
 DEPTH M. 0.021 0.011 0.011 0.011 0.011 0.011 0.011 0.011
 VELOCITY M/S 0.317 0.317 0.317 0.317 0.317 0.317 0.317 0.317
 FLOW RATE L/S 0.317 0.317 0.317 0.317 0.317 0.317 0.317 0.317
 WAVE SPD. M/S 0.317 0.317 0.317 0.317 0.317 0.317 0.317 0.317
 FSOL = -0.0202 FP2 = 0.1846

SOLID VELOCITY
 = 0.360 M/S.

TIME = 8.18 S. POSITION FROM
 ENTRY M. U. 1.500 3.000 4.524 4.524 6.000 7.500 15.000 15.000
 DEPTH M. 0.021 0.011 0.011 0.011 0.011 0.011 0.011 0.011
 VELOCITY M/S 0.317 0.317 0.317 0.317 0.317 0.317 0.317 0.317
 FLOW RATE L/S 0.317 0.317 0.317 0.317 0.317 0.317 0.317 0.317
 WAVE SPD. M/S 0.317 0.317 0.317 0.317 0.317 0.317 0.317 0.317
 FSOL = -0.0044 FP2 = 0.1846

SOLID VELOCITY
 = 0.360 M/S.

TIME = 8.43 S. POSITION FROM
 ENTRY M. U. 1.500 3.000 4.610 4.610 6.000 7.500 15.000 15.000
 DEPTH M. 0.021 0.011 0.011 0.011 0.011 0.011 0.011 0.011
 VELOCITY M/S 0.317 0.317 0.317 0.317 0.317 0.317 0.317 0.317
 FLOW RATE L/S 0.317 0.317 0.317 0.317 0.317 0.317 0.317 0.317
 WAVE SPD. M/S 0.317 0.317 0.317 0.317 0.317 0.317 0.317 0.317
 FSOL = -0.0011 FP2 = 0.1846

SOLID VELOCITY
 = 0.360 M/S.

TIME = 8.68 S. POSITION FROM
 ENTRY M. U. 1.500 3.000 4.696 4.696 6.000 7.500 15.000 15.000
 DEPTH M. 0.021 0.011 0.011 0.011 0.011 0.011 0.011 0.011
 VELOCITY M/S 0.317 0.317 0.317 0.317 0.317 0.317 0.317 0.317
 FLOW RATE L/S 0.317 0.317 0.317 0.317 0.317 0.317 0.317 0.317
 WAVE SPD. M/S 0.317 0.317 0.317 0.317 0.317 0.317 0.317 0.317
 FSOL = -0.0011 FP2 = 0.1846

FLOW RATE L/S= 0.3647 0.2776 1.0003 1.5504 1.5504 1.6169 1.6435 2.1959
 WAVE SPD. M/S= 0.3893 0.4622 0.5126 0.5020 0.5110 0.5250 0.4711 0.3035
 FSOL= 0.0062 FPZ= 0.6064 FSUR= 0.1847

SOLID VELOCITY
 = 0.335 M/S.

POSITION FROM
 ENTRY M. U. L. 0.00 3.300 4.777 4.777 6.300 7.800 15.000
 TIME = 0.92 S. DEPTH M= 0.0208 0.1306 0.0371 0.0456 0.0391 0.0373 0.0301 0.0137
 VELOCITY M/S= 0.2658 0.1964 0.4099 0.4547 0.4576 0.4593 0.4110 0.3035
 FLOW RATE L/S= 0.3152 0.4054 1.0863 1.5860 1.5860 1.6025 1.6293 2.1959
 WAVE SPD. M/S= 0.3764 0.4652 0.5192 0.5064 0.5347 0.5207 0.4648 0.3035
 FSOL= -0.0197 FPZ= 0.6062 FSUR= 0.1846

SOLID VELOCITY
 = 0.341 M/S.

POSITION FROM
 ENTRY M. U. L. 0.00 3.300 4.861 4.861 6.300 7.800 15.000
 TIME = 0.17 S. DEPTH M= 0.0196 0.0299 0.0366 0.0443 0.0385 0.0374 0.0316 0.0137
 VELOCITY M/S= 0.2436 0.3387 0.4055 0.4521 0.4543 0.4587 0.4109 0.3035
 FLOW RATE L/S= 0.2742 0.2679 1.0558 1.5177 1.5177 1.5801 1.6209 0.1959
 WAVE SPD. M/S= 0.3463 0.4260 0.5184 0.5762 0.5335 0.5216 0.4721 0.3035
 FSOL= -0.0002 FPZ= 0.6064 FSUR= 0.1846

SOLID VELOCITY
 = 0.321 M/S.

POSITION FROM
 ENTRY M. U. L. 0.00 3.300 4.944 4.944 6.300 7.800 15.000
 TIME = 0.43 S. DEPTH M= 0.0182 0.0293 0.0361 0.0446 0.0381 0.0374 0.0324 0.0117
 VELOCITY M/S= 0.2189 0.3107 0.4010 0.4337 0.4362 0.4370 0.4076 0.1036
 FLOW RATE L/S= 0.2146 0.2798 1.0234 1.4671 1.4671 1.5521 1.5936 0.1959
 WAVE SPD. M/S= 0.3529 0.4545 0.5106 0.5779 0.5266 0.5217 0.4808 0.3035
 FSOL= 0.0004 FPZ= 0.6064 FSUR= 0.1846

SOLID VELOCITY
 = 0.321 M/S.

POSITION FROM
 ENTRY M. U. L. 0.00 3.300 5.025 5.025 6.300 7.800 15.000
 TIME = 0.68 S. DEPTH M= 0.0177 0.0295 0.0369 0.0447 0.0392 0.0370 0.0316 0.0137
 VELOCITY M/S= 0.2143 0.3107 0.4010 0.4337 0.4362 0.4370 0.4076 0.1036
 FLOW RATE L/S= 0.2003 0.2798 1.0234 1.4671 1.4671 1.5521 1.5936 0.1959
 WAVE SPD. M/S= 0.3464 0.4545 0.5106 0.5779 0.5266 0.5217 0.4808 0.3035
 FSOL= -0.0146 FPZ= 0.6064 FSUR= 0.1846

SOLID VELOCITY
 = 0.321 M/S.

POSITION FROM
 ENTRY M. U. L. 0.00 3.300 5.106 5.106 6.300 7.800 15.000
 TIME = 0.93 S. DEPTH M= 0.0174 0.0295 0.0369 0.0448 0.0392 0.0370 0.0316 0.0137
 VELOCITY M/S= 0.2143 0.3107 0.4010 0.4337 0.4362 0.4370 0.4076 0.1036
 FLOW RATE L/S= 0.2003 0.2798 1.0234 1.4671 1.4671 1.5521 1.5936 0.1959
 WAVE SPD. M/S= 0.3464 0.4545 0.5106 0.5779 0.5266 0.5217 0.4808 0.3035
 FSOL= -0.0146 FPZ= 0.6064 FSUR= 0.1846

SOLID VELOCITY
= 0.307 M/S.

POSITION FROM
ENTRY M.
DEPTH M.
TIME = 10.19 S.
VELOCITY M/S
FLOW RATE L/S
WAVE SPD. M/S
FSOL =
0.0004 FP2 =

0. 2.100 3.600 5.100 5.186 6.600 8.100 15.000
0.0172 0.0276 0.0357 0.0437 0.0522 0.0609 0.0692 0.0777
0.2222 0.1763 0.3307 0.4143 0.5147 0.5574 0.5917 0.6106
0.1947 0.2855 0.3555 1.1713 1.1713 1.4685 1.4685 0.1960
0.3418 0.4456 0.5087 0.5717 0.5717 0.5175 0.4675 0.3036
0.6067 FSUR = 0.1846

SOLID VELOCITY
= 0.304 M/S.

POSITION FROM
ENTRY M.
DEPTH M.
TIME = 10.45 S.
VELOCITY M/S
FLOW RATE L/S
WAVE SPD. M/S
FSOL =
0.0004 FP2 =

0. 2.100 3.600 5.100 5.264 6.600 8.100 15.000
0.0170 0.0276 0.0353 0.0437 0.0521 0.0609 0.0692 0.0777
0.2267 0.1676 0.3861 0.4114 0.5126 0.5508 0.5875 0.6036
0.2004 0.2441 0.3564 1.1564 1.1564 1.4532 1.4532 0.1960
0.3348 0.4401 0.5043 0.5715 0.5715 0.5187 0.4623 0.3036
0.6045 FSUR = 0.1846

SOLID VELOCITY
= 0.304 M/S.

POSITION FROM
ENTRY M.
DEPTH M.
TIME = 10.70 S.
VELOCITY M/S
FLOW RATE L/S
WAVE SPD. M/S
FSOL =
-0.0131 FP2 =

0. 2.400 3.900 5.342 5.342 6.900 8.400 15.000
0.0166 0.0276 0.0363 0.0441 0.0523 0.0606 0.0692 0.0777
0.2306 0.1725 0.3812 0.4139 0.5171 0.5510 0.5897 0.6036
0.2065 0.2470 0.3662 1.1830 1.1830 1.4357 1.4357 0.1960
0.3376 0.4451 0.5124 0.5747 0.5747 0.5151 0.4670 0.3036
0.6070 FSUR = 0.1846

SOLID VELOCITY
= 0.309 M/S.

POSITION FROM
ENTRY M.
DEPTH M.
TIME = 10.96 S.
VELOCITY M/S
FLOW RATE L/S
WAVE SPD. M/S
FSOL =
-0.0001 FP2 =

0. 2.400 3.900 5.421 5.421 6.900 8.400 15.000
0.0166 0.0276 0.0357 0.0432 0.0520 0.0606 0.0692 0.0777
0.2240 0.1628 0.3740 0.4130 0.5091 0.5437 0.5897 0.6036
0.2000 0.2414 0.3547 1.1444 1.1444 1.4157 1.4157 0.1960
0.3357 0.4403 0.5078 0.5677 0.5677 0.5149 0.4611 0.3036
0.6066 FSUR = 0.1846

SOLID VELOCITY
= 0.295 M/S.

POSITION FROM
ENTRY M.
DEPTH M.
TIME = 11.22 S.
VELOCITY M/S
FLOW RATE L/S
WAVE SPD. M/S
FSOL =
-0.0007 FP2 =

0. 2.400 3.900 5.499 5.499 6.900 8.400 15.000
0.0164 0.0271 0.0351 0.0433 0.0520 0.0606 0.0692 0.0777
0.2277 0.1511 0.3747 0.4100 0.5091 0.5437 0.5897 0.6036
0.2000 0.2414 0.3547 1.1444 1.1444 1.4157 1.4157 0.1960
0.3357 0.4403 0.5078 0.5677 0.5677 0.5149 0.4611 0.3036
0.6066 FSUR = 0.1846

SOLID VELOCITY

FLOW RATE L/S = 0.2005 0.4786 0.7769 1.2206 1.2206 1.2510 1.2439 0.1963
 WAVE SPD. M/S = 0.3199 0.4701 0.4689 0.5769 0.5769 0.5056 0.4961 0.3037
 FSOL = 0.0022 FP2 = 0.6072 FSUR = 0.1845

SOLID VELOCITY
 = 0.276 M/S.

TIME = 14.43 S.
 POSITION FROM
 ENTRY M. 0. 3.100 4.800 6.428 7.800 9.300 15.000
 DEPTH M = 0.0141 0.0248 0.0328 0.0422 0.0551 0.0355 0.0344 0.0137
 VELOCITY M/S = 0.2700 0.3025 0.3338 0.3736 0.4278 0.4999 0.5112 0.1037
 FLOW RATE L/S = 0.2004 0.4603 0.7474 1.1765 1.2765 1.2466 1.2314 0.1963
 WAVE SPD. M/S = 0.3191 0.4156 0.4617 0.5591 0.5910 0.5056 0.4958 0.1037
 FSOL = 0.0016 FP2 = 0.6072 FSUR = 0.1845

SOLID VELOCITY
 = 0.278 M/S.

TIME = 14.70 S.
 POSITION FROM
 ENTRY M. 0. 3.300 4.800 6.504 7.800 9.300 15.000
 DEPTH M = 0.0150 0.0244 0.0321 0.0422 0.0352 0.0353 0.0344 0.0137
 VELOCITY M/S = 0.2714 0.3000 0.3248 0.3762 0.4279 0.4953 0.5146 0.1037
 FLOW RATE L/S = 0.2001 0.4440 0.7190 1.1439 1.1819 1.2305 1.2333 0.1963
 WAVE SPD. M/S = 0.3183 0.4113 0.4765 0.5592 0.5934 0.5096 0.4974 0.1037
 FSOL = 0.0114 FP2 = 0.6069 FSUR = 0.1846

SOLID VELOCITY
 = 0.280 M/S.

TIME = 14.98 S.
 POSITION FROM
 ENTRY M. 0. 3.600 5.100 6.540 7.800 9.300 15.000
 DEPTH M = 0.0149 0.0253 0.0333 0.0424 0.0357 0.0352 0.0342 0.0137
 VELOCITY M/S = 0.2726 0.3038 0.3302 0.3823 0.4401 0.4969 0.5148 0.1037
 FLOW RATE L/S = 0.1995 0.4731 0.7349 1.2319 1.2319 1.2279 1.2216 0.1963
 WAVE SPD. M/S = 0.3175 0.4193 0.4879 0.5651 0.5973 0.5037 0.4953 0.1037
 FSOL = -0.0195 FP2 = 0.6077 FSUR = 0.1845

SOLID VELOCITY
 = 0.292 M/S.

TIME = 15.25 S.
 POSITION FROM
 ENTRY M. 0. 3.600 5.100 6.659 7.800 9.300 15.000
 DEPTH M = 0.0149 0.0248 0.0327 0.0415 0.0352 0.0352 0.0343 0.0137
 VELOCITY M/S = 0.2742 0.3016 0.3265 0.3765 0.4403 0.4942 0.5120 0.1038
 FLOW RATE L/S = 0.1994 0.4575 0.7276 1.1494 1.1854 1.2182 1.2211 0.1964
 WAVE SPD. M/S = 0.3170 0.4151 0.4474 0.5514 0.5914 0.5032 0.4942 0.1038
 FSOL = 0.0027 FP2 = 0.6073 FSUR = 0.1845

SOLID VELOCITY
 = 0.271 M/S.

TIME = 15.51 S.
 POSITION FROM
 ENTRY M. 0. 3.600 5.100 6.736 7.800 9.300 15.000
 DEPTH M = 0.0146 0.0246 0.0320 0.0418 0.0346 0.0352 0.0344 0.0117
 VELOCITY M/S = 0.2735 0.2997 0.3231 0.3766 0.4406 0.4927 0.5037 0.1038
 FLOW RATE L/S = 0.1996 0.4477 0.7011 1.1376 1.1376 1.2145 1.2137 0.1965
 WAVE SPD. M/S = 0.3164 0.4111 0.4777 0.5593 0.5970 0.5032 0.4957 0.1038
 FSOL = 0.0014 FP2 = 0.6073 FSUR = 0.1845

TIME = 15.01 S.		POSITION FROM									
DEPTH	M	W	U	3-600	5-100	6-011	6-011	8-101	9-610	15-010	
VELOCITY	M/S	0.0148	0.0739	0.0114	0.0418	0.0347	0.0347	0.0450	0.0194	0.0137	
WAVELENGTH	M	0.2766	0.4102	0.1199	0.1700	0.4741	0.4741	0.5073	0.5073	0.1060	
WAVE SQR.	M/S	0.3154	0.9077	0.4727	0.5573	0.4993	0.4993	0.5021	0.4972	0.1040	
FSQL		0.0604	0.1446								

[illegible]

TIME =	16.36	5.	POSITION FROM
DEPTH M.	M =		
VELOCITY	M/S =		
WAVE RATE	L/S =		
WAVE SPT.	M/S =		
FSDOL =			

TIME = 16.64 S.	POSITION FROM									
	ENTRY NO.	DEPTH	M =	VELOCITY	M/S =	FLOW RATE	L/S =	WAVE SPD.	M/S =	F50L =
	1	0.0147	0.0240	0.0315	0.0414	0.3143	0.0147	0.0443	0.0443	0.0443
	2	0.0147	0.0240	0.0315	0.0414	0.3143	0.0147	0.0443	0.0443	0.0443
	3	0.0147	0.0240	0.0315	0.0414	0.3143	0.0147	0.0443	0.0443	0.0443
	4	0.0147	0.0240	0.0315	0.0414	0.3143	0.0147	0.0443	0.0443	0.0443
	5	0.0147	0.0240	0.0315	0.0414	0.3143	0.0147	0.0443	0.0443	0.0443
	6	0.0147	0.0240	0.0315	0.0414	0.3143	0.0147	0.0443	0.0443	0.0443
	7	0.0147	0.0240	0.0315	0.0414	0.3143	0.0147	0.0443	0.0443	0.0443
	8	0.0147	0.0240	0.0315	0.0414	0.3143	0.0147	0.0443	0.0443	0.0443
	9	0.0147	0.0240	0.0315	0.0414	0.3143	0.0147	0.0443	0.0443	0.0443
	10	0.0147	0.0240	0.0315	0.0414	0.3143	0.0147	0.0443	0.0443	0.0443
	11	0.0147	0.0240	0.0315	0.0414	0.3143	0.0147	0.0443	0.0443	0.0443
	12	0.0147	0.0240	0.0315	0.0414	0.3143	0.0147	0.0443	0.0443	0.0443
	13	0.0147	0.0240	0.0315	0.0414	0.3143	0.0147	0.0443	0.0443	0.0443
	14	0.0147	0.0240	0.0315	0.0414	0.3143	0.0147	0.0443	0.0443	0.0443
	15	0.0147	0.0240	0.0315	0.0414	0.3143	0.0147	0.0443	0.0443	0.0443
	16	0.0147	0.0240	0.0315	0.0414	0.3143	0.0147	0.0443	0.0443	0.0443
	17	0.0147	0.0240	0.0315	0.0414	0.3143	0.0147	0.0443	0.0443	0.0443
	18	0.0147	0.0240	0.0315	0.0414	0.3143	0.0147	0.0443	0.0443	0.0443
	19	0.0147	0.0240	0.0315	0.0414	0.3143	0.0147	0.0443	0.0443	0.0443
	20	0.0147	0.0240	0.0315	0.0414	0.3143	0.0147	0.0443	0.0443	0.0443
	21	0.0147	0.0240	0.0315	0.0414	0.3143	0.0147	0.0443	0.0443	0.0443
	22	0.0147	0.0240	0.0315	0.0414	0.3143	0.0147	0.0443	0.0443	0.0443
	23	0.0147	0.0240	0.0315	0.0414	0.3143	0.0147	0.0443	0.0443	0.0443
	24	0.0147	0.0240	0.0315	0.0414	0.3143	0.0147	0.0443	0.0443	0.0443
	25	0.0147	0.0240	0.0315	0.0414	0.3143	0.0147	0.0443	0.0443	0.0443
	26	0.0147	0.0240	0.0315	0.0414	0.3143	0.0147	0.0443	0.0443	0.0443
	27	0.0147	0.0240	0.0315	0.0414	0.3143	0.0147	0.0443	0.0443	0.0443
	28	0.0147	0.0240	0.0315	0.0414	0.3143	0.0147	0.0443	0.0443	0.0443
	29	0.0147	0.0240	0.0315	0.0414	0.3143	0.0147	0.0443	0.0443	0.0443
	30	0.0147	0.0240	0.0315	0.0414	0.3143	0.0147	0.0443	0.0443	0.0443
	31	0.0147	0.0240	0.0315	0.0414	0.3143	0.0147	0.0443	0.0443	0.0443

TIME =	16.02 S.	POSITION FROM									
		U.	3.700	5.506	7.118	7.118	8.800	9.970	15.000		
ENTRY M.	M =	0.0140	0.0120	0.0109	0.0815	0.3184	0.0147	0.0344	0.0151		
VELOCITY	M/S =	0.2749	0.2720	0.1174	0.1174	0.8775	0.8775	0.8930	0.1174		
WAVE LENGTH	L/S =	0.1145	0.0700	0.0880	1.1210	1.0710	1.1277	1.1912	0.2174		
WAVE S.D.	M/S =	0.1145	0.0700	0.0880	1.1210	1.0710	1.1277	1.1912	0.2174		
PSOL =		0.0140	0.0120	0.0109	0.0815	0.3184	0.0147	0.0344	0.0151		

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POSITION FROM
 ENTRY M.
 TIME = 17.20 S. DEPTH M= 0.0146 0.0246 0.0321 0.0427 0.0533 0.0639 0.0745 0.0851 0.0957 0.1063 0.1169 0.1275 0.1381 0.1487 0.1593 0.1699 0.1805 0.1911 0.2017 0.2123 0.2229 0.2335 0.2441 0.2547 0.2653 0.2759 0.2865 0.2971 0.3077 0.3183 0.3289 0.3395 0.3501 0.3607 0.3713 0.3819 0.3925 0.4031 0.4137 0.4243 0.4349 0.4455 0.4561 0.4667 0.4773 0.4879 0.4985 0.5091 0.5197 0.5303 0.5409 0.5515 0.5621 0.5727 0.5833 0.5939 0.6045 0.6151 0.6257 0.6363 0.6469 0.6575 0.6681 0.6787 0.6893 0.6999 0.7105 0.7211 0.7317 0.7423 0.7529 0.7635 0.7741 0.7847 0.7953 0.8059 0.8165 0.8271 0.8377 0.8483 0.8589 0.8695 0.8801 0.8907 0.9013 0.9119 0.9225 0.9331 0.9437 0.9543 0.9649 0.9755 0.9861 0.9967 1.0073 1.0179 1.0285 1.0391 1.0497 1.0603 1.0709 1.0815 1.0921 1.1027 1.1133 1.1239 1.1345 1.1451 1.1557 1.1663 1.1769 1.1875 1.1981 1.2087 1.2193 1.2299 1.2405 1.2511 1.2617 1.2723 1.2829 1.2935 1.3041 1.3147 1.3253 1.3359 1.3465 1.3571 1.3677 1.3783 1.3889 1.3995 1.4101 1.4207 1.4313 1.4419 1.4525 1.4631 1.4737 1.4843 1.4949 1.5055 1.5161 1.5267 1.5373 1.5479 1.5585 1.5691 1.5797 1.5903 1.6009 1.6115 1.6221 1.6327 1.6433 1.6539 1.6645 1.6751 1.6857 1.6963 1.7069 1.7175 1.7281 1.7387 1.7493 1.7599 1.7705 1.7811 1.7917 1.8023 1.8129 1.8235 1.8341 1.8447 1.8553 1.8659 1.8765 1.8871 1.8977 1.9083 1.9189 1.9295 1.9401 1.9507 1.9613 1.9719 1.9825 1.9931 2.0037 2.0143 2.0249 2.0355 2.0461 2.0567 2.0673 2.0779 2.0885 2.0991 2.1097 2.1203 2.1309 2.1415 2.1521 2.1627 2.1733 2.1839 2.1945 2.2051 2.2157 2.2263 2.2369 2.2475 2.2581 2.2687 2.2793 2.2899 2.3005 2.3111 2.3217 2.3323 2.3429 2.3535 2.3641 2.3747 2.3853 2.3959 2.4065 2.4171 2.4277 2.4383 2.4489 2.4595 2.4701 2.4807 2.4913 2.5019 2.5125 2.5231 2.5337 2.5443 2.5549 2.5655 2.5761 2.5867 2.5973 2.6079 2.6185 2.6291 2.6397 2.6503 2.6609 2.6715 2.6821 2.6927 2.7033 2.7139 2.7245 2.7351 2.7457 2.7563 2.7669 2.7775 2.7881 2.7987 2.8093 2.8199 2.8305 2.8411 2.8517 2.8623 2.8729 2.8835 2.8941 2.9047 2.9153 2.9259 2.9365 2.9471 2.9577 2.9683 2.9789 2.9895 2.9999 3.0105 3.0211 3.0317 3.0423 3.0529 3.0635 3.0741 3.0847 3.0953 3.1059 3.1165 3.1271 3.1377 3.1483 3.1589 3.1695 3.1801 3.1907 3.2013 3.2119 3.2225 3.2331 3.2437 3.2543 3.2649 3.2755 3.2861 3.2967 3.3073 3.3179 3.3285 3.3391 3.3497 3.3603 3.3709 3.3815 3.3921 3.4027 3.4133 3.4239 3.4345 3.4451 3.4557 3.4663 3.4769 3.4875 3.4981 3.5087 3.5193 3.5299 3.5405 3.5511 3.5617 3.5723 3.5829 3.5935 3.6041 3.6147 3.6253 3.6359 3.6465 3.6571 3.6677 3.6783 3.6889 3.6995 3.7101 3.7207 3.7313 3.7419 3.7525 3.7631 3.7737 3.7843 3.7949 3.8055 3.8161 3.8267 3.8373 3.8479 3.8585 3.8691 3.8797 3.8903 3.9009 3.9115 3.9221 3.9327 3.9433 3.9539 3.9645 3.9751 3.9857 3.9963 4.0069 4.0175 4.0281 4.0387 4.0493 4.0599 4.0705 4.0811 4.0917 4.1023 4.1129 4.1235 4.1341 4.1447 4.1553 4.1659 4.1765 4.1871 4.1977 4.2083 4.2189 4.2295 4.2401 4.2507 4.2613 4.2719 4.2825 4.2931 4.3037 4.3143 4.3249 4.3355 4.3461 4.3567 4.3673 4.3779 4.3885 4.3991 4.4097 4.4203 4.4309 4.4415 4.4521 4.4627 4.4733 4.4839 4.4945 4.5051 4.5157 4.5263 4.5369 4.5475 4.5581 4.5687 4.5793 4.5899 4.6005 4.6111 4.6217 4.6323 4.6429 4.6535 4.6641 4.6747 4.6853 4.6959 4.7065 4.7171 4.7277 4.7383 4.7489 4.7595 4.7701 4.7807 4.7913 4.8019 4.8125 4.8231 4.8337 4.8443 4.8549 4.8655 4.8761 4.8867 4.8973 4.9079 4.9185 4.9291 4.9397 4.9503 4.9609 4.9715 4.9821 4.9927 5.0033 5.0139 5.0245 5.0351 5.0457 5.0563 5.0669 5.0775 5.0881 5.0987 5.1093 5.1199 5.1305 5.1411 5.1517 5.1623 5.1729 5.1835 5.1941 5.2047 5.2153 5.2259 5.2365 5.2471 5.2577 5.2683 5.2789 5.2895 5.2999 5.3105 5.3211 5.3317 5.3423 5.3529 5.3635 5.3741 5.3847 5.3953 5.4059 5.4165 5.4271 5.4377 5.4483 5.4589 5.4695 5.4801 5.4907 5.5013 5.5119 5.5225 5.5331 5.5437 5.5543 5.5649 5.5755 5.5861 5.5967 5.6073 5.6179 5.6285 5.6391 5.6497 5.6603 5.6709 5.6815 5.6921 5.7027 5.7133 5.7239 5.7345 5.7451 5.7557 5.7663 5.7769 5.7875 5.7981 5.8087 5.8193 5.8299 5.8405 5.8511 5.8617 5.8723 5.8829 5.8935 5.9041 5.9147 5.9253 5.9359 5.9465 5.9571 5.9677 5.9783 5.9889 5.9995 6.0101 6.0207 6.0313 6.0419 6.0525 6.0631 6.0737 6.0843 6.0949 6.1055 6.1161 6.1267 6.1373 6.1479 6.1585 6.1691 6.1797 6.1903 6.2009 6.2115 6.2221 6.2327 6.2433 6.2539 6.2645 6.2751 6.2857 6.2963 6.3069 6.3175 6.3281 6.3387 6.3493 6.3599 6.3705 6.3811 6.3917 6.4023 6.4129 6.4235 6.4341 6.4447 6.4553 6.4659 6.4765 6.4871 6.4977 6.5083 6.5189 6.5295 6.5401 6.5507 6.5613 6.5719 6.5825 6.5931 6.6037 6.6143 6.6249 6.6355 6.6461 6.6567 6.6673 6.6779 6.6885 6.6991 6.7097 6.7203 6.7309 6.7415 6.7521 6.7627 6.7733 6.7839 6.7945 6.8051 6.8157 6.8263 6.8369 6.8475 6.8581 6.8687 6.8793 6.8899 6.9005 6.9111 6.9217 6.9323 6.9429 6.9535 6.9641 6.9747 6.9853 6.9959 7.0065 7.0171 7.0277 7.0383 7.0489 7.0595 7.0701 7.0807 7.0913 7.1019 7.1125 7.1231 7.1337 7.1443 7.1549 7.1655 7.1761 7.1867 7.1973 7.2079 7.2185 7.2291 7.2397 7.2503 7.2609 7.2715 7.2821 7.2927 7.3033 7.3139 7.3245 7.3351 7.3457 7.3563 7.3669 7.3775 7.3881 7.3987 7.4093 7.4199 7.4305 7.4411 7.4517 7.4623 7.4729 7.4835 7.4941 7.5047 7.5153 7.5259 7.5365 7.5471 7.5577 7.5683 7.5789 7.5895 7.5999 7.6105 7.6211 7.6317 7.6423 7.6529 7.6635 7.6741 7.6847 7.6953 7.7059 7.7165 7.7271 7.7377 7.7483 7.7589 7.7695 7.7801 7.7907 7.8013 7.8119 7.8225 7.8331 7.8437 7.8543 7.8649 7.8755 7.8861 7.8967 7.9073 7.9179 7.9285 7.9391 7.9497 7.9603 7.9709 7.9815 7.9921 8.0027 8.0133 8.0239 8.0345 8.0451 8.0557 8.0663 8.0769 8.0875 8.0981 8.1087 8.1193 8.1299 8.1405 8.1511 8.1617 8.1723 8.1829 8.1935 8.2041 8.2147 8.2253 8.2359 8.2465 8.2571 8.2677 8.2783 8.2889 8.2995 8.3101 8.3207 8.3313 8.3419 8.3525 8.3631 8.3737 8.3843 8.3949 8.4055 8.4161 8.4267 8.4373 8.4479 8.4585 8.4691 8.4797 8.4903 8.5009 8.5115 8.5221 8.5327 8.5433 8.5539 8.5645 8.5751 8.5857 8.5963 8.6069 8.6175 8.6281 8.6387 8.6493 8.6599 8.6705 8.6811 8.6917 8.7023 8.7129 8.7235 8.7341 8.7447 8.7553 8.7659 8.7765 8.7871 8.7977 8.8083 8.8189 8.8295 8.8401 8.8507 8.8613 8.8719 8.8825 8.8931 8.9037 8.9143 8.9249 8.9355 8.9461 8.9567 8.9673 8.9779 8.9885 8.9991 9.0097 9.0203 9.0309 9.0415 9.0521 9.0627 9.0733 9.0839 9.0945 9.1051 9.1157 9.1263 9.1369 9.1475 9.1581 9.1687 9.1793 9.1899 9.2005 9.2111 9.2217 9.2323 9.2429 9.2535 9.2641 9.2747 9.2853 9.2959 9.3065 9.3171 9.3277 9.3383 9.3489 9.3595 9.3701 9.3807 9.3913 9.4019 9.4125 9.4231 9.4337 9.4443 9.4549 9.4655 9.4761 9.4867 9.4973 9.5079 9.5185 9.5291 9.5397 9.5503 9.5609 9.5715 9.5821 9.5927 9.6033 9.6139 9.6245 9.6351 9.6457 9.6563 9.6669 9.6775 9.6881 9.6987 9.7093 9.7199 9.7305 9.7411 9.7517 9.7623 9.7729 9.7835 9.7941 9.8047 9.8153 9.8259 9.8365 9.8471 9.8577 9.8683 9.8789 9.8895 9.8999 9.9105 9.9211 9.9317 9.9423 9.9529 9.9635 9.9741 9.9847 9.9953 10.0059 10.0165 10.0271 10.0377 10.0483 10.0589 10.0695 10.0801 10.0907 10.1013 10.1119 10.1225 10.1331 10.1437 10.1543 10.1649 10.1755 10.1861 10.1967 10.2073 10.2179 10.2285 10.2391 10.2497 10.2603 10.2709 10.2815 10.2921 10.3027 10.3133 10.3239 10.3345 10.3451 10.3557 10.3663 10.3769 10.3875 10.3981 10.4087 10.4193 10.4299 10.4405 10.4511 10.4617 10.4723 10.4829 10.4935 10.5041 10.5147 10.5253 10.5359 10.5465 10.5571 10.5677 10.5783 10.5889 10.5995 10.6101 10.6207 10.6313 10.6419 10.6525 10.6631 10.6737 10.6843 10.6949 10.7055 10.7161 10.7267 10.7373 10.7479 10.7585 10.7691 10.7797 10.7903 10.8009 10.8115 10.8221 10.8327 10.8433 10.8539 10.8645 10.8751 10.8857 10.8963 10.9069 10.9175 10.9281 10.9387 10.9493 10.9599 10.9705 10.9811 10.9917 11.0023 11.0129 11.0235 11.0341 11.0447 11.0553 11.0659 11.0765 11.0871 11.0977 11.1083 11.1189 11.1295 11.1401 11.1507 11.1613 11.1719 11.1825 11.1931 11.2037 11.2143 11.2249 11.2355 11.2461 11.2567 11.2673 11.2779 11.2885 11.2991 11.3097 11.3203 11.3309 11.3415 11.3521 11.3627 11.3733 11.3839 11.3945 11.4051 11.4157 11.4263 11.4369 11.4475 11.4581 11.4687 11.4793 11.4899 11.5005 11.5111 11.5217 11.5323 11.5429 11.5535 11.5641 11.5747 11.5853 11.5959 11.6065 11.6171 11.6277 11.6383 11.6489 11.6595 11.6701 11.6807 11.6913 11.7019 11.7125 11.7231 11.7337 11.7443 11.7549 11.7655 11.7761 11.7867 11.7973 11.8079 11.8185 11.8291 11.8397 11.8503 11.8609 11.8715 11.8821 11.8927 11.9033 11.9139 11.9245 11.9351 11.9457 11.9563 11.9669 11.9775 11.9881 11.9987 12.0093 12.0199 12.0305 12.0411 12.0517 12.0623 12.0729 12.0835 12.0941 12.1047 12.1153 12.1259 12.1365 12.1471 12.1577 12.1683 12.1789 12.1895 12.1999 12.2105 12.2211 12.2317 12.2423 12.2529 12.2635 12.2741 12.2847 12.2953 12.3059 12.3165 12.3271 12.3377 12.3483 12.3589 12.3695 12.3801 12.3907 12.4013 12.4119 12.4225 12.4331 12.4437 12.4543 12.4649 12.4755 12.4861 12.4967 12.5073 12.5179 12.5285 12.5391 12.5497 12.5603 12.5709 12.5815 12.5921 12.6027 12.6133 12.6239 12.6345 12.6451 12.6557 12.6663 12.6769 12.6875 12.6981 12.7087 12.7193 12.7299 12.7405 12.7511 12.7617 12.7723 12.7829 12.7935 12.8041 12.8147 12.8253 12.8359 12.8465 12.8571 12.8677 12.8783 12.8889 12.8995 12.9101 12.9207 12.9313 12.9419 12.9525 12.9631 12.9737 12.9843 12.9949 13.0055 13.0161 13.0267 13.0373 13.0479 13.0585 13.0691 13.0797 13.0903 13.1009 13.1115 13.1221 13.1327 13.1433 13.1539 13.1645 13.1751 13.1857 13.1963 13.2069 13.2175 13.2281 13.2387 13.2493 13.2599 13.2705 13.2811 13.2917 13.3023 13.3129 13.3235 13.3341 13.3447 13.3553 13.3659 13.3765 13.3871 13.3977 13.4083 13.4189 13.4295 13.4401 13.4507 13.4613 13.4719 13.4825 13.4931 13.5037 13.5143 13.5249 13.5355 13.5461 13.5567 13.5673 13.5779 13.5885 13.5991 13.6097 13.6203 13.6309 13.6415 13.6521 13.6627 13.6733 13.6839 13.6945 13.7051 13.7157 13.7263 13.7369 13.7475 13.7581 13.7687 13.7793 13.7899 13.8005 13.8111 13.8217 13.8323 13.8429 13.8535 13.8641 13.8747 13.8853 13.8959 13.9065 13.9171 13.9277 13.9383 13.9489 13.9595 13.9701 13.9807 13.9913 14.0019 14.0125 14.0231 14.0337 14.0443 14.0549 14.0655 14.0761 14.0867 14.0973 14.1079 14.1185 14.1291 14.1397 14.1503 14.1609 14.1715 14.1821 14.1927 14.2033 14.2139 14.2245 14.2351 14.2457 14.2563 14.2669 14.2775 14.2881 14.2987 14.3093 14.3199 14.3305 14.3411 14.3517 14.3623 14.3729 14.3835 14.3941 14.4047 14.4153 14.4259 14.4365 14.4471 14.4577 14.4683 14.4789 14.4895 14.5001 14.5107 14.5213 14.5319 14.5425 14.5531 14.5637 14.5743 14.5849 14.5955 14.6061 14.6167 14.6273 14.6379 14.6485 14.6591 14.6697 14.6803 14.6909 14.7015 14.7121 14.7227 14.7333 14.7439 14.7545 14.7651 14.7757 14.7863 14.7969 14.8075 14.8181 14.8287 14.8393 14.8499 14.8605 14.8711 14.8817 14.8923 14.9029 14.9135 14.9241 14.9347 14.9453 14.9559 14.9665 14.9771 14.9877 14.9983 15.0089 15.0195 15.0301 15.0407 15.0513 15.0619 15.0725 15.0831 15.0937 15.1043 15.1149 15.1255 15.1361 15.1467 15.1573 15.1679 15.1785 15.1891 15.1997 15.2103 15.2209 15.2315 15.2421 15.2527 15.2633 15.2739 15.2845 15.2951 15.3057 15.3163 15.3269 15.3375 15.3481 15.3587 15.3693 15.3799 15.3905 15.4011 15.4117 15.4223 15.4329 15.4435 15.4541 15.4647 15.4753 15.4859 15.4965 15.5071 15.5177 15.5283 15.5389 15.5495 15.5601 15.5707 15.5813 15.5919 15.6025 15.6131 15.6237 15.6343 15.6449 15.6555 15.6661 15.6767 15.6873 15.6979 15.7085 15.7191 15.7297 15.7403 15.7509 15.7615 15.7721 15.7827 15.7933 15.8039 15.8145 15.8251 15.8357 15.8463 15.8569 15.8675 15.8781 15.8887 15.8993 15.9099 15.9205 15.9311 15.9417 15.9523 15.9629 15.9735 15.9841 15.9947 16.0053 16.0159 16.0265 16.0371 16.0477 16.0583 16.0689 16.0795 16.0901 16.1007 16.1113 16.1219 16.1325 16.1431 16.1537 16.1643 16.1749 16.1855 16.1961 16.2067 16.2173 16.2279 16.2385 16.2491 16.2597 16.2703 16.2809 16.2915 16.3021 16.3127 16.3233 16.3339 16.3445 16.3551 16.3657 16.3763 16.3869 16.3975 16.4081 16.4187 16.4293 16.4399 16.4505 16.4611 16.4717 16.4823 16.4929 16.5035 16.5141 16.5247 16.5353 16.5459 16.5565 16.5671 16.5777 16.5883 16.5989 16.6095 16.6201 16.6307 16.6413 16.6519 16.6625 16.6731 16.6837 16.6943 16.7049 16.7155 16.7261 16.7367 16.7473 16.7579 16.7685 16.7791 16.7897 16.8003 16.8109 16.8215 16.8321 16.8427 16.8533 16.8639 16.8745 16.8851 16.8957 16.9063 16.9169 16.9275 16.9381 16.9487 16.9593 16.9699 16.9805 16.9911 17.0017 17.0123 17.0229 17.0335 17.0441 17.0547 17.0653 17.0759 17.0865 17.0971 17.1077 17.1183 17.1289 17.1395 17.1501 17.1607 17.1713 17.1819 17.1925 17.2031 17.2137 17.2243 17.2349 17.2455 17.2561 17.2667 17.2773 17.2879 17.2985 17.3091 17.3197 17.3303 17.3409 17.3515 17.3621 17.3727 17.3833 17.3939 17.4045 17.4151 17.4257 17.4363 17.4469 17.4575 17.4681 17.4787 17.4893 17.4999 17.5105 17.5211 17.5317 17.5423 17.5529 17.5635 17.5741 17.5

TIME - 10.61 S.
 ENTRY M. U_z 4.500 6.000 7.074 7.574 9.000 10.500 15.000
 DEPTH 0.0145 0.0237 0.0312 0.0402 0.0473 0.0541 0.0622
 VELOCITY M/S 0.0042 0.0085 0.0105 0.0130 0.0150 0.0164 0.0173
 FLOW RATE L/S 0.2004 0.4255 0.6178 0.7700 0.9230 1.0761 1.2291
 WAVE SPD. M/S 0.3134 0.4054 0.4703 0.5147 0.5447 0.5658 0.5773
 FSQL- 0.0001 FPZ- 0.0145

SOLID VELOCITY
 = 0.252 M/S.

POSITION FROM
 TIME - 10.90 S.
 ENTRY M. U_z 4.500 6.000 7.074 7.574 9.000 10.500 15.000
 DEPTH 0.0145 0.0233 0.0306 0.0401 0.0473 0.0541 0.0622
 VELOCITY M/S 0.0042 0.0079 0.0104 0.0129 0.0149 0.0164 0.0173
 FLOW RATE L/S 0.1997 0.4150 0.6216 0.7705 0.9205 1.0730 1.2259
 WAVE SPD. M/S 0.3129 0.4019 0.4660 0.5125 0.5430 0.5658 0.5750
 FSQL- 0.0061 FPZ- 0.0077 FSQL- 0.1045

SOLID VELOCITY
 = 0.252 M/S.

POSITION FROM
 TIME - 10.10 S.
 ENTRY M. U_z 4.500 6.000 7.074 7.574 9.000 10.500 15.000
 DEPTH 0.0145 0.0230 0.0301 0.0405 0.0479 0.0541 0.0622
 VELOCITY M/S 0.0049 0.0073 0.0104 0.0132 0.0149 0.0164 0.0173
 FLOW RATE L/S 0.2002 0.4049 0.6050 0.7715 0.9115 1.0757 1.2281
 WAVE SPD. M/S 0.3129 0.4085 0.4717 0.5125 0.5430 0.5658 0.5750
 FSQL- 0.0139 FPZ- 0.0074 FSQL- 0.1045

SOLID VELOCITY
 = 0.259 M/S.

POSITION FROM
 TIME - 10.47 S.
 ENTRY M. U_z 4.500 6.000 7.074 7.574 9.000 10.500 15.000
 DEPTH 0.0145 0.0236 0.0313 0.0413 0.0486 0.0541 0.0622
 VELOCITY M/S 0.0049 0.0085 0.0104 0.0131 0.0149 0.0164 0.0173
 FLOW RATE L/S 0.1994 0.4281 0.6390 0.7759 0.9259 1.0759 1.2281
 WAVE SPD. M/S 0.3126 0.4064 0.4714 0.5122 0.5430 0.5658 0.5750
 FSQL- -0.0192 FPZ- 0.0084 FSQL- 0.1045

SOLID VELOCITY
 = 0.274 M/S.

POSITION FROM
 TIME - 10.75 S.
 ENTRY M. U_z 4.500 6.000 7.074 7.574 9.000 10.500 15.000
 DEPTH 0.0145 0.0235 0.0308 0.0408 0.0481 0.0541 0.0622
 VELOCITY M/S 0.0049 0.0079 0.0104 0.0131 0.0149 0.0164 0.0173
 FLOW RATE L/S 0.2004 0.4179 0.6276 0.7776 0.9276 1.0776 1.2276
 WAVE SPD. M/S 0.3126 0.4030 0.4681 0.5149 0.5450 0.5658 0.5750
 FSQL- 0.0037 FPZ- 0.0145

SOLID VELOCITY
 = 0.251 M/S.

POSITION FROM
 TIME - 20.03 S.
 ENTRY M. U_z 4.500 6.000 7.074 7.574 9.000 10.500 15.000
 DEPTH 0.0145 0.0233 0.0306 0.0401 0.0473 0.0541 0.0622
 VELOCITY M/S 0.0049 0.0079 0.0104 0.0129 0.0149 0.0164 0.0173
 FLOW RATE L/S 0.2004 0.4150 0.6216 0.7705 0.9205 1.0730 1.2259
 WAVE SPD. M/S 0.3129 0.4019 0.4660 0.5125 0.5430 0.5658 0.5750
 FSQL- 0.0061 FPZ- 0.0077 FSQL- 0.1045

FLUM RATE L/S= 0.0025
 WAVE SPD. M/S= 0.0025
 FSOL= 0.0025

SOLID VELOCITY
 = 0.257 M/S.

TIME = 20.31 S.
 POSITION FROM
 ENTRY M. 0.0144
 DEPTH M. 0.0144
 VELOCITY M/S. 0.0144
 FLOW RATE L/S. 0.0144
 WAVE SPD. M/S. 0.0144
 FSOL= 0.0144

SOLID VELOCITY
 = 0.259 M/S.

TIME = 20.59 S.
 POSITION FROM
 ENTRY M. 0.0144
 DEPTH M. 0.0144
 VELOCITY M/S. 0.0144
 FLOW RATE L/S. 0.0144
 WAVE SPD. M/S. 0.0144
 FSOL= 0.0144

SOLID VELOCITY
 = 0.278 M/S.

TIME = 20.87 S.
 POSITION FROM
 ENTRY M. 0.0144
 DEPTH M. 0.0144
 VELOCITY M/S. 0.0144
 FLOW RATE L/S. 0.0144
 WAVE SPD. M/S. 0.0144
 FSOL= 0.0144

SOLID VELOCITY
 = 0.252 M/S.

TIME = 21.15 S.
 POSITION FROM
 ENTRY M. 0.0144
 DEPTH M. 0.0144
 VELOCITY M/S. 0.0144
 FLOW RATE L/S. 0.0144
 WAVE SPD. M/S. 0.0144
 FSOL= 0.0144

SOLID VELOCITY
 = 0.255 M/S.

TIME = 21.43 S.
 POSITION FROM
 ENTRY M. 0.0144
 DEPTH M. 0.0144
 VELOCITY M/S. 0.0144
 FLOW RATE L/S. 0.0144
 WAVE SPD. M/S. 0.0144
 FSOL= 0.0144

POSITION FROM
 ENTRY M. U. S. 400 6.400 8.400 8.476 8.476 9.900 11.400 15.000
 TIME = 21.71 S. DEPTH M. 0.0144 0.0234 0.0310 0.0409 0.0311 0.0330 0.0316 0.0311
 VELOCITY M/S 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000
 FLOW RATE L/S 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000
 WAVE SPD. M/S 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000
 FSOL = -0.0223 FP2 = 0.0000
 SOLID VELOCITY
 = 0.257 M/S.

POSITION FROM
 ENTRY M. U. S. 400 6.400 8.400 8.471 8.471 9.900 11.400 15.000
 TIME = 21.99 S. DEPTH M. 0.0144 0.0230 0.0305 0.0342 0.0326 0.0330 0.0335 0.0313
 VELOCITY M/S 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000
 FLOW RATE L/S 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000
 WAVE SPD. M/S 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000
 FSOL = 0.0019 FP2 = 0.0000
 SOLID VELOCITY
 = 0.274 M/S.

POSITION FROM
 ENTRY M. U. S. 400 6.400 8.400 8.523 8.523 9.900 11.400 15.000
 TIME = 22.27 S. DEPTH M. 0.0144 0.0227 0.0300 0.0346 0.0321 0.0330 0.0333 0.0315
 VELOCITY M/S 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000
 FLOW RATE L/S 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000
 WAVE SPD. M/S 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000
 FSOL = 0.0026 FP2 = 0.0000
 SOLID VELOCITY
 = 0.250 M/S.

POSITION FROM
 ENTRY M. U. S. 400 6.400 8.400 8.594 8.594 9.900 11.400 15.000
 TIME = 22.55 S. DEPTH M. 0.0144 0.0223 0.0294 0.0347 0.0321 0.0328 0.0331 0.0316
 VELOCITY M/S 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000
 FLOW RATE L/S 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000
 WAVE SPD. M/S 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000
 FSOL = 0.0016 FP2 = 0.0000
 SOLID VELOCITY
 = 0.252 M/S.

POSITION FROM
 ENTRY M. U. S. 400 6.400 8.400 8.660 8.660 10.200 11.700 15.000
 TIME = 22.83 S. DEPTH M. 0.0144 0.0212 0.0288 0.0345 0.0326 0.0328 0.0331 0.0318
 VELOCITY M/S 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000
 FLOW RATE L/S 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000
 WAVE SPD. M/S 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000
 FSOL = -0.0011 FP2 = 0.0000
 SOLID VELOCITY
 = 0.255 M/S.

POSITION FROM
 ENTRY M. M= 0.0144 0.0224 7.200 0.719 0.719 10.200 11.700 15.000
 DEPTH M= 0.2171 0.2197 0.2190 0.1903 1.4411 0.4574 0.4600 0.4763
 VELOCITY M/S= 0.2162 0.1996 0.5973 0.9720 3.1790 1.0212 1.0223 1.0265
 FLOW RATE L/S= 0.3121 0.3121 0.3121 0.3121 0.3121 0.3121 0.3121 0.3121
 WAVE SPD. M/S= 0.0000 FPD= 0.0000 FSD= 0.1844
 FSOL=

SOLID VELOCITY
 = 0.247 M/S.

POSITION FROM
 ENTRY M. M= 0.0144 0.0225 7.200 0.812 0.812 10.200 11.700 15.000
 DEPTH M= 0.2872 0.2453 0.2448 0.1275 0.4156 0.4327 0.4310 0.4320
 VELOCITY M/S= 0.2003 0.3404 0.5789 0.9351 0.7151 1.0222 1.0551 1.0323
 FLOW RATE L/S= 0.3121 0.3451 0.4589 0.5357 0.4741 0.4833 0.4855 0.4771
 WAVE SPD. M/S= 0.0000 FPD= 0.0000 FSD= 0.1844
 FSOL=

SOLID VELOCITY
 = 0.248 M/S.

POSITION FROM
 ENTRY M. M= 0.0144 0.0222 7.200 0.882 0.882 10.200 11.700 15.000
 DEPTH M= 0.2872 0.2449 0.2446 0.1263 0.4413 0.4549 0.4641 0.4778
 VELOCITY M/S= 0.2003 0.3416 0.5658 0.9424 0.7424 1.0092 1.0462 1.0380
 FLOW RATE L/S= 0.3121 0.3409 0.4549 0.5354 0.4745 0.4819 0.4851 0.4778
 WAVE SPD. M/S= 0.0000 FPD= 0.0000 FSD= 0.1844
 FSOL=

SOLID VELOCITY
 = 0.249 M/S.

POSITION FROM
 ENTRY M. M= 0.0144 0.0230 7.500 0.953 0.953 10.500 12.000 15.000
 DEPTH M= 0.2873 0.2452 0.2447 0.1339 0.4506 0.4560 0.4649 0.4784
 VELOCITY M/S= 0.2004 0.3429 0.5462 0.9767 0.7287 1.0128 1.0471 1.0426
 FLOW RATE L/S= 0.3121 0.3494 0.4653 0.5417 0.4776 0.4821 0.4849 0.4744
 WAVE SPD. M/S= 0.0000 FPD= 0.0000 FSD= 0.1844
 FSOL=

SOLID VELOCITY
 = 0.2462 M/S.

POSITION FROM
 ENTRY M. M= 0.0144 0.0227 7.500 0.926 0.926 10.500 12.000 15.000
 DEPTH M= 0.2874 0.2447 0.2440 0.1363 0.4435 0.4539 0.4647 0.4714
 VELOCITY M/S= 0.2004 0.3417 0.5448 0.9471 0.7471 1.0022 1.0438 1.0432
 FLOW RATE L/S= 0.3121 0.3486 0.4612 0.5307 0.4745 0.4810 0.4847 0.4719
 WAVE SPD. M/S= 0.0000 FPD= 0.0000 FSD= 0.1844
 FSOL=

SOLID VELOCITY
 = 0.2451 M/S.

POSITION FROM

TIME = 24.54 S. POSITION FROM
 ENTRY M. U. 6.0000 7.5000 9.0000 10.5000 12.000 13.5000
 VELOCITY M/S= 0.0144 0.0222 0.0299 0.0376 0.0454 0.0531 0.0608 0.0685 0.0762 0.0839
 FLW RATE L/S= 0.2875 0.2936 0.2997 0.3058 0.3119 0.3180 0.3241 0.3302 0.3363 0.3424
 WAVE SPN. M/S= 0.0121 0.0197 0.0274 0.0351 0.0428 0.0505 0.0582 0.0659 0.0736 0.0813
 F50L= 0.0001 FP2= 0.0144

SOLID VELOCITY
 = 0.244 M/S.

TIME = 24.83 S. POSITION FROM
 ENTRY M. U. 6.0000 7.5000 9.0000 10.500 12.000 13.500 15.000
 VELOCITY M/S= 0.0144 0.0220 0.0296 0.0372 0.0448 0.0524 0.0600 0.0676 0.0752 0.0828
 FLW RATE L/S= 0.2875 0.2936 0.2997 0.3058 0.3119 0.3180 0.3241 0.3302 0.3363 0.3424
 WAVE SPN. M/S= 0.0121 0.0193 0.0265 0.0337 0.0409 0.0481 0.0553 0.0625 0.0697 0.0769
 F50L= 0.0100 FP2= 0.0144

SOLID VELOCITY
 = 0.245 M/S.

TIME = 25.12 S. POSITION FROM
 ENTRY M. U. 6.0000 7.5000 9.0000 10.500 12.000 13.500 15.000
 VELOCITY M/S= 0.0144 0.0220 0.0296 0.0372 0.0448 0.0524 0.0600 0.0676 0.0752 0.0828
 FLW RATE L/S= 0.2875 0.2936 0.2997 0.3058 0.3119 0.3180 0.3241 0.3302 0.3363 0.3424
 WAVE SPN. M/S= 0.0121 0.0197 0.0274 0.0351 0.0428 0.0505 0.0582 0.0659 0.0736 0.0813
 F50L= -0.0150 FP2= 0.0144

SOLID VELOCITY
 = 0.256 M/S.

TIME = 25.41 S. POSITION FROM
 ENTRY M. U. 6.0000 7.5000 9.0000 10.500 12.000 13.500 15.000
 VELOCITY M/S= 0.0144 0.0220 0.0296 0.0372 0.0448 0.0524 0.0600 0.0676 0.0752 0.0828
 FLW RATE L/S= 0.2875 0.2936 0.2997 0.3058 0.3119 0.3180 0.3241 0.3302 0.3363 0.3424
 WAVE SPN. M/S= 0.0121 0.0197 0.0274 0.0351 0.0428 0.0505 0.0582 0.0659 0.0736 0.0813
 F50L= 0.0013 FP2= 0.0144

SOLID VELOCITY
 = 0.234 M/S.

TIME = 25.70 S. POSITION FROM
 ENTRY M. U. 6.0000 7.5000 9.0000 10.500 12.000 13.500 15.000
 VELOCITY M/S= 0.0144 0.0222 0.0299 0.0376 0.0454 0.0531 0.0608 0.0685 0.0762 0.0839
 FLW RATE L/S= 0.2875 0.2936 0.2997 0.3058 0.3119 0.3180 0.3241 0.3302 0.3363 0.3424
 WAVE SPN. M/S= 0.0121 0.0197 0.0274 0.0351 0.0428 0.0505 0.0582 0.0659 0.0736 0.0813
 F50L= 0.0007 FP2= 0.0144

SOLID VELOCITY
 = 0.240 M/S.

TIME = 25.99 S. POSITION FROM
 ENTRY M. U. 6.0000 7.5000 9.0000 10.500 12.000 13.500 15.000
 VELOCITY M/S= 0.0144 0.0220 0.0296 0.0372 0.0448 0.0524 0.0600 0.0676 0.0752 0.0828
 FLW RATE L/S= 0.2875 0.2936 0.2997 0.3058 0.3119 0.3180 0.3241 0.3302 0.3363 0.3424
 WAVE SPN. M/S= 0.0121 0.0197 0.0274 0.0351 0.0428 0.0505 0.0582 0.0659 0.0736 0.0813
 F50L= 0.0007 FP2= 0.0144

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5. AUTHOR(S) J.A. Swaffield			
6. PERFORMING ORGANIZATION (If joint or other than NBS, see instructions) NATIONAL BUREAU OF STANDARDS DEPARTMENT OF COMMERCE WASHINGTON, D C 20234			7. Contract/Grant No. 8. Type of Report & Period Covered Final
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10. SUPPLEMENTARY NOTES Library of Congress Catalog Card Number: 81-600198 <input type="checkbox"/> Document describes a computer program; SF-185, FIPS Software Summary, is attached.			
11. ABSTRACT (A 200-word or less factual summary of most significant information. If document includes a significant bibliography or literature survey, mention it here) <p>The flow depth and velocity changes across a moving solid in partially-filled pipe flow are predicted by means of the application of the method of characteristics to solve the unsteady flow equations.</p> <p>Simplified force models are presented which, when used in conjunction with empirical relationships linking leakage flow past the solid to upstream specific energy, are sufficient to provide the required moving solid boundary conditions that allow solid velocity prediction.</p> <p>A wide range of simulated transport conditions are presented that confirm the applicability of this technique as a basis for the future evaluation of more complex body force models.</p> <p>The predicted solid velocity during drain transport is shown to be compatible with laboratory observations of the influence of solid dimensions and position in inflow profile on transport characteristics.</p>			
12. KEY WORDS (Six to twelve entries; alphabetical order; capitalize only proper names; and separate key words by semicolons) computer based model; drainage; solid transport; unsteady flow,			
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